



# **Particle Wall-loss Correction Methods in Smog Chamber Experiments**

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# 10 Abstract

The interaction of particles with the chamber walls has been a significant source of uncertainty when analyzing results of secondary organic aerosol (SOA) formation experiments performed in Teflon chambers. A number of particle wall-loss correction methods have been proposed including the use of a size-independent loss rate constant, ratio of suspended organic

15 mass to that of a conserved tracer (e.g., sulfate seeds), size-dependent loss rate constant, etc. For complex experiments such as chemical aging of SOA, the results of the SOA quantification analysis can be quite sensitive to the adopted correction method due to the evolution of the particle size distribution and the duration of these experiments.

We evaluated the performance of several particle wall-loss correction methods for aging 20 experiments of  $\alpha$ -pinene ozonolysis products. Determining the loss rates from seed loss periods is necessary for this system because it is not clear when chemistry is over. Results from the organic to sulfate ratio and the size-independent correction methods can be influenced significantly by the size-dependence of the particle wall-loss process. Coagulation can also affect the particle size distribution, especially for particles with diameter less than 100 nm, thus introducing errors in the

25 results of the wall-loss correction. The corresponding loss rate constants may vary from experiment to experiment, and even during a specific experiment. Friction between the Teflon





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chamber walls and non-conductive surfaces can significantly increase particle wall-loss rates and the chamber may require weeks to recover to its original condition. Experimental procedures are proposed for the characterization of particle losses during different stages of these experiments and the evaluation of corresponding particle wall-loss correction.

#### **1. Introduction**

Smog chamber experiments have been an important tool for the study of atmospheric aerosol processes. One major challenge of smog chamber experiments is the particle wall-loss
processes. The aerosols inside the chamber are lost to its walls due to Brownian diffusion, convection, electrostatic effects (especially for Teflon chambers) and gravitational sedimentation (Crump and Seinfeld, 1981). The particle wall-loss process is first-order and the particle wall-loss rate constant, *k*, is defined as,

$$\frac{\partial N(D_p,t)}{\partial t} = -k(D_p,t)N(D_p,t),\tag{1}$$

- 40 where  $N(D_p, t)$  is the number concentration of particles with diameter  $D_p$  at time *t*. For an aerosol population, *k* is in general a function of particle size and time. Smaller-sized particles (less than 50 nm) have a higher loss rate due to diffusion-dominated wall-loss process while particles larger than one micron are lost mainly due to sedimentation for a reactor with low air motion inside. Electrostatic effect can play a major role for intermediate sizes (McMurry and Rader, 1985).
- 45 Early studies of chamber simulations of secondary organic aerosol (SOA) formation and growth assumed that the particle wall loss is negligible in fairly large chambers (~30 m<sup>3</sup>) when determining SOA yields (Stern et al., 1987). Several particle wall-loss correction methods have since been developed and adopted in chamber studies. Pathak et al. (2007) proposed a semiempirical wall-loss correction method that involves determining the first-order particle wall-loss
- For rate constant, k, from the SMPS-measured SOA mass concentration after chemical reactions have been completed. This total mass concentration-based method is based on the assumption that k is independent of particle size for the size range of particles present in the experiment and remains constant during the course of an experiment. The constant k is found as the slope of the linear regression:



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$$\ln[C_{SOA}^{sus}(t)] = -kt + Q, \tag{2}$$

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where  $C_{SOA}^{sus}(t)$  is the measured SOA mass concentration at time t and Q is an arbitrary constant. The values of  $C_{SOA}^{sus}(t)$  used for the fit are taken after the SOA production has finished (condensation/evaporation is minimal). The corrected SOA concentration can be found by:

$$C_{SOA}^{tot} = C_{SOA}^{sus}(t) + k \int_0^t C_{SOA}^{sus}(t) dt - C_{seed}(0), \tag{3}$$

60 where  $C_{seed}(0)$  is the seed mass concentration when SOA formation begins. This approach is relatively accurate when k remains more or less constant over the size range of the aerosol population inside the chamber, and accounts for the experiment-to-experiment variability of the particle wall-loss rates. However, it requires a period during which no reactions are taking place in the chamber and assumes that the rate constant does not vary during the experiment.

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The size-dependent correction method involves determining a first-order  $k(D_p)$  through the aforementioned linear fitting of the number concentration of the suspended particles, for each size, usually with the help of a scanning mobility particle sizer (SMPS). Several studies that adopted this method determined the  $k(D_p)$  profile for the corresponding chamber through seed experiments where inert (e.g., ammonium sulfate) particles were used (McMurry and Grojean,

<sup>70</sup> 1985; Keywood et al., 2004; Ng et al., 2007; Nah et al., 2017; Fry et al., 2014). In these studies, an average  $k(D_p)$  profile was applied to all experiments. This method takes care of the size dependence of k but not its potential variation from experiment to experiment. Ng et al. (2007) and Wang et al. (2017) determined a  $k(D_p)$  profile using the initial seed wall-loss period for each of their experiments, thus accounting for the experiment-to-experiment variation.

