



**A Steady State Continuous Flow Chamber
for the Study of Daytime and Nighttime Chemistry
under Atmospherically Relevant NO levels**

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1 Abstract

2 Experiments performed in laboratory chambers have contributed significantly to the
3 understanding of the fundamental kinetics and mechanisms of the chemical reactions occurring
4 in the atmosphere. Two chemical regimes, classified as ‘high-NO’ versus ‘zero-NO’ conditions,
5 have been extensively studied in previous chamber experiments. Results derived from these two
6 chemical scenarios are widely parameterized in chemical transport models to represent key
7 atmospheric processes in urban and pristine environments. As the anthropogenic NO_x emissions
8 in the United States have decreased remarkably in the past few decades, the classic ‘high-NO’
9 and ‘zero-NO’ conditions are no longer applicable to many regions that are constantly impacted
10 by both polluted and background air masses. We present here the development and
11 characterization of the NCAR Atmospheric Simulation Chamber, which is operated in steady
12 state continuous flow mode for the study of atmospheric chemistry under ‘intermediate NO’
13 conditions. This particular chemical regime is characterized by constant sub-ppb levels of NO
14 and can be created in the chamber by precise control of the inflow NO concentration and the
15 ratio of chamber mixing to residence timescales. Over the range of conditions achievable in the
16 chamber, the lifetime of peroxy radicals (RO₂), a key intermediate from the atmospheric
17 degradation of volatile organic compounds (VOCs), can be extended to several minutes, and a
18 diverse array of reaction pathways, including unimolecular pathways and bimolecular reactions
19 with NO and HO₂, can thus be explored. Characterization experiments under photolytic and dark
20 conditions were performed and, in conjunction with model predictions, provide a basis for
21 interpretation of prevailing atmospheric processes in environments with intertwined biogenic and
22 anthropogenic activities. We demonstrate the proof of concept of the steady state continuous
23 flow chamber operation through measurements of major first-generation products, methacrolein
24 (MACR) and methyl vinyl ketone (MVK), from OH- and NO₃-initiated oxidation of isoprene.



25 1. Introduction

26 With the discovery of the role of biogenic volatile organic compounds (BVOCs) in urban
27 photochemical smog (Chameides et al., 1988), the interactions of biogenic emissions with man-
28 made pollution and their subsequent impact on the atmosphere's oxidative capacity and aerosol
29 burden have received extensive studies in the ensuing decades (De Gouw et al., 2005; Ng et al.,
30 2007; Goldstein et al., 2009; Surratt et al., 2010; Rollins et al., 2012; Shilling et al., 2013; Xu et
31 al., 2015). A particular research focus has been understanding the influence of nitrogen oxides
32 ($\text{NO}_x = \text{NO} + \text{NO}_2$) on the atmospheric oxidation cascades of BVOCs, which ultimately generate
33 ozone (O_3) and secondary organic aerosols (SOA). Nitrogen oxides alter the distribution of
34 BVOC oxidation products by primarily modulating the fate of peroxy radicals (RO_2), a key
35 intermediate produced from the atmospheric degradation of VOCs by major oxidants including
36 OH, O_3 , and NO_3 . In the absence of NO_x , RO_2 reacts predominantly with HO_2 radicals yielding
37 organic peroxides and other products, and to a lesser extent, undergoes self/cross-reactions
38 yielding carbonyls, alcohols, and multifunctional species. In the presence of elevated NO_x , the
39 dominant fate of RO_2 is to react with NO leading to ozone production, and also to organic
40 nitrates. During the night, RO_2 also reacts with NO_3 which is produced by the reaction between
41 O_3 and NO_2 . In addition, reaction of peroxyacyl radicals (RC(O)O_2) with NO_2 produces
42 peroxyacyl nitrates that constitute a large reservoir of reactive nitrogen and a potentially
43 important SOA precursor (Singh and Hanst, 1981; Nguyen et al., 2015).

44 Much of our understanding of the extent to which NO_x mediates the oxidation chemistry of
45 BVOC in the atmosphere has been derived from measurements in laboratory chambers, where
46 two extreme experimental conditions, i.e., 'high NO ' vs. 'zero- NO ', were mostly performed to
47 examine the reaction pathways of RO_2 radicals (Kroll and Seinfeld, 2008; Orlando and Tyndall,
48 2012; Ziemann and Atkinson, 2012). Results from these two chemical regimes have been widely
49 incorporated into chemical transport models to represent key atmospheric processes in urban and
50 pristine environments, respectively (Kanakidou et al., 2005). In the actual atmosphere, however,
51 the fate of RO_2 radicals is rather more complicated than simply undergoing bimolecular reactions
52 with NO/HO_2 as observed under the two extreme chamber conditions. It has been recently
53 revealed that RO_2 radicals may undergo an internal H-shift followed by sequential O_2 addition,
54 leading to highly oxygenated multifunctional peroxides (Ehn et al., 2014; Jokinen et al., 2015;
55 Kurtén et al., 2015; Kirkby et al., 2016; Zhang et al., 2017). The rate of H-shift largely depends
56 on the thermochemistry of the nascent alkyl radicals and can be reasonably fast, on a time scale
57 of seconds to minutes (Crouse et al., 2013). Further, depending on the stability of the RO_2
58 precursor (alkyl radicals), RO_2 radicals may lose O_2 in competition with bimolecular reactions
59 with NO , NO_3 , RO_2 , and HO_2 . Recent theoretical and laboratory studies have found that the
60 hydroxy peroxy radical conformers produced from isoprene photooxidation decompose readily
61 to allylic radicals on time scales faster than bimolecular processes under atmospherically relevant
62 NO/HO_2 levels (tens to hundreds of parts per trillion by volume). This highly dynamic system
63 leads to formation of distinctly different products that depend on the concentrations of
64 bimolecular reaction partners from those observed in chamber experiments under 'high- NO ' and
65 'zero- NO ' conditions (Teng et al., 2017).

66 Anthropogenic NO_x emissions in the United States have decreased remarkably in the past
67 few decades (EPA, 2014), resulting in significant changes in the degradation mechanisms of
68 BVOCs, especially in regions impacted by both background and polluted air masses such as the
69 Southeastern United States. However, the ultimate fate of peroxy radicals in environments with



70 sub-ppb NO levels is still poorly constrained, in part due to a lack of consistent measurements
71 under well controlled conditions. Experimental environments with a controlled NO production at
72 sub-ppb levels have been recently introduced to examine the various RO₂ fates in the
73 atmosphere. For example, a ‘slow chemistry’ scenario initiated by photolyzing methyl nitrite
74 (CH₃ONO) under extremely low UV intensities as the OH radical source ($J_{\text{CH}_3\text{ONO}} \sim 10^{-5} \text{ s}^{-1}$) was
75 created to study the autoxidation chemistry of peroxy radicals produced from isoprene
76 photooxidation (Crouse et al., 2011; Crouse et al., 2012; Teng et al., 2017). The resulting NO
77 and HO₂ mixing ratios are maintained at ~ ppt (parts per trillion by volume) level (CH₃ONO +
78 O₂ + $h\nu \rightarrow$ HO₂ + NO + HCHO) over the course of several hours of reaction, and the average
79 OH concentration (OH ~ 10⁵ molec cm⁻³) is approximately one order magnitude lower than that
80 in the typical daytime ambient atmosphere. Another example relates to a recent method
81 development in the Potential Aerosol Mass (PAM) flow tube reactor where nitrous oxide (N₂O)
82 was used to produce ~ ppb (parts per billion by volume) level of NO (O₃ + $h\nu \rightarrow$ O₂ + O(¹D);
83 O(¹D) + N₂O → 2NO) (Lambe et al., 2017). Timescales for chemical reactions and gas-particle
84 partitioning are ultimately limited to the mean residence time (~80 s) of the PAM reactor.

