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Gravimetrically-Prepared Carbon Dioxide Standards in Support of Atmospheric Research 1 2 3 <sup>1</sup>Bradley D. Hall\*, <sup>1,2</sup>Andrew M. Crotwell, <sup>1,2</sup>Benjamin R. Miller, 4 <sup>3</sup>Michael Schibig, and <sup>1</sup>James W. Elkins 5 6 <sup>1</sup>National Oceanic and Atmospheric Administration, Global Monitoring Division, 325 Broadway, 7 Boulder, Colorado 80305, USA 8 <sup>2</sup>University of Colorado, Cooperative Institute for Research in Environmental Science, Boulder, 9 Colorado 80309, USA <sup>3</sup>Climate and Environmental Physics, Physics Institute and Oeschger Centre for Climate Change 10 11 Research, University of Bern, Switzerland 12 13 \*corresponding author: Bradley.Hall@noaa.gov 14 15 16 Abstract 17 18 We have explored a one-step method for gravimetric preparation of CO<sub>2</sub>-in-air standards in 19 aluminum cylinders. We consider both adsorption to stainless steel surfaces used in the 20 transfer of highly-pure CO2, and adsorption of CO2 to cylinder walls. We demonstrate that CO2-21 in-air standards can be prepared with relatively low uncertainty (~0.04%, ~95% Confidence 22 Level) by introducing aliquots whose masses are know to high precision, and by using well-23 characterized cylinders. Five gravimetric standards, prepared over the nominal range 350 to 24 490 μmol mol<sup>-1</sup> (parts per million, ppm), showed excellent internal consistency, with residuals from a linear fit equal to 0.05 ppm. This work compliments efforts to maintain the World 25 Meteorological Organization, Global Atmosphere Watch, mole fraction scale for carbon dioxide, 26 27 widely used for atmospheric monitoring. This gravimetric technique could be extended to other 28 atmospheric trace gases, depending on the vapor pressure of the gas. 29 30 31 Introduction 32 33 Numerous laboratories make routine measurements of atmospheric carbon dioxide to better 34 understand its sources, sinks, and temporal variability. These measurements are typically 35 calibrated using high-pressure gas standards containing CO2 in air (typically natural air with

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2 absolute methods, such as manometry (Keeling et al., 1986; Zhao and Tans, 2006) and 3 gravimetry (Machida et al., 2011;Rhoderick et al., 2016;Brewer et al., 2014), which provide 4 traceability to the SI. The World Meteorological Organization (WMO), Global Atmosphere 5 Watch (GAW) initially adopted the Scripps Institution of Oceanography scale (Keeling et al., 6 1986) and subsequently the National Oceanic and Atmospheric Administration (NOAA) scale 7 (Zhao et al., 1997), both of which are based on repeated manometric measurements of a suite 8 of primary standards, for WMO-affiliated monitoring networks. The WMO-GAW scale has been 9 updated over the years as understanding has improved and measurement records of primary standards have increased (Keeling et al., 2002; Keeling et al., 1986; Zhao and Tans, 2006). 10 11 12 Determining the absolute amount of CO<sub>2</sub> in air is a challenge for both gravimetric and 13 manometric methods, particularly since the relative uncertainties must be very small (~0.01% 14 1-sigma) in order to assess changes (drift) in cylinders over many years. Long-term monitoring of atmospheric CO<sub>2</sub> requires a stable reference, sufficient to identify small atmospheric 15 gradients (of order  $0.1 \,\mu\text{mol mol}^{-1}$ , or  $0.1 \,\text{ppm}$ , in the remote troposphere). Hereafter we will 16 17 use ppm (parts per million) for µmol mol<sup>-1</sup>. Both methods can be influenced by the adsorption 18 of CO<sub>2</sub> to surfaces. There is increasing evidence that CO<sub>2</sub> can adsorb to the internal surfaces of 19 cylinders and desorb with decreasing pressure (Langenfelds et al., 1996; Miller et al., 20 2015; Leuenberger et al., 2015; Brewer et al., 2018; Schibig et al., 2018). This impacts both the 21 gravimetrically-assigned mole fraction and the mole fraction of CO<sub>2</sub> in air withdrawn from 22 cylinders over time. Further, since cylinder characteristics may differ among cylinder 23 manufacturers, understanding the behavior of CO<sub>2</sub> in cylinders is critical to maintaining stable 24 scales over time. 25 26 The gravimetric technique can employ multiple steps, in which the target gas (CO<sub>2</sub> in this case) 27 is diluted to the desired amount fraction. For example, Brewer et al. (2014) first prepared 28 standards with mole fractions of a few percent, then made dilutions of those to the range 29 needed for ambient monitoring (~400 ppm). Others have opted to dilute CO₂ to ppm levels in

assigned CO<sub>2</sub> mole fractions), traceable to primary standards prepared or analyzed using

