



## Abstract

The mass and effective density of black carbon (BC) particles generated from aqueous suspensions of Aquadag and fullerene soot was measured and parametrized as a function of their mobility diameter. The measurements were made by two independent research groups by operating a differential mobility analyser (DMA) in series with an aerosol particle mass analyser (APM) or a Couette centrifugal particle mass analyser (CPMA). Consistent and reproducible results were found in this study for different production lots of Aquadag, indicating that the effective density of these particles is a stable quantity and largely unaffected by differences in aerosol generation procedures and suspension treatments. The effective density of fullerene soot particles from one production lot was also found to be stable and independent of suspension treatments. Some difference to previous literature data was observed for both Aquadag and fullerene soot at larger particle diameters. Knowledge of the exact relationship between mobility diameter and particle mass is of great importance, as DMAs are commonly used to size-select particles from BC reference materials for calibration of single particle soot photometers (SP2), which quantitatively detect the BC mass in single particles.

## 1 Motivation

Black carbon, BC, is the main absorbing component of atmospheric aerosols and estimates show that it may be the second strongest contributor to global warming (Ramanathan and Carmichael, 2008). Traffic-related BC particles have also been shown to cause adverse health effects (e.g. Laden et al., 2000; Slama et al., 2007). Quantitative measurements of BC mass concentrations in atmospheric aerosols are most commonly done with optical, thermal, combined thermal-optical or photo-acoustic methods (Gelencsér, 2004). Recently the single particle soot photometer (SP2; Stephens et al., 2003) was introduced as an alternative method, using laser-induced incandescence

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(LII) for quantitative detection of refractory BC mass. All BC measurement methods have their advantages and disadvantages, though recent studies showed that consistent results can be obtained for BC measured by different methods, if appropriate calibrations, sampling techniques and data analysis procedures are applied (e.g. Kondo et al., 2011).

The SP2 is a highly sensitive method for selective and quantitative detection of refractory BC in single particles. The peak height of the incandescence signal is nearly linearly dependent on the mass of refractory BC in the particle, largely independent of particle morphology, and without interference from non-refractory coatings (Schwarz et al., 2006; Slowik et al., 2007; Moteki and Kondo, 2007; Cross et al., 2010). Nevertheless, empirical calibration of the SP2 is still required to obtain absolute BC mass measurements. This is commonly done with BC reference materials such as Aquadag®, glassy carbon or fullerene soot. It has been shown that subtle differences in the SP2's response exist between different BC materials and that fullerene soot behaves most similar to ambient BC in some ways (Moteki and Kondo, 2010; Moteki et al., 2010; Kondo et al., 2011). The calibration curve of the SP2 is obtained by recording the incandescence signal peak height for pure BC particles of known mass over the whole dynamic range of the SP2. Selecting particles by mass is ideally done with an aerosol particle mass analyser (APM) or a Couette centrifugal particle mass analyser (CPMA). However, most research groups operating an SP2 do not have access to such a device. Thus the calibration particles are often selected by their mobility diameter using a differential mobility analyser (DMA) instead. Unfortunately particles of many BC reference materials are not compact spheres (Moteki et al., 2009), instead possessing a fractal-like or other irregular shape. Thus, the effective density ( $\rho_{\text{eff}}$ ), defined as

$$\rho_{\text{eff}} = \frac{6m}{\pi D_{\text{mob}}^3}, \quad (1)$$

needs to be known in order to calculate the mass ( $m$ ) of the size-selected particles from their mobility diameter ( $D_{\text{mob}}$ ). This particular definition of effective density corresponds

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to the first variant of effective density discussed in DeCarlo et al. (2004).

Factory calibration of the SP2 is done with Aquadag. The manufacturer also distributes batches of Aquadag, originating from different production lots, to all SP2 users. The size-resolved effective density of Aquadag and fullerene soot has been measured by Moteki and Kondo (2010). However, little is known about the influence of e.g. batch-to-batch variability on the effective density of these calibration materials. For this reason we present size-resolved effective density measurements of Aquadag and fullerene soot, including different production lots, varied sample suspension treatments, and measurements by two independent research groups.