85 An alternative experimental platform to the batch-mode chamber and flow tube reactor
86 described above is a well-mixed steady-state chamber with continuous feed of reactants and
87 continuous withdrawal of reactor contents (Shilling et al., 2008). An attribute of the continuous
88 flow steady state chamber is that, by control of the inlet reactant concentrations and the ratio of
89 mixing to residence timescales, it is possible to simulate atmospheric oxidation under stable
90 conditions over a wide range of time periods and chemical scenarios. In this study, we present
91 the development and characterization of the NCAR Atmospheric Simulation Chamber, which is
92 operated in steady state continuous flow mode for simulating atmospheric daytime and nighttime
93 chemistry over chemical regimes not accessible in static chamber experiments. We focus on
94 establishing an ‘intermediate NO’ regime characterized by a constant steady-state NO level
95 ranging from tens of ppt to a few ppb in the chamber. This particular chemical regime is well
96 suited for the study of atmospheric behavior of RO₂ radicals, as they can survive up to minutes
97 and embrace various reaction possibilities as opposed to reaction with NO, NO₃, HO₂, and RO₂
98 as their dominant fate observed in most batch-mode chamber experiments. We employ the
99 ‘intermediate NO’ regimes to reexamine the daytime and nocturnal chemistry of isoprene
100 through the measurements of two first-generation products, methacrolein (MACR) and methyl
101 vinyl ketone (MVK).

102 2. Experimental

103 2.1 NCAR Atmospheric Simulation Chamber Facilities

104 The NCAR Atmospheric Simulation Chamber consists of a 10 m³ FEP Teflon (0.005” thick)
105 bag that is housed in a cubic enclosure with UV reflective surfaces and a bank of 128 wall-
106 mounted blacklight tubes (32W, Type F32T8/BL). To characterize photolytic conditions in the
107 chamber, irradiance spectra were collected in the wavelength range of 180–600 nm at ~0.8 nm
108 resolution by a custom-built spectroradiometer (Petropavlovskikh et al., 2007). Photolysis
109 frequencies were calculated based on the measured downwelling spectral actinic fluxes. The
110 computed photolysis rate of NO₂ ($J_{\text{NO}_2} \sim 1.27 \times 10^{-3} \text{ s}^{-1}$) agrees within 3% with that measured by
111 photolyzing 18.6 ppb NO₂ in the chamber and monitoring the NO production rate. The chamber
112 is equipped with a standard set of measurements, including an integrated temperature and



113 humidity probe (Model 50U, VAISALA, CO) and a Magnehelic differential pressure indicating
114 transmitter (Model 605-11, Dwyer Instruments, IN). The chamber temperature is controlled at
115 295 K by the building's air conditioning system and increases to 305–306 K under maximum
116 irradiation conditions. The relative humidity of the chamber air is below 10% under dry
117 conditions and can be varied in the range of ~10–50% by flowing a portion of the purified dry
118 flushing air into the chamber through a temperature-controlled water reservoir. The chamber
119 internal pressure is maintained slightly above the ambient pressure to minimize the enclosure air
120 contamination via penetration through the Teflon film.

121 Prior to each experiment, the chamber was flushed with purified dry air from a zero air
122 generator (Model 737, Aadco Instruments, OH) for >12 h until ozone and NO_x levels were below
123 1 ppb. During the operation of the steady state continuous flow mode, the chamber was
124 constantly flushed with purified dry air at 40 L min⁻¹, which gives an average chamber residence
125 time of 4.17 hours. The incoming and outgoing flows were balanced by a feedback control
126 system that maintains a constant internal pressure of 1.2–4.9×10⁻⁴ atm above the ambient. The
127 characteristic mixing time in the chamber was determined to be ~9 min (~4% of the residence
128 time) by rapid injection of tracer compounds including CO₂ and NO. Under such conditions, the
129 gas/particle-phase composition in the outflow can be assumed identical to that in the well-mixed
130 core of the chamber.

131 To mimic daytime photochemistry in the continuous flow mode, steady-state OH mixing
132 ratio was created by photolyzing hydrogen peroxide (H₂O₂) vapor that was continuously flowing
133 into the chamber (H₂O₂+hν→2OH, J_{H₂O₂}~3.93×10⁻⁷ s⁻¹). Specifically, a 20 mL syringe
134 (NORM-JECT, Henke-Sass Wolf, MA) held on a syringe pump (Model 100, kdScientific, MA)
135 kept at ~4 °C was used to deliver H₂O₂ solution (1–30 wt%, Sigma Aldrich, MO) into a glass
136 bulb that was gently warmed at ~32 °C. The liquid delivery rate was sufficiently slow (100–300
137 μL min⁻¹) that all the H₂O₂ vapor was released into the glass bulb through evaporation of a small
138 droplet hanging on the needle tip. An air stream (5 L/min) swept the H₂O₂ vapor into the
139 chamber, resulting in an H₂O₂ mixing ratio in the range of 600 ppb to 16.22 ppm in the injection
140 flow as a function of the concentration of H₂O₂ aqueous solution used. A spreadsheet (Table S2)
141 for calculating the inflow H₂O₂ mixing ratio using the above input method is provided in the
142 Supplement. As H₂O₂-laden air was continuously entering the chamber, it took approximately
143 three turnover times (~12.5 hr) for the desired H₂O₂ vapor mixing ratio to reach steady state in
144 the chamber. The H₂O₂ vapor concentration in the chamber, though not measured, can be
145 estimated from the steady-state OH mixing ratio derived from the observed exponential decay of
146 a given parent hydrocarbon. Constant NO injection flow was achieved by diluting the gas flow
147 from a concentrated NO cylinder (NO = 133.16 ppm, balance N₂) to a desired mixing ratio
148 (0.1–100 ppb) using a set of mass flow controllers (Tylan FC260 and FC262, Mykrolis Corp.,
149 MA). Note that for experiments performed in the absence of any VOC precursor, H₂O₂ and NO
150 were the only two species that were continuously input into the chamber for the establishment of
151 a combination of different photochemical conditions as denoted by the O₃ and NO_x
152 measurements. For the isoprene photooxidation experiments, an isoprene standard (C₅H₈ = 531
153 ppm, balance N₂) was constantly injected into the chamber and diluted with the flushing air to
154 achieve an inflow concentration of ~20 ppb.

155 To mimic the nighttime chemistry in the continuous flow mode, steady-state NO₃ mixing
156 ratio was created by constantly flowing diluted O₃ and NO air into the chamber (NO+O₃



157 $\rightarrow\text{NO}_2+\text{O}_2$; $\text{NO}_2+\text{O}_3\rightarrow\text{NO}_3+\text{O}_2$). The NO source can be replaced by NO_2 , although the absolute
158 absence of NO does not necessarily represent the actual atmospheric conditions. O_3 was
159 produced by photolyzing O_2 in air at 185 nm using a mercury “Pen-Ray” lamp (UVP LLC, CA).
160 Ozone concentration in the injection flow can be controlled from 3.5 ppb to 457 ppb
161 automatically by adjusting the mercury lamp duty cycle. To study the RO_2+HO_2 pathway,
162 formaldehyde (CH_2O) was input into the chamber along with NO and O_3 to initiate HO_2
163 production ($\text{NO}_3+\text{CH}_2\text{O}+\text{O}_2\rightarrow\text{HNO}_3+\text{HO}_2+\text{CO}$). Formaldehyde aqueous solution (37 wt%,
164 Sigma Aldrich, MO) was diluted with ultrapure water (Milli-Q, Merck Millipore, MA) to 0.2–1.0
165 wt% and continuously input into the chamber using the same method used for H_2O_2 input
166 described above. It is worth noting that the formaldehyde aqueous solution contains 10–15%
167 methanol as stabilizer to prevent polymerization. The presence of methanol in the chamber does
168 not significantly impact the nocturnal chemistry as it consumes OH and NO_3 radicals to generate
169 formaldehyde and additional HO_2 ($\text{CH}_3\text{OH}+\text{NO}_3\rightarrow\text{HNO}_3+\text{CH}_2\text{O}+\text{HO}_2$,
170 $\text{CH}_3\text{OH}+\text{OH}\rightarrow\text{H}_2\text{O}+\text{CH}_2\text{O}+\text{HO}_2$) (Atkinson et al., 2006). The use of formaldehyde as an HO_2
171 source mimics closely the atmospheric nighttime conditions in forest environments (Schwantes
172 et al., 2015). To study the NO_3 -initiated oxidation of isoprene, an injection flow of diluted
173 isoprene (~ 10 ppb) was achieved using the procedure described above.

