Supplemental Information for:

Quantification of peroxynitric acid and peroxyacyl nitrates using an ethane-based thermal dissociation peroxy radical chemical amplification cavity ring-down spectrometer

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S1.0 Box simulations of ethane PERCA chemistry

Box model simulations were carried out using a subset of reactions in the "Master Chemical Mechanism" (MCM) (Jenkin et al., 1997; Saunders et al., 2003; Jenkin et al., 2012) to aid in the interpretation of experimental data and are not intended as accurate representations of experiments. To reproduce the experimental data in PERCA reaction chambers, models need to make assumptions about the magnitudes and temperature dependencies of wall loss rates (which are not known). An additional limitations is that the MCM has only been validated at ambient temperature and below, and the rate constants are more uncertain at elevated temperatures. In addition, thermal gradients within the PERCA chambers are not taken into account. Thus, simulations are poor a priori predictors of experimental chain lengths and should not be viewed as such.

In section S1 below, we carried out simulations using only a subset of reactions in the MCM to probe the temperature dependence of gas-phase reactions. In section S2, we added pseudo first-order loss rates for OH and RO₂ radicals to simulate the potential effects of inner walls of the PERCA reactor. In section S3, we investigated the humidity dependence of PERCA, adding HO₂·H₂O chemistry using the equilibrium constants by Kanno et al. (2006) and the reactions of HO₂·H₂O with HO₂ (Kanno et al., 2006) and NO (Butkovskaya et al., 2007)

S1.1 MCM only simulations

The chemistry in the PERCA reactor was modelled at temperatures of 25 °C or 250 °C using a subset of the MCM V3.3.1 obtained from http://mcm.leeds.ac.uk/MCM by adding ethane to the marked list and extracting the subset in the Kinetic Preprocessor (KPP) (Sandu and Sander, 2006) format along with inorganic reactions and generic rate coefficients. A plug flow modelling approach was used where initial conditions and mixing ratios were set and the model allowed to proceed without any additional inputs or outputs. Radical wall-loss reactions were not added.

Simulations were performed using the optimized PERCA reagent gas concentrations (i.e., 650 ppbv NO; 1.65 % ethane) at either 25 °C or 250 °C. Table S1 provides an overview of the model inputs. The model runs were also initialized with an initial input of 15, 100, 300, 600, 900, or 1200 pptv of either HO₂ or CH_3O_2 .

	Mixing Ratio	Number density at 25 °C (molecules cm ⁻³)	Number density at 250 °C (molecules cm ⁻³)
М	-	$2.14 imes10^{19}$	1.22×10^{19}
NO	650 ppbv	1.39×10^{13}	7.92×10^{12}
C_2H_6	1.65%	$3.53 imes 10^{17}$	2.01×10^{17}
O ₂	20.1%	4.29×10^{18}	2.45×10^{18}
N_2	77.6%	1.66×10^{19}	$9.46 imes 10^{18}$

Table S1. Model inputs for simulations run at 25 °C and 250 °C



Figure S1. Time series of peroxy radicals (left-hand axis) and hydroxyl radicals (right-hand axis) for a simulation initiated with 15 pptv of HO_2 at 25 °C.



Figure S2. Time series of peroxy radicals (left-hand axis) and hydroxyl radicals for a simulation initiated with 15 pptv of HO₂ at 250 °C.

Figures S1 and S2 show peroxy and hydroxyl radical concentrations during the first 5 seconds of simulations initiated with 15 pptv of HO₂ at 25 °C and 250 °C, respectively. In our chamber, the PERCA reactions are stopped as the radicals encounter the filter after 2.3 s in the dual channel setup. Due to the lower gas density at higher temperatures, a lower concentration of RO₂ radicals is present initially (even though the mixing ratio is the same in both cases). Reactions of HO₂ and RO₂ with NO (e.g., R3, Table 2 of the main manuscript) have negative activation energies and are hence slower at higher temperatures, leading to a lower rate of OH radical production and, since OH loss rates are similar, to lower OH concentrations (maximum of ~ 1.9×10^4 molecules cm⁻³ at 250 °C vs. 2.2×10^5 molecules cm⁻³ at 25 °C) and lower turnover numbers.

Figure S3 shows the CL (number of NO₂ molecules produced divided by molecules of RO₂ present originally) as a function of temperature and mixing ratio of radicals added initially. Simulations initiated with HO₂ radicals gave identical results to simulations initiated with CH₃O₂ radicals. For simulations conducted at 25 °C, CL is concentration dependent and decrease with increasing concentration. For simulations conducted at 250 °C, the chain length is still concentration dependent, albeit to a much lesser extent than at room temperature. At 250 °C, the CL in the initial 2.3 s of reaction time is well below the CL obtained at 25 °C, inconsistent with experiment which showed a CL of 69±5 at 250 °C (much higher than CL obtained at 25 °C. This suggests that experimental CL are largely a function of wall reactions not included in the simulations.



Figure S3. Time series of CL for simulations initiated with 100, 300, 600, 900, and 1200 pptv of CH₃O₂ at 25 °C (blue colors) and 250 °C (red colors).

