Supplement of

Simulation-aided characterization of a versatile water-based condensation particle counter for atmospheric airborne research

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Numerical simulation of three-stage water-based CPC operation

Assumption

1. Water vapor through a cylindrical growth tube is described by the energy equation of a Newtonian fluid under steady laminar flow conditions.
2. The particle flow is assumed to be an incompressible Newtonian fluid with a fully developed parabolic flow profile: \( v_z(r) = v_0 \left(1 - \frac{r^2}{R^2}\right) = v_0(1 - x^2) \), where \( v_0 \), \( r \), and \( R \) represent initial velocity (m/s), radial position (mm), and growth tube radius, respectively, and \( x \) is the dimensionless length.
3. Axial thermal diffusion and other second-order effects such as Stefan flow are ignored.

Simplified 1-D heat and mass transfer

The 1-D heat transfer: a partial differential equation of steady laminar flow:

\[
v_0 \left(1 - \frac{r^2}{R^2}\right) \frac{\partial T}{\partial z} = D_{th} \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r}\right) + \frac{\partial^2 T}{\partial z^2}\right]
\]  

(1)

\( D_{th} \) is the thermal diffusivity of the air, 0.215 cm\(^2\)/sec at STP. At the other operation condition in this study, we assume it is constant and the pressure effect is negligible.

The 1-D mass transfer: a partial differential equation for partial vapor pressure:

\[
v_0 \left(1 - \frac{r^2}{R^2}\right) \frac{\partial P_{va}}{\partial z} = D_{va} \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial P_{va}}{\partial r}\right) + \frac{\partial^2 P_{va}}{\partial z^2}\right]
\]  

(2)

\( D_{va} \) is the mass diffusivity of the water vapor, 0.251 cm\(^2\)/sec at STP. At the other operation condition, \( D_{va,P} = D_{va}/(P/1(\text{atm})) \ast \left(\frac{T}{273}\right)^{1.94} \).

The relative humidity or saturation ratio is defined as the ratio of the partial pressure of water vapor \( (P_{va}) \) to the equilibrium saturated vapor pressure of water \( (P_{sat,T}) \) at a given temperature:

\[
S = RH = \frac{P_{va}}{P_{sat,T}}
\]  

(3)

The saturated water vapor pressure can be calculated using Antoine equation (Bridgeman and Aldrich, 1964): \( P_{sat,T} = 10^{(A-B/(T+C))} \)

\( A = 5.2039 \), \( B = 1733.926 \), \( C = -39.485 \), and \( T \) is the temperature in K, and \( P \) is the pressure in Pa.

Thus, the above equation can be converted to:

\[
v_0 \left(1 - \frac{r^2}{R^2}\right) \frac{\partial S}{\partial z} = D_{va} \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial S}{\partial r}\right) + \frac{\partial^2 S}{\partial z^2}\right]
\]  

(4)

Simulation condition

1. The growth tube diameter is 6.3 mm (R=3.15 mm);
2. The conditioner, initiator and moderator tubing lengths are 73 mm, 30 mm, and 73 mm;
3. Inlet conditions: \( T_0, P_0 \) is the partial water vapor pressure at \( T_0 \).
4. Wall conditions: \( T_{w1}, T_{w2}, \) and \( T_{w3}, \) \( P_{w1}, P_{w2}, \) and \( P_{w3} \).
Although the configuration of CPC 3789 is different from the previous studies, two fundamental characteristic times can describe how fast the thermal diffusion and the mass diffusion processes will proceed.

$$\tau_{\text{thermal}} = \frac{r^2}{D_{th}} = \frac{r^2}{k_a/\rho_a C_p}$$  \hspace{1cm} (5)$$

$$\tau_{\text{mass}} = \frac{r^2}{D_{va}}$$  \hspace{1cm} (6)$$

The ratio of those two characteristic times can be designated as the ratio of the thermal diffusivity to the molecular diffusivity of mass, which is also called the Lewis number.

$$Le = \frac{\tau_{\text{mass}}}{\tau_{\text{thermal}}} = \frac{D_{th}}{D_{va}} = \frac{k_a}{D_{va} \rho_a C_p}$$ \hspace{1cm} (7)$$

Where $r$ is the radius of the growth tubing, $D_{th}$ is the thermal diffusivity of the air and mainly a function of temperature. $D_{va}$ is the mass diffusivity of the water vapor, which depends on the pressure and temperature, as detailed above. (Seinfeld and Pandis, 2016)

Based on the dimensionless analysis in Fig. S1, with the decrease of the operation pressure, the Lewis number decreases, which means that the difference between the mass transfer rate and the thermal transfer rate increased with the decrease of the operating pressure. Because the current numerical model and theoretical analysis do not predict this observation, if we assume the water depletion and
condensational heat release are negligible, two factors most likely contribute to the counting efficiency decreases under the low-pressure condition: the significant loss inside the growth tube (wall effect or through the focusing nozzle) and the insufficient droplet growth inside the three-stage tube.

