

Measuring the
atmospheric organic
aerosol volatility

E. Karnezi et al.

Measuring the atmospheric organic aerosol volatility distribution: a theoretical analysis

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Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

⏪

⏩

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Abstract

Organic compounds represent a significant fraction of submicrometer atmospheric aerosol mass. Even if most of these compounds are semi-volatile in atmospheric concentrations, the ambient organic aerosol volatility is quite uncertain. The most common volatility measurement method relies on the use of a thermodenuder (TD). The aerosol passes through a heated tube where its more volatile components evaporate leaving the less volatile behind in the particulate phase. The typical result of a thermodenuder measurement is the mass fraction remaining (MFR), which depends among other factors on the organic aerosol (OA) vaporization enthalpy and the accommodation coefficient. We use a new method combining forward modeling, introduction of “experimental” error and inverse modeling with error minimization for the interpretation of TD measurements. The OA volatility distribution, its effective vaporization enthalpy, the mass accommodation coefficient and the corresponding uncertainty ranges are calculated. Our results indicate that existing TD-based approaches quite often cannot estimate reliably the OA volatility distribution, leading to large uncertainties, since there are many different combinations of the three properties that can lead to similar thermograms. We propose an improved experimental approach combining TD and isothermal dilution measurements. We evaluate this experimental approach using the same model and show that it is suitable for studies of OA volatility in the lab and the field.

1 Introduction

Atmospheric aerosol particles play an important role in the Earth’s energy balance by absorbing and scattering solar radiation (direct effect) and influencing the properties of clouds and lifetime (indirect effects) (IPCC, 2007). They have significant negative effects on human health, including premature death, increases in respiratory illnesses and cardiopulmonary mortality (Nel et al., 2005; Pope and Dockery, 2006).

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Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Aerosols contain a wide variety of inorganic and organic compounds, with organics representing about 50 % of the fine ($< 1 \mu\text{m}$) aerosol mass (Zhang et al., 2007). Organic aerosol (OA) originates from many different natural and anthropogenic sources and processes. It can be emitted directly, e.g. from fossil fuels and biomass combustion (so called primary organic aerosol) or formed by atmospheric oxidation of volatile organic compounds (VOCs) (secondary organic aerosol, SOA). Since the oxidation pathways for VOCs are complex and the reactions lead to hundreds or thousands of oxygenated products, our understanding of organic aerosol formation mechanisms and the OA chemical and physical properties is still incomplete.

The volatility of atmospheric OA is one of its most important physical properties. It determines the partitioning of these organic compounds between the gas and particulate phases, the organic aerosol concentration, the rate of reactions and the atmospheric fate of the corresponding compounds. Measurement of the OA volatility distribution has been recognized as one of the major challenges in our efforts to quantify the rates of formation of secondary organic particulate matter (Donahue et al., 2012).

OA consists of thousands of compounds, too few of which have been identified. The volatility basis set framework (Donahue et al., 2006) was developed to describe absorptive partitioning by lumping all these compounds into surrogates along an axis of volatility. This approach typically employs species with effective saturation concentrations at 298 K separated by one order of magnitude (bin), with values ranging from, say, 0.01 to $10^6 \mu\text{g m}^{-3}$. By quantifying the volatility distributions of primary and secondary OA, a physically reasonable, yet suitable for large-scale chemical transport models, description of semi-volatile organics can be obtained (Pathak et al., 2007; Stanier et al., 2008).

Thermodenuders (TD) have been developed to measure the volatility of ambient aerosol (Burtsher et al., 2001; Wehner et al., 2002, 2004; Kalberer et al., 2004; An et al., 2007). A TD consists of 2 basic parts: a heated tube where the more volatile particle components evaporate, leaving less volatile species behind and the denuder tube containing usually activated carbon where the evaporated material is adsorbed

avoiding potential re-condensation when the sample is cooled to room temperature. The aerosol mass fraction remaining (MFR) at a given temperature, after passing through the TD, is the most common way of reporting the TD measurements.

The measurement of the volatility of OA has received considerable attention recently and has been carried out both in the field (Engler et al., 2007; Huffman et al., 2009; Lee et al., 2010; Cappa and Jimenez, 2010) and in the laboratory (An et al., 2007; Jonsson et al., 2007; Faulhaber et al., 2009). Riipinen et al. (2010) have shown that the OA practically never reaches equilibrium in a TD in ambient concentration levels. The MFR of OA in a TD thus depends on many factors, more importantly on the vaporization enthalpy and potential mass transfer resistances as the particles evaporate. The inversion of the TD measurements to calculate the OA volatility distribution has proven to be challenging because of the many parameters affecting the resulting MFR.

Previous studies have assumed a priori values for the effective vaporization enthalpy and the mass accommodation coefficient in order to estimate the OA volatility. Lee et al. (2010) trying to measure the volatility of ambient OA assumed values for the vaporization enthalpy and the accommodation coefficient equal to 80 kJ mol^{-1} and 0.05 accordingly. They used the time dependent evaporation model by Riipinen et al. (2010), with least squares minimization, to reproduce ambient measurements collected in the Eastern Mediterranean. For most measurements it was difficult to estimate the volatility distribution especially for the less volatile components. Moreover, a change of the accommodation coefficient from 0.05 to 1 resulted in shifting of the estimated volatility distribution by one order of magnitude. Lee et al. (2011) used the same mass transfer model in order to reproduce experimental measurements from different precursors assuming values for the vaporization enthalpy and the accommodation coefficient. Cappa (2010) developed a new model of evaporation in a TD accounting for the cooling section and the velocity profile across the TD tube. They demonstrated the importance of the vaporization enthalpy especially for values less than 100 kJ mol^{-1} . They also underlined the importance of constraining the value of accommodation coefficient in order to quantify the volatility distribution of OA. Cappa and Jimenez (2010) used the model of

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Cappa (2010) to quantify the volatility distribution of ambient OA in Mexico City using measurements from the MILAGRO campaign. Assuming several values for the vaporization enthalpy, either using the relationship from Epstein et al. (2010) or assuming that the vaporization enthalpy depended linearly on temperature or that it had constant values from 50 to 150 kJ mol⁻¹ they estimated different volatility distributions. Changing the value of the accommodation coefficient from 1 to 0.1 the estimated volatility distribution was shifted to higher values by approximately one order of magnitude.

Previous studies (An et al., 2006; Lee et al., 2010, 2011; Riipinen et al., 2010) have stressed the importance of performing the volatility measurements at a range of residence times. An et al. (2006) introduced an improved TD allowing larger residence times. Lee et al. (2010) performed thermodenuder experiments at two residence times in order to estimate the volatility distribution. Their results were sensitive to the mass accommodation coefficient values and authors concluded that even higher residence times (minutes) might be needed in order to estimate reliably OA volatility distributions. Lee et al. (2011) argued that multiple residence times are needed in order to decouple mass transfer effects from thermodynamics, since particles do not reach equilibrium with the surrounding gas phase in the range of residence times used in the experiments. Similar conclusions were reached by Riipinen et al. (2010) and Cappa (2010).