## 2 Experimental methods

Two independent research groups from the Laboratory of Atmospheric Chemistry at the Paul Scherrer Institut (PSI) and from the Department of Mechanical Engineering at the University of Alberta (UofA) contributed to the effective density measurements presented in this study. Experiment procedures applied by these two groups were similar, though not perfectly equal, as detailed in the following.

### 2.1 Aerosol generation

Several jars of Aquadag® (Aqueous Deflocculated Acheson Graphite) from Acheson Inc., USA, were purchased by Droplet Measurement Technologies. They took small batches from the production lots #9054 (“classic”) and #9627 (“new bottle”) and distributed each to PSI and UofA. Aquadag is a colloidal dispersion of aggregates of irregular flakes of graphite (Moteki et al., 2009) in water (~80 % H<sub>2</sub>O as delivered).

Fullerene soot was obtained from Alfa Aesar (stock #40971, lot #FS12S011). This very fullerene soot sample is of particular interest as it was used for several DMA based SP2 calibrations, e.g. during an SP2 intercomparison workshop (Laborde et al., 2011). Fullerene soot particles are aggregates of spherical primary particles with a

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diameter of  $\sim 50$  nm (Moteki et al., 2009) and they are composed of  $\geq 90$  % amorphous carbon (carbon black) and  $\leq 10$  % fullerenes (mainly  $C_{60}$ ) according to Alfa Aesar's specifications.

Materials used for SP2 calibration should ideally have an elemental carbon (EC) mass fraction close to 100 % and give similar incandescence signal amplitude per carbon mass in the SP2 as ambient BC. Thermal-optical analysis of dried Aquadag revealed that  $\sim 90$ – $93$  % of the total carbon (TC) content are EC and  $\sim 7$ – $10$  % organic carbon (OC). The TC content accounts for  $\sim 83$  % of the total gravimetrically determined mass, and consequently EC makes up  $\sim 76$  % of the total mass. Tests with thermodenuding Aquadag particles at  $400^\circ\text{C}$  before selecting them by mass resulted in  $\sim 13$  % higher SP2 signal amplitude per particle mass compared to non-thermodenuded Aquadag. This indicates that thermodenuding removes most of the non-EC components, thereby increasing the EC mass fraction. Similarly, thermodenuding also increased the SP2 signal amplitude per particle mass for fullerene soot particles by  $\sim 20$  %. However, here we report effective density measurements of non-thermodenuded Aquadag and fullerene soot for the following reasons: This is the way it has been done in previous studies relating the properties of BC calibration materials to those of ambient BC (Moteki and Kondo, 2010; Moteki et al., 2010) and it is common calibration practice among the SP2 users.

## 2.2 Effective density measurements

The experimental setup (Fig. 1) applied here was used in previous studies for effective density measurements (e.g. Olfert et al., 2007; Scheckman et al., 2009). Aquadag and fullerene soot were suspended in ultrapure water and BC aerosol particles were generated from the suspension by means of an atomizer connected to a silica gel diffusion dryer and a  $^{85}\text{Kr}$ -neutralizer. A DMA (TSI model 3080L; Knutson and Whitby, 1975) was then used to size-select BC particles by their mobility diameter, before passing them through an APM (Kanomax Model APM-3600; Ehara et al., 1996) or a CPMA (Olfert and Collings, 2005) for subsequent selection by particle mass. The mass of

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particles with a well-defined mobility diameter (fixed DMA voltage) was obtained by stepping the APM (or CPMA) voltage, with simultaneous counting of the particle concentration at the APM (or CPMA) outlet using a condensation particle counter (CPC). Experimental differences between the two research groups contributing to this study were only minor. PSI used a custom-built collision type atomizer, an APM for mass selection, a TSI CPC model 3022, and additionally an SP2 sampling in parallel to the CPC. UofA used a TSI collision type atomizer model 3776, a CPMA for mass selection, and a TSI CPC model 3076.