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The OA/Sulfate correction method was proposed by Hildebrandt et al. (2009) using the organic and the sulfate mass concentration measured by the aerosol mass spectrometer (AMS). This approach assumes that the loss rate constant of organic species and sulfate are the same during an experiment as there are no processes affecting sulfate other than losses to the walls (e.g., no added SO<sub>2</sub> or other sulfate precursor). The corrected OA mass concentration is then calculated as,

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$$C_{OA}(t) = \frac{C_{OA}^{SUS}(t)}{C_{seed}(t)} C_{seed}(0)$$
(4)

where  $C_{OA}^{sus}(t)/C_{seed}(t)$  is the AMS-derived organic to sulfate ratio and  $C_{seed}(0)$  is the seed concentration in the chamber when SOA formation starts. Several chamber studies have adopted this method (Henry and Donahue, 2012; Loza et al., 2012). Other variations of this method including use the ratio of OA to other inert tracers like black carbon (BC) which are present in





experiments investigating the evolution of primary OA from combustion sources (Hennigan et al., 2011). This method involving the use of OA-to-tracer ratio is accurate when the OA and the tracer have the same size distribution during the experiment or when the loss rate constant is close to size independent. However, in experiments in which SOA condenses more onto smaller-sized particles, the size dependence of the loss rate can introduce significant uncertainty in the corrected results
90 especially for time scales of several hours (Wang et al., 2017).

An alternative method for particle wall-loss correction is the use of models of aerosol dynamics. Pierce et al. (2008) developed the Aerosol Parameter Estimation (APE) model that simulates the processes of condensation/evaporation, coagulation and particle wall loss during a chamber experiment. By constraining the unknown parameters with the SMPS-measured particle

- 95 size distribution, the model can predict SOA formation for each experiment accounting for wall losses. The predicted particle wall-loss rates are both size- and time- dependent. The APE model predicts the particle wall-loss rates by assuming specific functional forms of its dependence on particle size (Crump and Seinfeld, 1981). The model has performed well in experiments in which the reaction time scale was short, but produced more uncertain results in experiments with slower
- 100 reacting systems. Nah et al. (2017) adopted a modified version of the APE model that calculates the size-dependent wall-loss rate necessary to reproduce the observed size distribution assuming Brownian coagulation was the only other particle process occurring in the chamber (i.e. no condensation/evaporation occurred during the analyzed portion of the experiment). The sizedependent, instantaneous particle loss rates were calculated directly from the SMPS-measured
- 105 seed number size distribution at each time step. These instantaneous  $k(D_p)$  values were then averaged over the initial seed loss period of the experiment (or a separate experiment where  $k(D_p)$ was characterized). This determined  $k(D_p)$  can then be applied to the SOA formation period of experiments to correct for the size-dependent wall loss. This approach, focusing on specific wallloss characterization experiments, has the advantage that the functional dependence of the wall-
- 110 loss rate constant is directly calculated from the measurements by simply removing the effect of coagulation. Its disadvantage compared to APE is that it requires additional time/experiments for seed measurements and can no longer address the potential time dependence of k over the course of a complex experiment.

The aforementioned methods each has its own advantages and disadvantages, and may perform well for specific experiments and chambers. However, for long-lasting experiments such





as SOA aging where particle size distribution may shift across a wide size range due to several generations of condensation, it is important to address both the time- and size-dependence of the particle loss rates for the purpose of SOA quantification. In this work, we adopt the modified APE model following Nah et al. (2017) and derived the size-dependent particle loss rate constants,  $k(D_p)$ , based on seed periods during the experiments. As an attempt to evaluate the time-dependence of 120 the loss rates, we derive a second  $k(D_p)$  at the end of each experiment with a second seed injection and loss characterization period. To probe the effect of electrostatic forces on particle wall loss, we regularly measured the  $k(D_p)$  during the time period when the chamber was experiencing changes (e.g., changes in its surroundings, location or air motion inside). We explore the coagulation effect on the estimated particle wall-loss rates and particle number/volume 125 concentration in both a 12 m<sup>3</sup> Teflon chamber and a smaller 1.5 m<sup>3</sup> Teflon reactor. We evaluate the performance of the aforementioned particle wall-loss correction methods for relatively complex aging experiments involving 2 or 3 generations of condensation of the  $\alpha$ -pinene ozonolysis products.

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#### 2. Experimental approach

# 2.1 Particle wall-loss rate constant measurements in the 12 m<sup>3</sup> CMU Teflon chamber

The CMU smog chamber is a 12 m<sup>3</sup> Teflon reactor (Welch Fluorocarbons) suspended in a temperature-controlled room. The walls of the room are covered with UV lights (GE10526 and 10244). Prior to each experiment, the chamber is flushed overnight with purified air under UV illumination to remove any residual particles and vapors. Purified air is generated by passing house air through a high-efficiency particulate air (HEPA) filter to remove particles, a Purafil filter to remove NO<sub>x</sub> and an activated carbon filter to remove any organics followed by a silica gel filter, keeping relative humidity (RH) below 20% throughout the experiments performed in this work.

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A list of experiments performed in this work is presented in Table 1, together with the experimental conditions. To characterize the particle wall-loss rates, we performed experiments with ammonium sulfate (AS) particles during a full year, with one listed in Table 1. We used both 1 g L<sup>-1</sup> and 5 g L<sup>-1</sup> ammonium sulfate solutions to generate particles, with the latter producing more particles at larger sizes. The ammonium sulfate solution was fed to an atomizer (TSI, model 3076) at a constant rate of 90 mL h<sup>-1</sup> to produce droplets. The droplets passed through a diffusion

145 3076) at a constant rate of 90 mL h<sup>-1</sup> to produce droplets. The droplets passed through a diffusion dryer and a neutralizer to produce dry ammonium sulfate particles. This process produced seeds





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with a number mode diameter of around 100 nm. The initial seed number concentration in the chamber ranged from  $2-5 \times 10^4$  cm<sup>-3</sup>, corresponding to mass concentration of 40-200 µg m<sup>-3</sup> and surface area concentration of 1100-4600 µm<sup>2</sup> cm<sup>-3</sup>. After injecting the particles, the particle wall loss was quantified for 3-4 hours. We measured the particle size distribution with a Scanning Mobility Particle Sizer (SMPS, TSI classifier model 3080; DMA model 3081; CPC model 3010

or 3772).

