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An experiment to measure raindrop collection efficiencies: influence of rear capture

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The analysis of radioactive aerosol scavenged by rain after the Chernobyl accident highlights certain differences between the modelling studies and the environmental measurements. Part of these discrepancies can probably be attributed to uncertainties in the efficiencies used to calculate aerosol particle collection by raindrops, particularly drops with a diameter larger than one millimetre. In order to improve the issue of these uncertainties, an experimental study was performed to close the gaps still existing for this key microphysical parameter. In the present article, attention is first focused on the efficiency with which aerosol particles, in the accumulation mode are collected by raindrops with a diameter of 2 mm. The collections efficiencies measured for aerosol particle in the sub-micron range are quantitatively consistent with previous theoretical model developed by Beard (1974) and thus highlight the major role of rear capture in the submicron range.

1 Introduction

Aerosol particles are an important component of the atmosphere. They significantly contribute to the Earth's energy budget, by directly interacting with radiation as well as serving as nuclei during cloud formation. The second effect, also called the indirect effect, is currently the main source of uncertainties in forecasting the future climate. In addition, particulate matter and its physical properties (size of particles, affinity with water, etc.) are key parameters in defining air composition and quality, and are of great importance in terms of health hazard.

Aerosol particles originate in many ways. The primary natural sources are sea spray, wind-driven dust, volcanic eruptions, and a secondary source is the condensation from the vapour phase. The size of these particles greatly varies and ranges from one nanometre to several hundred microns. One major origin of particulate matter is from anthropogenic sources. From all man-made pollution, one is particularly dangerous to

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human health and the quality of the environment: the radioactive releases from a nuclear accident.

Just like all other particles, once emitted, radioactive particles undergo physical processes that drastically change their size distribution during their transport in the atmosphere. Small particles disappear by coagulation and large particles are large enough to sediment to the ground. However, there is a significant range of particle sizes in the atmosphere, mostly unaffected by these removal mechanisms, called the accumulation mode (Whitby, 1973). This mode is made up of aerosol particles with diameters between 0.1 μm and 1 μm . These particles may remain in the atmosphere for several months (Pruppacher and Klett, 1997), and this particulate matter can be transported over long distances, crossing the continents. However, even this particulate matter does not accumulate endlessly in the atmosphere as clouds and their precipitation scavenge them from the atmosphere. Particles of the accumulation mode will be taken out of the atmosphere by what is called “wet removal”. This includes many processes such as their activation in cloud droplets or ice crystals, their collection by falling hydrometeors either inside or below the clouds during precipitation.

Different physical processes need to be taken into account to understand how the atmospheric concentration of particulate matter changes with size in the accumulation mode, how particles are removed, and how they can contaminate the ground. Certain aspects of these processes are still not well understood. While in-cloud processes and their interaction with aerosol particles have been studied extensively (e.g. Flossmann and Wobrock, 2010), the processes taking place below the cloud in the precipitation region have received less attention. In this study, however, we will focus on the below-cloud removal of particles by precipitation, the so-called wash-out process. Volken and Schumann (1993) and Laakso et al. (2003) showed that considerable differences appeared between their environmental scavenging coefficients and those calculated using the model described by Slinn (1977). A crucial parameter for these calculations are the collection efficiencies that appear in the calculation of particle collection by a falling hydrometeor, i.e., how many particles are collected by a falling drop compared to the