The sensitivity of TD results to several additional parameters has also been investigated in past studies. Lee et al. (2010) concluded that a monodisperse approximation using one effective value for the diameter of the particles instead of the full distribution resulted in changes of the thermograms of less than 2%. Lee et al. (2011) explored the effect of the cooling section and the role of surface free energy and Cappa (2010) the role of the assumed value for the diffusion coefficient or the average effective diameter of the particles. Once again the conclusion was that these parameters were not as important as the vaporization enthalpy and the accommodation coefficient for the estimation of the volatility distribution. Volatility measurements at longer timescales, where equilibrium of the system can be reached, have been performed by Grieshop et al. (2009). They used isothermal dilution measurements evaporating OA in a smog

chamber. They assumed low values for the accommodation coefficient from 0.001 to 0.1 and estimated the corresponding volatility distributions. Then, using TD measurements they further constrained the volatility distribution for primary OA assuming effective values for the vaporization enthalpy.

In this study, we explore methods for estimating the OA volatility distribution together with the effective vaporization enthalpy and mass accommodation coefficient. We develop a method combining forward modeling with known values for the three properties that we will try to estimate, introduction of random “experimental” error and finally inverse modeling with least squares error minimization for the estimation of the OA volatility distribution, its effective vaporization enthalpy and the mass accommodation coefficient. We propose an approach for the estimation of the corresponding uncertainties. Experimental approaches to improve these estimates and to reduce the corresponding uncertainties are explored. We examine the utility of using two residence times, using isothermal dilution instead of thermodenuder measurements (Grieshop et al., 2009), and finally combining TD and isothermal dilution measurements.

2 Thermodenuder model

We use the mass transfer model of Riipinen et al. (2010) modeling the time-dependent evaporation of multicomponent aerosol particles by solving the mass transfer equations for a monodisperse population of particles suspended in air. The mass flux of compound i from the gas phase to the particles, I_i , is calculated by (Seinfeld and Pandis, 2006):

$$I_i = \frac{2\pi d_p M_i \beta_{mi} D_i}{RT_{TD}} (p_i - p_i^0), \quad (1)$$

where d_p is the particle diameter, R the ideal gas constant, M_i and D_i the molecular weight and diffusion coefficient of compound i in the gas phase at temperature T_{TD} (the temperature in the heated part of the TD), and p_i^0 and p_i are the partial vapor pressures

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

⏪

⏩

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



of i at the particle surface and far away from the particle, respectively. In our simulations we assume a particle diameter of 200 nm, a molecular weight of 0.2 kg mol^{-1} and a diffusion coefficient of $10^{-5} \text{ m}^2 \text{ s}^{-1}$.

The mass flux is corrected for kinetic and transition regime effects with the factor β_{mi} (Fuchs and Sutugin, 1970):

$$\beta_{\text{mi}} = \frac{1 + Kn_i}{1 + \left(\frac{4}{3a_{\text{mi}}} + 0.377\right) Kn_i + \frac{4}{3a_{\text{mi}}} Kn_i^2} \quad (2)$$

where Kn_i is the Knudsen number, that is the ratio of the mean free path of vapor i and the particle radius, and a_{mi} the mass accommodation coefficient of i on the particles. The mean free path is estimated by:

$$\lambda_i = \frac{3 \cdot D_i}{\bar{c}} \quad (3)$$

where \bar{c} is the mean velocity of the gas molecules, given by:

$$\bar{c} = \sqrt{\frac{8 \cdot R \cdot T_{\text{TD}}}{\pi \cdot M_i}} \quad (4)$$

The partial vapor pressure of i at the particle surface, p_i^0 is given by:

$$p_i^0 = x_i \gamma_i p_{\text{sat},i} \exp\left(\frac{4M_i\sigma}{RT_p\rho d_p}\right) = x_{\text{mi}} \frac{C_i^* RT_{\text{TD}}}{M_i} \exp\left(\frac{4M_i\sigma}{RT_p\rho d_p}\right) \quad (5)$$

where x_i is the mole fraction and γ_i the activity coefficient of i in the particle phase, $p_{\text{sat},i}$ the pure component vapor pressure of i over a flat surface, T_p the particle temperature, C_i^* represents the effective saturation concentration of i in the volatility basis set (Donahue et al., 2006) and x_{mi} is the mass fraction of i in the particle. In this study, we

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



will be using a fixed basis set with four volatility bins with effective saturation concentrations 0.01, 0.1, 1 and 10 $\mu\text{g m}^{-3}$ for each volatility bin. We assume a surface tension of 0.05 N m^{-1} and a density of the surrogate compounds of 1500 kg m^{-3} .

5 The saturation concentrations of the evaporating species at T_{TD} are estimated using the integrated form of the Clausius–Clapeyron equation:

$$C_i^*(T_{\text{TD}}) = C_i^*(298 \text{ K}) \exp \left[\frac{\Delta H_{\text{vap},i}}{R} \left(\frac{1}{298} - \frac{1}{T_{\text{TD}}} \right) \right] \left(\frac{298}{T_{\text{TD}}} \right) \quad (6)$$

where $\Delta H_{\text{vap},i}$ is the vaporization enthalpy of species i . The temperature dependence of the diffusion coefficients of the evaporating species is taken into account by using:

$$D_i(T_{\text{TD}}) = D_i(298) \left(\frac{T_{\text{TD}}}{298} \right)^\mu \quad (7)$$

10 where μ is a constant usually ranging from 1.5 to 2.0 (Chen and Othmer, 1962). We used the value of 1.75 for all the studied compounds.

The time-dependent evaporation of the organic aerosol is simulated by solving the differential equations for total particle mass m_p and gas phase concentrations C_i of the evaporating species:

$$15 \quad \frac{dm_p}{dt} = - \sum_{i=1}^n I_i$$

$$\frac{dC_i}{dt} = I_i \cdot N_{\text{tot}} \quad (8)$$

20 where N_{tot} is the total number concentration of the particles (assuming a monodisperse particle population). The MFR is then calculated from the ratio of the particle mass at $t = t_{\text{res}}$ (where t_{res} is the residence time through the heating tube) to the initial mass of the particles. We focus on the particles moving along the centerline of the TD and at the corresponding centerline temperature.

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page	
Abstract	Introduction
Conclusions	References
Tables	Figures
◀	▶
◀	▶
Back	Close
Full Screen / Esc	
Printer-friendly Version	
Interactive Discussion	



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



We use, as inputs, values for the geometry of the TD (the length and the residence time in the heated tube), the temperature inside the TD (T_{TD}), the initial mass concentration of the organic aerosol (C_{aer}) and the properties of the organic compounds (such as the volatility distribution, vaporization enthalpy, accommodation coefficient, etc.). For the description of the geometry of the TD we used the values for the Carnegie Mellon TD of Lee et al. (2010). Specifically for the heated tube we used a length of 55 cm and a centerline residence time of 17 s.

Using the mass transfer model of Riipinen et al. (2010), modeling the time-dependent evaporation of multicomponent aerosol particles, we constructed theoretical thermograms (MFR vs. T_{TD}). Previous studies have often assumed that thermograms can be directly connected to the volatility of OA. Figure 1 indicates that we can have very similar thermograms for organic aerosols with very different volatilities (orders of magnitude different). In this example, the reduction of saturation concentration is balanced by changes in the accommodation coefficient and the vaporization enthalpy. The similarity of these suggests that the inversion of the thermograms in order to calculate the OA volatility will be very challenging.