For a number of  $\alpha$ -pinene ozonolysis experiments, we characterized the particle wall-loss rates twice, once before and once after the main experiment. The rationale behind the second injection is to ensure that the wall loss rate constant profile remains relatively consistent (no major change) throughout each experiment. Due to the length of these aging experiments, few particles were left after the main experiment for a robust characterization of the profile, and thus we inject additional seed particles for a second time. At the beginning of each aging experiment, we used the 1 g L<sup>-1</sup> ammonium sulfate solution to generate seed particles to provide enough surface area for the vapors to condense on. From the 3-4 h wall-loss time period, we were able to characterize the initial  $k(D_p)$  profile for this experiment. At the end of each experiment, we injected additional ammonium sulfate seeds into the chamber using the same method with a more concentrated solution (5 g L<sup>-1</sup>) (to generate bigger particles) in order to characterize the particle wall-loss rate

constants a second time. Details about the experimental procedure for these aging experiments can

165 be found in Wang et al. (2017).

## 2.2 Particle wall-loss rate constant measurements in a 1.5 m<sup>3</sup> Teflon reactor

We performed additional particle wall-loss measurements in a dual smog chamber system consisting of a set of two identical Teflon chambers (1.5 m<sup>3</sup> each). The two pillow-shaped chambers are mounted on metal frames with wheels on the bottom for portability. Details about the portable dual-chamber system can be found in Kaltsonoudis et al. (2018). The system was tested inside the laboratory in the present study. We used both ammonium sulfate and PSL particles (700 nm, Duke Scientific Corporation) for measurements in these chambers.





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## 3. Data analysis

#### 180 **3.1 Particle loss rate constants**

The particle loss rate constants derived from methods accounting for the coagulation of particles are denoted as  $k_c$  in the rest of the paper, while the apparent particle loss rate constants neglecting the role of coagulation as  $k_a$ .

## 185 **3.1.1** The coagulation-corrected particle loss rate constants, $k_c(D_p)$

The coagulation-corrected particle wall-loss rate constants were derived based on the model used by Nah et al. (2017). The model assumes that only two processes take place: particle wall loss and coagulation. With a given particle number size distribution at a specific time step, the model predicts how the distribution evolves at the next step assuming coagulation is the only process based on the Brownian coagulation kernel in Seinfeld and Pandis (2006). The model attributes the difference between the predicted size distribution and the measured one to particle wall loss. Then the model calculates the instantaneous wall-loss rate constants at each time step for each size. To obtain the coagulation-corrected particle wall-loss rate constant,  $k_c(D_p)$ , the

instantaneous rate constants are averaged over time. The reported uncertainty is calculated 195  $as \sigma_{k_c}/\sqrt{N-1}$  where  $\sigma_{k_c}$  is the standard deviation of  $k_c$  for a certain size bin and N is the total number of time steps used. To minimize the uncertainty of  $k_c$ , we used a time step of 15 min for the averaging of the measurements. Only SMPS measurements from the seed wall-loss periods were used as the inputs for the model.

#### **3.1.2** The apparent particle wall-loss rate constants, $k_a(D_p)$

The apparent particle loss rate constants, denoted as  $k_a$  in this work, were derived from the size-dependent loss rate constant. Details can be found in Wang et al. (2017). This approach uses the SMPS-measured seed particle number size distribution as input, and calculates a first-order loss rate constant for particles of a certain size across all measured sizes. These  $k_a$ 's intrinsically represent the combined loss effect of both particle wall loss and coagulation.

For particles in size bin *i*,  $k_{a,i}$  is found by:

$$\ln[N_i^{sus}(t)] = -k_{a,i}t + Q \tag{5}$$





where  $N_i^{sus}(t)$  is the suspended aerosol number concentration at size bin *i* measured by SMPS and *Q* is an arbitrary constant.

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# 3.2 Size-dependent particle loss correction

Both  $k_c$  and  $k_a$  are size-dependent. The corrected particle number concentration at size bin i,  $N_i^{tot}(t)$ , is calculated by,

$$N_{i}^{tot}(t) = N_{i}^{sus}(t) + k_{a/c,i} \int_{0}^{t} N_{i}^{sus}(t) dt.$$
(6)

215 We can then derive the corrected particle volume concentration of size bin i,  $V_i^{tot}(t)$ .

The organic aerosol mass concentration corrected for wall losses can be then calculated during a seeded experiment using:

$$C_{SOA}^{tot}(t) = (V^{tot}(t) - V_s)\rho_{SOA},\tag{7}$$

where  $V^{tot}(t)$  is the corrected total particle volume concentration summed across all sizes and  $V_s$ is the corrected seed volume concentration.