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particles in the volume that the drop has swept. Following streamlines around the drop prevents particles from being caught. For the small ones, brownian motion allows them to leave the streamlines and, for large particles, inertia or interception are phenomena that increase the collection efficiency. In the intermediate size range, collection efficiencies are low and these minimum values are known as the Greenfield gap (Greenfield, 1957), contributing to the creation of an accumulation mode. Scavenging models similar to the Slinn (1977) model use parameterisation to account for Brownian motion, inertial impaction and interception. Several hypotheses have been put forward to explain why these modelled scavenging coefficients still differ from measurements. Skibin et al. (1986) emphasised the effect of downdraft or updraft on the variation of aerosol concentrations. Davenport and Peters (1978) and Flossmann (1991) highlighted the influence of aerosol hygroscopicity on their washout. Wang et al. (1978) discussed the influence of electric effects that can increase the collection efficiencies up to an order of magnitude in the Greenfield gap. Finally, an additional uncertainty, according to Wang and Pruppacher (1977), involves the lack of knowledge on the collection efficiencies of large raindrops (with a diameter larger than 1 mm). First, large drops oscillate during their fall (Szakáll et al., 2009, 2010), additionally eddies develop downstream of large drops allowing small aerosol to be embedded in that secondary circulation and be captured at the rear of the drops or shed with the eddies (Beard, 1974). These two phenomena are the reason why modelling of the flow around a large drop is not feasible and that those collection efficiencies cannot be theoretically determined. Experiments have provided efficiencies for this size range (e.g. Kerker and Hampl, 1974; Grover et al., 1977; Wang and Pruppacher, 1977; Lai et al., 1978; Pranessa and Kamra, 1996; Vohl et al., 1999). However, these measurements only provide a patchy inside on the drop/particle collection process, as in particular for particles larger than 1 μm and drops between 0.2 mm and 3 mm diameter almost no observations exist (see Fig. 1 of Quérel et al., 2013).

For the current study, thus, we designed an experiment to lower the collection efficiency uncertainties in these unexplored regions. In the first section below we present

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velocity, oscillate and obtain a shape similar to atmospheric raindrops. The collection will then occur in the aerosol chamber in which aerosol particle concentration and the volume swept by the drop are known. To determine the collection efficiency as precisely as possible, concentrations of aerosol both in suspension in the aerosol chamber as well as collected by the drops are measured in mass quantities. The three parts of the facility are described below, and details can be found in Quérel (2012).

2.1 Drop generator

The BERGAME drop generator was developed following Lai et al. (1978). It consists of a 30 cm high vertical tube with a 5 cm internal diameter. It is equipped with a hypodermic needle at its base and overflows at different heights. This cylinder is fed at constant water flow rate. Thus, the water height inside the cylinder remains constant and the injection pressure inside the needle remains very stable. Therefore the generator can produce drop after drop with a diameter mono-dispersedly distributed ranging from 2 mm to 4 mm at a stable frequency. To avoid any electric charging of the drop, the generator is grounded. In this study, we focus on drops with a diameter between 2 and 2.6 mm in diameter.

2.2 Free fall shaft

The free fall shaft is ten meters high and has a square cross section of 0.45 m × 0.45 m. According to Wang and Pruppacher (1977), it is tall enough for drops with a diameter of around 2 mm to reach 99% of their terminal velocity. This shaft is equipped with windows at three levels in order to enable the probing of inside airflows. In this way, the use of a Particle Imaging Velocity technique (PIV, Quérel, 2012) verified that no convective flow occurred inside the shaft. Relative humidity within the shaft is monitored but not controlled. To account for any evaporation during the fall, measurements of the drop size are performed after the fall shaft, directly inside the aerosol chamber.

2.3 Aerosol chamber

The aerosol chamber is a stainless steel rectangular cube of 1 m height (H , in Eq. 5) and with a cross section of $0.8\text{m} \times 0.8\text{m}$. The chamber is equipped with two apertures: an inlet at the top to allow the drops, coming from the free fall shaft, to fall through the chamber; an outlet at the bottom to allow the collection of the drops after their path through the chamber. Dynamic containment systems (Mocho, 1996) ensure the non-contamination of the shaft and the laboratory with aerosol particles.

The in situ characterisation of the drops during their fall inside the chamber is performed through three existing windows, allowing non-intrusive measurements by optical techniques. The shadowgraphy technique provides the distribution and axis ratio of drops, and the PIV technique gives drop velocity. The complete optical setup is detailed by Quérel (2012). Figure 3 presents the axis ratio distribution measured in the BERGAME aerosol chamber for drops with a diameter of 2 mm.