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one step (Machida et al., 2011). Matrix gases can also be added in different ways: CO2 can be 1 2 mixed with individual gases (N2, O2, Ar) to form an air-like matrix, or CO2 can be added to 3 natural air from which the CO<sub>2</sub> has been removed. Methods of targeting stable isotopes of CO<sub>2</sub> 4 (e.g. <sup>13</sup>C-CO<sub>2</sub>) to better match natural abundances have also been explored (Brewer et al., 5 2014). 6 7 Here we describe one-step preparation of CO<sub>2</sub>-in-air compressed gas standards in aluminum 8 cylinders. We used information gained from recent decanting experiments (Schibig et al., 2018) 9 to correct for CO<sub>2</sub> adsorption to the cylinder walls. This work was undertaken to support NOAA 10 manometric efforts and learn more about the behavior of CO<sub>2</sub> in aluminum cylinders. 11 12 **Experimental Methods** 13 14 Standards were prepared in 29.5-L Luxfer aluminum cylinders (Scott Marrin, Inc. Riverside, CA), 15 with brass, packless valves (Ceoduex). We chose these cylinders for two reasons. First, we 16 wanted to perform the dilutions in one step, and therefore needed relatively large cylinders. 17 Second, we wanted to use cylinders that were well-characterized. We have considerable 18 experience with CO2-in-air in this type of cylinder. Specific to this work, all cylinders used were 19 filled with natural air and decanted several times for CO2 adsorption studies (Schibig et al., 20 2018) prior to being used for gravimetric standards described here. 21 22 For this gravimetric work, each cylinder was evacuated to ~30 mtorr (4 Pa) and weighed on a 23 mass comparator (Sartorius CCE40K3) relative to a control cylinder of similar mass and volume. The mass comparator was calibrated using a 10 kg mass (Troemner), and linearity over the 24 25 working range was confirmed by adding a 5 kg mass (Mettler Toledo) to the reference cylinder. 26 We then added ~50 psi (0.34 MPa) natural air containing 402 or 408 ppm CO<sub>2</sub> determined by 27 analysis (WMO X2007 scale). Cylinders were then vented, partially evacuated to  $\sim$  400 torr (53 28 kPa), and weighed. The mass of residual air along with the mole fraction of CO<sub>2</sub> were used to 29 calculate the initial mass of CO<sub>2</sub> in the cylinder. We did not evacuate the cylinders further

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because CO<sub>2</sub> adsorption studies (Schibig et al., 2018) were performed at pressures ranging from 1 2 0.1-13.8 MPa. The Schibig et al. (2018) work provided a means to determine the amount of CO<sub>2</sub> 3 adsorbed to cylinder walls, and we wanted to perform the gravimetric addition with a small 4 amount of residual CO2 in the cylinders, consistent with that work. For the standards presented 5 here, the initial CO<sub>2</sub> in the cylinder corresponds to < 0.8% of the total CO<sub>2</sub>, and so the 6 uncertainty associated with the mole fraction of initial CO2, derived from an independent CO2 7 calibration (Zhao and Tans, 2006), makes a negligible contribution to the total uncertainty 8 (Table 1). The majority of the uncertainty in the mass of CO<sub>2</sub> originally in the cylinder results 9 from uncertainty in the mass determination of the residual air. Nevertheless, we include a standard uncertainty of 0.025% on the NOAA X2007 CO<sub>2</sub> scale 10 (https://www.esrl.noaa.gov/gmd/ccl/ccl\_uncertainties\_co2.html). 11 12 13 An initial aliquot of high-purity CO<sub>2</sub> was added to an evacuated 50-mL stainless steel container 14 with a single metal bellows valve (Swagelok, model SS-4H) (pressure rated to 1000 psi, or 6.90 15 MPa, at 37 °C). After CO<sub>2</sub> was loaded into the 50-mL container at the desired pressure, it was 16 cryogenically transferred to a 5-mL stainless steel container, also with a metal bellows valve 17 (total mass ~150g) that had been evacuated and weighed previously. The CO₂ was cryogenically 18 purified by freezing at -197 °C and pumping off non-condensible gases. We estimate the purity 19 of the CO<sub>2</sub> source at 99.994% and that of the cryogenically-purified CO<sub>2</sub> aliquots at 99.997 ± 20 0.002% (Table 2). In this smaller volume, both liquid and vapor phases of CO<sub>2</sub> would be present 21 at room temperature (18 °C in this case). Note that the vapor pressure of CO2 at 18 °C is ~795 22 psi (5.48 MPa), and that our 5-mL container and valve was rated to 1000 psi (6.89 MPa). We 23 employed this secondary transfer to a smaller container so that we could weigh ~1.5g CO₂ on a balance with 0.01mg readability (Mettler Toledo AT201, 200g capacity). The 50-mL container 24 25 used in the first step is too large to be weighed on the AT-201. This is an important aspect of 26 this work. Without this secondary step, our uncertainties would have been about a factor of 10 27 larger. The mass of CO<sub>2</sub> in each 5-mL aliquot was determined by weighing the 5-mL container