174 2.2 Analytical measurements

175 A suite of instruments was used to monitor gas-phase concentrations in the chamber
176 outflow. O_3 was monitored by absorption spectroscopy with 0.5 ppb detection limit (Model 49,
177 Thermo Scientific, CO). The O_3 monitor was calibrated using an Ozone Primary Standard in the
178 range of 0 to 200 ppb (Model 49i-PS, Thermo Scientific, CO). The O_3 monitor used for chamber
179 experiments was periodically checked with the primary standard and was shown to be stable over
180 long periods of time (less than 1 ppb drift in over 1 year). NO was monitored by
181 chemiluminescence with 0.5 ppb detection limit (Model CLD 88Y, Eco Physics, MI). Zero-point
182 and span calibrations of the NO_x monitor were performed prior to each experiment by supplying
183 the instrument with pure N_2 gas and diluted NO, respectively. Multi-point calibration was
184 performed on a weekly basis and has shown a good stability and linearity in the NO
185 measurement ranging from 1 ppb to 200 ppb. NO_x ($\text{NO}+\text{NO}_2$) measurements were performed
186 using a photolytic converter that selectively converts NO_2 to NO upstream of the photo-
187 multiplier tube in the CLD 88Y NO monitor. This converter uses two opposing arrays of UV
188 LEDs shining into a cylindrical quartz mixing tube to achieve approximately 50% conversion of
189 NO_2 to NO per second. The total efficiency for the equipment described here is approximately
190 70% as determined by measuring calibrated NO_2 standards. The sample path always includes
191 the photolytic converter, and typical experiments cycle the power for the LED lights to switch
192 between measuring NO (lights off) and NO_x (lights on). NO_2 concentrations were then
193 determined by subtracting the NO from the adjacent NO_x measurements.

194 A customized Proton Transfer Reaction Quadrupole Mass Spectrometer (PTR-Q-MS) was
195 used to measure volatile organic compounds including isoprene (C_5H_8), methacrolein (MACR,
196 $\text{C}_4\text{H}_6\text{O}$), and methyl vinyl ketone (MVK, $\text{C}_4\text{H}_6\text{O}$). The instrument was operated at 2.3 mbar drift
197 pressure and 560 V drift voltage. Measurements reported here were obtained at a sampling rate
198 of 10 Hz. In positive-mode operation, a given analyte [M] undergoes proton transfer reaction,
199 producing an ion of the form $[\text{M}+\text{H}]^+$. The instrument background was collected by sampling the
200 chamber air for at least 30 min prior to each experiment. Measured ion intensities for isoprene
201 (C_5H_9^+ , m/z 69) and MACR and MVK ($\text{C}_4\text{H}_7\text{O}^+$, m/z 71) were calculated as the signal of each ion



202 (counts per seconds) normalized to the total ion signal of H_3O^+ . The instrument sensitivities
203 towards isoprene, MACR and MVK were calibrated with a mixture of diluted gas standards. The
204 instrument sensitivity towards MACR is identical to that of MVK, and as a result, the measured
205 $\text{C}_4\text{H}_7\text{O}^+$ signal represents the sum of MACR and MVK in the sampling air. Since artifacts in the
206 measured $\text{C}_4\text{H}_7\text{O}^+$ signal can be produced through thermal decomposition of isoprene oxidation
207 products, such as the peroxides, nitrates, and epoxides, on contact with hot metal surface (Liu et
208 al., 2013; Nguyen et al., 2014; Rivera-Rios et al., 2014), a cold-trap system was used to avoid
209 bias in the interpretation of the PTR-MS data. Specifically, a 1 m section of Teflon tubing was
210 submerged in a low temperature ethanol bath (-40 ± 2 °C) that could trap oxidized products less
211 volatile than the authentic MACR and MVK standards after steady state was established in the
212 chamber. The quantification of the sum of MACR and MVK was then based on the PTR-MS
213 measured $\text{C}_4\text{H}_7\text{O}^+$ (m/z 71) signal downstream of the cold-trap.

214 3. Kinetic Modeling

215 Reaction kinetics and mechanisms for the gas-phase photochemistry were extracted from the
216 Master Chemical Mechanism (MCMv3.3.1, accessible at <http://mcm.leeds.ac.uk/MCM/>). The
217 inorganic reaction scheme includes 21 species and 48 reactions; and the isoprene oxidation
218 system includes 611 species and 1974 reactions. The kinetic schemes were implemented in
219 Matlab (Mathworks) to simulate the temporal profile of a given compound i in the chamber
220 operated in the steady state continuous flow mode:

$$221 \quad \frac{dC_i}{dt} \cdot \tau = C_{i,0} + P_i - C_i - \sum k_i \cdot \tau \cdot C_i \quad (\text{Eq1})$$

222 where C_i (molec cm^{-3}) is the gas-phase concentration of compound i in the well-mixed core of
223 the chamber; $C_{i,0}$ (molec cm^{-3}) is the initial gas-phase concentration of compound i in the
224 injection flow; k_i (s^{-1}) is the pseudo-1st-order rate coefficient for a chemical reaction that
225 consumes compound i ; τ (s) is the chamber mean residence time and can be calculated as the
226 total chamber volume divided by the incoming/outgoing flow rate; and P_i (molec cm^{-3}) is the
227 increment in the concentration of compound i through chemical production during one residence
228 time. Note that two terms are neglected in Equation (1), i.e., organic vapor condensation onto
229 particles and deposition on the chamber wall. This is a reasonable simplification here owing to
230 the relatively high volatility ($\geq 10^{-1}$ atm) of compounds studied. Incorporation of these two terms
231 into Equation (1) is feasible given the vapor pressure of compound i , suspended particle size
232 distribution, gas-particle and gas-wall partitioning coefficient, accommodation coefficients of
233 compound i on particles and walls, and the effective absorbing organic masses on the wall
234 (Zhang et al., 2014a; Zhang et al., 2015b; Huang et al., 2016; McVay et al., 2016; Nah et al.,
235 2016).

236 Model simulations used for comparison with chamber measurements were initialized using
237 experimental conditions summarized in Table S1 in the Supplement. Model input parameters for
238 all simulations include temperature (295 at dark and 306 K under irradiation), local pressure
239 (8.6×10^4 Pa), relative humidity (8% at dark and 5% under irradiation), light intensity
240 ($J_{\text{NO}_2} = 1.27 \times 10^{-3} \text{ s}^{-1}$ under irradiation and 0 at dark), chamber mean residence time (4.17 h), and
241 input mixing ratios of H_2O_2 (0.11–16.2 ppm for photolytic experiments), NO (0.1–100 ppb for
242 photolytic experiments and 10–20 ppb for dark experiments), O_3 (22–225 ppb for dark
243 experiments), HCHO (0–600 ppb for dark experiments), and isoprene (19.9 ppb for photolytic



244 experiments and 10.2 ppb for dark experiments). The model was propagated numerically for 25 h
245 duration for each experiment.

246 4. Results and Discussions

247 4.1 Optimal operating conditions for daytime photochemistry

248 Figure 1 shows the model predicted steady-state mixing ratios of OH, HO₂, NO₃, NO, NO₂,
249 and O₃ in the chamber after 20 hours of photochemical reactions as a function of the H₂O₂ and
250 NO concentrations in the continuous injection flow. Six blank chamber experiments were
251 compared with simulations. In general, the model captures the evolution patterns of NO_x and O₃
252 well. The predicted mixing ratios of NO, NO₂, and O₃ agree within 69%, 11%, and 33%,
253 respectively, with the measurements (see Table S1 and Figure S1 in the Supplement). The
254 relatively large NO uncertainties originate from the measurements that were performed close to
255 the instrument detection limit (0.5 ppb).