## 4. Results and discussion

## 4.1 Role of coagulation in particle wall-loss processes

- Fig. 1 shows the apparent (k<sub>a</sub>) and coagulation-corrected (k<sub>c</sub>) particle wall-loss rate
  constants as a function of particle size for the 1.5 m<sup>3</sup> Teflon reactor (Exp. 1) and the 12 m<sup>3</sup> chamber (Exp. 2) after both systems have remained undisturbed in the lab for weeks. According to the aerosol dynamics model, coagulation was a significant loss process in Exp. 1 for particles with diameters smaller than 250 nm and for particles smaller than 150 nm in Exp. 2. In Exp. 1, the apparent loss rate constant for 100 nm particles was 0.5 h<sup>-1</sup>, while the actual rate constant after correcting for coagulation was only 0.2 h<sup>-1</sup>. For 200 nm particles, the corresponding values were 0.3 h<sup>-1</sup> and 0.2 h<sup>-1</sup> respectively. The coagulation effects were minor for particles larger than 250 nm in both cases. Once corrected for coagulation, the particle wall-loss rate constants indicated little size dependence for particles larger than 100 nm in both experiments. The corresponding values were 0.25 h<sup>-1</sup> for the small reactor, and 0.1 h<sup>-1</sup> for the 12 m<sup>3</sup> chamber. The uncertainty of
- the aerosol dynamics model for the larger particles is significantly higher than that of the direct calculation based on Eq. 5. This is due to the reliance of the model on observed small changes of small number concentrations versus the linear regression that uses measured values. We suggest





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using twice the uncertainty of the linear regression as representative of the uncertainty of the rate loss constants of particles larger than 300 nm given the small impact of coagulation on particle concentrations and sizes in this range.

To evaluate the coagulation effect on particle number and volume concentrations, we corrected them for wall loss with both  $k_a(D_p)$  and  $k_c(D_p)$ . The results for the 1.5 m<sup>3</sup> reactor (Exp. 1) are shown in Fig. 2 as an example. To estimate the  $k_a(D_p)$ 's at  $D_p < 50$  nm (and the  $k_c(D_p)$ 's at  $D_p < 70$  nm), we used a linear fit of the  $k_a(D_p)$ 's from 50 to 70 nm (and of the  $k_c(D_p)$ 's from 70 to

- 100 nm) to back extrapolate the  $k_a$ 's at smaller sizes. Coagulation caused the particle number concentration to decrease by 27 % over a 5 h period in this case, but had, as expected, negligible effect on particle volume concentration. Please note that even if the overall effect of coagulation on total particle number is moderate, it is mostly concentrated in the lower end of the size distribution. As a result, the coagulation effect is almost an order of magnitude higher than average
- 250 for the rate constants of particles smaller than 100 nm. In this case there is little difference in the calculated total volume concentration, which is the most important quantity for SOA studies. However, this difference depends in general on the particle size distribution. If a significant part of the volume (or mass) is in particles with diameters less than 200 nm or so, the effect of coagulation will be significant for the corrected particle volume too. Nah et al. (2017) also studied
- the effect of coagulation on corrected SOA volume for the  $\alpha$ -pinene ozonolysis system, and found that coagulation plays minor role in experiments with initial seed surface area of  $<3000 \ \mu m^2 \ cm^{-3}$ while in experiments with high seed surface area (>8000  $\mu m^2 \ cm^{-3}$ ), the SOA can be substantially overestimated if one ignores coagulation. Our results are consistent with their low seed surface area experiments.
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#### 4.2 Particle wall-loss rate constants in the CMU chamber over three years

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Fig. 3 shows the coagulation corrected  $k_c(D_p)$  profiles together with their corresponding uncertainties in the 12 m<sup>3</sup> CMU smog chamber over a span of three years. All these measurements were performed during periods in which the chamber was undisturbed. The rate constants show a monotonic decreasing trend with sharp decrease initially until 100 nm due to diffusion dominating the wall-loss processes. Then the loss rate constants gradually decrease until 300 nm, after which they stay almost constant until the end of the measured size range. Using the  $k_c(D_p)$  determined in 2017 as an example,  $k_c$  decreased from 0.3 h<sup>-1</sup> at 50 nm, to 0.14 h<sup>-1</sup> at 100 nm, then gradually to





0.05 h<sup>-1</sup> at 300 nm and stayed constant until approximately 500 nm. The k<sub>c</sub>(D<sub>p</sub>) profiles over the
past three years stayed fairly consistent with values equal to 0.32±0.03 h<sup>-1</sup> at 50 nm, 0.16±0.03 h<sup>-1</sup> at 100 nm, 0.10±0.02 h<sup>-1</sup> at 200 nm and 0.07±0.01 h<sup>-1</sup> at 300 nm. The behavior of the chamber after disturbances (e.g., repairs, upgrades) will be discussed in a subsequent section.

# 4.3 Applying different particle wall-loss correction methods to SOA aging experiments

The measured particle volume concentration time series of a typical aging experiment (Exp. 275 3) of  $\alpha$ -pinene ozonolysis products in the 12 m<sup>3</sup> CMU Teflon chamber is shown in Fig. 4. In this experiment there were three separate stages. We injected ammonium sulfate seeds both at the beginning (t = -4.5 h) of the experiment and at t=3.5 h. At t=0, ozone was introduced into the chamber to react with  $\alpha$ -pinene producing SOA in the dark. HONO was bubbled into the chamber 280 twice at t=0.5 h and 1.2 h to produce OH radicals under UV illumination, leading to a second round of reactions in the system. The size-dependent  $k_a(D_p)$  and  $k_c(D_p)$  derived from the initial 4.5 h seed loss period differed by up to  $0.2 h^{-1}$  for particles smaller than 100 nm and were practically the same in absolute values for particles larger than 100 nm (Fig. 4c). The size-independent loss rate constants  $k_1 - k_3$  were derived during the three periods when condensation/evaporation was minimal. A value of  $k_1 = 0.05 h^{-1} (R^2 = 1)$  was derived from volume concentration 285 measurements from t=-4.5 to 0 h according to Eq. 2,  $k_2 = 0.04 h^{-1} (R^2 = 0.8)$  from t=2 to 3.4 h and  $k_3 = 0.03 h^{-1} (R^2 = 0.9)$  from t=4.7 to 8.4 h. One major contributor to the difference in these three k's is the size dependence of the particle wall-loss rate constants.  $k_2$  was calculated from the period after three rounds of condensation ( $\alpha$ -pinene ozonolysis and two doses of HONO). The particle size distribution shifted to larger sizes (Fig. 4b) and thus resulted in a smaller value 290

compared to  $k_1$ .  $k_3$  was derived from the final seed loss period when relatively large seed particles were present due to the higher concentration of the atomized ammonium sulfate solution.