relative to a control object of similar mass and density (sequence ABABA....). The AT-201 was

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calibrated using internal weights, and span-checked by adding a 2.0000g mass to the 5-mL 1 2 container. 3 4 Each purified CO<sub>2</sub> aliquot was transferred from the 5-mL container to a partially-evacuated 5 cylinder on a stainless steel vacuum manifold using a pressurization/expansion method 6 (Dlugokencky et al., 2005). The cylinder was connected to the vacuum manifold using a 1/8" OD 7 AT-steel transfer line. AT-steel, also known as "activity tested steel" (Grace Discovery Science, 8 Columbia, MD) is treated using vapor deposition to improve surface inertness. In initial tests we 9 found that AT-steel performed better than other types of stainless steel, but in subsequent tests both 1/8" O.D. stainless steel and 1/8" O.D. AT-steel performed similarly (see Results and 10 11 Discussion). 12 13 To transfer the aliquot to the cylinder, the manifold and transfer line were pre-heated to ~60 °C 14 and evacuated to 5 mtorr. In quick succession, the cylinder valve was opened and the valve on 15 the 5-mL container was opened allowing CO<sub>2</sub> to expand into the cylinder. The expansion of CO<sub>2</sub> 16 resulted in significant cooling of the 5-mL container, so we heated the 5-mL container, 17 manifold, and transfer lines to ~60 °C while alternately pressurizing the 5-mL container to ~200 18 psi (1.38 MPa) with CO<sub>2</sub>-free air (dilution gas) and expanding into the cylinder. After about 20 19 pressurization/expansion cycles, the valve on the 5-mL container was closed and the cylinder 20 pressurized with dilution gas. The 5-mL container was removed from the manifold at a cylinder 21 pressure of ~ 500 psi (3.45 MPa), and the cylinder was then further pressurized to 1000 psi 22 (6.90 MPa) with dilution gas. Dilution gas consisted of scrubbed natural air (Cryogenic Ultra-23 pure grade, Scott Marrin Inc; now Praxair, Los Angeles, CA). This gas was analyzed for CO<sub>2</sub> by non-dispersive infrared analysis (NDIR; Licor Li-7000). Samples of dilution gas were compared to 24 25 a reference of dry nitrogen (99.999%) scrubbed using Ascarite II (Sigma Aldrich). All cylinders of 26 dilution gas contained  $0.01 \pm 0.01$  ppm  $CO_2$ . After cylinders cooled to room temperature, they 27 were weighed on the mass comparator relative to the control cylinder.

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1 The mole fraction of  $CO_2$ ,  $X_{CO2}$ , was calculated using equation (1), where  $n_a$  is the moles of  $CO_2$ 

2 transferred from the 5-mL container,  $n_b$  is the moles of CO<sub>2</sub> initially present in the cylinder,  $n_{air}$ 

3 is the total moles of air, p is the purity coefficient, f is the transfer efficiency,  $X_{CO2,ad}$  is a

4 correction for the amount of CO<sub>2</sub> adsorbed to the cylinder walls ( $X_{CO2,ad}$  < 0) expressed in ppm,

5 and  $X_{CO2,dil}$  is the amount of  $CO_2$  in the dilution air, also expressed in ppm.

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$$X_{CO2} = \frac{pfn_a + n_b}{pfn_a + n_b + n_{air}} + X_{Co2,ad} + X_{CO2,dil}$$
 (1)

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The number of moles of each component was determined from the mass and molecular weight.