256 Simulated steady-state mixing ratios of OH radicals ([OH]_{ss}) range from $\sim 5 \times 10^5$ to $\sim 4 \times 10^6$
257 molec cm⁻³, which over ~ 4 hours chamber residence time would be roughly equivalent to ~ 1 h to
258 ~ 8 h of atmospheric OH exposure (1×10^6 molec cm⁻³). As expected, [OH]_{ss} increases with
259 increasing NO influxes due to the enhanced NO_x/O₃ cycling but decreases with increasing H₂O₂
260 influxes owing to the overwhelming reaction OH+H₂O₂→H₂O+HO₂. As a consequence, the
261 steady-state mixing ratios of HO₂ radicals ([HO₂]_{ss}) reach up to $\sim 7 \times 10^9$ molec cm⁻³ when 16.2
262 ppm H₂O₂ is continuously injected into the chamber. If 110 ppb H₂O₂ is used instead, the
263 resulting [HO₂]_{ss} levels fall close to the ambient range ($\sim 10^8$ molec cm⁻³).

264 Simulated steady-state NO mixing ratios in the chamber range from ~ 2 ppt to ~ 0.9 ppb from
265 combinations of 0.1–20 ppb NO and 0.11–16.22 ppm H₂O₂ in the injection flow. The ratio of
266 inflow NO concentration to the steady-state NO concentration in the chamber ranges from 5 to
267 93, demonstrating the importance of chemical removal in controlling the overall steady-state NO
268 levels. O₃ accumulation is an inevitable consequence under photolytic conditions and, for
269 example, the presence of 10 ppb O₃ leads to the chemical removal term ($k_{O_3+NO} \cdot [O_3] \cdot \tau$) in
270 Equation (1) that reduces the steady-state NO concentration by a factor of 60. It is worth noting
271 that under all simulated conditions in the continuous flow mode, O₃ (~ 1 –126 ppb) coexists with
272 NO (~ 0.002 –0.9 ppb). This particular chemical scenario, which is impossible to achieve in
273 batch-mode reactors due to prompt conversion of NO to NO₂, could then be used to mimic
274 ambient ozonolysis chemistry, for example, in forest regions that frequently encounter polluted
275 air masses from nearby urban areas. The steady-state mixing ratios of NO₂ ([NO₂]_{ss}) exhibit a
276 strong linear correlation with NO influxes. The use of less than 20 ppb NO in the injection flow
277 results in a few to tens of ppb [NO₂]_{ss} that is higher than the range typically found in the ambient.
278 The potential ‘quenching’ effect of NO₂ on RO₂ radicals through reversible termolecular
279 reactions is discussed shortly.

280 In the so-called ‘high-NO_x’ chamber experiments, the NO₃ radical is an unavoidable side-
281 product when black lights are used as a representative of the solar radiation in mimicking the
282 daytime photochemistry in the troposphere. The photolysis of NO₃, although its primary sink in
283 the atmosphere, proceeds rather slowly ($J_{NO_3} \sim 1.8 \times 10^{-3} \text{ s}^{-1}$) under the present chamber
284 photolytic conditions, thereby leading to a significant accumulation of NO₃ radicals
285 (7.9×10^4 – 2.8×10^8 molec cm⁻³) at steady state. The simulated NO₃/OH ratio dictates the extent to



286 which the NO_3 (nighttime) chemistry competes with the OH-initiated (daytime) photochemistry.
287 For compounds that are highly reactive towards NO_3 such as isoprene, NO_3 -initiated oxidation
288 accounts for up to ~60% of the overall isoprene degradation pathways at the highest NO_3/OH
289 ratio (~255) simulated. Low concentrations of NO (< 20 ppb) and H_2O_2 (< 2 ppm) in the
290 injection flow are therefore necessary to limit the interferences of NO_3 -initiated chemistry.
291 Again, taking isoprene as an example, the NO_3 oxidation pathway contributes less than 0.1% of
292 the overall isoprene degradation kinetics at the lowest NO_3/OH ratio (~0.13) simulated here.

293 Also given in Figure 1 is the calculated lifetime (τ_{RO_2}) of an RO_2 radical with respect to
294 reactions with NO and HO_2 at 306 K. In most batch-mode chamber experiments, τ_{RO_2} of only
295 several seconds or less can be achieved, due to the presence of tens to hundreds of ppb levels of
296 NO and HO_2 . Here τ_{RO_2} could extend to 60 s or even longer with the continuous input of low
297 mixing ratios of H_2O_2 (≤ 110 ppb) and NO (≤ 0.2 ppb). Note that the presence of tens of ppb
298 NO_2 in the chamber might impose a ‘quenching’ effect on the steady state RO_2 level through
299 rapid reversible reactions ($\text{RO}_2 + \text{NO}_2 + \text{M} \leftrightarrow \text{RO}_2\text{NO}_2 + \text{M}$). We evaluate this potential ‘quenching
300 effect’ using ethylperoxy radical ($\text{C}_2\text{H}_5\text{O}_2$) generated from OH-oxidation of ethane as an
301 example. Simulations shown in Figure S2 in the Supplement reveal that incorporation of the
302 $\text{C}_2\text{H}_5\text{O}_2 + \text{NO}_2 + \text{M} \leftrightarrow \text{C}_2\text{H}_5\text{O}_2\text{NO}_2 + \text{M}$ reaction into the mechanism in the presence of ~1–80 ppb
303 NO_2 does not notably change the behavior of $\text{C}_2\text{H}_5\text{O}_2$ radical. One exception is the peroxyacyl
304 radical, which combines with NO_2 yielding peroxyacyl nitrate. For example, under 0.1–16 ppb
305 $[\text{NO}_2]_{\text{ss}}$ as displayed in Figure 1, we calculate that the time needed for peroxyacetyl radical
306 ($\text{CH}_3\text{C}(\text{O})\text{O}_2$) to reach equilibrium with peroxyacetyl nitrate
307 ($\text{CH}_3\text{C}(\text{O})\text{O}_2 + \text{NO}_2 + \text{M} \leftrightarrow \text{CH}_3\text{C}(\text{O})\text{O}_2\text{NO}_2 + \text{M}$) ranges from ~1 to ~10 s, suggesting that the
308 lifetime of peroxyacyl radicals is ultimately controlled by NO_2 instead of NO/ HO_2 in the reaction
309 system, and consequently, peroxyacyl radicals are not expected to be long-lived in the current
310 chamber configuration.

311 4.2 Application to OH-initiated oxidation of isoprene

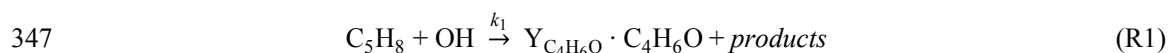
312 Methacrolein (MACR) and methyl vinyl ketone (MVK) are major first-generation products
313 from the OH-initiated oxidation of isoprene in the presence of NO (Wennberg et al., 2017). They
314 are produced from the decomposition of β -ISOPO alkoxy radicals that are primarily formed from
315 the reaction of β -ISOPOO peroxy radicals (β -1-OH-2-OO and β -4-OH-3-OO) with NO, see
316 mechanisms displayed in Figure 2 (A). Reactions of β -ISOPOO peroxy radicals with HO_2 and
317 RO_2 also partially yield β -ISOPO alkoxy radicals that ultimately lead to MACR and MVK,
318 although these pathways are considered to be minor in the presence of hundreds to thousands of
319 ppt NO in the atmosphere. The molar yields determined from previous studies range from
320 30–35% for MVK and 20–25% for MACR under high NO conditions ($\text{NO} > 60$ ppb) (Tuazon
321 and Atkinson, 1990; Paulson and Seinfeld, 1992; Miyoshi et al., 1994; Ruppert and Becker,
322 2000; Galloway et al., 2011). It has been recently shown that the six hydroxyl peroxy radicals
323 (ISOPOO) produced from the initial OH addition to the double bonds of isoprene undergo rapid
324 interconversion by removal/addition of O_2 that competes with bimolecular reactions under
325 atmospherically relevant NO levels (Peeters et al., 2014; Teng et al., 2017). As a result, the
326 distribution of ISOPOO radical isomers and their subsequent reaction products varies with their
327 lifetimes with respect to bimolecular reactions. In the presence of hundreds of ppb NO as done
328 by most previous experimental studies, the reaction of ISOPOO radicals with NO dominates over
329 their interconversion, and the production of β -ISOPOO peroxy radical is less favored, leading



330 the experiments to underestimate the MACR and MVK yields typically obtained in ambient
 331 conditions. Measurements by Liu et al. (2013) conducted at NO concentrations comparable to
 332 the urban environment (~1 ppb) found much higher MACR (~31.8%) and MVK (~44.5%) yields
 333 than other previous studies.