The particle wall-loss corrected SOA mass concentration ( $\rho = 1.4 \ \mu g \ m^{-3}$ ) time series based on SMPS measurements using both the size-independent  $k_1 \cdot k_3$  and the size-dependent  $k_a(D_p)$  and  $k_c(D_p)$  for Exp. 3 are shown in Fig. 5. Applying  $k_1 \cdot k_3$  to Eq. 3 resulted in corrected SOA mass concentration differing up to 20%. To estimate the  $k(D_p)$ 's at  $D_p < 50 \ nm$  and  $D_p > 300 \ nm$ , we used a linear fit of the  $k(D_p)$ 's from 50 to 70 nm to back extrapolate the k's at smaller sizes and assumed a constant k value equal to that at 300 nm for particles larger than 300 nm (Fig. S2). We corrected for total particle number concentration applying the size-dependent loss rates to Eq. 6, and then





calculated the corrected SOA mass concentration using Eq. 7. The k<sub>a</sub>(D<sub>p</sub>)- and the k<sub>c</sub>(D<sub>p</sub>)-corrected SOA mass concentration time series were practically the same for this experiment, because the majority of the formed SOA mass condensed on particles with diameters exceeding 100 nm. If one is interested in the total produced SOA after 3.5 hours the differences among the results of the different corrections are 20% or less. If one is interested in the SOA produced during the aging phases the estimates vary by 25-30%.

## 4.4 Effect of size-dependent wall loss on organic to sulfate ratio

Fig. 6 shows the AMS-measured organic to sulfate ratio (OA/Sulfate) for Exp. 3. In the beginning, the ratio increased to 1.2 at *t*=0.6 h due to the first generation of SOA formation. It then
stayed practically constant until OH was introduced into the chamber at *t*=0.9 h. The second-generation of SOA formation led to an increase of the ratio to 1.6 at *t*=1.1 h. The ratio decreased gradually to 1.5 until the second introduction of HONO. This decrease could be explained as a loss of SOA due to photodegradation or other chemical processes such as SOA evaporation driven by organic-vapor uptake by the walls (Bian et al., 2015). Another explanation for the decreasing trend

- of OA/Sulfate during this period is the size dependence of the particle wall-loss rates. Particles of smaller sizes with higher organic to sulfate ratios can be lost to the walls at a faster rate, thus causing the OA/Sulfate to decrease during periods when wall loss is the dominant process in the chamber. The strong size dependence of the OA/Sulfate ratio in this experiment is indicated in Fig. 7. The organic mass distribution peaked at an aerodynamic vacuum diameter (*D*<sub>va</sub>) equal to around 300 nm, while the sulfate one at 450 nm. This indicates that the majority of the organic vapors condensed onto smaller particles with a higher surface to volume ratio. Fig. 7b shows the OA/Sulfate derived from the AMS-measured mass distribution (averaged from *t*=1.1 to 3.5 h) as a function of the particle vacuum aerodynamic diameter. For particles with *D*<sub>va</sub> from 200 to 300 nm, the ratio dropped dramatically from 10 to 3. It then decreased gradually and stabilized at 1
- 325 from  $D_{va}$ =300 to 1000 nm.

To further analyze the effect of size-dependent wall loss on OA/Sulfate, we adopted the method suggested in Wang et al. (2017). This approach allows the estimation of mass-weighted wall-loss rate constants for both species,  $\bar{k}_{SO_4}$  and  $\bar{k}_{OA}$ , by discretizing the AMS-measured mass distribution in the diameter space and assigning the corresponding  $k_c(D_p)$ . For periods during the experiment when particle wall-loss is the only process, the loss-corrected OA/Sulfate can be





estimated as:  $(OA/Sulfate)_m(t)\exp(\bar{k}_{SO_4} - \bar{k}_{OA})t$ , where  $(OA/Sulfate)_m(t)$  is the measured OA/Sulfate. For Exp. 3 in this work, we discretized the AMS-measured mass distribution (averaged from t=1.2 to 1.7 h) into 10 diameter bins and found  $\bar{k}_{Org} = 0.06 h^{-1}$  and  $\bar{k}_{SO_4} = 0.05 h^{-1}$ . The particle wall-loss corrected OA/Sulfate for the chosen time period is shown in the inset of Fig. 6. The loss-corrected ratio remained relatively constant, indicating that the decrease observed in the measured OA/Sulfate was caused by the size-dependent particle wall-loss process coupled with the different size distributions of the organics and sulfate.

# 4.5 Time dependence of particle wall-loss rates during an experiment

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When the CMU chamber is undisturbed the wall loss rate constant is around 0.1 h<sup>-1</sup> for particles larger than 100 nm. However, friction with the Teflon walls induced by small repairs (addition of a sampling line, replacement of lights, etc.) around the chamber can increase the loss rates dramatically and the effects can last for weeks. During these periods the size-dependent coagulation-corrected particle wall-loss rate constants,  $k_c(D_p)$ , can change significantly during the course of an experiment. The results of such an experiment in a "disturbed" smog chamber are described below.