11 For CO<sub>2</sub> we used a molecular weight of 44.0096 ± 0.0006 g mol<sup>-1</sup> (consistent with a <sup>13</sup>C-CO<sub>2</sub>

12 content of -29 per mil on the VPDB scale, determined using off-axis integrated cavity output

spectroscopy (Los Gatos Research) traceable to the University of Colorado (INSTAAR) Stable

14 Isotope Laboratory realization of VPDB (Trolier et al., 1996; Tans et al., 2017). For the dilution

15 gas, we used a molecular weight of 28.9621 ± 0.0042 g mol<sup>-1</sup>. The oxygen content of the

16 dilution gas was measured using a paramagnetic method (Beckman, E2) traceable to NIST SRM

17 2659A ( $20.863\% \pm 0.011\% O_2$  in  $N_2$ ). Argon was taken as 0.933% (Sutour et al., 2007), and the

18 noble gases Xe, Ne, and Kr were taken as 0.09, 18.0 and 1.14 ppm, respectively. We assumed

19 100% transfer efficiency with an uncertainty of 0.01% (rectangular distribution) (see Results and

20 Discussion).

21 The mole fraction correction for CO<sub>2</sub> adsorbed to the cylinder walls (X<sub>CO2,ad</sub>) was determined

22 from multiple decanting experiments (Schibig et al., 2018). Briefly, in those experiments,

23 cylinders were filled with dry natural air (~400 ppm), and drained at 0.3 L min<sup>-1</sup> and analyzed

24 continuously for CO<sub>2</sub> by NDIR. These studies showed remarkably consistent results: that the

25 mole fraction of CO<sub>2</sub> exiting the cylinder increased as the cylinder pressure decreased, and that

the data can be described with a Langmuir isotherm (Figure 1). By fitting the data with a

27 Langmuir isotherm as derived by Leuenberger et al. (2015), and integrating the area between

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the Langmuir fit and the initial X<sub>CO2</sub>, we determined the amount of CO<sub>2</sub> that desorbs from the 1 2 walls as the cylinder is vented slowly to near-ambient pressure (Fig 1). The amount of CO2 3 adsorbed to the walls, expressed as a fraction of total CO<sub>2</sub> in the cylinder, was typically about 4 0.004% (Table 3). This corresponds to 0.016 ppm  $CO_2$  at 400 ppm. 5 6 The Schibig et al. (2018) decanting tests reveal substantially less CO2 adsorbed compared to 7 mother/daughter tests (Miller et al., 2015; Brewer et al., 2018), in which half the contents of 8 one cylinder are transferred to an equal size cylinder and the adsorption determined based on 9 the resulting mole fraction difference. From mother/daughter tests on 5.9-L cylinders from Airgas (Riverton, NJ) and 5-L cylinders from Air Products (Vilvoorde, Belgium), Miller et al. 10 (2015) estimated that about 0.02% of the CO<sub>2</sub> was adsorbed to the walls. Brewer et al. (2018) 11 12 performed similar tests on 10-L aluminum cylinders treated with the BOC Spectra Seal process, 13 and found CO<sub>2</sub> adsorption fractions of about 0.05%. 14 In preparation for this work, we performed mother/daughter tests on both 5.9-L and 29.5-L 15 aluminum cylinders (Scott Marrin, Riverside, CA), including cylinders CB11941 and CB11873 16 used in this work. Cylinders CB11941 and CB11873 were filled with natural air, vented, and then 17 evacuated to 5 psia (0.03 MPa). Air from two "mother" cylinders containing natural air was 18 transferred into CB11941 and CB11873. We found that the CO₂ in daughter cylinders CB11941 19 and CB11873 was 0.16-0.19 ppm lower than their respective mothers after transfer (Table 4), 20 similar to the results of Miller et al. (2015) and Brewer et al. (2018). Our tests with 5.9-L 21 cylinders showed ~0.2 ppm differences (not shown). 22 Mother/daughter tests suggest five to ten times more adsorption than that determined from 23 the Schibig et al. (2018) low-flow data. The difference between mother/daughter tests and the 24 low-flow experiments could be related to thermal fractionation. Schibig et al. (2018) performed 25 both low-flow (0.3 L min<sup>-1</sup>) and high-flow (5.0 L min<sup>-1</sup>) tests, and measured significant 26 temperature gradients on the cylinder surfaces during the high-flow tests, but not during the 27 low-flow tests. They concluded that both adsorption and fractionation were occurring at high 28 flow. During our mother/daughter tests, the mother cylinders experienced significant cooling