2.1 Pseudo-experimental data

In order to evaluate how well we can estimate the volatility distribution we used “pseudo-experiments” corrupting the output of the TD model, for systems with known volatility distributions and properties, with randomly generated “experimental” error. In this way we could produce relatively realistic “experimental results” for systems with known volatility distributions and properties. We “corrupted” the TD model predictions with random error assuming a normal distribution, based on the variability of laboratory measurements with the same TD conducted by Paciga et al. (2013), with a standard deviation given by:

$$\sigma = 0.51 \cdot \text{MFR}_{\text{true}} - 0.5 \cdot \text{MFR}_{\text{true}}^2 \quad (9)$$

where MFR_{true} are the correct MFR values. A typical example is shown in Fig. 2.

2.2 Optimum OA volatility distribution

The MATLAB least-squares fitting algorithm `lsqcurvefit` was used in order to obtain the best possible fit between the “measured” and modeled MFRs. Four lognormally equally spaced volatility bins were used with volatilities from 10^{-2} to $10 \mu\text{g m}^{-3}$. The corresponding volatility distribution, vaporization enthalpy and mass accommodation coefficient were estimated by the algorithm minimizing the sum of the squared differences between the MFR model predictions and the pseudo-measurements. In the least squares optimization a total of 12 pseudo-measurements were used in all cases.

A wide variety of compositions were tested during the simulations, including one component, two component or multicomponent aerosols, with various volatility distributions, and with different values for the vaporization enthalpy and the accommodation coefficient. The results for three of these tests that are used as illustrative examples are shown in Table 1. For Test 1 corresponding to OA consisting of very low and high volatility material (60 % $0.01 \mu\text{g m}^{-3}$ and 40 % $10 \mu\text{g m}^{-3}$) the optimization resulted in absolute volatility error of less than 10 % for all bins. The vaporization enthalpy was well-estimated (relative error equal to 8 %) and the mass accommodation coefficient was estimated within a factor of two (0.97 instead of 0.5). For Test 2 corresponding to multicomponent OA (10 % $0.1 \mu\text{g m}^{-3}$, 30 % $1 \mu\text{g m}^{-3}$ and 60 % $10 \mu\text{g m}^{-3}$), the estimated volatility distribution had a different shape than the true one, with more material predicted for the bin of $1 \mu\text{g m}^{-3}$ (predicted mass fraction equal to 0.49 instead of 0.3) and less for the $10 \mu\text{g m}^{-3}$ bin (predicted mass fraction equal to 0.31 instead of 0.6). Also some very low volatility material was estimated (predicted mass fraction equal to 0.07 while none was present). The vaporization enthalpy was estimated with a relative error equal to 40 % and the accommodation coefficient was well estimated (0.72 instead of unity). For Test 3 with the case of one component OA with a volatility of $1 \mu\text{g m}^{-3}$, the estimates of all properties were far from the truth. Most of the material (88 %) was estimated to be in the $0.1 \mu\text{g m}^{-3}$ bin instead of $1 \mu\text{g m}^{-3}$ and some material (12 %) was predicted in the highest volatility bin of $10 \mu\text{g m}^{-3}$. The estimated vaporiza-

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



tion enthalpy was more than a factor of two higher than the true value and the estimated accommodation coefficient was a factor of 25 lower than it should be.

The results, using different initial guesses, for the case of multiple component OA (Test 2) are shown in Fig. 3. For an initial guess of [0 0 0.3 0.7] for the mass fractions of the volatility bins ($C^* = [0.01 \ 0.1 \ 1 \ 10] \mu\text{g m}^{-3}$), 50 kJ mol^{-1} for the vaporization enthalpy and 0.5 for the accommodation coefficient, the shape of the volatility distribution was estimated correctly but with significant errors of 0.1–0.2 in the 0.1, 1 and 10 $\mu\text{g m}^{-3}$ bins. The vaporization enthalpy estimation error was 24 % and the estimated accommodation coefficient was 0.9 close to the true value of unity. This is however a local minimum of the objective function. The global minimum (minimum error) was found when we used an initial guess of [0.1 0.1 0.3 0.5] for the mass fractions, 80 kJ mol^{-1} for ΔH_{vap} and 0.2 for a_m . The estimated OA volatility distribution, in this case, is shown in Fig. 3b. In this case, the shape of the volatility distribution is not correct and there are errors in the mass fractions of the volatility bins as large as 0.3. The estimated vaporization enthalpy and accommodation coefficient were similar to those of the previous guess with a relative error of 35 % for ΔH_{vap} . Due to the experimental error, the global minimum can correspond to volatility distributions that are far from the true values. We conclude that the optimization method may not be appropriate for the estimation of the volatility distribution, the vaporization enthalpy and the mass accommodation coefficient. It is also clear that we need an approach for estimating the corresponding uncertainties.

2.3 Estimation of uncertainty

In an effort to explore in more detail the solution space for the problem we discretized the parameter space and simulated all combinations of volatilities, ΔH_{vap} and a_m . We used once more four bins for volatilities from 10^{-2} to 10 $\mu\text{g m}^{-3}$ and varied the mass fraction of each bin from 0 to 1 with a step of 0.1. The values used for ΔH_{vap} were from 20 to 200 with discrete values of 20, 50, 80, 100, 150 and 200 kJ mol^{-1} and for

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



a_m the values were from 0.01 (large mass resistance) to 1 (no mass resistance) with discrete values of 0.01, 0.05, 0.1, 0.2, 0.5 and 1. We tried in our simulations also other discretizations for the values of the vaporization enthalpy and the mass accommodation coefficient and they did not affect the results. In the rest of the paper, the discretizations for the ΔH_{vap} and the a_m described above will be used for all of the simulations. For each simulation the percent error was estimated from:

$$E_i = \frac{100}{n} \sqrt{\sum_i^n (\text{MFR}_{i,\text{guess}} - \text{MFR}_i)^2} \quad (10)$$

where $\text{MFR}_{i,\text{guess}}$ is the MFR for a certain combination of parameters for data point i (corresponding to a specific temperature), MFR_i is the “measured” MFR and n is the number of the different temperatures T_{TD} used in our “measurements”.

After performing simulations for all combinations of all properties we identified the combinations which led to small errors (less than 2%). From these values we then calculated a “best estimate” using the inverse error as a weighting factor:

$$\bar{x} = \frac{\sum_i^N \left[(x_i) \cdot \left(\frac{1}{E_i} \right) \right]}{\sum_i^N \left[\frac{1}{E_i} \right]} \quad (11)$$

where x_i is the value of property i (the mass fractions of volatility bin i or the vaporization enthalpy ΔH_{vap} or accommodation coefficient $\log(a_m)$).

We also calculated the uncertainty range for all three properties calculating the standard deviation (σ) of the corresponding values:

$$\sigma = \sqrt{\frac{\sum_i^N \left[\left((x_i - \bar{x})^2 \cdot \left(\frac{1}{E_i} \right) \right) \right]}{\sum_i^N \left[\frac{1}{E_i} \right]}} \quad (12)$$

The logarithms of the accommodation coefficient values were used in order to avoid negative accommodation coefficient values inside the uncertainty range. We report \pm one standard deviation as the uncertainty range in the rest of the paper.