The comparison of the two k<sub>c</sub>(D<sub>p</sub>) profiles derived from the initial and the final seed periods for Exp. 4 are shown in Fig. 8, together with the raw and the corrected aerosol volume concentration time series. This is a similar aging experiment of α-pinene ozonolysis products as
Exp. 3, but with only one HONO injection. Before *t*=0, ammonium sulfate seed particles were lost to chamber walls. At *t*=0, ozone was added into the chamber to react with α-pinene. The aerosol volume increased due to condensation of the first-generation products. At *t*=2.5h, HONO was introduced into the chamber and OH were produced at *t*=3 h under UV illumination. The aerosol volume increased again due to additional SOA formation from the second-generation oxidation.

- At *t*=4 h, we injected ammonium sulfate particles into the chamber to characterize the particle wall loss rates for a second time. The final  $k_c$ 's were statistically higher than their initial counterparts at every size, and both sets of  $k_c$ 's were higher than their usual values in the chamber (Fig. 3). Comparing the initial  $k_c$ 's with the averaged usual values under undisturbed chamber conditions, the initial  $k_c$  was 0.33 h<sup>-1</sup> as compared to the usual 0.16 h<sup>-1</sup> at 100 nm, 0.21 h<sup>-1</sup> compared to 0.10
- 360  $h^{-1}$  at 200 nm, and 0.15  $h^{-1}$  compared to 0.07  $h^{-1}$  at 300 nm. The final  $k_c(D_p)$ -corrected volume concentration was higher than the one corrected using the initial  $k_c(D_p)$  by 37 % at *t*=4 h. The time





dependence of  $k_c(D_p)$  during the course of this experiment introduced a 40% or so uncertainty in the corrected aerosol mass or volume concentration.

We define the chamber conditions under which these abnormally high loss rates and 365 exacerbated time dependence of  $k_c(D_p)$  were observed as "disturbed". The  $k_c(D_p)$  profiles shown in Fig. 3 were under "undisturbed" chamber conditions. Since electrostatic forces start to dominate the wall-loss process when particles are usually larger than 100 nm (McMurry and Rader, 1985), we postulate that excess electrostatic forces within the chamber are most likely the cause of the "disturbed" conditions. Friction created with the Teflon walls was found to be a major contributor 370 to the exacerbated electrostatic forces and the "disturbed" chamber conditions.

Fig. 9 shows the  $k_c(D_p)$  profiles measured over a span of five months after some major maintenance work (Jan. 2016) in the room where the chamber is suspended. During the one-week maintenance, friction with Teflon walls was created by partially deflating the chamber, moving and touching it repeatedly. The measured  $k_c(D_p)$  profile changed drastically in shape for days after.

The 16-day post-maintenance  $k_c(D_p)$  profile presented an increasing trend from 75 nm to 300 nm, with particles bigger than 200 nm getting lost at a rate 3-4 times faster than before. Once we noticed the abnormally high particle loss rates in the chamber, we refrained from being in any form of contact with the chamber walls. The chamber was left suspended and full during those five months. Records of experiments performed in the chamber during that time support the previous statements.

About a month later, the  $k_c$ 's recovered to the decreasing trend, but were in general high as compared to their pre-maintenance counterparts with values > 0.2 h<sup>-1</sup> at 300 nm. Three months after the maintenance, particles smaller than 100 nm recovered to its pre-maintenance values while particles bigger than 150 nm still had loss rate constants up to 0.1 h<sup>-1</sup> higher than before. Five months after, the  $k_c(D_p)$ 's made a full recovery, with values decreased further to 0.13 h<sup>-1</sup> at 100

- nm, 0.09 h<sup>-1</sup> at 200 nm and 0.06 h<sup>-1</sup> at 300 nm. During the 5 months, the chamber was left fully inflated, stationary and suspended in the room. Only steps necessary for an experiment (overnight flushing, injection flow etc.) were taken. Exp. 4 was performed a month after the major maintenance when  $k_c(D_p)$  was still in recovery, and thus the exacerbated electrostatic forces within the chamber likely played a major role in the extra time sensitivity of the  $k_c(D_p)$ 's in Exp. 4.
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To test whether certain steps during an experiment cause changes in the particle loss rates, we explored potential impact on  $k_c(D_p)$  of turning on the UV lights, injecting HONO and overnight flushing individually in separate seed experiments. Experiments 5-8 were designed to test each of





these factors individually. These experiments were performed about 3 months after the maintenance when particle wall loss rates have almost recovered to its pre-maintenance values, indicating the chamber has mostly recovered to "undisturbed" conditions. Turning on the UV 395 lights inside the room where the chamber is suspended can cause changes in the air circulation around the chamber walls, thus affecting the turbulence. Carrying HONO into the chamber with a clean air flow at a rate of ~ 5 L min<sup>-1</sup> for 20 mins may potentially impact the turbulence within the chamber. Though cleaning the chamber with overnight flushing may not have a direct impact of 400  $k_c$  during the day of an experiment, flow rates higher than 100 L min<sup>-1</sup> into the chamber may well have an effect. The results of Experiments 5-8 are shown in Fig. 10 and none of the aforementioned processes had evident impact on  $k_c(D_p)$ . t-test results indicated that of the  $k_c(D_p)$ profiles derived before and after each factor were statistically the same. We thus conclude that the usual steps taken during a typical SOA aging experiment do not have a significant impact on  $k_c$  if the chamber is in its undisturbed state. However, when the chamber has been disturbed and the 405 losses are already high they also become sensitive to routine changes in the experimental conditions.