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during transfer, which could have caused fractionation as cooler air sinks in the center core of

2 the cylinder, with CO<sub>2</sub> preferentially remaining in the mother cylinders. In fact, after

3 transferring half of the gas from a mother cylinder to a respective daughter cylinder, the mole

4 fraction of  $CO_2$  in each mother cylinder increased 0.06  $\pm$  0.01 ppm relative to its value

5 determined prior to transfer (Table 4). Figure 1, which represents a typical low-flow decanting

6 result, suggests that the increase due to desorption from the cylinder walls should be far

7 smaller than 0.06 ppm at 50% of the original cylinder pressure. Because mother/daughter tests

8 appear to be subject to both thermal fractionation and surface adsorption, we estimated  $X_{CO2,ad}$ 

9 exclusively from the Schibig et al. (2018) low-flow data (Table 3).

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## **Results and Discussion**

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13 Five standards were prepared gravimetrically, with  $CO_2$  mole fractions ranging from 357 to 492

ppm, and evaluated by analysis using laser spectroscopy (Tans et al., 2017). Preparation

uncertainties were determined by propagating uncertainties associated with variables in

equation (1) (Table 1), using software available from the National Institute of Standards and

Technology (NIST) (https://www.nist.gov/programs-projects/metrology-software-project). The

two most important factors influencing uncertainty are repeatability associated with weighing

the purified  $CO_2$  aliquot (~25%) and the molecular weight of air (~65%) . For  $MW_{air}$ , the

20 uncertainty is partially limited by our ability to measure  $O_2$  and calibrate the  $O_2$  analyzer.

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22 Each standard was analyzed twice over a period of two weeks. The response was expressed as

the mole fraction of CO<sub>2</sub>, calculated on the WMO X2007 CO2 scale, relative to that of CB11941,

and fit with a linear function (Figure 2, Table 5). We use this relative response because mole

fraction assignments on the X2007 scale account for differences in the abundances of stable

isotopes of CO<sub>2</sub> (mainly <sup>13</sup>C-CO<sub>2</sub>) between the gravimetric standards and secondary standards

used for calibration (Tans et al., 2017). For comparison, we also calculated response based on

the analyzer signal derived from a single  $CO_2$  isotopologue ( $^{16}O^{-12}C^{-16}O$ , 626). Differences in the

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1 residuals from a linear fit were less than 0.005 ppm compared those derived using the response 2 derived from X2007 assignments (Table 5). 3 4 Table 5 shows the best-fit results and residuals (difference between best fit and prepared mole 5 fraction). All standards agree (within expanded uncertainties) with the regression line. The 6 standard deviation of residuals is 0.05 ppm and the largest residual is 0.09 ppm. Since the 7 uncertainty associated with the molecular weight of air is the largest contributor to the total 8 uncertainty, but is common to all standards, it is worth recalculating uncertainty without this 9 contribution in order to assess consistency. Without µ\_MWair, standard uncertainties for each 10 standard are 40-60% lower than when µ\_MWair is included. Recalculating the regression using these lower uncertainties, we find that the residuals do not change appreciably. However, the 11 12 residual for cylinder CB11941 becomes 0.098 ppm, compared to a standard uncertainty of 13 0.046 ppm. Thus, CB11941 is not consistent with the rest of the standards. This may be the 14 result of preparation. Cylinder CB11941 was the first standard prepared, and followed testing 15 that involved injecting high concentrations of CO2 into the manifold and transfer line. It is 16 possible that some residual CO<sub>2</sub> remained in the manifold and transfer line, and was introduced 17 into CB11941 when the manifold and transfer line were heated. The other standards were 18 prepared following several heating cycles, and are less likely to be influenced by any residual 19  $CO_2$ . 20 21 To support our assumption of 100% transfer efficiency, we examined both the potential for 22 adsorption of CO<sub>2</sub> in the manifold and transfer line, and the efficiency of transferring CO<sub>2</sub> from 23 the 5-mL container to a cylinder. We tested the transfer line by flowing air containing 0.1 ppm CO<sub>2</sub> at 0.2 L min<sup>-1</sup> through 1/8" AT-steel tubing to an NDIR analyzer. Then we injected 0.6mL of 24 25 10% CO<sub>2</sub>-in-air into this air stream. After the initial slug of CO<sub>2</sub> was observed and the NDIR 26 signal returned to baseline, we heated the transfer line and measured the additional CO2 27 coming off (Figure 3). Comparing the area of the CO2 released upon heating with that of the 28 main sample injected, we found that our AT-steel transfer line (length 1m) retained about 29 0.04% of CO<sub>2</sub> in the sample. We were able to drive off most of this CO<sub>2</sub> on the first heating

