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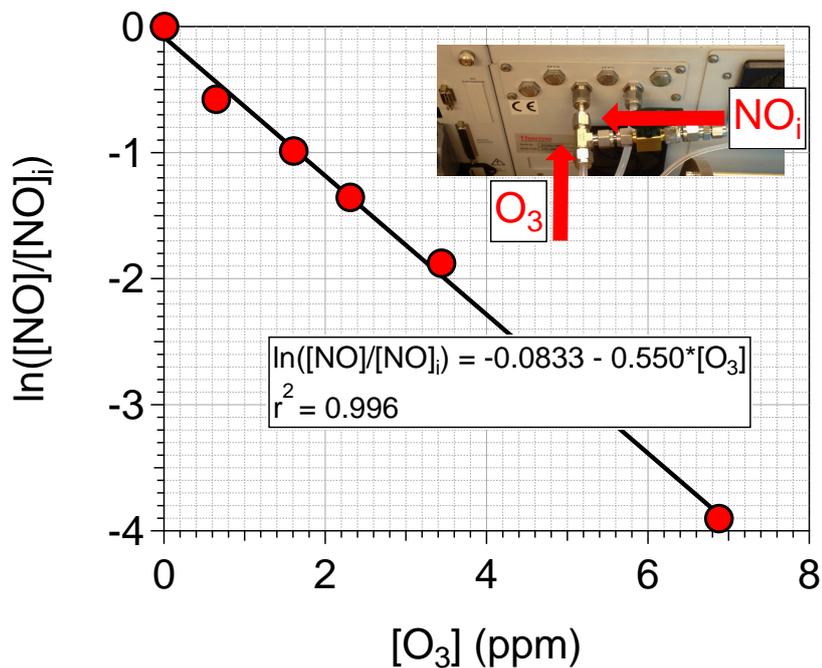
*Supplement of*