#### 4.6 Teflon chamber maintenance and operating procedure of chamber experiments

410 Routine seed experiments appear to be necessary for the quantification of the particle loss rates in Teflon chambers. Any deviation in the particle wall-loss rate constants from the usual values can be a sign of "disturbed" chamber conditions, which may result in higher particle loss rates and time sensitivity of  $k_c(D_p)$  during an experiment. As discussed above, friction with the chamber walls can introduce excess electrostatic forces within the chamber and thus introduce 415 significant uncertainty in the particle loss rates. In order to maintain minimum particle loss in Teflon chambers, one should refrain from creating any type of friction with the chamber walls such as touching the walls or having the walls rubbing against each other. When transporting the chambers such the dual-chamber system, it is ideal to leave them full or at least half-filled with air and fixed onto a rigid structure that can be packed during the transportation. This can minimize 420 potential friction and shorten the recovery time for the particle loss rates. Use of metal gloves is recommended when it is absolutely necessary to touch the chamber.

When the chamber is in a "disturbed" state, the  $k_c(D_p)$ 's can vary with time during the course of an experiment. It is thus vital in these cases to include two seed loss periods, one at the





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beginning and the other at the end, for each SOA experiment to characterize the  $k_c(D_p)$ , especially if the chambers are recently subjected to friction. When performing SOA experiments in a Teflon chamber, we recommend the following operating procedure:

1. injection of seeds and initial  $k_c(D_p)$  characterization for 3-4 hours;

2. perform necessary steps for the SOA experiment and wait until the mass loadings in the chamber become low;

430 3. if the losses in step 1 are high, a second injection and another 3-4 hours of measurements for final  $k_c(D_p)$  characterization are necessary.

# 5. Conclusions

- Particle number losses in chamber experiments due to coagulation can be significant for small particles (< 150 nm under conditions in this work). It is thus important to correct for this coagulation effect when calculating the particle wall-loss rate constants especially for experiments in which the behavior of the nanoparticles is important (e.g., when they carry a significant fraction of the total particle mass).
- The Teflon chamber used in this study appeared to operate in two different states: an 440 undisturbed and a disturbed one. The chamber entered the second state after either major repairs or even after smaller changes (e.g., addition of a sampling line or replacement of a few lights) probably because it was touched by the researchers or because friction was created during the repairs causing charge build-up. The disturbed state could last for several weeks or even months. In this state the particle loss rates increased by more than a factor of 3-4 and their size dependence 445 became more pronounced. There was significant variation of the losses from experiment to experiment and even within the same experiment. In the undisturbed state, the loss rate constant was less than 0.1 h<sup>-1</sup> for particles larger than approximately 200 nm and was constant from experiment to experiment. Under these conditions the cleaning of the chamber, turning on the chamber lights, injection of reactants, etc., did not have a statistically significant impact on the loss 450 rate constants.
  - The accuracy of the use of size-independent loss rate constants for the correction of the experimental results depends on the state of the chamber and the size distribution of the aerosol during the experiment. If the aerosol volume is dominated by particles larger than 200 nm and the chamber is undisturbed, the corresponding results can be quite accurate under conditions in this





455 work. However, if the chamber has been disturbed or if the size distribution during some phase of the experiment includes a lot of ultrafine particles, significant errors can be introduced.

The correction based on the OA/Sulfate ratio can also introduce uncertainties under at least some conditions. The SOA mass distribution is usually shifted towards the smaller particles compared to that of the sulfate seeds. As a result, the losses of sulfate can be different than those of the organics. The sign and the magnitude of the error depends on both the differences between the two size distributions and also the size dependence of the losses in this specific experiment. A method to correct the OA/Sulfate ratio for these effects has been developed. In one of the experiment, this explains the apparent decreases of the ratio from 1.0 to 0.9 in less than one hour. The errors appear to be of the order of 20% or less, but may lead to problematic conclusions about 465 potential processes taking place at longer timescales (e.g., photolysis and loss of SOA).

Due to the above complexities, seed experiments for testing the particle loss rates in Teflon chambers should be performed regularly, probable before each experiment. If the rates are high a second measurement of the losses should be performed after the end of the experiment to constrain any potential changes. The use of size-dependent corrections accounting for coagulation effects is

470 the preferred approach even if in a number of experiments when the chamber is undisturbed the errors introduced by neglecting the size dependence or the role of coagulation could be small. However, this depends a lot on the evolution of the aerosol volume distribution during the experiment and especially on the importance of the particles smaller than 200 nm or so for the objectives of the experiment.

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Table 1: List of experiments and experimental conditions

Exp.	Chamber volume	Туре	Number of seed	Initial seed number/surface/volume concentration <sup>a</sup>			Notes
	(111)		loss periods	(cm <sup>-3</sup> )	$(\mu m^2 cm^{-3})$	(µm <sup>3</sup> cm <sup>-3</sup> )	
1	1.5	Seed	1	13×10 <sup>4</sup>	19500	1890	Regular seed wall-loss exp.
2	12	Seed	1	3.1×10 <sup>4</sup>	1630	53	Regular seed wall-loss exp.
3	12	Seed+ SOA	2	1.8×10 <sup>4</sup>	1076	39	Aging exp. of α-pinene ozonolysis
4	12	Seed+ SOA	2	2.8×10 <sup>4</sup>	1390	42	Aging exp. of α-pinene ozonolysis
5	12	Seed	2	2.3×10 <sup>4</sup>	1870	75	UV lights on for 3 h before final seed
6	12	Seed	2	5.2×10 <sup>4</sup>	4600	200	HONO addition (5 L min <sup>-1</sup> for 20 min) before final seed
7	12	Seed	1	2.6×10 <sup>4</sup>	1270	40	Regular seed wall-loss exp. with overnight flushing after
8	12	Seed	1	3.4×10 <sup>4</sup>	1330	1330	Regular seed wall-loss experiment ran on the day after Exp. 7
9	12	Seed+ SOA	2	2.2×10 <sup>4</sup>	910	910	α-pinene ozonolysis

<sup>a</sup>Maximum concentration after initial seed injection (before wall loss of these seed particles).