334 Here we perform a steady-state continuous-mode experiment to measure the production of
 335 MACR and MVK from the OH-initiated oxidation of isoprene in the presence of ~0.45 ppb NO.
 336 Figure 3 shows the observed and simulated temporal profiles of NO_x, O₃, C₅H₈, and C₄H₆O over
 337 24 hours photooxidation of isoprene. In this experiment, C₅H₈, H₂O₂, and NO were continuously
 338 fed into the chamber, with constant inflow concentrations of 19.9 ppb, 600 ppb, and 19 ppb,
 339 respectively. An outgoing flow at 40 L min⁻¹ continuously withdrew air from the chamber to
 340 balance the pressure. After approaching steady state, the sampling tube was submerged into an
 341 ethanol low temperature bath (-40±2 °C) to trap oxidized products that would otherwise undergo
 342 thermal decomposition introducing interferences in the C₄H₇O⁺ (*m/z* 71) signal. The measured
 343 concentrations of C₅H₈ and C₄H₆O upon cold-trapping agree within 2.8% and 4.6% uncertainties
 344 with the model simulations, see Fig.3 (C) and (D).

345 To calculate the total molar yield (*Y*_{C₄H₆O}) of MACR and MVK, two reactions are
 346 considered:



349 where *k*₁ is the rate constant for OH reaction with isoprene, and *k*₂ is taken as the average of rate
 350 constants for OH reactions with MACR and MVK. Uncertainties associated with the
 351 simplification of *k*₂ in calculating the MACR and MVK yields will be discussed shortly. Also
 352 note that the ozonolysis and NO₃-initiated oxidation in total account for less than 6% of isoprene
 353 degradation pathway under current experimental conditions and are neglected in the calculation.

354 In the continuous-mode operation, two mass conservation equations are satisfied at steady
 355 state:

$$356 \quad \frac{d[\text{C}_5\text{H}_8]_{\text{ss}}}{dt} = [\text{C}_5\text{H}_8]_0/\tau - [\text{C}_5\text{H}_8]_{\text{ss}}/\tau - k_1 \cdot [\text{OH}]_{\text{ss}} \cdot [\text{C}_5\text{H}_8]_{\text{ss}} = 0 \quad (\text{Eq2})$$

$$357 \quad \frac{d[\text{C}_4\text{H}_6\text{O}]_{\text{ss}}}{dt} = Y_{\text{C}_4\text{H}_6\text{O}} \cdot k_1 \cdot [\text{OH}]_{\text{ss}} \cdot [\text{C}_5\text{H}_8]_{\text{ss}} - k_2 \cdot [\text{OH}]_{\text{ss}} \cdot [\text{C}_4\text{H}_6\text{O}]_{\text{ss}} - [\text{C}_4\text{H}_6\text{O}]_{\text{ss}}/\tau = 0 \quad (\text{Eq3})$$

358 where [C₅H₈]_{ss} and [C₄H₆O]_{ss} are the PTRMS measured steady-state concentrations of isoprene
 359 and the sum of MACR and MVK when using the cold trap, respectively, [C₅H₈]₀ is the initial
 360 concentration of isoprene, and τ is the chamber mean residence time and can be calculated as the
 361 total chamber volume divided by the incoming/outgoing flow rate. The steady state OH radical
 362 concentration ([OH]_{ss}) can be derived by solving Equation (2). The calculated [OH]_{ss} (3.13×10⁶
 363 molec cm⁻³) is 12% higher than the model prediction (2.74×10⁶ molec cm⁻³). The molar yield of
 364 the sum of MACR and MVK from isoprene OH oxidation pathway in the presence of ~0.45 ppb
 365 NO is thus given by Equation (4) and calculated as 76.7±5.8%:

$$366 \quad Y_{\text{C}_4\text{H}_6\text{O}} = \frac{[\text{C}_4\text{H}_6\text{O}]_{\text{ss}} + k_2 \cdot [\text{OH}]_{\text{ss}} \cdot \tau \cdot [\text{C}_4\text{H}_6\text{O}]_{\text{ss}}}{k_1 \cdot [\text{OH}]_{\text{ss}} \cdot \tau \cdot [\text{C}_5\text{H}_8]_{\text{ss}}} \times f_{\beta\text{-ISOPOO+NO}} \quad (\text{Eq4})$$



367 Here a 5.8% uncertainty originates from the assumption that MACR+OH and MVK+OH
368 proceed with equal reaction rate, although the rate constant for MVK+OH is ~31% lower than
369 that of MACR+OH. Another potential uncertainty relates to the accuracy of the simulated steady
370 state HO₂ and RO₂ concentrations and the contribution of β-ISOPROO+HO₂ and β-ISOPROO+RO₂
371 reaction pathways to the overall β-ISOPROO fate. The fraction of β-ISOPROO radicals that reacts
372 with NO ($f_{\beta\text{-ISOPROO+NO}}$) was predicted as 0.88, which was used here to scale the final
373 MACR+MVK yield, see Eq(4).

374 In summary, the measured yield of the sum of MACR and MVK in this study is close to that
375 reported by Liu et al. (2013), but ~27–52% higher than the majority of previous measurements
376 performed under high NO conditions (NO > 60 ppb). This is consistent with the dynamic nature
377 of the six ISOPROO radical isomers that undergo rapid interconversion by addition/removal of O₂.
378 In the presence of ~0.45 ppb NO as performed in this study, lifetimes of the β-1-OH-2-OO
379 peroxy radical with respect to reaction with NO and loss of O₂ are estimated as 9.4 s and 0.2 s,
380 respectively, implying that the rapid interconversion between β-ISOPROO and δ-ISOPROO
381 radicals essentially governs their distribution, and under such conditions, the production of
382 thermodynamically more stable β-ISOPROO isomers is favored, leading to higher yields of
383 MACR and MVK. Here the reported MACR and MVK yield from isoprene OH oxidation in the
384 presence of ~0.45 ppb NO represents an illustration of chamber operation at steady state
385 continuous flow mode for the establishment of certain experimental conditions that are not easily
386 accessible from traditional batch-mode chamber experiments. A complete measurement of first-
387 generation oxidation products from isoprene OH reaction under a wide range of NO levels
388 (ISOPROO bimolecular lifetimes) will be forthcoming in a future publication.

389 4.3 Optimal operating conditions for nighttime chemistry

390 Figure 4 shows the model simulated steady-state mixing ratios of HO₂, NO₃, NO, NO₂, and
391 O₃ after 16 hours of dark reactions in the chamber as a function of the HCHO concentration and
392 O₃/NO ratio in the continuous chamber inflow. Blank experiments were compared with
393 simulations in five cases (see Table S1 in the Supplement). The model captures the evolution
394 patterns of NO_x and O₃ well. The observed mixing ratios of NO₂ and O₃ agree with the
395 simulations to within 11% and 6%, respectively (Figure S3 in the Supplement).

396 Compared with the photochemical reaction schemes discussed earlier, the nocturnal
397 chemistry is rather straightforward; that is, the inflow O₃/NO ratio governs the steady-state
398 concentrations of NO₃, NO_x, and O₃, while the inflow HCHO concentration ultimately controls
399 the steady-state HO₂ level. Increasing the O₃/NO ratio from 1 to 9 in the continuous inflow leads
400 to increased NO₃ from 2.4×10⁵ to 1.1×10⁹ molec cm⁻³, but decreased NO from 1.8 ppb to 20 ppt
401 and decreased NO₂ from 18 to 7 ppb. At a fixed inflow O₃/NO ratio, doubling the NO and O₃
402 concentrations leads to elevated NO₃, NO_x, and O₃ by a factor of 2.0–3.2, 1.5–2.0, and 1.4–2.0,
403 respectively. The use of HCHO as an effective dark HO₂ source does not significantly impact the
404 steady-state mixing ratios of NO_x and O₃, but slightly weakens the NO₃ production.