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**Conclusions** 



cycle, with < 0.01% released on subsequent heating. Tests with stainless steel (not AT-steel) 1 2 showed similar results. By heating the lines multiple times and passing a large amount of CO2-3 free air through them, it is unlikely that a significant amount of CO<sub>2</sub> would remain in the 4 manifold or transfer line. 5 6 We tested the transfer efficiency from the 5-mL container by cryogenically moving aliquots of 7 CO<sub>2</sub> from one 5-mL container to another on a vacuum line (using liquid N<sub>2</sub>), without additional 8 flushing, by measuring changes in mass. When both the initial 5-mL container and transfer line 9 were heated, a transfer efficiency of 99.9 ± 0.1% was achieved. Without heating, the same test revealed only 99% efficiency. We expect that repeated pressurization/expansion with CO<sub>2</sub>-free 10 air, in addition to heating, would improve the transfer efficiency of the CO2 aliquot to near 11 12 100%. The relatively good agreement among the four standards prepared after CB11941 supports this assumption. It seems unlikely that this level of agreement could be achieved with 13 14 poor or variable transfer efficiency. 15 16 We also can compare these standards to the WMO X2007 CO<sub>2</sub> scale. The mean ratio, comparing 17 the gravimetrically assigned mole fractions to values assigned on the WMO X2007 scale is 18 1.00052 with standard deviation 0.00017. Thus, the WMO X2007 scale is 0.05% lower than a 19 scale based on these gravimetric standards. However, this difference is not outside the range of 20 uncertainties (~0.05% for WMO X2007 and ~0.033 % for this work, ~95% Confidence Level, or 21 coverage factor k=2). While the <sup>13</sup>C-CO<sub>2</sub> content of these gravimetrically-prepared standards is 22 lower than that of natural air (-29 per mil, compared to about -8 per mil for natural air), and these standards were compared to WMO secondary standards with <sup>13</sup>C-CO<sub>2</sub> at ambient levels 23 during analysis, this introduces negligible bias because the analytical method compensates for 24 25 different isotopic abundances (Tans et al., 2017). Further discussion on differences between the 26 WMO scale and these gravimetric standards will be included in a subsequent publication. 27

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- 1 Five gravimetric CO<sub>2</sub>-in-air standards, prepared at the ppm level in one dilution step, show
- 2 excellent internal consistency. Prepared mole fractions were adjusted for CO<sub>2</sub> expected to
- 3 adsorb to cylinder walls. This correction was determined from low-flow decanting studies, and
- 4 is a factor of 5-10 smaller than that inferred from mother/daughter tests. With improved
- 5 understanding of CO<sub>2</sub> adsorption characteristics, and by introducing condensed-phase aliquots
- of CO<sub>2</sub> into small vessels that can be weighed with sufficient repeatability, CO<sub>2</sub>-in-air standards
- 7 can be prepared with relatively low uncertainty. This work supports parallel efforts to maintain
- 8 the WMO/GAW mole fraction scale for CO<sub>2</sub>.

9 10

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14 15

Supporting Information

Table 1 landscape.docx

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 Table 1: Components and standard uncertainties associated with standard preparation.