3 Results

3.1 Number of measurements of TD experiment

The first parameter of the thermodenuder experiments explored was the number of measurements. In previous studies, thermodenuder measurements vary between 6 (An et al., 2006) and 12 measurements (Faulhaber et al., 2009).

A wide variety of cases of OA were tested during the simulations once more. The results for a multicomponent OA with mostly nonvolatile material (80 % $0.01 \mu\text{g m}^{-3}$, 5 % $0.1 \mu\text{g m}^{-3}$, 10 % $1 \mu\text{g m}^{-3}$ and 5 % $10 \mu\text{g m}^{-3}$), for the case of 6 and 12 measurements, are given in Fig. 4 as a representative example. For the first experiment, with a small number of measurements (6 points), there is large uncertainty in the two least volatile bins (with a standard deviation up to 0.25). The uncertainty range, in the least and most volatile bins (0.01 and $10 \mu\text{g m}^{-3}$) does not include the correct values for the distribution. In the second experiment, twice as many measurements were used (12 points), the estimated uncertainty range is smaller (the standard deviation of all the

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



predicted mass fractions is less than 0.08) and it contains the correct volatility distribution. The relative error of the estimated ΔH_{vap} is 13 %, in both experiments. Finally, the a_m is underestimated for both experiments but with the second experiment (using 12 measurements) the uncertainty range includes the correct value.

For cases of OA with more uniform volatility distributions (e.g., cases where the mass fraction varies less than 0.2 between the bins), the use of 12 measurements instead of 6 gave similar estimates for the three properties (volatility distribution, vaporization enthalpy and mass accommodation coefficient) and the same uncertainty ranges. In cases of extreme volatility distributions, where most material is in one or two volatility bins, as in the case of the example in Fig. 4, using more measurements resulted in better estimates and smaller uncertainty ranges than using only a small number of measurements.

In Fig. 5, we examine two more cases of OA with extreme volatility distributions using 12 pseudo-measurements. In the first test, which is the same OA as in Test 1 discussed in Sect. 2.2, the OA consists of two components: very low volatility material (60 % $0.01 \mu\text{g m}^{-3}$) and high volatility material (40 % $10 \mu\text{g m}^{-3}$). The estimated uncertainty range is large especially for the two least volatile bins (with an uncertainty equal to 0.2) but it includes the actual volatility distribution. Also the estimated volatility distribution has the correct shape. The estimated vaporization enthalpy has an error of 5 % while the accommodation coefficient error is around 20 %.

In the second test, we assume that the OA consists of very low volatility material (50 % $0.01 \mu\text{g m}^{-3}$) and relatively high volatility material (50 % $1 \mu\text{g m}^{-3}$). The shape of the volatility distribution of the OA is not captured by the inversion results, the estimated uncertainty range is large (the uncertainty of all the predicted mass fractions is around 0.2) and the uncertainty range does not contain the actual volatility distribution. The error of the estimated ΔH_{vap} is 8 %. The accommodation coefficient is under-predicted by one order of magnitude (value equal to 0.15 instead of unity). The TD measurements are not sufficient in this case for the accurate estimation of the OA volatility distribution.

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



In order to evaluate how general are the above results of the proposed volatility estimation method we performed additional tests using ten randomly generated volatility distributions. The sets of parameters used are shown in Table 2. The ten first parameter sets have random OA volatility distributions, a vaporization enthalpy equal to 90 kJ mol⁻¹ (chosen as a reasonable intermediate value between 20 and 200 kJ mol⁻¹) and an accommodation coefficient of 0.1 (chosen as a medium mass resistance). Additional cases with either low (sets 11–13) or high mass transfer resistance (sets 14–16) and cases with low (sets 11 and 13) or higher vaporization enthalpies (sets 12, 15 and 16) were also examined.

The inversion results are shown in Table 3. They include the average absolute errors for the VBS bins, the relative error (%) for the vaporization enthalpy and the errors for a_m (in orders of magnitude). These results indicate that an accurate estimation of the OA volatility distribution is challenging in most cases. The volatility distribution was estimated with average absolute errors less than 0.1 for six out of the sixteen cases tested (sets 1, 4, 8, 9 10 and 13) and for the rest of the cases the errors were up to 0.22. The highest relative error for the ΔH_{vap} was 25 % and the average relative error was roughly 10 %. The error for the estimated accommodation coefficient, for the cases of OA, with a value equal to 0.1, was less than half order of magnitude (from 0.02 to 0.45) and for the cases with values of 0.01 or unity the error was half to almost one and half order of magnitude (from 0.3 to 1.22). Concerning the uncertainties (not shown), the uncertainty range of the volatility distribution in most of the cases was large (around 0.2). Exceptions are the cases with most material in the lowest and highest volatility bins where the uncertainty range is 0.05–0.15. The uncertainty of the estimated ΔH_{vap} for most of cases was around 20 %. The estimated accommodation coefficient, for the cases of OA, with a value equal to 0.1, had an uncertainty of less than one order of magnitude and for the cases with values of 0.01 or unity the uncertainty was closer to two orders of magnitude.

Based on the above results, it is evident that it is very difficult to estimate the three properties accurately and with a small uncertainty range since there are many

combinations of properties than can lead to a thermogram quite similar to the one from the pseudo-experiment. So, even if the uncertainty estimation method proposed here is a step forward, the TD inversion results are either too uncertain or sometimes erroneous. The TD measurements using one residence time (17 s) are not sufficient to constrain the three properties. It is clear that improvements in the volatility measurement approach itself are needed. A number of ideas are explored in the next section. These include, using more than one TD residence times, or, using measurements at much longer timescales (e.g., isothermal dilution measurements).

4 Improvements of volatility measurement method

4.1 Use of two residence times

In order to improve the method for the estimation of the OA volatility distribution, ΔH_{vap} and a_m , we simulated “measurements” using two residence times (Lee et al., 2010) but with half the data points for each measurement (6 points for each residence time). We used two residence times of 17 and 34 s. The estimation of the volatility distributions was improved, but the improvement in most cases was small to modest. For example, for the case of OA consisting of very low volatility material (50 % $0.01 \mu\text{g m}^{-3}$) and relatively high volatility material (50 % $1 \mu\text{g m}^{-3}$), the correct volatility distribution was still not retrieved, the uncertainty range once again was large (equal to 0.2) and it did not contain the actual volatility distribution. The relative error of the estimated ΔH_{vap} was 6 %. The accommodation coefficient was under-predicted by one order of magnitude (value equal to 0.12 instead of unity).

We performed a number of tests with different OA systems. The use of two residence times resulted in improved estimates in some cases (e.g., single component systems) but in the majority of the cases the improvement was marginal. The results were often quite similar to those of the one residence time discussed above (with twice the data points). We concluded that just doubling the residence time was not sufficient and the

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



next step was the exploration of the utility of evaporation measurements at much longer timescales than those that can be reached with a TD.