Fig. S2. Saturation ratio calculated along the centerline under different ambient pressures for various conditioner temperatures. The solid lines are for $T_{\text{cond}} = 30^\circ\text{C}$. The dashed lines are for $T_{\text{cond}} = 27^\circ\text{C}$, and the dotted lines are for $T_{\text{cond}} = 24^\circ\text{C}$. The colors indicate pressure in the hPa.
Simplified condensation effects on droplet size inside of the initiator

Latham and Nenes (2011) examined the supersaturation profile generated in a continuous-flow streamwise thermal-gradient growth tubing. Their work shows when water vapor depletion can have an essential impact on supersaturation under certain conditions. The depletion effects on the supersaturation ($s$) can be described by:

$$s = s_0 - \frac{\pi R^2 R_g T^2}{\Delta H_v G Q P_s} \dot{C}$$

(8)

Where $T$ is the temperature, $Q$ is the aerosol flow rate, $R$ is the radius of the growth tube, $P_s$ is the saturation pressure of the water, and assuming $G = \frac{dT}{dz}$, and $s_0$ denotes the maximum supersaturation ratio in the instrument for "zero" particle condition. $R_g$ is the specific gas constant for water vapor. $\Delta H_v$ is the enthalpy of evaporation of water, $\dot{C}$ describes the condensational loss (Seinfeld and Pandis, 2016). The depletion effect leads to a lower supersaturation ($s$), hence a lower droplet size at the exit of the growth tubing (Nenes and Seinfeld, 2003; Seinfeld and Pandis, 2016).
Where $D_{p0}$ is the average droplet size at "zero" particle concentration for $\dot{C} \rightarrow 0$.

$\Gamma$ is a growth parameter that depends on the droplet size and the water vapor mass transfer coefficient (Seinfeld and Pandis, 2016).

$\Gamma = \frac{\rho_wRT_\infty}{4P_{sat,T-D_{va,P}^2M_w}} \frac{1}{\Delta H_T} \frac{M_w}{2kT_\infty} \left( \frac{M_w}{T_\infty} - 1 \right)$ \hspace{1cm} (10)

Where $k_*'$ is a modified thermal conductivity described as equation (17.72) by Seinfeld and Pandis (2016). $D_{va,P}$ is a modified mass diffusivity described as equation (17.62) by Seinfeld and Pandis (2016).

When calculated the above two modified conductivities, we assume the value of the thermal accommodation coefficient ($\alpha_T$) was set equal to the mass accommodation coefficient ($\alpha_c$) in this simplified analysis.

To further simplify the equation (8) and (9), more convenient forms can be derived if $\dot{C}$ is explicitly written as a function of $D_p$, $N$, and $\Gamma$. The average droplet size $\overline{D_p} = \frac{1}{N} \sum_{i} N_i D_{pi}$.

$\dot{C} = \frac{\pi R^* T \rho_w}{2 M_w} \Gamma N \overline{D_p}$ \hspace{1cm} (11)

If we write $\Phi = \frac{\pi^2 R^2 R^* \rho_w^2 R^* \rho_w}{\Delta H_T G Q p_s M_w}$, equation (8) can be simplified as

$\frac{s}{s_0} = \frac{1}{1 + \frac{\Phi}{\Gamma} \frac{N \overline{D_p}}{s}}$ \hspace{1cm} (12)

Where $R^*$, $M_w$, $\rho_w$ are the universal gas constant (8.314 J/mol/K), the molecular weight and density of liquid water.

The simplification of the droplet size depression equation results from equation (9) and (10)

$\frac{D_p}{D_{p0}} = \left( 1 + \Phi \Gamma \overline{D_p} \right)^{-1/2}$ \hspace{1cm} (13)

The value of $\alpha_c$ was varied from 1 for rapidly activating aerosol to 0.01 which for slowly activating aerosol. However, based on the estimation, this variation did not significantly affect the saturation and droplet size, as shown in Fig. S4. Additionally, reducing the conditioner temperature also has influenced (<20% with the 15% reduction of s) the saturation profile. Previous studies showed that the droplet size exiting the moderator tube might have up to 90% particle loss if the droplet size is larger than 10 $\mu$m (Chen and Pui, 1995; Fletcher et al., 2009; Takegawa and Sakurai, 2011). Meanwhile, the signal-to-noise ratio is too high for small droplets. Thus, this simulation assumed the droplet size exiting the initiator is between 1 to 7 $\mu$m.
Fig. S4. Predicted supersaturation depletion and droplet size depression ratio as a function of aerosol number concentration. Results are shown for different mass accommodation coefficients and conditioner temperatures setting.