**Figure 1:** The apparent (red symbols) and coagulation-corrected (black symbols) particle wallloss rate constants as a function of particle size for **a**) the 1.5 m<sup>3</sup> Teflon reactor and **b**) the 12 m<sup>3</sup> CMU smog chamber after the two systems have been left undisturbed in the lab for weeks. The particle loss rate constants were derived based on SMPS measurements from Exp. 1 and Exp. 2. Only  $k_a$ 's with an R<sup>2</sup> > 0.5 are shown. The error bars correspond to one standard deviation. The grey area is the uncertainty associated with  $k_c$ .

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**Figure 2:** The SMPS-measured (black symbols) and the particle loss corrected **a**) number and **b**) volume concentration using the  $k_a(D_p)$  profile (red symbols) and the  $k_c(D_p)$  profile (blue symbols) for Exp. 1.

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**Figure 3:** The  $k_c(D_p)$  profiles for the 12 m<sup>3</sup> CMU Teflon chamber over a span of three years. The particle wall-loss rate constants were derived based on SMPS measurements from experiments with only ammonium sulfate particles.

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**Figure 4: a)** The SMPS-measured particle volume concentration time series for an aging experiment (Exp. 3) with 3 colored periods used to derive the corresponding size-independent particle wall-loss rate constants,  $k_1$ - $k_3$  (Eq. 2). The grey area indicates that the chamber was dark. The dashed lines mark the beginning and the end of bubbling HONO into the chamber twice; **b**) the averaged particle volume size distribution over the 3 periods used to develop  $k_1$ - $k_3$  based on the SMPS measurement for Exp. 3; **c**) the size-dependent particle wall-loss rate constants determined from SMPS-measured particle number concentration for Exp. 3. Only  $k_a$ 's (red symbols) with an  $R^2 > 0.5$  are shown. The error bars correspond to plus/minus one standard deviation. The grey area is the uncertainty associated with  $k_c$  (black symbols).







Figure 5: Particle loss corrected SOA mass concentration (ρ<sub>SOA</sub> = 1.4 μg m<sup>-3</sup>) time series based
on SMPS measurements using the size-independent k's (open symbols) and the size-dependent k(D<sub>p</sub>)'s (solid symbols) for Exp. 3. k<sub>1</sub> - k<sub>3</sub> were derived from the total mass concentration-based method (Eq. 2) when wall loss was the only process (t<sub>1</sub>= -4.5-0h; t<sub>2</sub>= 2-3.4h; t<sub>3</sub>= 4.7-8.4h). The k<sub>a</sub>(D<sub>p</sub>) and the k<sub>c</sub>(D<sub>p</sub>) profiles were derived from the two models based on the SMPS-measured number concentration of the seed wall-loss periods. The shaded area indicates that the chamber
was dark. The dashed lines mark the beginning and the end of bubbling HONO into the chamber.







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**Figure 6:** The organic to sulfate ratio time series derived from AMS measurements for Exp. 3 (data after the second HONO introduction is not shown). The inset is a blow-up of the OA/Sulfate from its maximum until the second HONO introduction. The black symbols are the size dependence corrected OA/Sulfate during that half hour. The shaded area indicates that the chamber was dark. The dashed lines mark the beginning and the end of the first HONO injection into the chamber.







Figure 7: a) The AMS-measured organic (green) and sulfate (red) mass distribution for Exp. 3; b)
the dependence of the AMS-derived organic to sulfate ratio on particle vacuum aerodynamic diameter. The results are based on particle time-of-flight (PToF) data averaged over ~2.5 h (t=1.1-3.5 h).







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**Figure 8: a)** The SMPS-measured (black symbols), the initial  $k_c(D_p)$ -corrected (red symbols) and the final  $k_c(D_p)$ -corrected (blue symbols) particle volume concentration time series for an aging experiment (Exp. 4), together with **b**) the initial (red symbols) and the final (blue symbols)  $k_c(D_p)$ profiles. The colored area are the uncertainties associated with the corresponding  $k_c(D_p)$ . The grey area indicates that the chamber was dark. The two dashed lines mark the beginning and the end of HONO addition into the chamber. Ammonium sulfate seed particles were injected into the chamber at *t*=4 h.







**Figure 9:** The coagulation-corrected particle wall-loss rate constant,  $k_c$ , at each diameter derived from experiments with only ammonium sulfate particles in the 12 m<sup>3</sup> CMU Teflon chamber before and after some major maintenance in the room where the chamber is suspended. The chamber was partially deflated and its walls subjected to friction repeatedly during the maintenance.







**Figure 10:** The coagulation-corrected particle wall-loss rate constant,  $k_c$ , at each diameter for a) Exp. 5, b) Exp. 6, c) Exp. 7 and Exp. 8. The uncertainties associated with the corresponding  $k_c(D_p)$  are either expressed as the grey area or the red error bars.