4.2 Isothermal dilution experiments

We tested the effectiveness of performing only isothermal dilution measurements instead of TD measurements. The isothermal evaporation of OA can take place in a smog chamber and allows residence times of a few hours (Grieshop et al., 2009). The isothermal evaporation results at room temperature do not depend on ΔH_{vap} , but only on C^* and a_m . We assume that we dilute our OA samples during the injection in the chamber with a 10-fold volume of clean air so in this way the initial gas and particle concentrations are lowered by a factor of 10 and the system is out of equilibrium. We allow the aerosol to evaporate in the chamber for 2 h, and assume that its concentration is measured every ten minutes. The error distribution used for the isothermal dilution is also based on the variability of the corresponding laboratory data. We “corrupted” the time dependent mass transfer model predictions with random error assuming a uniform distribution with a standard deviation given by:

$$\sigma = 0.05 \cdot \text{MFR}_{\text{true}} + 0.03 \quad (13)$$

where MFR_{true} are the correct MFR values.

A typical set of isothermal dilution “measurements” is shown in Fig. 6. The organic particles reach equilibrium with the gas phase after approximately thirty minutes in this pseudo-experiment. The inversion results for the case of OA consisting of very low volatility material (60 % $0.01 \mu\text{g m}^{-3}$) and high volatility material (40 % $10 \mu\text{g m}^{-3}$) and the OA with very low volatility material (50 % $0.01 \mu\text{g m}^{-3}$) and relatively high volatility material (50 % $1 \mu\text{g m}^{-3}$) are shown in Fig. 7. The estimated volatility distribution had significant error and the uncertainty was large (equal to 0.2). The accommodation coefficient was estimated within 20 %.

The dilution method was also used for the random sets of volatility distributions shown in Table 2 and the results are shown in Table 3. The average absolute errors

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



for the VBS bins were around 0.2 and the errors for the accommodation coefficient in all cases were up to one order of magnitude. Isothermal dilution did not consistently improve the estimated volatility distributions and the accommodation coefficient compared to the use of TD measurements. The uncertainty remains large, since there are still many combinations of the two properties that can lead to similar dilution curves.

4.3 Combination of TD and isothermal dilution measurements

We combined TD and isothermal dilution “measurements” performing the error minimization with the same method as before examining all possible solutions. In the case of Test 1 (Table 1) shown in Fig. 8 the estimated volatility distribution has the correct shape and the corresponding uncertainty range is small (uncertainty less or equal than 0.1). The ΔH_{vap} and the a_m were estimated within a few percent. In another challenging test (Fig. 9) the shape of the volatility distribution is again correctly predicted. The estimated value of the vaporization enthalpy has an error of only 7 % and the estimated accommodation coefficient is 0.4 instead of unity.

We also repeated all the tests of Table 2. The results are shown in Table 3. In 70 % of the cases, the volatility distribution was reproduced with absolute errors less than 0.1. The average relative error of the estimated ΔH_{vap} was roughly 7 %. The error for the estimated accommodation coefficient, for the cases of OA, with a value equal to 0.1, was less than half order of magnitude (up to 0.46) and for the cases with values of 0.01 or unity the error was up to one order of magnitude (from 0.24 to 1.22). The uncertainties (not shown) for the volatility distribution in 70 % of the cases were not higher than 0.05–0.1. The uncertainties for the vaporization enthalpy were around 10 %. The accommodation coefficient, for the cases of OA with a value equal to 0.1, had an uncertainty of half an order of magnitude. For cases where the accommodation coefficient was equal to unity, it was underpredicted with an uncertainty varying from half an order of magnitude (set 13), to one order of magnitude (set 11) to two orders of magnitude (set 12). For the cases of OA (sets 14 to 16), where the accommodation coefficient is equal to 0.01, it was overestimated by up to one order of magnitude.

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



even include the true value of the properties, with the exception in the estimation of the vaporization enthalpy where the errors are around 5–20 % in most cases tested.

Experimental approaches that would improve the method were explored. The performance of TD measurements under multiple residence times results in a small to modest improvement of the results. Use of isothermal dilution on its own instead of TD measurements usually leads to worse estimates of the volatility distribution compared to the TD. However, combining both TD and isothermal dilution measurements leads to promising results in the majority of the cases. Cases for which problems remain include those in which the OA does not come close to equilibrium after dilution or when the corresponding evaporated fraction is less than 20 %. Increased dilution and longer residence times can help in these cases. The approach combining TD and isothermal dilution measurements is recommended for future studies of OA volatility in both the lab and the field.

Acknowledgements. This research was supported by the US Department of Energy and the FP7 IDEAS project ATMOPACS.

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Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



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Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



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AMTD

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Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures



Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Table 1. Values of the true and estimated properties (volatility distribution, vaporization enthalpy, accommodation coefficient) for three OA examples.

	Test 1 OA with very low and high volatility material	Test 2 Multiple component OA	Test 3 One component OA
True values	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0.6 \ 0 \ 0 \ 0.4]$ $\Delta H_{\text{vap}} = 100 \text{ kJ mol}^{-1}$ $a_m = 0.5$	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0 \ 0.1 \ 0.3 \ 0.6]$ $\Delta H_{\text{vap}} = 50 \text{ kJ mol}^{-1}$ $a_m = 1$	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0 \ 0 \ 1 \ 0]$ $\Delta H_{\text{vap}} = 80 \text{ kJ mol}^{-1}$ $a_m = 1$
Optimization results	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0.63 \ 0 \ 0 \ 0.37]$ $\Delta H_{\text{vap}} = 92 \text{ kJ mol}^{-1}$ $a_m = 0.97$ $E_i = 1.09^a$	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0.07 \ 0.13 \ 0.49 \ 0.31]$ $\Delta H_{\text{vap}} = 70 \text{ kJ mol}^{-1}$ $a_m = 0.72$ $E_i = 0.3$	$C_i^* = [0.01 \ 0.1 \ 1 \ 1 \ 10]$ $X_i = [0 \ 0.88 \ 0 \ 0.12]$ $\Delta H_{\text{vap}} = 181 \text{ kJ mol}^{-1}$ $a_m = 0.04$ $E_i = 0.81$

^a The error, given by Eq. (10), describes the quality of the fit.

[Title Page](#)
[Abstract](#)
[Introduction](#)
[Conclusions](#)
[References](#)
[Tables](#)
[Figures](#)
[◀](#)
[▶](#)
[◀](#)
[▶](#)
[Back](#)
[Close](#)
[Full Screen / Esc](#)
[Printer-friendly Version](#)
[Interactive Discussion](#)


Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Table 2. Sets of random volatility distributions used for the evaluation of different inversion approaches.

OA Parameter Set	Mass Fraction				ΔH_{vap} (kJ mol ⁻¹)	a_m
	0.01 $\mu\text{g m}^{-3}$	0.1 $\mu\text{g m}^{-3}$	1 $\mu\text{g m}^{-3}$	10 $\mu\text{g m}^{-3}$		
1	0.135	0.06	0.14	0.665	90	0.1
2	0.45	0.04	0.315	0.195	90	0.1
3	0.255	0.115	0.47	0.16	90	0.1
4	0.235	0.045	0.025	0.695	90	0.1
5	0.565	0.23	0.175	0.03	90	0.1
6	0.105	0.21	0.59	0.095	90	0.1
7	0.375	0.405	0.15	0.07	90	0.1
8	0.375	0.095	0.07	0.46	90	0.1
9	0.145	0.435	0.25	0.17	90	0.1
10	0.245	0.085	0.08	0.59	90	0.1
11	0.565	0.23	0.175	0.03	70	1
12	0.565	0.23	0.175	0.03	140	1
13	0.245	0.085	0.08	0.59	60	1
14	0.245	0.085	0.08	0.59	120	0.01
15	0.135	0.06	0.14	0.665	120	0.01
16	0.105	0.21	0.59	0.095	140	0.01

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

Table 3. Results for the sets of random volatility distributions using different inversion approaches.