Accurate operation of the DMA+APM and the DMA+CPMA configurations was verified by measuring certified polystyrene microsphere size standards (PSL spheres; Duke Scientific, USA). The effective density determined for the PSL spheres was always found to be within 10 % of the value of  $1050 \text{ kg m}^{-3}$  stated by the manufacturer. Thus, the accuracy of the effective density measurements is estimated to be 10 % given the diameter uncertainty of the PSL spheres of  $\sim 3 \%$ .

An example measurement with the DMA-APM system of the effective density of fullerene soot particles with a mobility diameter of  $D_{\text{mob}} = 456 \text{ nm}$  is shown in Fig. 2. The rotational speed of the APM is held constant and the voltage is stepped. The mass of the monodisperse particles is obtained by fitting the data to find the voltage where the number concentration is at a maximum,  $V_c$ , and using the following relationship,

$$m = \frac{qV_c}{\omega^2 r_c^2 \ln(r_o/r_i)}, \quad (2)$$

$r_o$  are the inner and outer radii of the cylinders,  $\omega$  is the rotational speed of the cylinders, and  $r_c = (r_i + r_o)/2$ . In general, PSI operated the DMA and the APM with resolutions of 0.10–0.23 and 0.06–0.25<sup>1</sup>, respectively, expressed as full width at half

<sup>1</sup>At one point the APM was operated at a resolution of 0.46, which might lead to increased uncertainty in the mass measurement if multiply-charged particles were significant. However, SP2 data was used to verify that multiply-charged particles had an insignificant effect on the APM data fit.



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The effective density of Aquadag decreases from  $\sim 1000 \text{ kg m}^{-3}$  at  $D_{\text{mob}} = 60 \text{ nm}$  to  $< 400 \text{ kg m}^{-3}$  at  $D_{\text{mob}} = 700 \text{ nm}$  (all data are also tabulated in the Supplement). The black line is a polynomial fit through both PSI and UofA data, and the grey shading indicates  $\pm 10\%$  deviation from this fit, which corresponds to the estimated accuracy of the measurements. The measurements done by PSI and UofA agree within uncertainty across the whole common diameter range. Furthermore, no significant difference in effective density was observed between the Aquadag batches “classic” (diamonds) and “new bottle” (circles) by either investigator. The data series of UofA contains multiple data points at certain mobility diameters because additional effective density measurements were made from suspensions with doubled and halved Aquadag concentration (not distinguished in Fig. 3 for clarity reasons). Variation of suspension concentration has also no significant effect on the measured effective density. Recapitulating, the relationship between mobility diameter and effective density (and mass) of Aquadag particles seems to be largely independent of production lot and aerosol generation procedures. Thus it can be expected that the polynomial fit shown in Fig. 3 makes reproducible Aquadag based SP2 calibrations possible, even if only a DMA is available for selecting particles by their mobility diameter. The mass as a function of mobility diameter is either obtained by combining the parametrization of the effective density with Eq. (1) or from a direct parametrization of the mass. Polynomial coefficients of both parametrizations are provided in Table 1.

The effective density measurements of Aquadag, previously made by Moteki and Kondo (2010) using a similar DMA+APM setup, are added to Fig. 3 as green squares. Their results agree with this study within experimental uncertainty at mobility diameters  $D_{\text{mob}} < 240 \text{ nm}$  ( $m \approx 5 \text{ fg}$ ). However, they reported higher effective density at larger mobility diameters with deviations of up to  $\sim 35\%$  in the range  $D_{\text{mob}} \approx 500\text{--}750 \text{ nm}$ . The reason for this systematic difference is unclear, but a similar deviation was also observed for fullerene soot as will be shown in Sect. 3.2.