## **Controlled nitric oxide production via $O(^1D) + N_2O$ reactions for use in oxidation flow reactor studies**

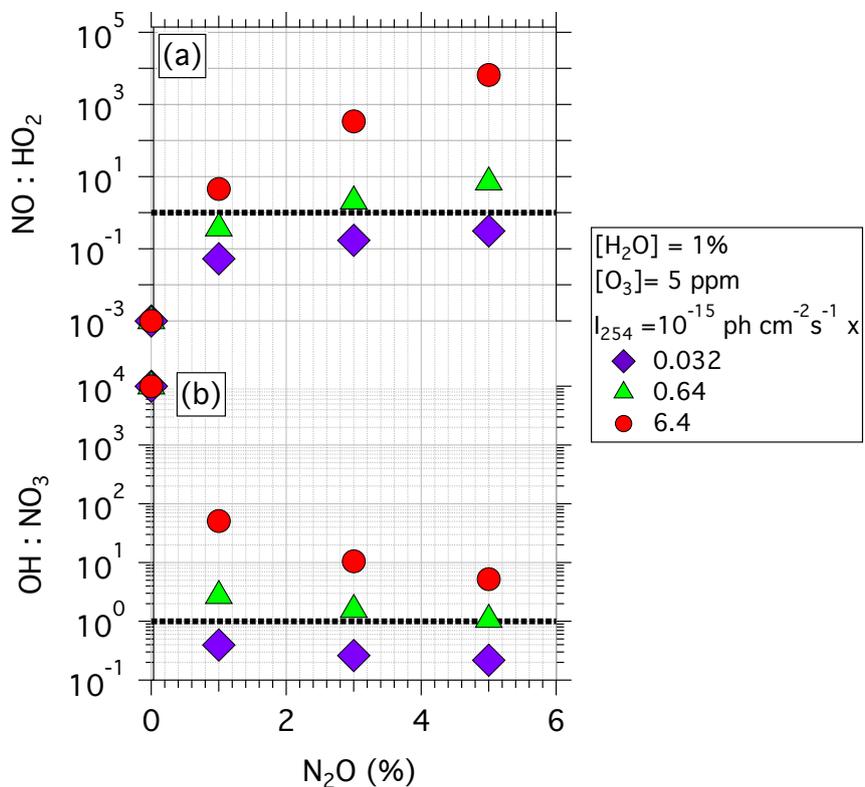
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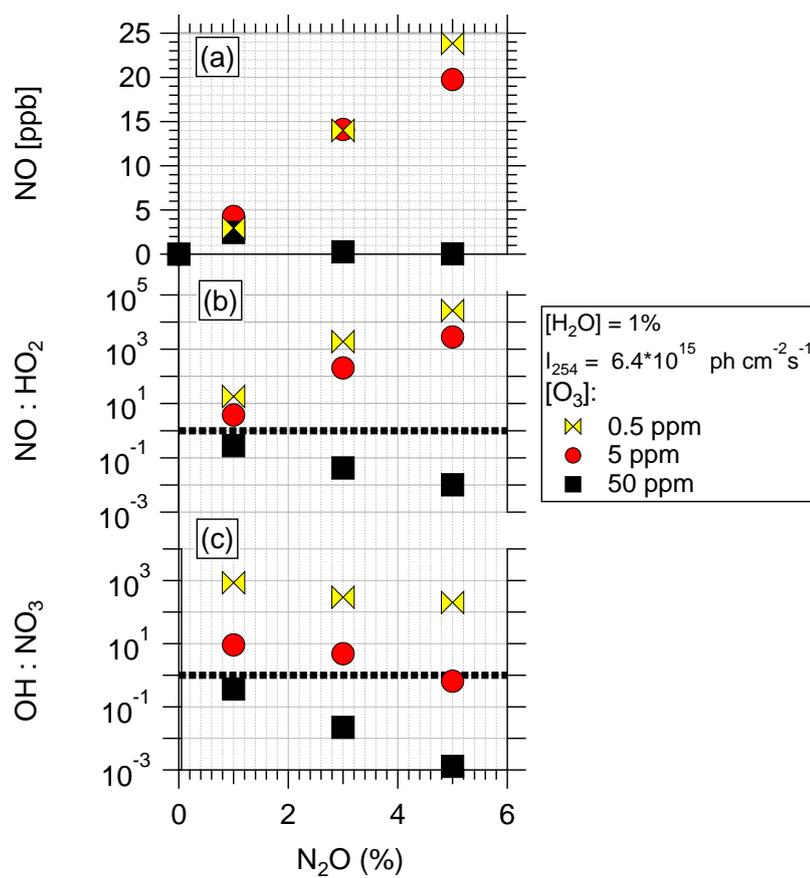
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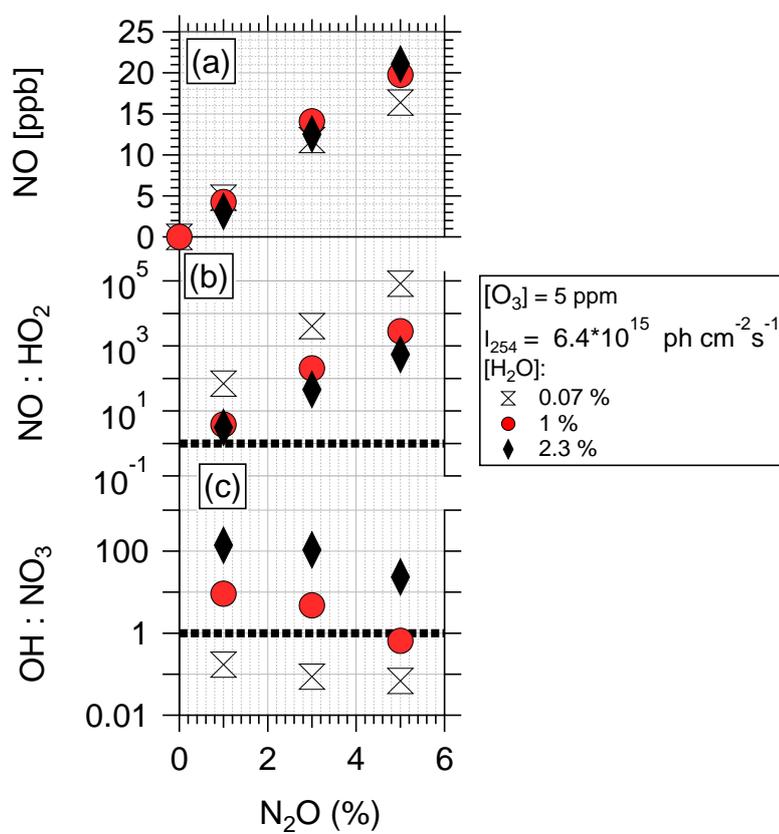
**Figure S1.** Nitric oxide (NO) depletion inside the NO analyzer due to reaction of 50 ppb initial NO ( $\text{NO}_i$ ) with  $\text{O}_3$ . NO was introduced from a calibration cylinder, and  $\text{O}_3$  was introduced from the output of the PAM reactor.