Table 1 presents the mean and standard deviations of drop velocities (V_d) and axis ratios measured in the aerosol chamber, compared with the Beard (1976) model for terminal velocity (V_∞) and the Beard and Chuang (1987) model for axis ratio. These models have been supported by both wind tunnel measurements (Szakáll et al., 2009; Thurai et al., 2009) and in situ environmental measurements (Bringi et al., 2003). In Table 1 the drop Reynolds number is calculated using Eq. (2).

$$Re = \frac{V_d D_d}{\nu_{\text{air}}} \quad (2)$$

The agreement of these measurements with the literature models ensures the representativeness of the BERGAME set-up to simulate raindrops with a diameter up to 2.7 mm. Moreover, this proves that the dynamic containment we added to avoid contamination of the shaft with aerosol particles does not disturb the drops in terms of velocity and axis ratio.

Temperature and relative humidity inside the chamber are monitored continuously during the experiments using a thermocouple and a capacitive hygrometer. To measure

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the mass density of aerosol particles inside the chamber, a known volume is pumped through a HEPA filter, and analysed with a fluorimetric method. Finally, the Particle Size Distribution (PSD) is measured inside the chamber in terms of aerodynamic diameters, by simultaneously using an Electrical Low Pressure Impactor (ELPI, Marjamaki et al., 2000) and an Aerodynamic Particle Sizer (APS, TSI-3321). These two particle sizers are used for their complementary size ranges (500 nm–20 μm for the APS, 7 nm–10 μm for the ELPI). The aerosol chamber is furnished with monodisperse aerosol particles generated with ultrasonic nebulisers.

2.4 Aerosol generator and particle characterisation

The aerosol particles studied in this work consist of pure fluorescein (C₁₀H₁₀Na₂O₅), successively generated with the help of two ultrasonic nebulisers (Sinaptec GA 2400, GA 500, Bemer and Tierce, 1996) producing monodisperse aerosol particles between 300 nm and 4 μm. These aerosol particles are selected because of their very important fluorescence properties. The principle of this atomiser is simple. Ultrasounds, produced by a piezoelectric ceramic, nebulise a solution of fluorescein (dissolved in distilled water at various concentrations) and thus generate droplets. These droplets are dried and the produced aerosol particles are carried in the aerosol chamber by a monitored airflow.

The diameters of the particles in the aerosol chamber are measured with both APS and ELPI in terms of their aerodynamic diameter (d_{ae}). This aerodynamic diameter is then converted into a physical diameter (d_{ap}) using Eq. (3) (Baron and Willeke, 2001). According to Motzkus (2007) the shape factor of fluorescein aerosol particles is close to unity, thus the physical diameter (d_{ap}) also corresponds to the equivalent volume diameter.

$$d_{ap} = d_{ae} \sqrt{\left(\frac{C_{c,d_{ae}}}{C_{c,d_{ap}}}\right) \left(\frac{\rho_0}{\rho_p}\right)} \quad (3)$$

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Where ρ_0 and ρ_p are respectively the standard density of liquid water (1000 kg m^{-3}) and aerosol particles, and C_c the Cunningham slip correction factor (Hinds, 1982).

The ratio $\frac{C_{c,d_{ae}}}{C_{c,d_{ap}}}$ is considered equal to Eq. (1). The density of the aerosol particles is determined with the help of Eq. (4), where the growth factor (GF) of fluorescein aerosol particles is measured with a Hygroscopic Tandem Differential Mobility Analyser (HTDMA, Villani et al., 2008). The measured growth factors as a function of relative humidity are presented in Fig. 4.

$$\rho_p = \frac{C_{\text{C}_{10}\text{H}_{10}\text{Na}_2\text{O}_5} + C_{\text{water}}(\text{GF}^3 - 1)}{\text{GF}^3} \quad (4)$$

2.5 Experimental procedure

Each experiment starts by flushing the aerosol chamber with dry filtered air. Then the drop generator is set to the desired drop size (2 mm or 2.6 mm in this set of experiments). The drops generated are characterised inside the aerosol chamber after their acceleration inside the free fall shaft (Fig. 3 and Table 1). This characterisation consists of measuring the droplet diameters, axis ratios, and velocities inside the aerosol chamber.