S1.2 Inclusion of HO₂·H₂O cluster in the mechanism

Another factor contributing to observed CL are radical losses due to HO₂ water cluster formation (i.e., HO₂.H₂O) (Kanno et al., 2006). To estimate the temperature dependent formation of HO₂.H₂O cluster the model assumed that equilibrium between the cluster and HO₂ and H₂O was established at every model time step (0.1 s) following the equilibrium rate constant reported by Kanno et al. (2006): $6.6 \times 10^{-17} \times T \times e^{(3700/T)}$. Upon formation, HO₂.H₂O can react with HO₂ (k = 6.0×10^{-13} cm³ molecule⁻¹ s⁻¹) (Kanno et al., 2006) or NO (k = $5.4 \times 10^{-11}e^{(-410/T)}$ cm³ molecule⁻¹ s⁻¹) (Butkovskaya et al., 2007; Butkovskaya et al., 2009).

Figure S4 shows the CL obtained after the inclusion of $HO_2 H_2O$ cluster as a function of RH at 25 °C and 250 °C initiated with 15 pptv HO₂. At 25 °C, the CL is strongly dependent on RH, whereas at 250 °C, there is very little RH dependence as the HO₂.H₂O cluster is thermally dissociated.

Figure S5 shows the concentration dependence at a RH of 20% after inclusion of water clusters in the model simulations. Ultimately, lower CL are observed in the 25 °C system while the 250 °C system chemistry, and associated CL, are relatively unchanged. Furthermore, CLs in the initial 2.3 s of reaction time were generally well below CL obtained at the lower temperature. Once again, this is inconsistent with our experiments where elevated temperatures provided for larger CL values.



Figure S4. Time series of CL for simulations at different RH and initiated with 15 pptv of HO₂ at 25 $^{\circ}$ C (blue colors) and 250 $^{\circ}$ C (red colors).



Figure S5. Time series of CL for simulations at 20% RH initiated with different HO₂ mixing ratios at 25 °C (blue colors) and 250 °C (red colors).

S1.3 Inclusion of wall losses in the mechanism

The dependence of CL on temperature and RH in the model simulations shown in S1 and S2 are inconsistent with experiment. To reconcile model simulations with experiment, pseudo-first order wall loss reactions of radicals were added to the mechanism. The room-temperature rate constants reported by Mihele et al. (1999) for HO₂ and RO₂ of 2.8 s⁻¹ and 0.8 s⁻¹ were used, respectively.

Figure S6 shows a time series of the CL for simulations conducted at 20% RH after inclusion of these wall losses in the model. Due to increased radical losses, radical chemistry ceases after ~ 1s. Furthermore, the CL dependence on radical concentration is reduced.

Inconsistent with experiment, the CL is still predicted to be larger at 25 °C than at 250 °C. This may be a result of the use of temperature independent wall loss rates that should be reduced at elevated temperatures.

Assuming, as a lower limit, no wall losses at 250 °C, and factoring in the 2.3 second residence time of our PERCA chamber, the simulations predict larger CL at elevated temperatures (a CL of 80 at 250 °C and a CL of 44 at 25 °C – shown as a green trace in Fig. S6).



Figure S6. Time series of CL for simulations at 20% RH initiated as a function of HO₂ mixing ratios at 25 °C (blue colors) and 250 °C (red colors) with $k_{wall}(HO_2)$ and $k_{wall}(RO_2)$ of 2.8 s⁻¹ and 0.8 s⁻¹, respectively.

S1.4 Inclusion of ethyl nitrite and ethyl peroxy nitrate formation in the mechanism

A potentially important radical chain termination reaction not included in the MCM is that between C_2H_5O and NO to form C_2H_5ONO (Mihele and Hastie, 2000; Wood et al., 2016). The rate of this reaction decreases slightly with temperature: At a pressure of 660 Torr and using kinetic parameters from (Burkholder et al., 2015), the rate coefficient decreases from 4.8×10^{-11} to 3.9×10^{-11} cm³ molecule⁻¹ s⁻¹ between 25 °C and 250 °C. Ethyl nitrite thermally decomposes with an activation barrier of ~157 kJ mol⁻¹ (Steacie and Shaw, 1934) and has a lifetime with respect to thermal decomposition (to NO and C_2H_5O) of ~40 s at 250 °C; this implies that for the temperature ranges shown in the manuscript, ethyl nitrite will not significantly decompose and constitutes a radical sink.

Another potentially important radical chain termination reaction not included in the MCM is that between $C_2H_5O_2$ and NO_2 to form $C_2H_5O_2NO_2$ (Wood et al., 2016). The rate of this reaction also decreases slightly with temperature: at a pressure of 660 Torr and using the kinetic parameters from (Burkholder et al., 2015), the rate coefficient decreases from 8.8×10^{-12} to 8.5×10^{-12} cm³ molecule⁻¹ s⁻¹ between 25 °C and 250 °C. $C_2H_5O_2NO_2$ thermally decomposes with an activation barrier of ~86.8 kJ mol⁻¹ and has lifetimes with respect to thermal decomposition (to NO₂ and $C_2H_5O_2$) of ~0.2 s and ~5×10⁻⁸ s at 25 °C and 250 °C, respectively. Formation of this molecule is hence expected to shift radical chemistry at 25 °C while having little effect at 250 °C.

Shown in Figure S7 are the simulations of Figure S6 with C_2H_5ONO and $C_2H_5O_2NO_2$ formation and thermal decomposition added to the mechanism.

Assuming, as a lower limit, no wall losses at 250 °C, and factoring in the 2.3 s residence time of our PERCA chamber, the simulations predict larger CL at elevated temperatures (a CL of 65 at 250 °C and a CL of 30 at 25 °C – shown as a green trace in Fig. S6). These values are consistent with experiment.



Figure S7. Same as Figure S6 but with C₂H₅ONO and C₂H₅O₂NO₂ formation and thermal decomposition included in the mechanism.

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