OA Parameter Set	TD measurements			Dilution measurements			TD and Dilution measurements		
	Average absolute error for VBS bins	Relative error (%) for ΔH_{vap}	Error for a_m (orders of magnitude)	Average absolute error for VBS bins	Error for a_m (orders of magnitude)	Average absolute error for VBS bins	Relative error (%) for ΔH_{vap}	Error for a_m (orders of magnitude)	
1	0.05	6	0.43	0.13	0.39	0.02	11	0	
2	0.13	3	0.06	0.11	0.17	0.02	2	0.16	
3	0.1	8	0.1	0.51	0.19	0.07	2	0.02	
4	0.08	10	0.45	0.19	0.36	0.02	4	0.1	
5	0.14	4	0.28	0.12	0.44	0.14	0.7	0.46	
6	0.1	10	0.02	0.15	0.02	0.07	10	0.04	
7	0.14	7	0.13	0.06	0.19	0.07	2	0.05	
8	0.07	4	0.17	0.18	0.34	0.04	0.9	0.06	
9	0.09	3	0.04	0.07	0.21	0.09	0.1	0.34	
10	0.06	11	0.45	0.16	0.46	0.06	11	0.37	
11	0.14	14	1.17	0.12	1.06	0.1	14	0.77	
12	0.11	14	0.95	0.12	1.06	0.06	23	0.96	
13	0.06	2	0.3	0.07	0.17	0.08	0.04	0.24	
14	0.18	25	1.22	0.2	0.75	0.33	17	1	
15	0.22	14	1.12	0.21	0.83	0.3	8	1.22	
16	0.11	11	0.63	0.18	0.50	0.17	4	0.32	

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

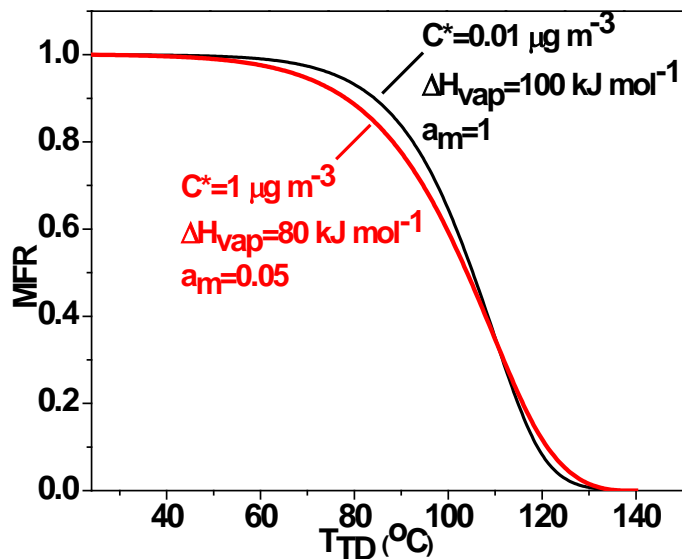


Fig. 1. Predicted thermograms (MFR vs. T_{TD}) for OA with different properties. A single component aerosol ($C^* = 1 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 80 \text{ kJ mol}^{-1}$ and $a_m = 0.05$) gives practically the same thermogram as one with a much lower volatility ($C^* = 0.01 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 100 \text{ kJ mol}^{-1}$ and $a_m = 1$).

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

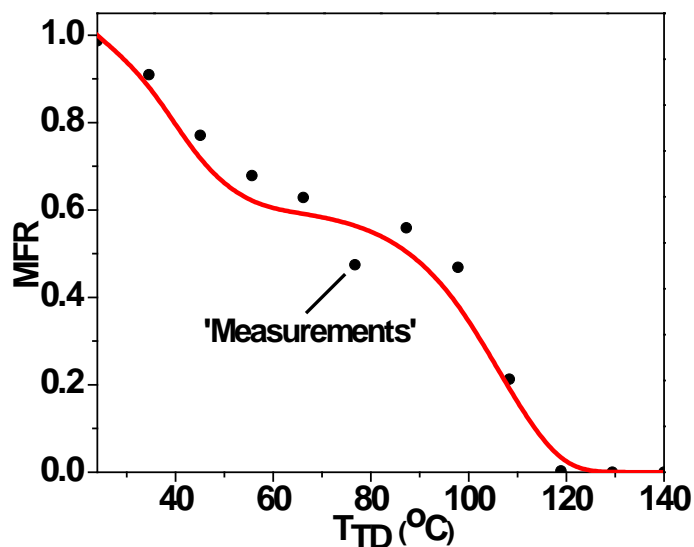


Fig. 2. Typical example of “construction” of TD pseudo-data. The red line is the thermogram corresponding to the true properties of the aerosol and the black dots correspond to the “measured” MFR vs. T_{TD} for an aerosol consisting of two components: very low volatility material (60 % $C^* = 0.01 \mu\text{g m}^{-3}$) and relatively high volatility material (40 % $C^* = 10 \mu\text{g m}^{-3}$), vaporization enthalpy and mass accommodation coefficient equal to 100kJ mol^{-1} and 1 correspondingly. Twelve “measurements” were constructed for equally spaced temperatures between 24 and 140°C by corrupting the correct values with random experimental error.

[Title Page](#)[Abstract](#)[Introduction](#)[Conclusions](#)[References](#)[Tables](#)[Figures](#)[◀](#)[▶](#)[◀](#)[▶](#)[Back](#)[Close](#)[Full Screen / Esc](#)[Printer-friendly Version](#)[Interactive Discussion](#)

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

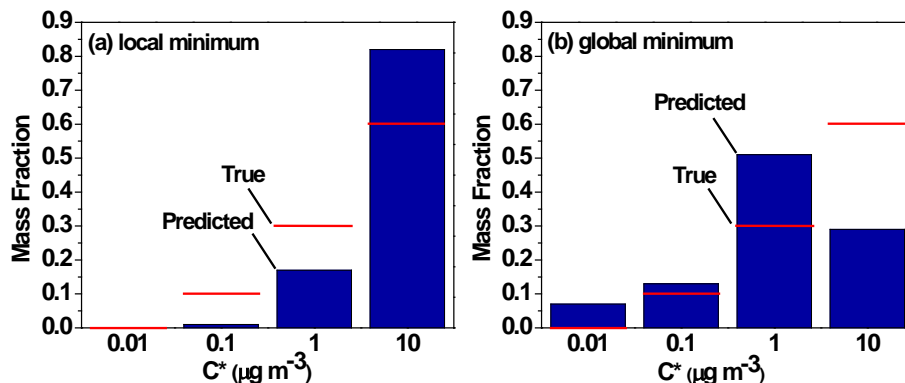


Fig. 3. Estimated (bars) and true (red lines) volatility distribution for OA consisting of 10 % $C^* = 0.1 \mu\text{g m}^{-3}$, 30 % $1 \mu\text{g m}^{-3}$, 60 % $10 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 50 \text{ kJ mol}^{-1}$ and $a_m = 1$, based on TD pseudo-data. **(a)** Solution corresponding to a local minimum of the objective function. The estimated vaporization enthalpy and accommodation coefficient are $\Delta H_{\text{vap}} = 38 \text{ kJ mol}^{-1}$ and $a_m = 0.9$. **(b)** Solution for the global minimum. The estimated ΔH_{vap} and a_m are 68 kJ mol^{-1} and 0.84 respectively.