Then, the aerosol chamber is filled with fluorescein aerosol particles, which size is measured continuously with both APS and ELPI. Figure 5 presents a characteristic aerosol particle size distribution measured in the aerosol chamber by means of the APS; the geometric standard deviation of the aerosol particle size distribution is in the order of 1.3. Finally, start the aerosol sampling on the HEPA filter at a flow rate of 1 L min^{-1} and the drop collection. For each measurement, a sample of 1.2 g of drops is collected (300 drops with a diameter of 2 mm). The mass of fluorescein collected on the filter and by the drops are both measured with fluorescence spectroscopy; they enable to determine respectively the mass concentration of fluorescein particles in suspension inside the aerosol chamber (C_{fluoAC}), and the concentration of fluorescein

inside the drops ($C_{\text{fluorDrop}}$). Since temperature and relative humidity are both monitored inside the aerosol chamber, the combination of all these measurements enables us to calculate the collection efficiency.

$$E(d_{\text{ap}}, D_d, \text{RH}) = \frac{2 D_d C_{\text{fluorDrop}}}{3 H C_{\text{fluorAC}}} \quad (5)$$

- 5 This entire procedure was conducted 399 times and provided measurements of the collection efficiencies of aerosol particles between 0.3 μm and 3.5 μm in diameter by drops between 2 and 2.6 mm in diameter.

3 Preventing sources of error and assessment of uncertainties

A careful assessment of all uncertainties revealed that the main source of error results from a potential fluorescein contamination of any item in the BERGAME set-up (free-fall shaft, aerosol chamber, or laboratory). This contamination is assessed before each experiment. A sample of 300 drops is collected just above the aerosol chamber after their acceleration in the free fall shaft. This sample is analysed by fluorescence spectroscopy. If the fluorescein mass concentration in this sample is not, at least, one order of magnitude lower than the mass concentration sampled in the drops that crossed the aerosol chamber ($C_{\text{fluorDrop}}$), the measurement is discarded, and the experimental device completely cleaned.

Furthermore, we retained only the measurement in which the:

- fluorescein concentration in the drops is at least twice the fluorometer's detection limit ($1 \times 10^{-11} \text{ g mL}^{-1}$),
- relative humidity is below 90 % in the aerosol chamber, to match the operating ranges of both the aerosol spectrometers,

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collection efficiency. This leads to an underestimation of the collection efficiency, for 0.3 μm particles, of one order of magnitude for the DESCAM model and two orders of magnitude for the Slinn model. In DESCAM the collection efficiencies are a compilation of measurements from publications without observations in that drop size range. For a discussion on how this underestimation can impact the total mass of aerosol particles washed out by rain, see Quérel et al. (2013).

Concerning the Slinn model, it lacks the increase because the hypothesis of potential flow is not valid, especially in the wake of the drop, where recirculating eddies seem to develop at Reynolds numbers larger than 20 (a drop of 280 μm diameter falling at terminal velocity has a Reynolds numbers of 20). Beard (1974) calculated the influence of these eddies on the collection efficiencies. He found that the smallest aerosol particles are trapped by the vortexes on the trailing side of the drop, which induce rear capture of these aerosols. A linear extrapolation of Beard (1974) calculations to our drop size is presented in Fig. 8. With regards to our experimental Reynolds numbers (Table 1), this extrapolation might seem daring because in his theoretical study, Beard (1974) predicted that eddy shedding should start at Reynolds numbers close to 450, leading to a decrease in aerosol particle collection efficiency in the submicron range. Nevertheless, this extrapolation is in line with our measurements in the submicron range. However, Beard (1974) proposed this transition for perfectly spherical drops, and the experiments highlight that 2 mm drops falling at terminal velocity are slightly oblate (Fig. 3), and moreover oscillate at high frequencies (Szakáll et al., 2009, 2010). As a consequence, it can be expected from current experiments that eddy shedding should start only at Reynolds numbers greater than 800. This expectation is confirmed by flow characterisations performed by Quérel (2012) with the help of PIV techniques (Adrian, 1986; see also Quérel et al., 2013; Fig. 4). These measurements highlight that at a Reynolds number of 800 the vortexes behind the drop could be still be stuck to the drop. In order to validate the mechanism of rear capture predicted by Beard (1974), it is planned to perform measurements of the collection efficiency of