## 3.2 Fullerene soot

The effective density of fullerene soot was measured by PSI with two different methods (see Sect. 2.2). Figure 4 shows results from the “traditional” APM+DMA approach as dark blue circles and results from the novel indirect method as light blue triangles (all data are also tabulated in the supplementary information). The black line is a polynomial fit through all data obtained from both methods, and the grey shading indicates  $\pm 10\%$  deviation from this fit, which corresponds to the estimated accuracy of the measurements. Differences of effective density data measured by the two methods are well within experimental uncertainty, which shows that a DMA combined with an SP2 can be used for fast effective density measurements of pure BC particles, if an accurate calibration of the SP2 has been done using an APM or CPMA. The effective density of fullerene soot decreases from  $\sim 1000 \text{ kg m}^{-3}$  at  $D_{\text{mob}} = 80 \text{ nm}$  to  $< 400 \text{ kg m}^{-3}$  at  $D_{\text{mob}} > 700 \text{ nm}$ . This is much lower than the bulk density of fullerene soot of  $\sim 1720 \text{ kg m}^{-3}$  (Kondo et al., 2011), and consistent with an agglomerate of small primary spheres (Moteki et al., 2009). The effective density measurements of fullerene soot, previously made by Moteki and Kondo (2010) using a similar DMA+APM setup, are added to Fig. 4 as green squares. Their results agree with this study within experimental uncertainty at mobility diameters  $D_{\text{mob}} < 440 \text{ nm}$  ( $m \approx 4.5 \text{ fg}$ ). However, they reported higher effective density at larger mobility diameters with deviations of 20–30% in the range  $D_{\text{mob}} = 500\text{--}750 \text{ nm}$ . This systematic difference is similar to the deviations observed for Aquadag at larger diameters. Careful analysis of the measurements done in this study gave no indication of any potential problem systematically occurring in the range of larger mobility diameters and higher mass. Hence the reason for the observed differences remains unclear.

The stability and reproducibility of the fullerene soot’s effective density as well as of DMA based SP2 calibrations was investigated by measuring the mass of size-selected fullerene soot particles generated from different suspensions with the SP2. Three different aqueous suspensions of fullerene soot originating from the same production lot

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were produced: dilute suspension, concentrated suspension and sonicated concentrated suspension. The relative broadband incandescence peak height detected by the SP2 for all three suspensions is shown in Fig. 5 as a function of selected mobility diameter. “Relative peak height” means that the broadband peak height detected for a certain suspension and mobility diameter was divided by the mean peak height detected for all suspensions at the same mobility diameter. Differences between the three suspensions are as small as  $\pm 6\%$ , which includes the variability of the effective density as well as the variability of the DMA and the SP2. Thus it can be expected that the polynomial fit shown in Fig. 4 makes reproducible fullerene soot based SP2 calibrations possible, even if only a DMA is available for selecting particles by their mobility diameter. Parametrizations of the effective density and mass of fullerene soot as a function of mobility diameter are provided in Table 1.

#### 4 Summary

The mass and effective density of Aquadag and fullerene soot particles generated from aqueous suspensions were measured as a function of their mobility diameter by operating a DMA and an APM or CPMA in series. Consistent and reproducible results were found for Aquadag by two research groups for different production lots and suspension treatments. The effective density of fullerene soot particles was also found to be independent of suspension treatments. Only one production lot has been tested and thus generalisation to any other production lot of fullerene soot is not possible. This study shows that the effective density of Aquadag and fullerene soot particles is a stable quantity and largely unaffected by differences in aerosol generation procedures. Stability and knowledge of the effective density of BC reference materials makes reproducible SP2 calibrations possible if only a DMA is available for size-selection of the BC particles.