405 The calculated RO₂ lifetime (τ_{RO_2}) with respect to reactions with NO, NO₃, and HO₂ at 295
406 K ranges from 3 to 225 s. The highest τ_{RO_2} was achieved in the absence of any HCHO source
407 and corresponds to a chemical regime that can be employed to study the intramolecular
408 isomerization (autoxidation) pathway of RO₂ radicals, if any. Adding a continuous flow of
409 HCHO to the system leads to the production of 10⁷–10⁹ molec cm⁻³ HO₂ radicals that then



410 constitute a significant sink of RO₂ radicals and represents prevailing forest environments during
411 nighttime.

412 4.4 Application to NO₃-initiated oxidation of isoprene

413 NO₃-initiated oxidation of isoprene proceeds by the NO₃ addition to the carbon double
414 bonds followed by O₂ addition, yielding six distinct nitrooxy peroxy radicals (INOO), including
415 two isomers (β-INOO) with O₂ added on the β-carbon to the nitrate group (see Figure 2B for
416 schematic illustration). The β-INOO radicals react further with NO₃, HO₂, NO, and RO₂,
417 producing nitrooxy alkoxy radicals (β-INO) with molar yields of 1.00, 0.53, 0.97, and 0.40,
418 respectively (Wennberg et al., 2017). The further decomposition of β-INO radicals produces
419 MACR and MVK, together with HCHO and NO₂. Depending on the actual fate of β-INOO
420 radicals, the yields of β-INO radicals can then vary from 0.4 to 1.0, resulting in a distinct
421 distribution of final oxidation products. It is thus important to specify the ultimate fate of INOO
422 radicals during quantification of oxidation products from isoprene reaction with NO₃. As an
423 illustration, we performed one continuous mode experiment that targets on controlling the
424 steady-state fate of INOO radicals to be their reaction with NO and HO₂ (46% and 38% INOO
425 radicals are predicted to react with NO and HO₂, respectively, as shown in Fig.5). Note that by
426 adjusting the concentrations and fractions of inflow reactants (O₃, NO, HCHO, and C₅H₈),
427 different chemical fates and lifetimes of INOO radicals can be achieved.

428 Figure 5 shows the observed and predicted temporal profiles of NO_x, O₃, C₅H₈, and C₄H₆O
429 over 25 hours of isoprene oxidation by NO₃, with continuous input of 10.2 ppb C₅H₈, 205 ppb
430 O₃, and 59 ppb NO into the chamber and a balancing outgoing flow at 40 L min⁻¹ carrying well-
431 mixed reactants and products. It took >16 hours to reach steady state for all the species
432 displayed. In general, the model captures the trends of O₃ and NO well, while underpredicting
433 the steady state NO₂ by ~26%. After ~18 hours of dark reaction, the PTR-MS sampling tubing
434 was submerged into an ethanol cold bath (-40±2 °C) to trap artifacts in the PTR-MS measured
435 C₄H₇O⁺ (*m/z* 71) signal. The simulated steady-state concentration of isoprene agrees within 9%
436 with the measurements. The derived concentration of the sum of MACR and MVK from the
437 measured C₄H₇O⁺ ion intensity upon cold-trapping is ~1.1 ppb, which is ~129% higher than the
438 model predictions (~0.48 ppb). This disagreement can be attributed, to a large extent, to the
439 oversimplified representation of the six different INOO radicals as one δ-INOO isomer in the
440 MCMv3.3.1 mechanism. As a result, the production of β-INOO radical, the important precursor
441 of MACR and MVK, from NO₃-initiated oxidation of isoprene is suppressed in the simulations.
442 The measured molar yield of the sum of MACR and MVK is 36.3±12.1%, with uncertainties
443 arising from the fact that 10.5% isoprene is predicted to react with OH as an additional source of
444 MACR and MVK. Using this value, the fraction of β-INOO over the sum of nitrooxy peroxy
445 radicals is estimated as 48.6±16.2%, which is close to that (~46.3%) reported by Schwantes et al.
446 (2015), although the estimated bimolecular lifetime of INOO radical in that study (~30 s) is
447 lower than that predicted in the present work (~50 s). As discussed above, the hydroxyl peroxy
448 radicals produced from OH-oxidation of isoprene could undergo rapid interconversion through
449 addition/removal of O₂ at atmospherically relevant lifetimes. This interconversion significantly
450 impacts the subsequent chemistry of individual ISOPOO radical isomers in terms of reaction
451 rates and product distributions. It is likely that the INOO radicals follow similar interconversion
452 due to the small R-OO bond dissociation energy, although no experimental evidence exists. A
453 full examination of the INOO chemistry, i.e., their kinetic and thermodynamic properties as well



454 as their chemical fate at different lifetimes, will be the focus of future studies using this
455 continuous flow chamber operation method.

456 5. Conclusions

457 We report here the development and characterization of the NCAR Atmospheric Simulation
458 Chamber operated at steady state continuous flow mode for simulating daytime and nocturnal
459 chemistry under atmospherically relevant NO levels. The chamber is designed to achieve a well-
460 controlled steady-state environment by continuous inflow of reactants and continuous
461 withdrawal of reactor contents. We use a combination of kinetic modeling and chamber
462 experiments to characterize the ‘intermediate-NO’ chemical regime (tens of ppt to a few ppb)
463 that can be achieved by precisely controlling the inlet reactant concentrations and the
464 mixing/residence timescales of the chamber.

465 To mimic daytime photochemistry, continuous input of H₂O₂ and NO gases is required,
466 resulting in steady state OH mixing ratios of 10⁵–10⁶ molec cm⁻³ under irradiation. Under such
467 conditions, the lifetime of a peroxy radical with respect to reaction with NO and HO₂ can be
468 extended to 60 s or even longer, thus providing a unique environment to study all reaction
469 possibilities of RO₂ radicals including the intramolecular isomerization (autoxidation) pathway.
470 When studying OH-initiated chemistry, care needs to be taken to avoid a range of experimental
471 conditions (e.g., inflow H₂O₂ > 2 ppm and NO > 20 ppb) where NO₃-oxidation might account for
472 a large fraction of the overall degradation pathway of certain parent hydrocarbons such as
473 alkenes.

474 To mimic nighttime chemistry, continuous input of NO (or NO₂) and O₃ is needed to
475 produce steady state NO₃ radicals in the range of 10⁶–10⁹ molec cm⁻³ in the dark. Under such
476 conditions, an RO₂ radical can live up to 4 min prior to finding a bimolecular reaction partner
477 (e.g., NO, NO₃, and HO₂), which were the dominant fates of RO₂ radicals in most batch-mode
478 chamber experiments. Again, the long lifetime of RO₂ radicals achieved by the steady state
479 continuous mode operation opens an avenue for close examination of RO₂ unimolecular
480 (isomerization) pathways in nocturnal environments.

481 In simulating both daytime and nighttime chemistry with continuous flow operation method,
482 O₃ accumulation is unavoidable. The extent to which ozonolysis interferes with OH- or NO₃-
483 initiated oxidation chemistry depends on the steady state O₃ concentration achieved in the
484 chamber and its reactivity towards various parent VOCs. Taking isoprene as an example,
485 ozonolysis accounts for <1% and <0.1% of the overall isoprene degradation kinetics,
486 respectively, under established steady-state photolytic and dark conditions described above.