1 mm raindrop, thus a direct comparison with Bear calculations could be performed without any extrapolation.

Another important result obtained is that the collection efficiency seems to be independent of relative humidity for drops with a diameter of 2 mm (Fig. 9).

Figure 9 shows that there is no measurable effect on the collection efficiency resulting from varying relative humidity. In order to understand this result, a confrontation of this measurement with the semi-empirical correlation introduced by Davenport and Peters (1978) to calculate the elementary collection efficiency due to diffusiophoresis (E_{dph} , Eq. 8), was performed and is presented in Fig. 9.

$$E_{\text{dph}} = \frac{4T_{\text{air}}D_{\text{w} \rightarrow \text{air}} \left(2 + 0.6Re^{\frac{1}{2}}Sc^{\frac{1}{3}}\right)}{P \cdot V_d \cdot D_d} \left(\frac{P_{\text{sat, air}}}{T_d} - \frac{P_{\text{sat, air}} \cdot RH}{T_{\text{air}}} \right) \sqrt{\frac{M_w}{M_{\text{air}}}} \quad (8)$$

Where $P_{\text{sat, air}}$ is the water vapour saturation pressure (Pa), $D_{\text{w} \rightarrow \text{air}}$ is the diffusion coefficient of water vapor in air ($\text{m}^2 \text{s}^{-1}$), M_w and M_{air} are respectively the molar masses of water and air (kg mol^{-1}), P the atmosphere pressure (Pa), and finally T_d and T_{air} are the respective temperatures of the drop and the air (K). Current measurements do not reveal any major inconsistency with that correlation. Indeed, for larger aerosol particles (diameter greater than $1.5 \mu\text{m}$) the collection efficiencies measured are at least one order of magnitude greater than the diffusiophoretic elementary collection efficiency of Eq. (8). Thus, in that aerosol particle size range, the aerosol collection is totally driven by inertial impaction, and no contribution of phoretic forces should be observed. Below $0.5 \mu\text{m}$, it is observed that the collection efficiencies measured are still one order of magnitude greater than the diffusiophoretic elementary collection efficiency. The Davenport and Peters (1978) equation is, thus, consistent with the measurements presented for both these size ranges.

It seems that, close to the minimum in efficiency (between $0.6 \mu\text{m}$ and $1.2 \mu\text{m}$), diffusiophoretic effects are overestimated by the Davenport and Peters (1978) equation. To confirm this observation, it would have been very interesting to make measurements in

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a minimum in this study. At a later date however, it will be necessary to explore this parameter in collection efficiencies of aerosol particles by 2 mm drops.

Finally, from a longer term point of view, if all these recommended experiments on the collection of particles by raindrops are conducted, it will be necessary to apply the same kind of thorough study on collection for the other hydrometeors (snow, hail, etc.) in order to improve our knowledge of below-cloud scavenging, and upgrade the modelling process.