Additional tests revealed that the Aquadag and fullerene soot calibration particles generated by atomization and diffusion drying contain substantial amounts of non-EC

components. The question whether the SP2 calibration curves should be corrected for the mass of the non-EC components remains to be answered. Further studies comparing the SP2's response to different calibration aerosols with the response to atmospheric BC are needed in order to identify the best calibration materials and aerosol generation procedures for atmospheric applications.

**Supplementary material related to this article is available online at:**  
<http://www.atmos-meas-tech-discuss.net/4/4937/2011/amtd-4-4937-2011-supplement.pdf>.

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**Table 1.** Polynomial coefficients for the mass,  $m$ , and effective density,  $\rho_{\text{eff}}$ , of Aquadag and fullerene soot as a function of mobility diameter,  $D_{\text{mob}}$ . *Warning: Do not round below coefficients to less significant digits.*

	Aquadag <sup>a</sup>		Fullerene soot <sup>b</sup>	
	$m(D_{\text{mob}})^c$	$\rho_{\text{eff}}(D_{\text{mob}})^d$	$m(D_{\text{mob}})^c$	$\rho_{\text{eff}}(D_{\text{mob}})^d$
c0	−0.096	1900	−0.298	2096
c1	0.00422	−25.959	0.01055	−24.952
c2	$-4.82 \times 10^{-5}$	0.239644	$-1.071 \times 10^{-4}$	0.191165
c3	$6.26 \times 10^{-7}$	$-1.21482 \times 10^{-3}$	$8.97 \times 10^{-7}$	$-8.3812 \times 10^{-4}$
c4	$-5.65 \times 10^{-10}$	$3.65087 \times 10^{-6}$	$-1.441 \times 10^{-9}$	$2.27956 \times 10^{-6}$
c5	$-1.99 \times 10^{-13}$	$-6.71352 \times 10^{-9}$	$1.412 \times 10^{-12}$	$-4.00845 \times 10^{-9}$
c6	$3.80 \times 10^{-16}$	$7.41508 \times 10^{-12}$	$-8.53 \times 10^{-16}$	$4.57438 \times 10^{-12}$
c7	–	$-4.51461 \times 10^{-15}$	$2.16 \times 10^{-19}$	$-3.27578 \times 10^{-15}$
c8	–	$1.16399 \times 10^{-18}$	–	$1.33853 \times 10^{-18}$
c9	–	–	–	$-2.3817 \times 10^{-22}$

<sup>a</sup>Parametrizations for Aquadag are valid between  $60 \text{ nm} < D_{\text{mob}} < 710 \text{ nm}$ .

<sup>b</sup>Parametrizations for fullerene soot are valid between  $65 \text{ nm} < D_{\text{mob}} < 900 \text{ nm}$ .

$$^c m(D_{\text{mob}}) = \sum_i c_i D_{\text{mob}}^i$$

$$^d \rho_{\text{eff}}(D_{\text{mob}}) = \sum_i c_i D_{\text{mob}}^i$$

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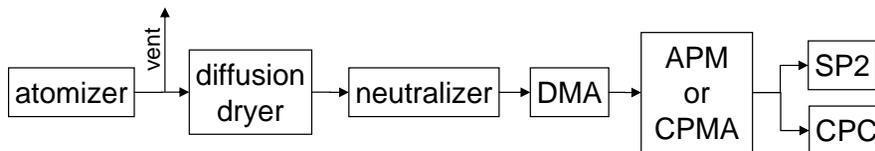
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**Fig. 1.** Experimental setup for effective density measurements.