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

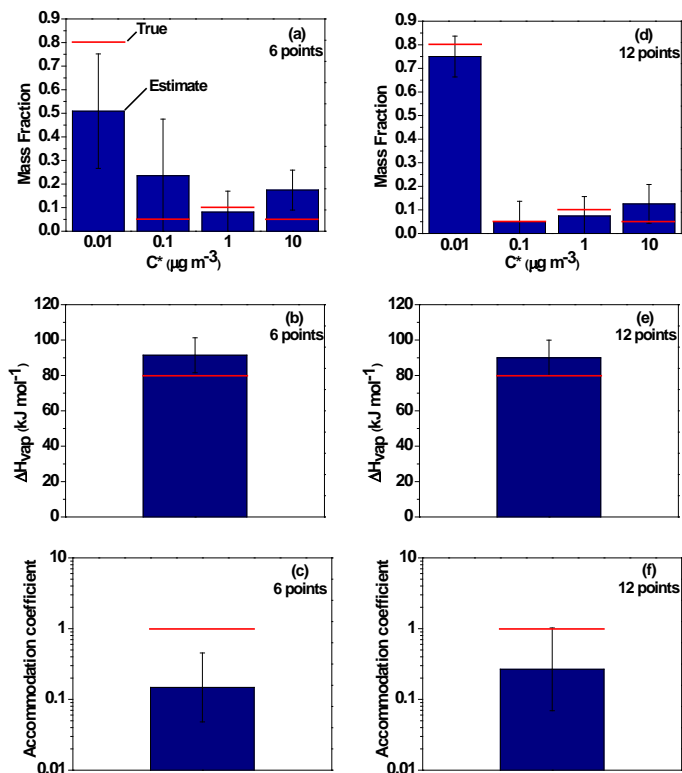


Fig. 4. Estimated (bars) and true (red lines) parameter values for an OA with 80 % $0.01 \mu\text{g m}^{-3}$, 5 % $0.1 \mu\text{g m}^{-3}$, 10 % $1 \mu\text{g m}^{-3}$, 5 % $10 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 80 \text{ kJ mol}^{-1}$ and $a_m = 1$ using 6 measurements for: **(a)** volatility distribution, **(b)** ΔH_{vap} , **(c)** a_m , and using 12 measurements for: **(d)** volatility distribution, **(e)** ΔH_{vap} and **(f)** a_m . The error bars represent the uncertainty of the estimated value.

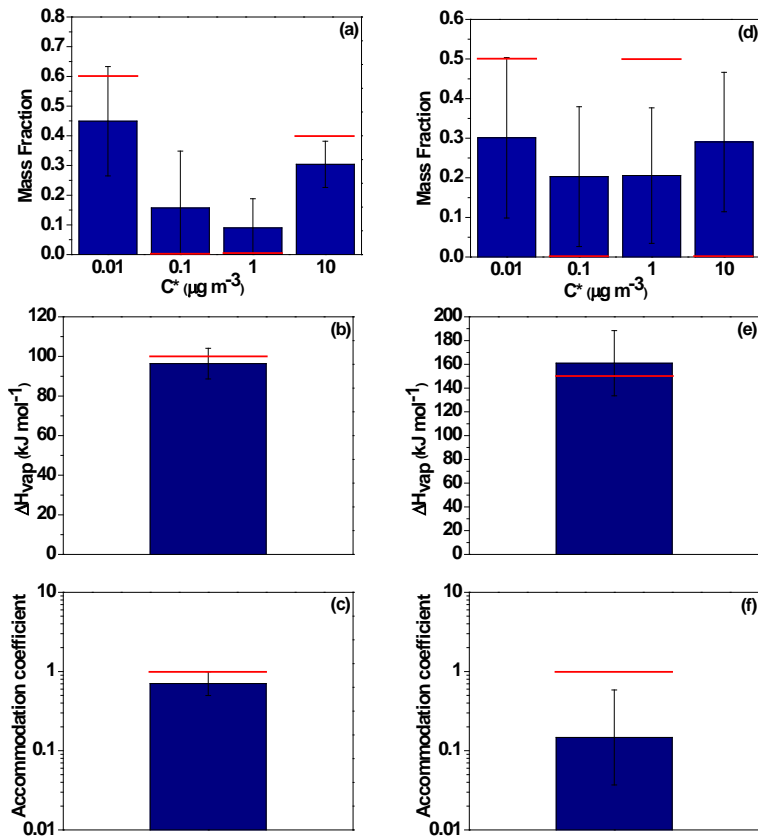


Fig. 5. Estimated (bars) and true property values (red lines) using 12 TD measurements, for two types of OA. **(a)** Volatility distribution, **(b)** ΔH_{vap} , **(c)** a_m for OA with 60% $0.01 \mu\text{g m}^{-3}$ and 40% $10 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 100 \text{ kJ mol}^{-1}$ and $a_m = 1$ and **(d)** volatility distribution, **(e)** ΔH_{vap} , **(f)** a_m for OA with 50% $0.01 \mu\text{g m}^{-3}$ and 50% $1 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 150 \text{ kJ mol}^{-1}$ and $a_m = 1$. The error bars represent the uncertainty of the estimated value.

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

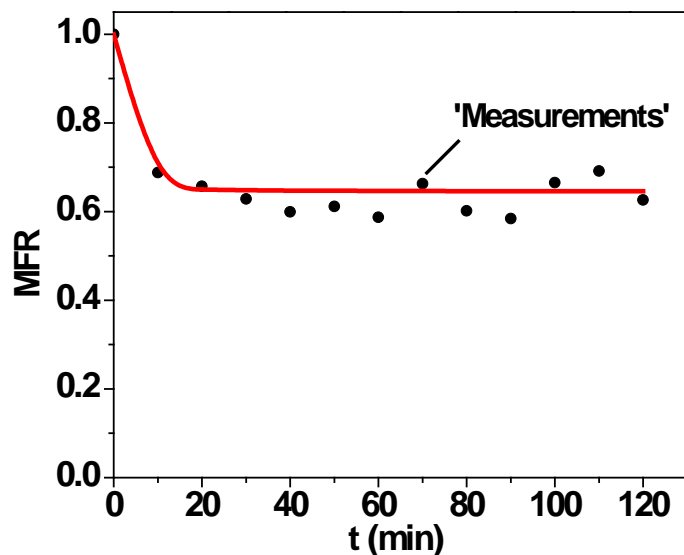


Fig. 6. Isothermal dilution measurements (MFR as function of time) for an aerosol with 60 % $0.01 \mu\text{g m}^{-3}$, 40 % $10 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 100 \text{ kJ mol}^{-1}$ and $a_m = 1$. The red line corresponds to the true properties of the aerosol and the black dots are the “measured” MFR values.