The wCPC monitors the height of the pulses generated in the optical detector and reports a status parameter to indicate the percentage of the sampled particles, which have an acceptably high pulse. Although the exact droplet size detected by the detector is unknown, this pulse height parameter indirectly shows insufficient particle growth in the detector chamber.

The saturation depletion and the droplet size depression are function of the aerosol number concentration at the ambient condition (1 atm), as shown in Fig. S4. The 10% reduction of $s$ and $D_p$ is predicted for $N_{1\mu m} \sim 6 \times 10^4$ (cm$^{-3}$), the mean droplet size at the initiator’s exit is 1 $\mu$m with the conditioner temperature setting is 30 $^\circ$C. Under the same temperature setting, if the mean droplet size at the exit of the initiator should be 7 $\mu$m to make sure the detector counts the particles, the 10% reduction of $s$ and $D_p$ happened when the $N_{7\mu m} \sim 8.5 \times 10^3$ (cm$^{-3}$). With the conditioner's temperature decreased to 24 $^\circ$C, the threshold concentration ($N_{1\mu m}$ and $N_{7\mu m}$) for the 10% reduction of $s$ and $D_p$ increased about 15% ($N_{1\mu m} \sim 7 \times 10^4$ (cm$^{-3}$) and $N_{7\mu m} \sim 1 \times 10^4$ (cm$^{-3}$)) from the concentration values under the 30 $^\circ$C conditioner temperature. Thus, the droplet size at the initiator’s exit determines the aerosol number concentration limits due to the saturation depletion and the droplet size depression.

The simulation results shown in Fig. S4 suggest that the droplet size at the initiator’s exit should be larger than 3 $\mu$m under the low-pressure. We examined the effect of the operating pressure on the 10% reduction threshold theoretically, as shown in Fig. S5. The theoretical analysis suggests that the 10% reduction threshold ($N_{3\mu m}$) is about $1.94 \times 10^4$ (cm$^{-3}$) at 1 atm, when the conditioner temperature is 24 $^\circ$C. Based on the theoretical analysis, with the decrease of the operating pressure, the 10% reduction threshold of $N_{3\mu m}$ reduced about 5% of the aerosol concentration ($1.85 \times 10^4$ (cm$^{-3}$) at 0.5 atm).
Fig. S5. Predicted supersaturation depletion and droplet size depression ratio as a function of aerosol number concentration. Results are shown for a droplet size of 3 µm exiting the initiator and the conditioner temperature at 24 °C. The insets are zoomed in plots for the narrowed $S/S_0$ range.
Fig. S6. The water depletion due to the aerosol number concentration, illustrated by (a) the pulse height generated in the optical detector, (b) the counting efficiency as a function of the inlet pressure. Results are shown with the conditioner temperatures set at 24 °C and 30 °C, with the initiator temperature at 59 °C and the moderator temperature at 10 °C.
Fig. S7. Predicted droplet size evolution along the growth tube of the CPC 3789 under the different conditioner temperatures (30 °C, 27 °C, and 24 °C), with the initiator temperature at 59 °C and the moderator temperature at 10 °C. Starting particle size is 20 nm.
Table S1. Properties of tested aerosol particles.

<table>
<thead>
<tr>
<th>Properties</th>
<th>Ammonium sulfate</th>
<th>PSL</th>
<th>Sucrose</th>
<th>Humic acid</th>
<th>Oleic acid</th>
<th>Water</th>
</tr>
</thead>
<tbody>
<tr>
<td>Molecular weight (g/mol)</td>
<td>132.14</td>
<td>N/A</td>
<td>342.3</td>
<td>227.17</td>
<td>282.47</td>
<td>18.02</td>
</tr>
<tr>
<td>Melting point (°C)</td>
<td>235 °C</td>
<td>100-110 °C*</td>
<td>186 °C</td>
<td>300 °C</td>
<td>13.4 °C</td>
<td>0 °C</td>
</tr>
<tr>
<td>Density (g/cm³)</td>
<td>1.77</td>
<td>1.055 (20 °C)</td>
<td>1.59</td>
<td>1.77</td>
<td>0.895</td>
<td>0.997 (20 °C))</td>
</tr>
<tr>
<td>Water solubility</td>
<td>70.6 g/100 g water</td>
<td>insoluble</td>
<td>greater than or equal to 100 mg/mL at 66°F</td>
<td>insoluble</td>
<td>insoluble</td>
<td>N/A</td>
</tr>
</tbody>
</table>

*Glass transition temperature

Takegawa, N. and Sakurai, H.: Laboratory evaluation of a TSI condensation particle counter (Model 3771) under airborne measurement conditions, Aerosol Sci Tech, 45, 272-283, 2011.