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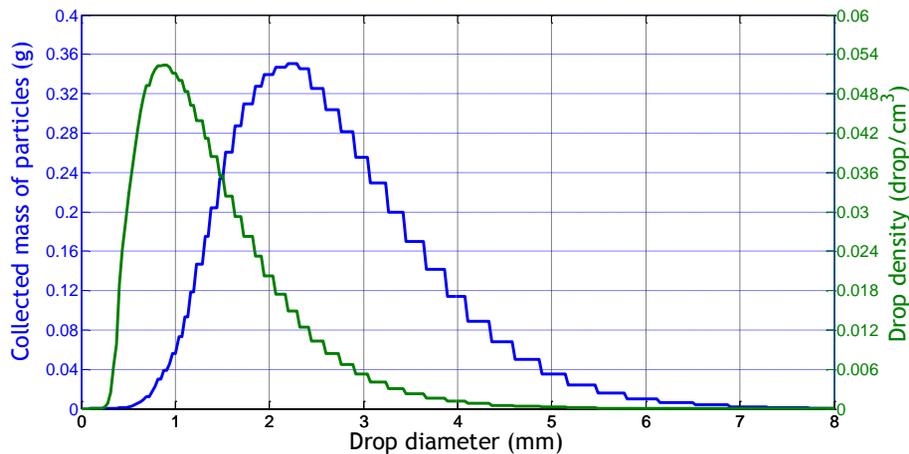


Fig. 1. Collected mass of particles and drop density as a function of the drop diameter (using DESCAM).

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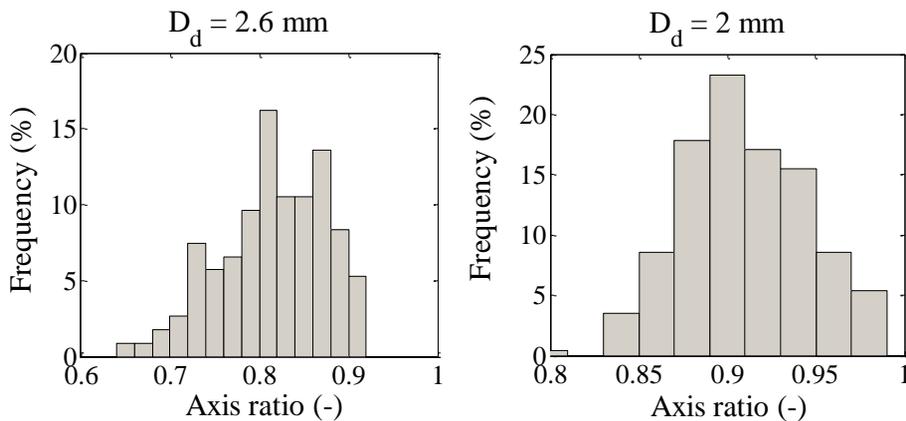


Fig. 3. Distribution of axis ratio of drops measured in the BERGAME aerosol chamber over a sample of 200 drops.

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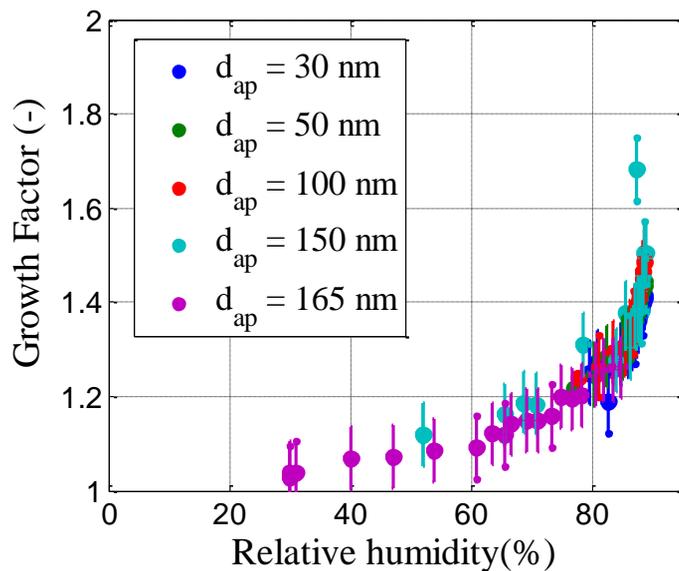


Fig. 4. Growth factor (GF) of fluorescein aerosol particles measured using an HTDMA (according to Villani et al., 2008 the RH and GF uncertainties are respectively less than 1 % and 0.07).