487 In atmospheric chemistry, the terms ‘zero-NO’ versus ‘high-NO’ have been widely used to
488 classify photooxidation conditions and delineate the gas-phase fate of the peroxy radicals (RO₂)
489 generated from VOCs oxidation (Cappa et al., 2013; Zhang and Seinfeld, 2013; Loza et al.,
490 2014; Schilling Fahnstock et al., 2014; Zhang et al., 2014b; Krechmer et al., 2015; Nguyen et
491 al., 2015; Zhang et al., 2015a; Riva et al., 2016; Schwantes et al., 2017). In the so-called ‘high-
492 NO’ regime, reaction with NO dominates the fate of RO₂ radicals, whereas in the ‘zero-NO’
493 regime, the RO₂ radicals primarily undergo reaction with HO₂ and, perhaps to a much lesser
494 degree, self/cross-combination. The importance of the ‘intermediate-NO’ regime lies in the fact
495 that at sub-ppb levels of NO, the RO₂+NO and RO₂+HO₂ reactions are expected to co-exist and
496 the RO₂ radical could survive up to several minutes before encountering a partner (NO/HO₂) for



497 bimolecular reactions. Under such conditions, the RO₂ radical isomers may undergo
498 interconversion by addition/removal of O₂ and intramolecular isomerization (autoxidation)
499 through H-shift. Here we use isoprene as an illustrative VOC to explore the fate of RO₂ radicals
500 under sub-ppb NO. Future work will focus on detailed characterization of oxidation products
501 from isoprene day- and nighttime chemistry with particular attention given to the controlled RO₂
502 fates and lifetimes.

503 **Data Availability**

504 Data presented in this manuscript are available upon request to the corresponding author.

505 **Competing interests**

506 The authors declare that they have no conflict of interest.

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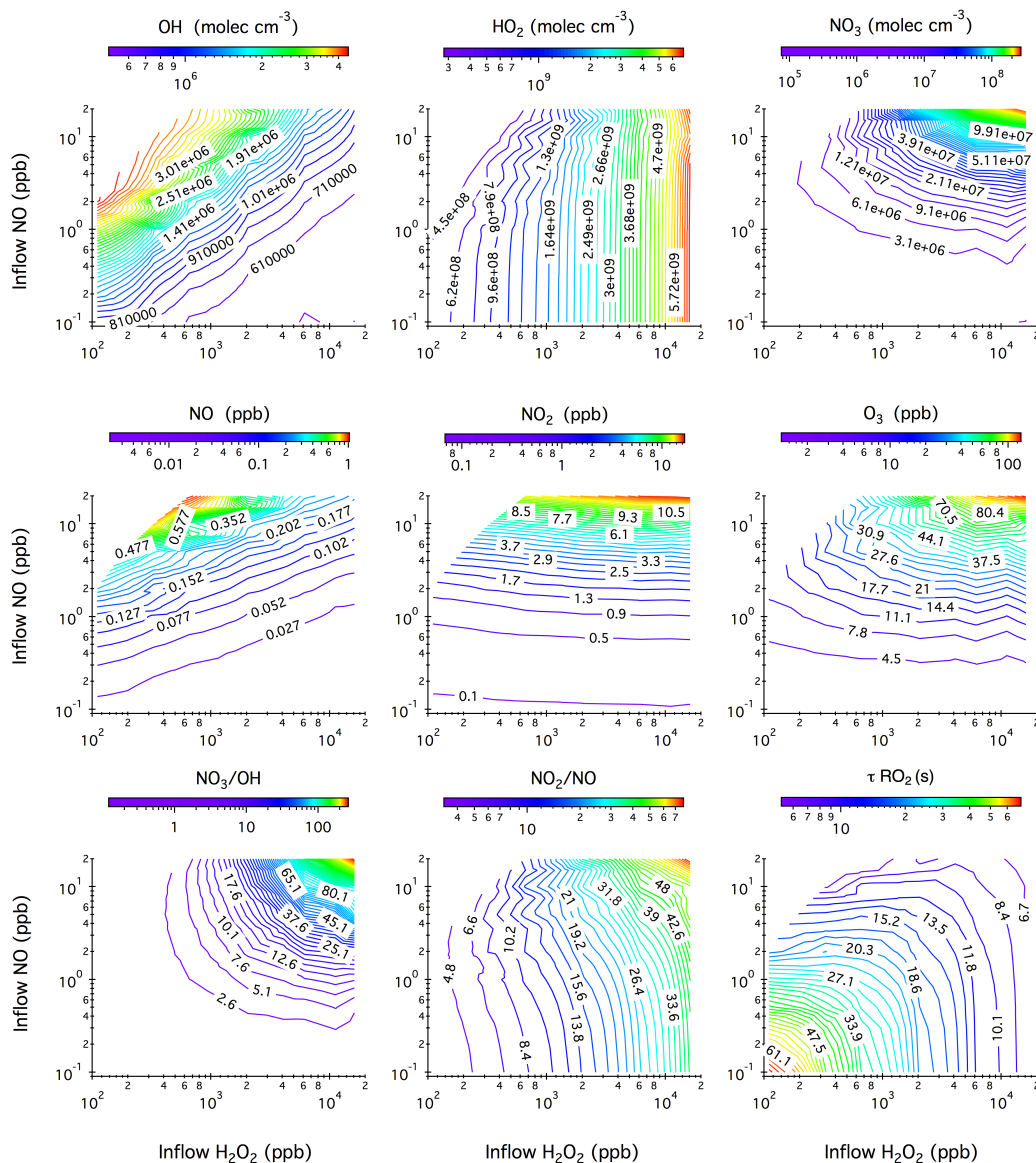


Figure 1. Contour plots showing the model predicted steady-state mixing ratios of OH, HO₂, NO₃, NO, NO₂, and O₃ after 20 hours of photochemical reactions in the chamber as a function of the concentrations of H₂O₂ and NO in the continuous injection flow. Also given here are the simulated NO₃ to OH ratio, NO₂ to NO ratio, and the lifetime of an RO₂ radical (τ_{RO_2}) with respect to reactions with NO and HO₂. Note that the ripples on the contour lines originate from the limited simulation datasets that are used to generate iso-response values.

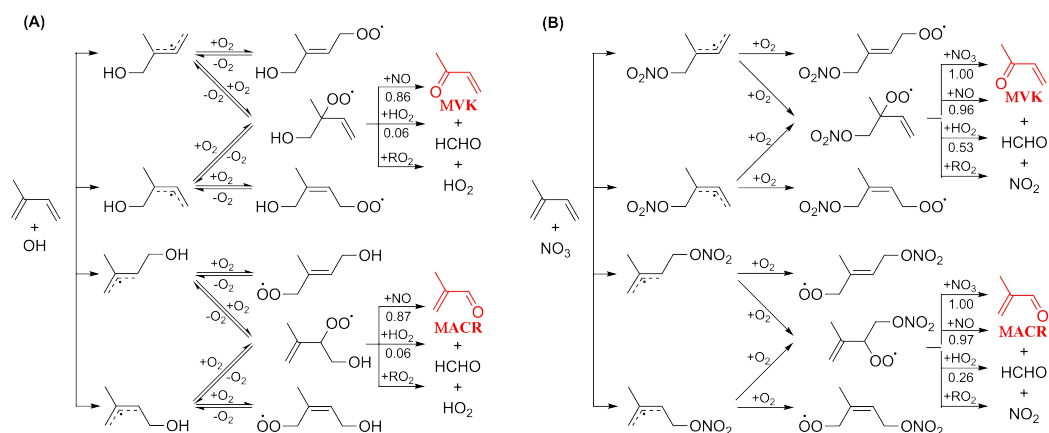


Figure 2. Representative mechanism for (A) OH- and (B) NO₃-initiated oxidation of isoprene that leads to the formation of MACR and MVK.