Components								
Cylinder	CO <sub>2</sub> _a	$\mu$ _CO $_2$ _a	CO <sub>2</sub> _b	μ_CO <sub>2</sub> _b	Air	μ_Air	n <sub>co2</sub>	ļ
	g	g	g	g	g	g	mol	
CB11873	6.80E-03	2.24E-05	1.36062	0.00008	2515.637	0.033	3.1070E-02	
CB11906	7.28E-03	1.25E-05	1.52917	0.00007	2542.399	0.026	3.4911E-02	
CB11941	1.07E-02	1.25E-05	1.51156	0.00015	2470.262	0.030	3.4589E-02	
CB11976	7.32E-03	1.18E-05	1.66307	0.00011	2445.198	0.014	3.7954E-02	
CB12009	7.72E-03	1.81E-05	1.71751	0.00007	2307.305	0.039	3.9200E-02	
				Adiustmen	ts		Amount Fraction	on-
					••		/ lillount indetic	
Cylinder	n <sub>air</sub>	μ_ n <sub>air</sub>	$X_{CO2,ad}$	μ X <sub>CO2,ad</sub>	X <sub>CO2,di1</sub>	$\mu$ $X_{CO2,dil}$	X <sub>CO2</sub>	
Cylinder	n <sub>air</sub> mol	μ_ n <sub>air</sub> mol	$X_{\mathrm{CO2,ad}} \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ $	•				
Cylinder CB11873	<del></del>	. —		$\mu\_X_{CO2,ad}$	$X_{\text{CO2,dil}}$	$\mu\_X_{CO2,dil}$	$X_{CO2}$	
,	mol	mol	ppm	$\begin{array}{c}\mu\_X_{\text{CO2,ad}}\\\text{ppm}\end{array}$	$\begin{array}{c} X_{\text{CO2,dil}} \\ \text{ppm} \end{array}$	$\underset{\text{ppm}}{\mu\_X_{\text{CO2,dil}}}$	$X_{\rm CO2}$ ppm	
CB11873	mol 86.8596	mol 0.0144	ppm -0.015	$\begin{array}{c} \mu\_X_{\text{CO2,ad}} \\ \text{ppm} \\ 0.001 \end{array}$	$\begin{array}{c} X_{CO2,dil} \\ \text{ppm} \\ 0.01 \end{array}$	$\begin{array}{c} \mu\_X_{CO2,dil} \\ \text{ppm} \\ 0.01 \end{array}$	X <sub>CO2</sub> ppm 357.569	
CB11873 CB11906	mol 86.8596 87.7836	mol 0.0144 0.0146	ppm -0.015 -0.015	$\begin{array}{c} \mu\_X_{\text{CO2,ad}} \\ \text{ppm} \\ 0.001 \\ 0.002 \end{array}$	$\begin{array}{c} X_{CO2,dil} \\ \text{ppm} \\ 0.01 \\ 0.01 \end{array}$	$\begin{array}{c} \mu\_X_{\text{CO2,dil}} \\ \text{ppm} \\ 0.01 \\ 0.01 \end{array}$	$X_{\rm CO2}$ ppm 357.569 397.523	

Note: Entries preceded by "  $\mu_{-}$  " represent standard uncertainties (~68% Confidence Level)

CO<sub>2</sub>\_a = initial mass of CO<sub>2</sub> in cylinder (based on analyzed mole fraction and mass of air)

 $CO_2_b$  = mass of  $CO_2$  aliquot in 5-mL container and added to cylinder

Air = mass of air

 $n_{CO2}$  = total moles of  $CO_2$  (0.99997 purity correction applied)

n<sub>air</sub> = total moles of air

 $X_{CO2,ad}$  = correction applied to account for adsorption to cylinder walls

 $X_{CO2,dil}$  = correction applied to account for  $CO_2$  in the dilution gas

 $X_{CO2}$  = mole fraction of  $CO_2$ 

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## **Table 2**: CO<sub>2</sub> purity assessment.

Component	Fraction	Method
CO <sub>2</sub> (source)	0.99994	
CO₂ (aliquot)*	0.99997	
H₂O	0.00003	electrolytic
CH <sub>4</sub>	0.00002	laser spectroscopy
CO	0.00001	laser spectroscopy
N₂O	2·10 <sup>-8</sup>	GC-ECD
ethyne	3·10 <sup>-9</sup>	GC-GCMS
ethene	2·10 <sup>-9</sup>	GC-GCMS
propane	2·10 <sup>-9</sup>	GC-GCMS
other hydrocarbons	< 2·10 <sup>-8</sup>	GC-GCMS
total non-condensible	0.00002	residual pressure
*		

\*Since the CO<sub>2</sub> aliquots were cryogenically purified to remove non-condensible gases, we calculate the aliquot purity based on H<sub>2</sub>O only. Non-condensibles include e.g., N<sub>2</sub>, O<sub>2</sub>, Ar, H<sub>2</sub>, CO, and CH<sub>4</sub>.

**Table 3**: Summary of CO<sub>2</sub> adsorption experiments. For each cylinder, the test was repeated N times. Adsorbed CO<sub>2</sub> is expressed as a fraction of the total CO<sub>2</sub> in the cylinder.

Cylinder	N	average	std. dev.	
		%	%	
CB11873	5	0.0043%	0.0003%	
CB11941	4	0.0042%	0.0003%	
CB11906	5	0.0038%	0.0004%	
CB11976	5	0.0044%	0.0005%	
CB12009	5	0.0044%	0.0002%	

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**Table 4**: Results of mother/daughter testing on 29.5-L aluminum cylinders. Note: Final pressures do not sum correctly due to thermal differences.