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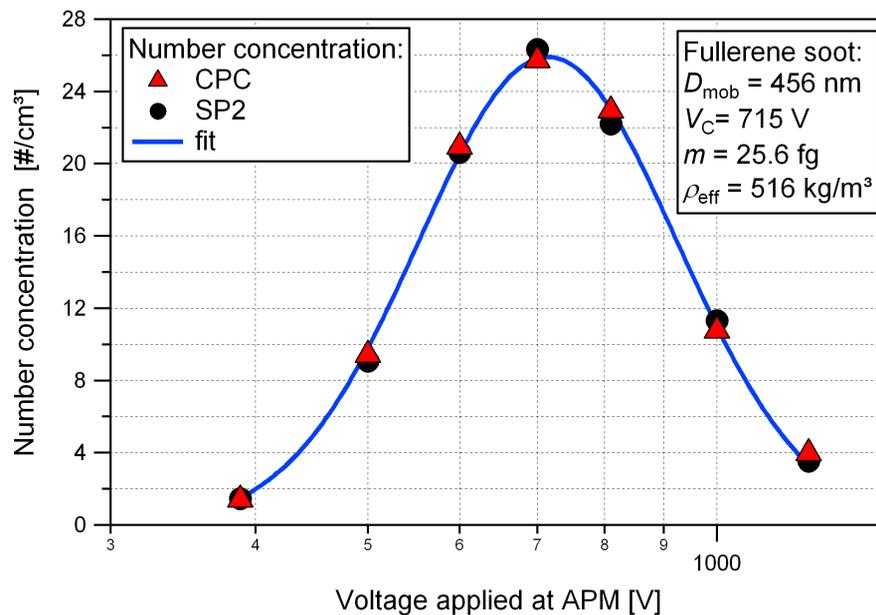
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**Fig. 2.** Classification of fullerene soot particles with mobility diameter  $D_{\text{mob}} = 456 \text{ nm}$  with the DMA-APM system (APM operated at 2000 rpm).

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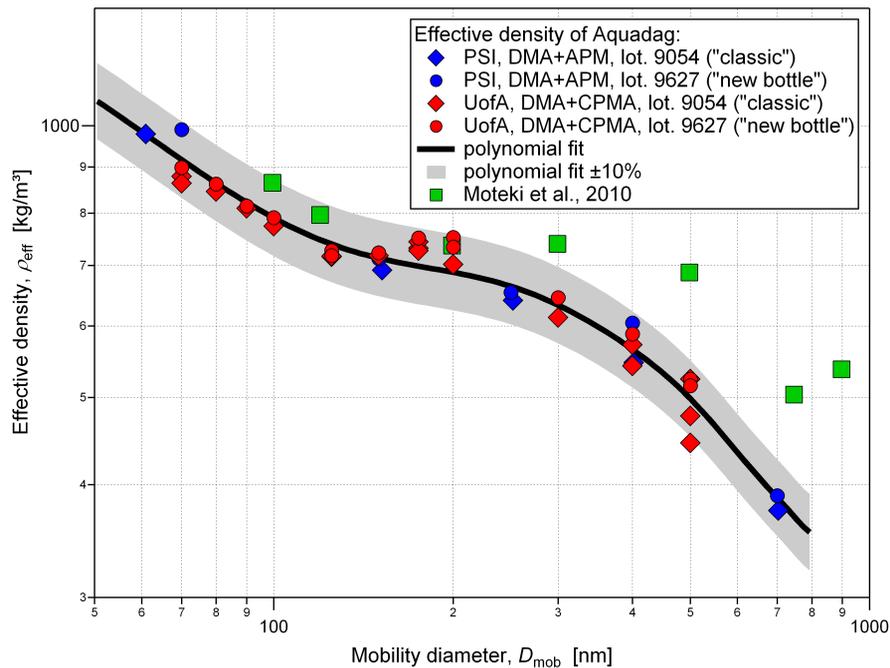
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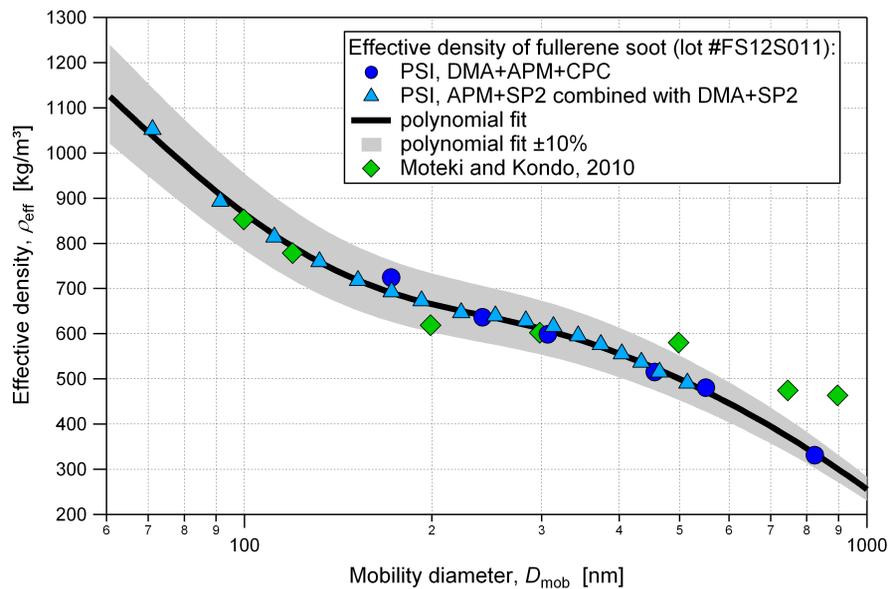
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**Fig. 3.** Effective density of Aquadag as a function of mobility diameter.[Title Page](#)[Abstract](#)[Introduction](#)[Conclusions](#)[References](#)[Tables](#)[Figures](#)[◀](#)[▶](#)[◀](#)[▶](#)[Back](#)[Close](#)[Full Screen / Esc](#)[Printer-friendly Version](#)[Interactive Discussion](#)