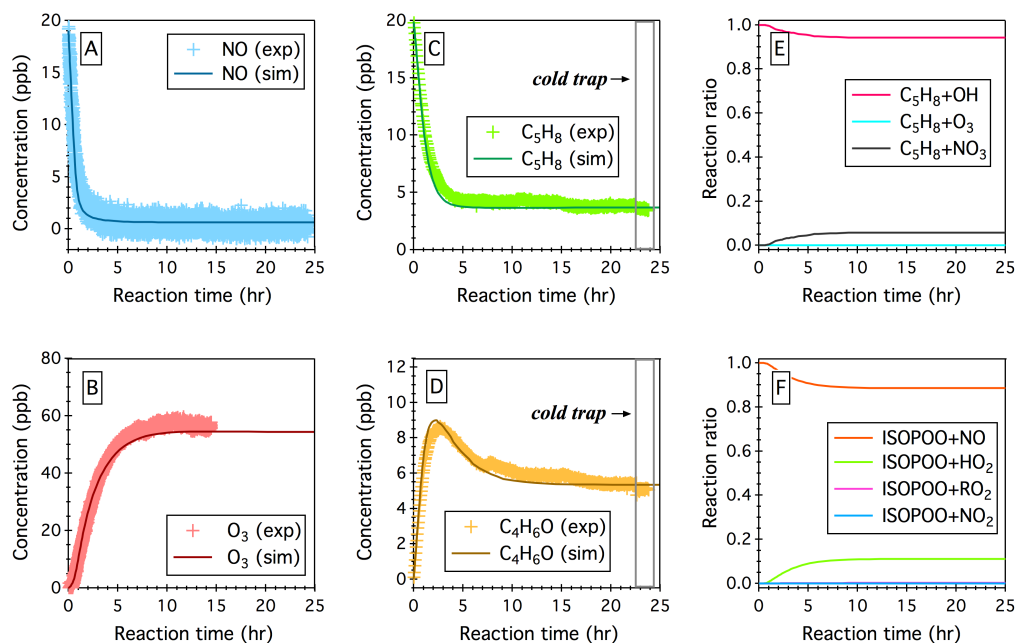


Figure 3. Simulated (sim.) and observed (exp.) temporal profiles of (A) NO, (B) O₃, (C) isoprene (C₅H₈), and (D) the sum of MACR and MVK (C₄H₆O) over 24 hours OH-initiated oxidation of isoprene in the continuous-flow mode chamber operation. Also displayed here include (E) simulated fractions of OH-oxidation, ozonolysis, and NO₃-oxidation as the removal pathways of isoprene, and (F) simulated fractions of ISOPROO radicals that react with NO, HO₂, RO₂, and NO₃. Time 0 is the point at which the chamber lights are turned on. Initial experimental conditions are 19 ppb NO, 0 ppb NO₂, 0 ppb O₃, 600 ppb H₂O₂, and 19.9 ppb C₅H₈, with continuous input of 600 ppb H₂O₂, 19 ppb NO, and 19.9 ppb C₅H₈ over the course of 24 hour photochemical reactions.

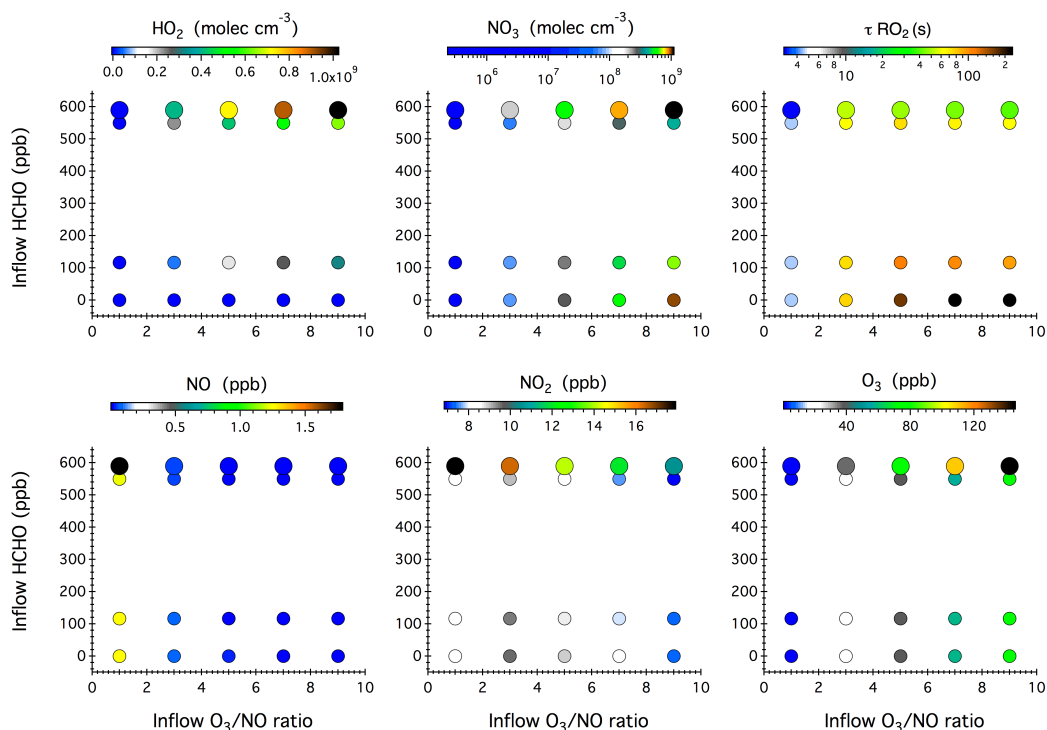


Figure 4. Simulated steady-state mixing ratios of HO_2 , NO_3 , NO , NO_2 , and O_3 after 16 hours of dark reactions in the chamber as a function of the concentrations of NO and O_3 in the continuous injection flow. The symbol size denotes different inflow NO concentrations, i.e., 10 ppb and 20 ppb. Also given here is the calculated lifetime of an RO_2 radical (τ_{RO_2}) with respect to reactions with NO , NO_3 , and HO_2 .

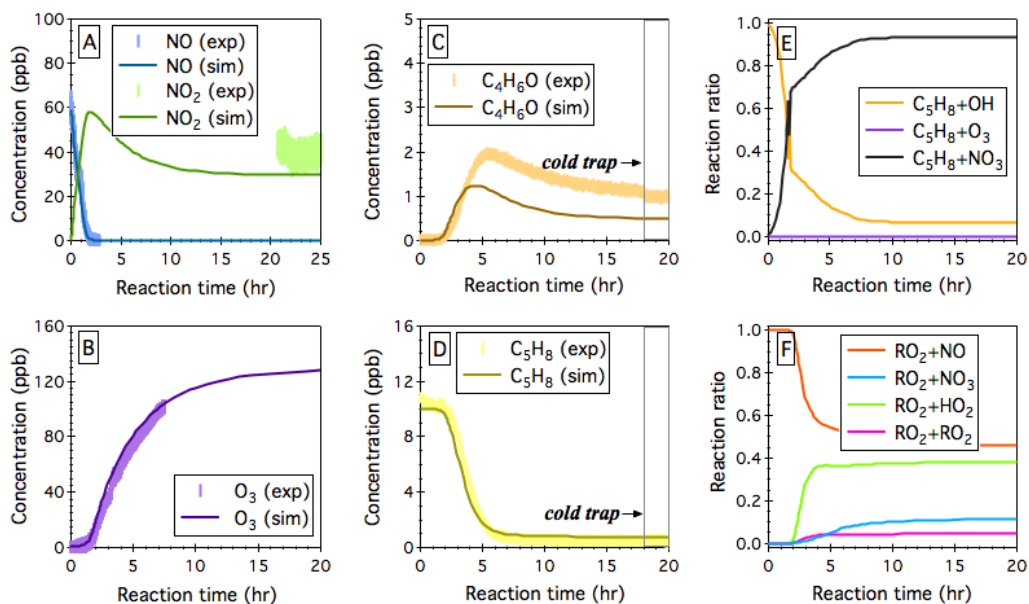


Figure 5. Simulated (sim.) and observed (exp.) evolution patterns of (A) NO_x , (B) O_3 , (C) the sum of MACR and MVK ($\text{C}_4\text{H}_6\text{O}$), and (D) isoprene (C_5H_8) over 25 hours NO_3 -initiated oxidation of isoprene under continuous-flow mode chamber operation. The fractions of isoprene that react with OH, O_3 , and NO_3 are given in panel (E), and the fractions of INOO radical that undergo bimolecular reactions with NO, NO_3 , HO_2 , and RO_2 are given in panel (F). Initial experimental conditions are 0 ppb O_3 , 59 ppb NO_x , and 10.2 ppb C_5H_8 , with continuous input of 205 ppb O_3 , 59 ppb NO , and 10.2 ppb C_5H_8 over the course of 25 hour dark reactions.