



## *Supplement of*

# A comprehensive evaluation of enhanced temperature influence on gas and aerosol chemistry in the lamp-enclosed oxidation flow reactor (OFR) system

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#### **S1 Supply power for Light Source and BHK lamps**

For the UV lamps from Light Source Inc., the supply power (8.9 W) was calculated as  $185 \text{ mA}/425 \text{ mA} \times 21 \text{ W}$ , where  $185$ mA is the measured current controlled by the ballast at 10 VAC (full) output; 425 mA and 21 W are the manufacturer specified current and power. For BHK lamps, the supply power (6.3 W) was measured directly with a Kill-A-Watt sensor on the outlet 5 of the lamp controller box at full AC output.

**S2 Calculation of the heating energy in OFR**

For the temperature measured for a lamp control voltage of 10 V (full AC power) and flow rate of 5 L min<sup>-1</sup> (Fig. 4), we calculated the fraction of heating energy transferred from the UV lamps to the gas inside the OFR  $(f_g)$ , the N<sub>2</sub> purge gas  $(f_{N_2})$ ,

10 and the OFR tube wall  $(f_s)$ . Results were estimated on the assumption that all the electrical input power of the lamps was finally converted into heat, which led to the rise in temperature. We did not consider the heat exchange between the gas inside the OFR,  $N_2$  purge gas, and OFR surface. The energy of gas inside the OFR (or  $N_2$  inside the lamp sleeves) would be lost due to the gas (or  $N_2$ ) entering and leaving the OFR (or lamps sleeve), depending on the flow rate and the temperature of the ambient gas (or  $N_2$ ,0.2 and 20 L min<sup>-1</sup>). Also, the OFR surface dissipate heat to the ambient air. Based on the timeseries of

15 measured temperature in Fig. 4, the 
$$
f_g
$$
,  $f_s$ , and  $f_{N_2}$  could be calculated as follows:

$$
f_g = \frac{Q_g}{Q_{Total}} = \frac{C_g \times M_g \times \Delta T_{i-(i-1)} + C_g \times m_g \times \Delta T_{i-a}}{Q_{Total}}
$$
 (1)  

$$
f_s = \frac{Q_s}{Q_{Total}} = \frac{C_s \times M_s \times \Delta T_{j-(j-1)} + F \times A \times \Delta T_{j-a}}{Q_{Total}}
$$
 (2)

$$
f_{N_2} = \frac{Q_{N_2}}{Q_{Total}} = \frac{C_{N_2} \times M_{N_2} \times \Delta T_{k-(k-1)} + C_{N_2} \times m_{N_2} \times \Delta T_{k-a}}{Q_{Total}}
$$
(3)

Where  $Q_g$ ,  $Q_s$ , and  $Q_{N_2}$  were the energy in 1 second of lamps allocated to the gas inside OFR, surface of OFR and N<sub>2</sub> purge 20 gas, respectively;  $Q_{Total}$  is the total energy from 4 lamps in 1 s (35.6 J, 8.9 W for each lamp at full VAC).  $C_q$ ,  $C_s$  and  $C_{N_2}$  were the specific heat capacity of gas (1.005 kJ kg<sup>-1</sup> K<sup>-1</sup> at 300 K), OFR surface (aluminium, 0.879 kJ kg<sup>-1</sup> K<sup>-1</sup> at 293 K) and N<sub>2</sub> (1.038 kJ kg<sup>-1</sup> K<sup>-1</sup> at 298 K);  $M_g$ ,  $M_s$  and  $M_{N_2}$  were the mass of gas inside OFR, OFR surface, and N<sub>2</sub> in lamp sleeves;  $\Delta T_{i-(i-1)}$ was the temperature difference between i<sup>th</sup> and (i-1)<sup>th</sup> second for gas inside OFR.  $\Delta T_{i-(i-1)}$  and  $\Delta T_{k-(k-1)}$  were similar, for the temperature of OFR surface and N<sub>2</sub> purge gas;  $m_q$  was the mass of gas entered or left OFR in one second;  $\Delta T_{i-q}$  was the 25 temperature difference between the gas left OFR at  $i<sup>th</sup>$  second and ambient air;  $F$  was the Heat dissipation area for OFR surface; A was the heat transfer coefficient (3.48 J m<sup>-2</sup> s<sup>-1</sup> K<sup>-1</sup>) and  $\Delta T_{j-a}$  was the temperature difference between the OFR surface at j<sup>th</sup> second and ambient air;  $m_N$ , was the mass entered or left lamps sleeve in one second;  $\Delta T_{k-a}$  was the temperature difference

between the N<sub>2</sub> left lamps sleeve at  $k<sup>th</sup>$  second and ambient air. Results were shown in Fig. S8.