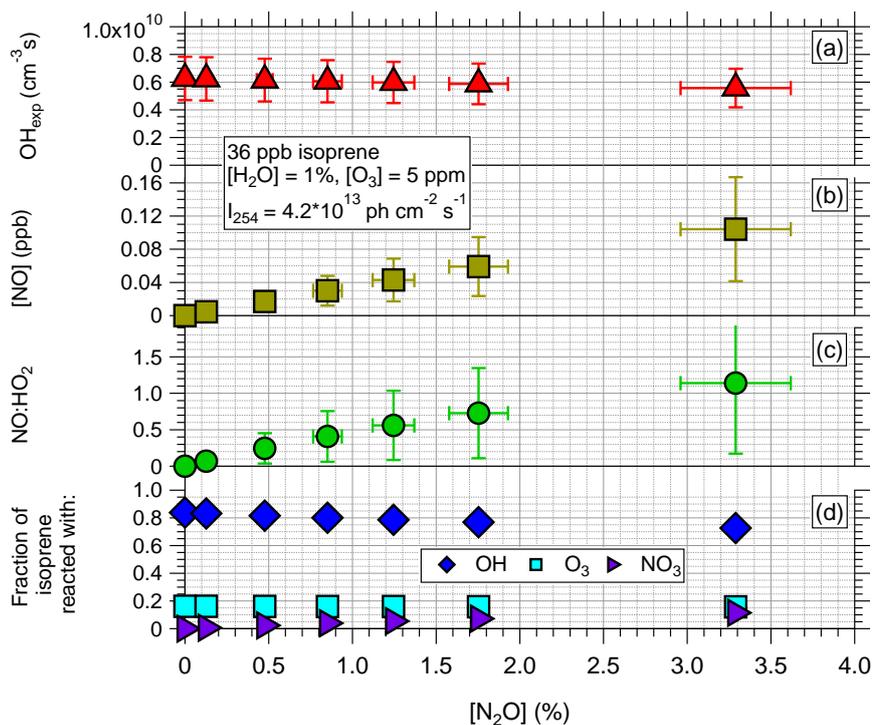
**Figure S2.** Modeled steady-state (a)  $\text{NO}:\text{HO}_2$ , and (b)  $\text{OH}:\text{NO}_3$  as a function of  $[\text{N}_2\text{O}]$  input to the PAM reactor with mean residence time = 80 sec for: low, medium, and high  $I_{254} = 0.032 \times 10^{15}$ ,  $0.64 \times 10^{15}$  and  $6.4 \times 10^{15}$   $\text{ph cm}^2 \text{ sec}$ , respectively, at fixed  $[\text{H}_2\text{O}] = 1\%$  and  $[\text{O}_3] = 5 \text{ ppm}$ .



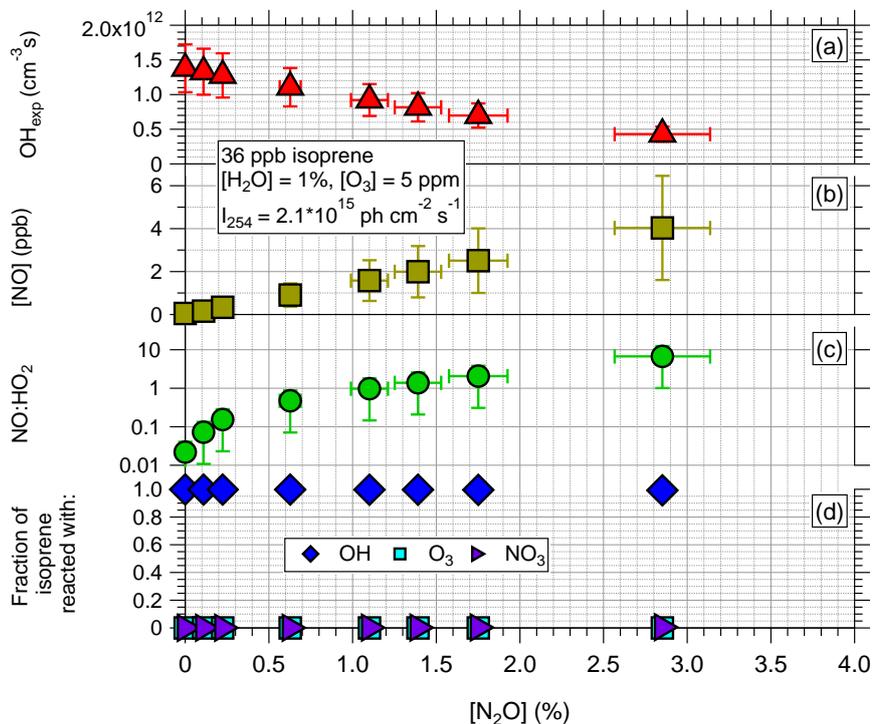
**Figure S3.** Modeled steady-state (a) NO, (b) NO:HO<sub>2</sub>, and (c) OH:NO<sub>3</sub> as a function of  $[N_2O]$  input to the PAM reactor with mean residence time = 80 sec for: low, medium, and high  $[O_3] = 0.5, 5,$  and 50 ppm respectively, at fixed  $[H_2O] = 1\%$  and  $I_{254} = 6.4 \times 10^{15} \text{ ph cm}^{-2} \text{ sec}$ .