[Title Page](#)[Abstract](#)[Introduction](#)[Conclusions](#)[References](#)[Tables](#)[Figures](#)[◀](#)[▶](#)[◀](#)[▶](#)[Back](#)[Close](#)[Full Screen / Esc](#)[Printer-friendly Version](#)[Interactive Discussion](#)

Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

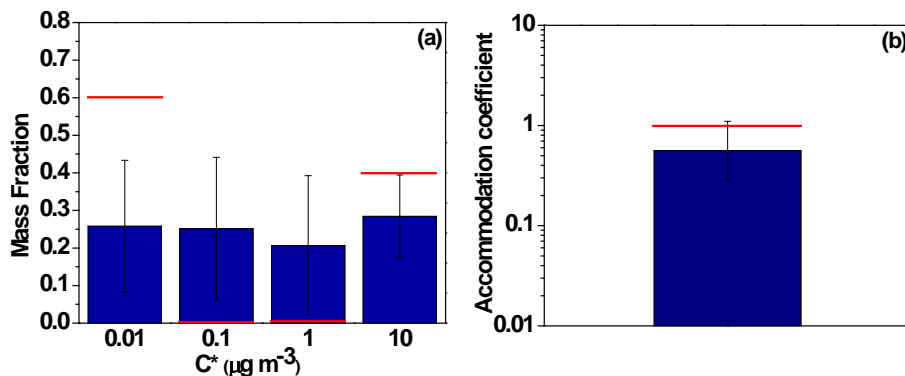


Fig. 7. Estimated (bars) volatility distribution and accommodation coefficient and true (red lines) values using isothermal dilution “measurements”, for an OA with 60 % $0.01 \mu\text{g m}^{-3}$ and 40 % $10 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 100 \text{ kJ mol}^{-1}$ and $a_m = 1$. **(a)** Volatility distribution and **(b)** a_m .

[Title Page](#)
[Abstract](#)
[Introduction](#)
[Conclusions](#)
[References](#)
[Tables](#)
[Figures](#)
[◀](#)
[▶](#)
[◀](#)
[▶](#)
[Back](#)
[Close](#)
[Full Screen / Esc](#)
[Printer-friendly Version](#)
[Interactive Discussion](#)


Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

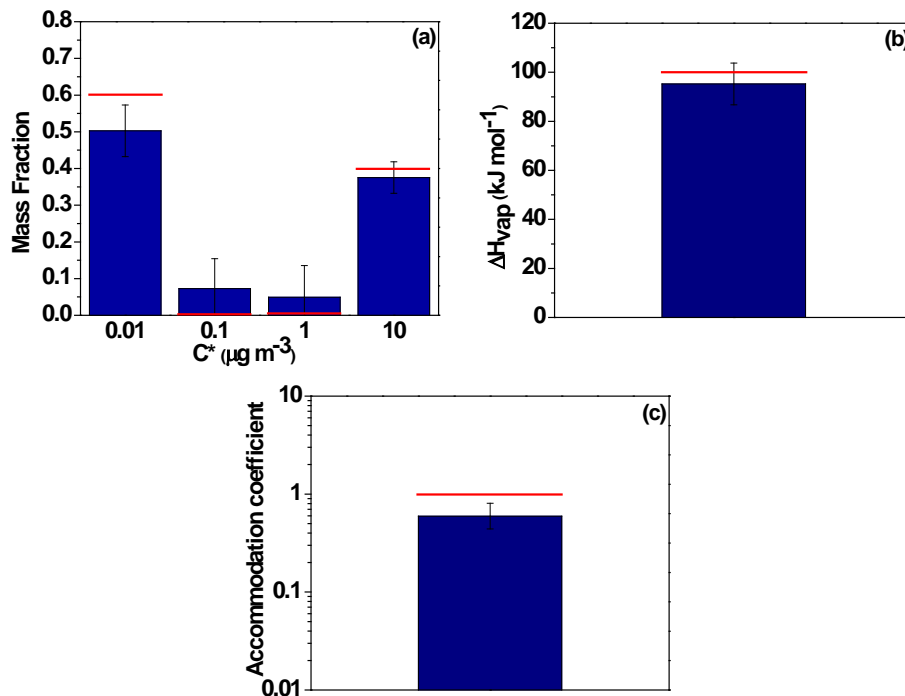


Fig. 8. Estimated (bars) and true (red lines) parameter values combining TD and isothermal dilution measurements, for an OA with 60 % 0.01 μg m⁻³ and 40 % 10 μg m⁻³, ΔH_{vap} = 100 kJ mol⁻¹ and a_m = 1 for: **(a)** volatility distribution, **(b)** ΔH_{vap}, **(c)** a_m.

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion



Measuring the atmospheric organic aerosol volatility

E. Karnezi et al.

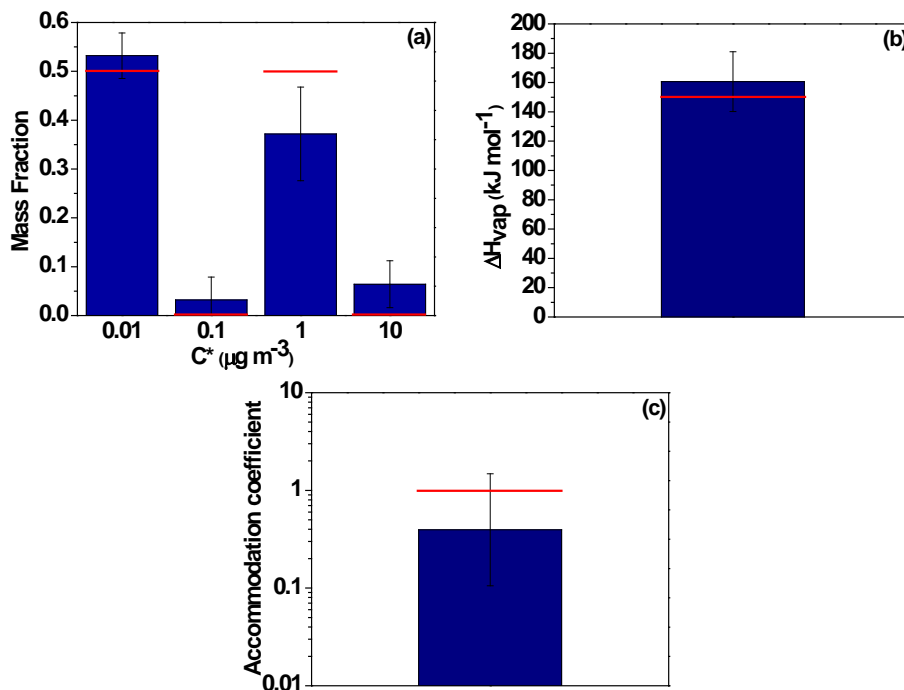


Fig. 9. Estimated (bars) and true (red lines) parameter values combining TD and isothermal dilution measurements, for an OA with 50% $0.01 \mu\text{g m}^{-3}$ and 50% $1 \mu\text{g m}^{-3}$, $\Delta H_{\text{vap}} = 150 \text{ kJ mol}^{-1}$ and $a_m = 1$ for: **(a)** volatility distribution, **(b)** ΔH_{vap} , **(c)** a_m .

Title Page

Abstract

Introduction

Conclusions

References

Tables

Figures

◀

▶

◀

▶

Back

Close

Full Screen / Esc

Printer-friendly Version

Interactive Discussion