#### 30 **S3 Calculation of the Richardson number**

The Richardson number, a dimensionless number that represents the ratio of buoyancy term to flow shear term, can be calculated as follow (Holman, 2010; Huang et al., 2017):

$$
R_i = \frac{g\beta D^3 \Delta T / v^2}{(\rho U_{avg} D / \mu)^2} \sim \frac{gD}{T U_{avg}^2} \Delta T
$$
 (4)

where g is the gravitational acceleration (9.78 m s<sup>-2</sup>),  $\beta$  is the thermal expansion coefficient of air (T<sup>-1</sup> for ideal gases), D is the 35 diameter of the flow tube (202 mm), T is the temperature at centerline (39 °C), ΔT is the temperature difference between the centerline and tube wall (4 °C),  $\nu$  is the kinematic viscosity of air (m<sup>2</sup> s<sup>-1</sup>),  $\rho$  is the density of air (kg m<sup>-3</sup>),  $U_{avg}$  is the average velocity on the cross-section of the flow tube  $(m s<sup>-1</sup>)$ , calculated based on the flow rate (5 L min<sup>-1</sup>) and D,  $\mu$  is the dynamic viscosity (N s m<sup>-2</sup>). When Ri<0.1, the natural convection is negligible; when Ri>10, the forced convection is negligible, and the buoyancy forces may lead to flow bifurcation and recirculation (Huang et al., 2017).

40

#### **Table S1: Temperature sensors used in temperature measurement.**





**Table S2: Detailed parameters of OFR temperature experiments.**

<sup>1</sup>Three types of lamps were used (Figure S2). '185 covered' transmits both 185 and 254 nm radiation, with 80% surface covered with heat-shrink

45 tubes. Lamps of '185' are the same type as '185 covered', but without covering. The lamp of '254' transmits only 254 nm radiation and is not covered.

<sup>2</sup> Two mesh screens are set inside OFR, one near the inlet (Front) and one near the outlet (Back).

<sup>3</sup> The OFR sensor is set in the backplate by default, as shown in Fig. S1.

<sup>4</sup> Extending the external temperature sensor into OFR from the inlet (so the 'Front' mesh screen must be removed). 4 depths were measured for

50 Exp.1-3 (100, 200, 300, and 400 mm from the inlet, respectively)

<sup>5</sup> '/' means no installation or no measurement.

<sup>6</sup> Only one voltage was used during measurement.

<sup>7</sup> Voltage of one setting cycle, each voltage was set to last for 16 min.

**precursor VOC surrogate NOx**  $m_{frag}$   $\Delta LVP$   $p_1$   $p_2$   $p_3$   $p_4$ **HOM yield<sup>1</sup> reference dodecane** dodecane low 2 1.83 0.999 0.001 0.001 0.001 Cappa et al. (2013) high 0.2627 1.4629 0.9657 0.0010 0.0020 0.0314 Loza et al. (2014) **α-pinene** α-pinene low 0.305 1.97 0.419 0.426 0.140 0.014 0.44% Chhabra et al. (2011) high 0.1312 1.9139 0.5991 0.2923 0.1079 0.0007 0.44% Chhabra et al. (2011) **toluene** toluene low 1.31 1.77 0.185 0.001 0.002 0.812 0.1% Zhang et al. (2014) high 1.3064 1.4169 0.5634 0.3413 0.0016 0.0937 0.1% Zhang et al. (2014) **m-xylene** m-xylene low 1.08 2.05 0.102 0.001 0.878 0.019 1.7% Ng et al. (2007) high 0.0736 1.4601 0.1418 0.2971 0.4571 0.1040 1.7% Ng et al. (2007)

**Table S3: SOM parameters used in this study.**

<sup>1</sup> Values are obtained in Bianchi et al. (2019).