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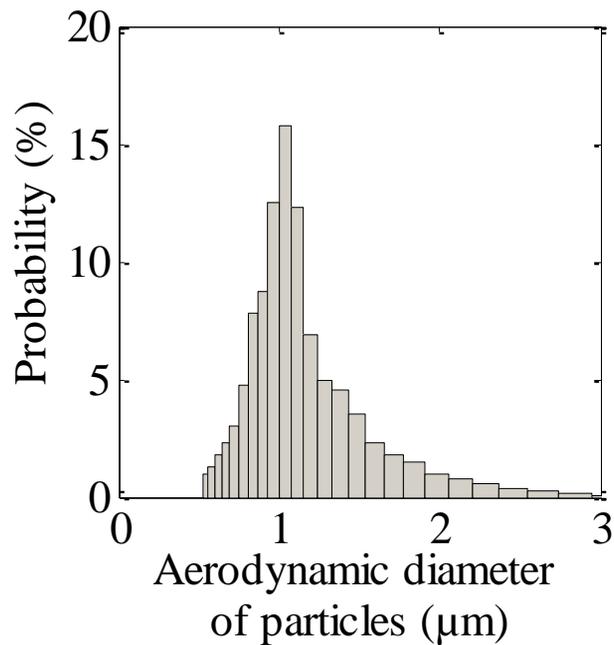


Fig. 5. Characteristic size distribution of aerosol particles measured in the aerosol chamber, with the Aerodynamic Particle Sizer.

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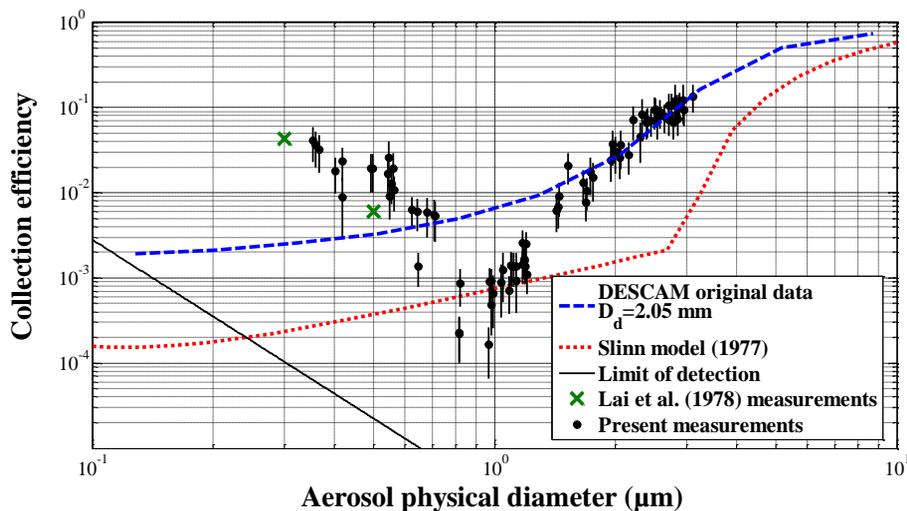


Fig. 6. Collection efficiencies measured in the BERGAME experiment for 2 mm and 2.6 mm as a function of particle diameter.

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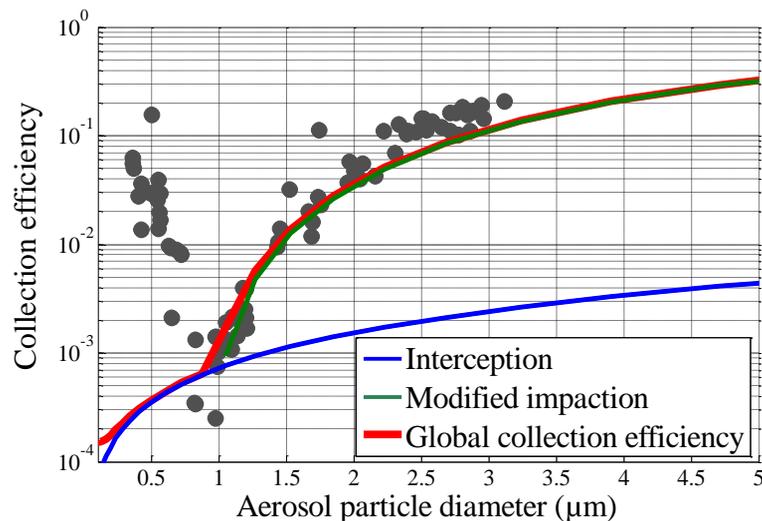