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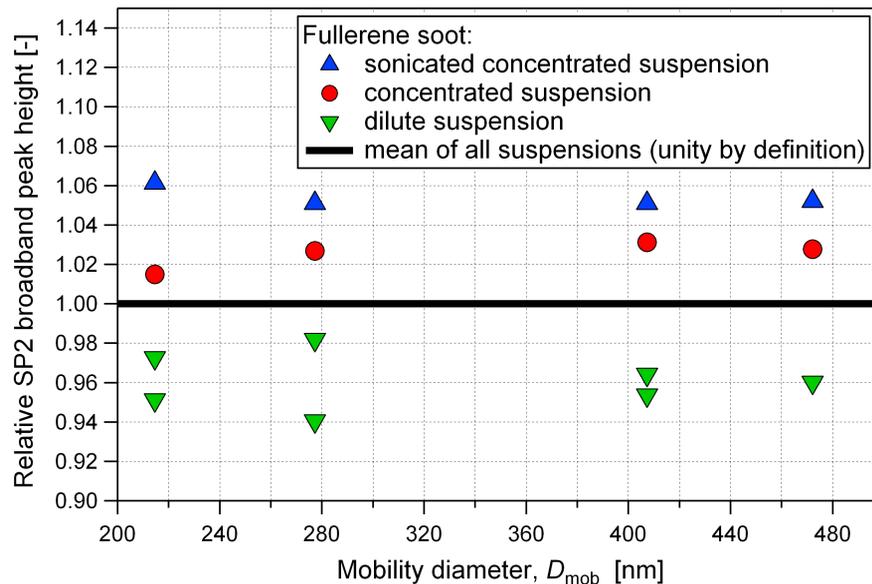


**Fig. 4.** Effective density of fullerene soot as a function of mobility diameter.

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**Fig. 5.** Effect of different fullerene soot suspension treatments on the SP2 calibration based on particle selection by a DMA. The relative SP2 broadband peak height is obtained by division of the broadband peak height measured for a certain suspension by the mean value of the broadband peak heights measured for all suspensions at equal mobility diameter.

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