**Table S4: The modeled variation of SOA yield per temperature (K). The concentration of organic aerosol seed is 15 μg m-3 for all cases. The range of model temperature is 20-40 °C.**

precursors	NOx	$H_i^{vap}$ evaporation enthalpy $(kJ \text{ mol}^{-1})$			
		Equation <sup>1</sup>	50	100	150
dodecane	high	$0.0041 - 0.0052$	0.0019-0.0022	0.0036-0.0050	0.0053-0.0095
	low	0.0062-0.0074	$0.0026 - 0.0029$	$0.0053 - 0.0070$	$0.0078 - 0.010$
$\alpha$ -pinene	high	0.0087-0.0089	0.0037-0.0039	0.0077-0.0088	$0.011 - 0.015$
	low	$0.011 - 0.013$	$0.0041 - 0.0053$	$0.0091 - 0.013$	$0.01 - 0.011$
toluene	high	0.0060-0.0068	$0.0023 - 0.0026$	0.0050-0.0063	$0.0075 - 0.010$
	low	$0.0083 - 0.023$	0.0044-0.0068	0.0077-0.018	$0.0095 - 0.030$
m-xylene	high	$0.0049 - 0.099$	$0.0025 - 0.0039$	0.0045-0.0094	$0.0064 - 0.016$
	low	$0.0078 - 0.018$	0.0043-0.0063	$0.0073 - 0.015$	$0.0091 - 0.023$

60  $\frac{1}{1}$  The equation is taken from Epstein et al. (2010),  $H_i^{vap} = -11 \times \log C_{i,ref}^* + 131$ .



65 **Figure S1: Schematic diagram of (a) OFR and UV lamps and photographs of (b) mesh screen near the inlet, (c) inlet and hexagon nut and (d) outlets and sensors of OFR.**



**Figure S2: Four types of lamps used in this research. Type (1) transmits both 185 and 254 nm radiation, with 80%**  70 **surface covered with heat shrink tubes (GPH436T5VH/4, Light Sources, Inc.). Type (2) is the same as type (1) but not** 

**covered. Type (3) transmits only 254 nm radiation and is not covered (GPH436T5L/4, Light Sources, Inc.). Type (4) transmits both 185 and 254 nm radiation (model no. 82-9304-03, BHK Inc.).**



**Figure S3: Comparison between different temperature measurements used in this research. The measured temperatures from the CEM sensor, which was used to measure the room temperature, are shown on the x-axis. The Vaisala sensor is used to measure the temperature inside the OFR. Thermocouple 1 and Thermocouple 2 are used to measure the temperature of the OFR exhaust and outside surface. Detailed information about different sensors can be**  80 **found in Table S1.** 



**Figure S4: Temperature variation for (a) four lamps and (b) two lamps. In this case, the front plate with a hexagon nut and mesh screen was installed, and the OFR sensor set in the backplate was extended into the center of OFR (probing depth: 300 mm). The mesh screen near the back plate was removed.**



**Figure S5: The correlation between OH exposures (right axis) and equivalent aging time (left axis) vs. light settings at each lamp. A sigmoidal function was used to fit the scatter plots. The OH exposures under low NOx condition in panel (a) and (b) were estimated based on the empirical parameterization in Hu et al. (2022), while OH exposures in panel (c)** 

90 **under high NOx conditions was estimated based on the parameterization reported in Peng et al. (2018). A water mixing ratio of 1.88% (60% RH at 25 °C) under low NOx conditions was assumed in the laboratory studies (Panel (a)). The mixing ratio in field studies (Panel (b) and (c)) were measured directly by RH&T sensor. The input flow rate was 5 L min-1 , which corresponds to a residence time of 167 s.**



**Figure S6: The measured temperature variation with different types of Light Source lamps: (a) lamps with 80% surface covered with heat-shrink tubes and lamps without covered, (b) lamps emit both 185 and 254 nm radiation and lamps emit only 254 nm radiation. The temperature of the gas inside OFR at a depth of 300 mm was measured.**



100 **Figure S7: Temperature measured by an external temperature sensor for an OFR with BHK lamps (a) in the vertical direction at different depths inside OFR, with the driving voltage set to 0.95 V for two lamps; (b) the measured temperature at different depths inside the OFR under different driving voltages; the "upper" indicates the position of 100 mm in the vertical direction and the "center" indicated the position measured at centerline. Flow through the OFR was 4.5 L min-1 .**