Fig. 7. Different parameterizations of the Slinn (1977) model for impaction scavenging; blue curve: classical Slinn model for interception; green curve: modified Slinn model for impaction (Eq. 7); red curve: global inertial contributions to collection efficiency.

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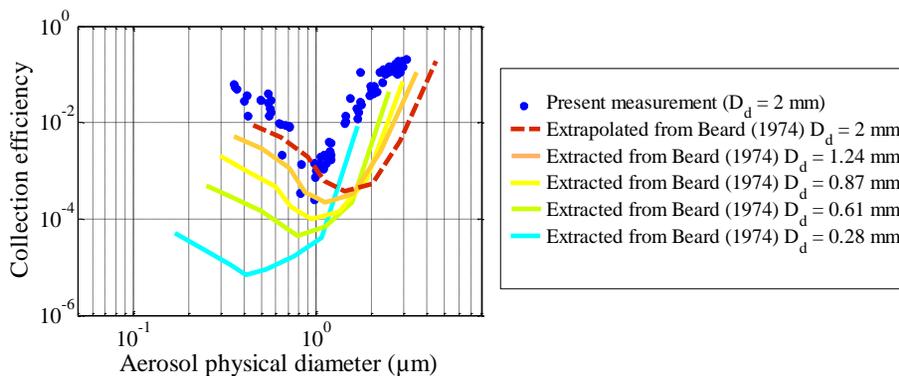


Fig. 8. Comparison of present experimental results (blue dots) to the Beard (1974) rear capture model; solid and dashed curves are respectively extracted and extrapolated from Beard (1974).

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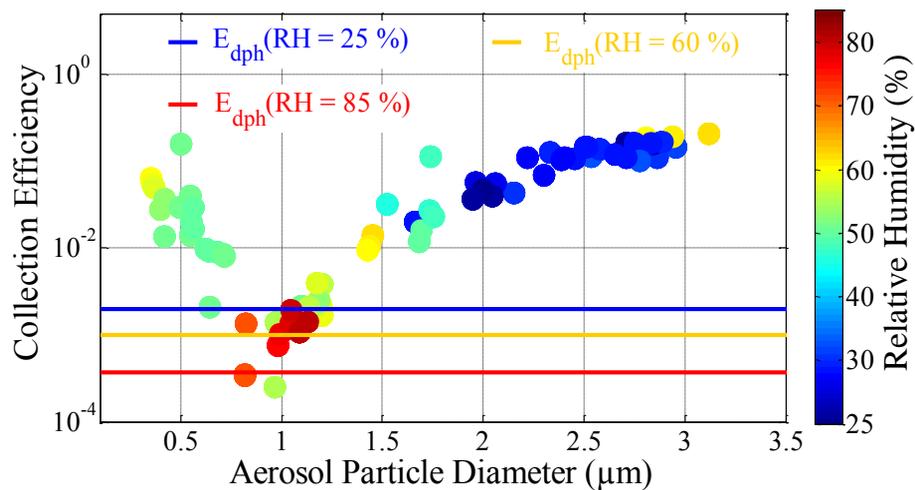


Fig. 9. Collection efficiencies measured for drops of 2 mm in diameter as a function of relative humidity, and comparison with the model of Davenport and Peters (1978), a semi-empirical correlation to evaluate diffusiophoretic elementary collection efficiency.