Cylinder	~	Pressure (MPa)		CO <sub>2</sub> (ppm)
CB11795	mother	12.07	initial	401.928
CB11795	mother	5.79	after transfer	401.988
CB11941	daughter	0.03	initial	
CB11941	daughter	5.72	after transfer	401.828
change in mother				0.060
daughter - mother			after transfer	-0.160
CB11088	mother	13.80	initial	408.125
CB11088	mother	6.69	after transfer	408.188
CB11873	daughter	0.03	initial	
CB11873	daughter	6.55	final	407.995
change in mother				0.063
daughter - mother			after transfer	-0.193

**Table 5**: Analysis of  $CO_2$ -in-air standards. "Best-fit" values were determined from a linear fit (response vs. prepared  $CO_2$ ) using orthogonal distance regression. Uncertainties (unc.) are shown as ~68% Confidence Level. Results are not sensitive to how the response was normalized.

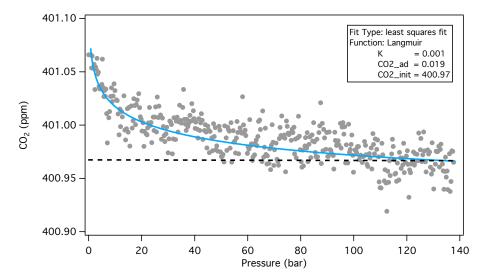
cylinder	prepared	unc.	response	unc.	best-fit	residual
	ppm	ppm			ppm	ppm
CB11873	357.569	0.058	0.881915	0.000028	357.535	-0.034
CB11906	397.523	0.062	0.980465	0.000025	397.527	0.004
CB11941	405.363	0.073	1.000000	0.000025	405.455	0.092
CB11976	449.330	0.074	1.108007	0.000025	449.285	-0.045
CB12009	491.795	0.077	1.212741	0.000039	491.787	-0.008

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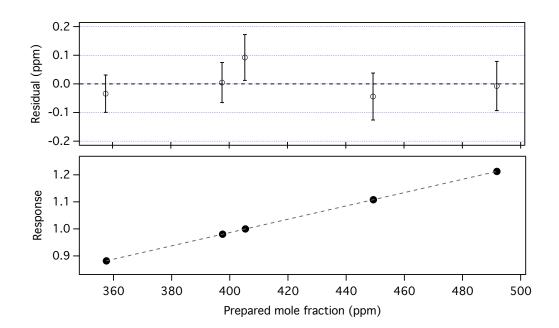
**Figure 1:** Typical result from  $CO_2$  decanting experiments showing an increase in  $X_{CO2}$  with decreasing cylinder pressure. The fraction of  $CO_2$  adsorbed was found by comparing the area under the Langmuir isotherm (blue line) with the area under the Langmuir isotherm but above the initial  $CO_2$  mole fraction (dashed line). The adsorbed  $CO_2$  calculated this way, expressed as a mole fraction, is similar to the parameter  $CO_{2,ad}$  from the Langmuir model (Leuenberger et al., 2015;Schibig et al., 2018).

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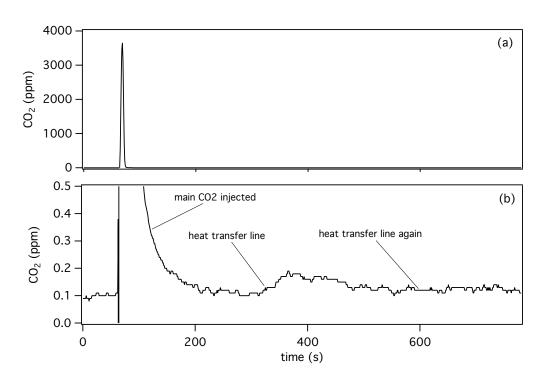
**Figure 2:** Normalized response of gravimetrically-prepared standards, analyzed by laser spectroscopy (lower panel). Residuals from linear fit are shown in upper panel, along with preparation uncertainties (~68% Confidence Level, or coverage factor k=1).

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**Figure 3**: Measure of  $CO_2$  passing through AT-steel transfer line. The peak in (a) results from 0.6cm<sup>3</sup> air containing 10%  $CO_2$  injected into  $CO_2$ -free air flowing at 0.2 L min<sup>-1</sup>. Panel (b) is an expanded view of panel (a), showing a second peak at ~ 400s, which results from  $CO_2$  driven off the tubing by heating.