**Figure S8: Schematic plot for the transfer of the heating energy inside the OFR from the UV lamps and the loss of energy to the ambient air. The fraction of energy from the UV lamps was obtained from Fig. S9. Note that only the power leading to the temperature increase (51% of total power, which is 35.6 W based on the calculation in Sec S1** and S2**) within OFR was considered for these three pathways.**



**Figure S9: (a) Energy from UV lamps (51% (based on calculation in Sect. S2) of total power (35.6 W), 8.9 W for each lamp, 4 lamps in total) to gas inside OFR, surface of OFR and N<sup>2</sup> purge gas (0.2 L min-1 ) as a function of time, with 4 lamps set to 10 V. The start time was when the lamps were turned on. The flow rate was 5 L min-1 . (b) Same as Fig. S9a, with the flow rate of N<sup>2</sup> purge gas increased to 20 L min-1 . Details of the energy calculation were presented in Sect.** 115 **S2.**



 **Figure S10: CFD simulation of the gases in OFR (a) without and (b) with the heating of lamps. In panel (b), the scenario of four lamps at 5 V was simulated.** 



125 **In this scenario, the 800 ppb of initial SO2, 2.2% water vapor mixing ratio (25 °C, 70% RH), and different photon flux at 185 nm and 254 nm (photon flux ratio of 254/185 nm= 0.05) were used. The simulated oxidant concentrations with** 

**measured RTD at 25 and 40 °C were both shown.** 



130 **Figure S12: Simulated SOA yield of α-pinene as a function of mass concentration of OA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of α-pinene from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 0.5 days by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



**Figure S13: Simulated SOA yield of toluene as a function of mass concentration of OA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of toluene from**  140 **different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



**Figure S14: Simulated SOA yield of xylene as a function of mass concentration of OA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results**  145 **using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of xylene from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



150 **Figure S15. Simulated size distribution of α-pinene SOA as a function of temperature by assuming the mass concentration of 30 μg m-3 for OA seed (inlet mass concentration) under (a) high NOx and (c) low NOx conditions, respectively. Simulated O: C ratio of α-pinene SOA as a function of temperature and mass concentration of OA seed (inlet mass concentration) under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 0.5 days by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molec cm−3 (Mao et al., 2009).**



**Figure S16: Simulated size distribution of toluene SOA as a function of temperature by assuming the mass concentration of 30 μg m-3 for OA seed (inlet mass concentration) under (a) high NOx and (c) low NOx conditions, respectively. Simulated O:C ratio of toluene SOA as a function of temperatures and mass concentration of OA seed**  160 **(inlet mass concentration) under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



**Figure S17**: **Simulated size distribution of m-xylene SOA as a function of temperature by assuming the mass concentration of 30 μg m-3 for OA seed (inlet mass concentration) under (a) high NOx and (c) low NOx conditions,**  165 **respectively. Simulated O:C ratio of m-xylene SOA as a function of temperatures and mass concentration of OA seed (inlet mass concentration) under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



170 **Figure S18: Simulated SOA yield of (a-b) α-pinene, (c-d) Toluene, (e-f) m-xylene as a function of temperature under**  different  $H_i^{vap}$  values (Unit: kJ mol<sup>-1</sup>). The mass concentration of OA seed (inlet mass concentration) was assumed to **be 15 μg m-3 . The equivalent aging time was 1 day assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**



**Figure S19. The SOA formation from benzene and OH radicals in the PAM-OFR as a function of light intensity. Two cases including PAM-OFR blown with fans and without fans were both shown. The room temperature and temperature measured with the primary Temp&RH sensor set in the back panel were shown in the right axis. Note** 

180 **the OFR temperature reported here is the lower limit as discussed in section 3.1.5. The gas-phase benzene (99.80%, Sigma-Aldrich) was generated with syringe pumps. Benzene was used as gas-phase precursor in this experiment due to its lower kOH, since benzene will not be totally consumed under the high OH exposure at high voltage settings in OFR. The flow rate in this experiment was 4.5 L min-1 , and the RH was ~30%.** 



185 **Figure S20. Simulated ratio of SOA yield with measured temperature vs. that under 25 °C under varied lamp settings. A 10-ppb toluene with mass concentration of 30 μg m-3 of OA seed (inlet mass concentration) was assumed. The equivalent aging time was calculated by assuming the ambient OH concentration equated to 1.5×10<sup>6</sup> molecule cm−3 (Mao et al., 2009).**

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