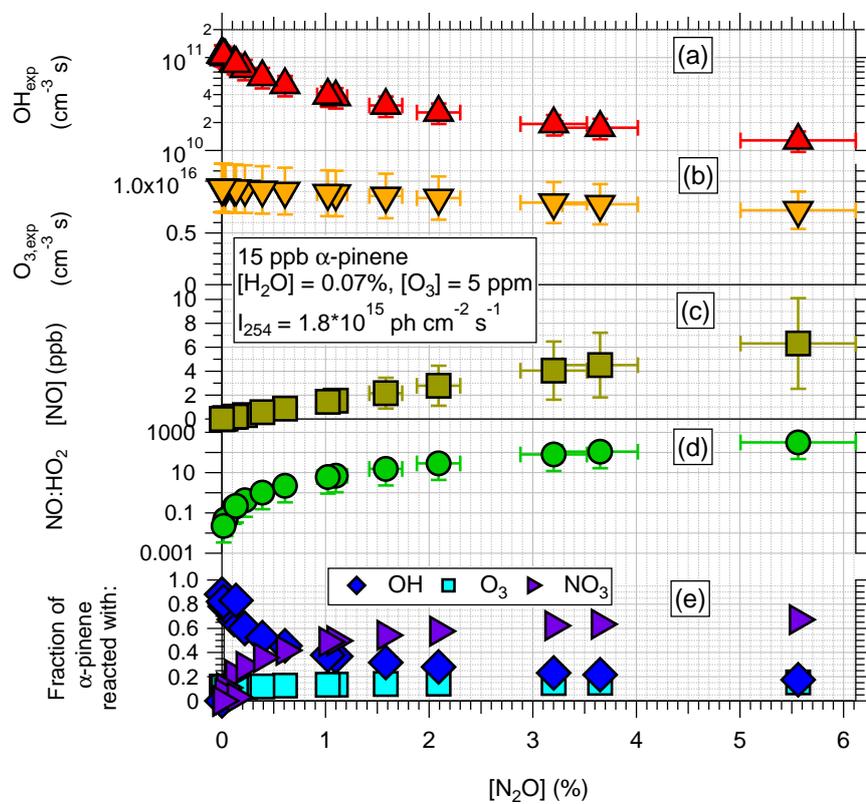
**Figure S4.** Modeled steady-state (a) NO, (b) NO:HO<sub>2</sub>, and (c) OH:NO<sub>3</sub> as a function of input  $[N_2O]$  in the PAM oxidation flow reactor with mean residence time = 80 sec for: low, medium, and high  $[H_2O] = 0.07, 1,$  and  $2.3\%$  respectively, at fixed  $[O_3] = 5$  ppm and  $I_{254} = 6.4 \times 10^{15}$  ph cm<sup>-2</sup> sec.



**Figure S5.** Modeled steady-state (a) OH exposure, (b) [NO], (c) NO:HO<sub>2</sub>, and (d) fractional oxidative loss to OH, O<sub>3</sub>, and NO<sub>3</sub> as a function of input [N<sub>2</sub>O] corresponding to isoprene oxidation conditions at low OH exposure in the PAM reactor. Error bars represent uncertainty in model outputs (Peng et al., 2015) and in accuracy of N<sub>2</sub>O flow controller.



**Figure S6.** Modeled steady-state (a) OH exposure, (b) [NO], (c) NO:HO<sub>2</sub>, and (d) fractional oxidative loss to OH, O<sub>3</sub>, and NO<sub>3</sub> as a function of input [N<sub>2</sub>O] corresponding to isoprene oxidation conditions at high OH exposure in the PAM reactor. Error bars represent uncertainty in model outputs (Peng et al., 2015) and in accuracy of N<sub>2</sub>O flow controller.



**Figure S7.** Modeled steady-state (a) OH exposure, (b)  $O_3$  exposure, (c)  $[NO]$ , (d)  $NO:HO_2$ , and (e) fractional oxidative loss to OH,  $O_3$ , and  $NO_3$  as a function of input  $[N_2O]$  corresponding to  $\alpha$ -pinene oxidation conditions at low OH exposure in the PAM reactor. Error bars represent uncertainty in model outputs (Peng et al., 2015) and in accuracy of  $N_2O$  flow controller.