

Author's response

Myriam Guillevic et al.

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1 Response to comments from Reviewer 1

This manuscript describes a dynamic dilution with cryogenic filling to produce pmol/mol reference materials in high-pressure cylinders. The method is well-described and the paper is well-written. The technique described is different to static dilution, which is commonly used to prepare low mole fraction reference standards for atmospheric measurement of trace gases that influence stratospheric ozone and climate. The authors provide comparisons to previous calibration scales, some of which are not well developed. These data will improve our understanding of the atmospheric abundance of HCFC-132b, HFC-125, HFO-1234yf, and CFC-13. This work will help provide SI traceability to current measurements, and the method could be useful for gases that are reactive or adsorb readily to dry surfaces. I have relatively few comments and technical corrections.

The authors would like to express their gratitude to Reviewer 1 for his/her considerable effort to improve the quality of this manuscript with knowledgeable and concise comments and input. We hereafter provide point by point replies to them.

P5, L26: In equation (1), V_m is listed as the molar volume of the carrier gas (L/mol), which makes sense, but in Table 2, it is listed with units of g/mol. Is V_m correct in Table 2?

There is indeed a mistake in Table 2, the unit of V_m should be L/mol, as in Equation (1). Table 2 is now corrected.

P5, L26: Is V_m calculated by assuming it is an ideal gas? We used NIST Tables of molar volumes (NIST Chemistry WebBook, <<https://webbook.nist.gov>>). The data are calculated for real gases, at 0°C and 1013.25 hPa. We added this information in the first occurrence of the quantity molar volume: 'Values are from the NIST Chemistry WebBook, assuming real gas'.

P7, L30: Im having a hard time with equation (5). The units dont seem to work out. On page 8 you say that equation (5) can be simplified by removing q_{V5} , but this is not obvious. It seems that q_{V5} remains in the term $x_{residual}/(t_{total} * q_{V5})$, unless an additional q_{V5} is missing from (5). Because of this and the confusion over V_m , I am unable to verify the calculations for SF₆ in cylinder MP-001 using data from Table 2.

There is indeed a mistake in Equation 5 as written in the manuscript, thank you for pointing this out. It should be written:

$$x_{prep,i,j} = \frac{x_{filled,i} \cdot q_{V5,j} \cdot \Delta t_{i,j} + x_{residual,i} \cdot q_{V5,j} \cdot (\Delta t_{total,j} - \Delta t_{i,j})}{\Delta t_{total,j} \cdot q_{V5,j}} \quad (1)$$

From the above correct equation, we can now simplify by removing the factor $q_{V5,j}$, and re-arrange to:

$$x_{prep,i,j} = x_{filled,i} \cdot \frac{\Delta t_{i,j}}{\Delta t_{total,j}} + x_{residual,i} \cdot \left(1 - \frac{\Delta t_{i,j}}{\Delta t_{total,j}}\right) \quad (2)$$

All calculations have been corrected and this does not change the results of the calculations, nor for the molar fractions neither for the ratios.

5

Table 2: The treatment of uncertainties seems reasonable, except for one minor component. You use the manufacturers data for purity (99%) and account for the uncertainty in the budget, which is acceptable. However, according to Vollmer at al. 2015 and references therein, HFC-125 is produced by hydrofluorination of perchloroethylene, with several intermediates, including HCFC-133a. Can you comment on the possibility that HFC-125 might contain HCFC-132b as an impurity? Does the purity uncertainty component for HCFC-132b need to be expanded to include this possibility?

Thank you for pointing this out. We fully agree that cross-contamination originating from impurities present in permeators can potentially be an important issue. We plan to investigate this in a more systematic way for the next generation of reference mixtures, by performing measurements of impurities present in each permeator. We have modified Section 4.2.2 of the main text to mention this:

15 'We plan for future reference gas mixture preparation to check the presence of substance impurities in permeators in a systematic way, to get a better estimate of the purity fraction as well as to quantify any potential cross-contamination, if any. For the METAS-2017 scale, we checked in particular the absence of HFC-132b as impurity in the HFC-125 permeator (see Section S5 in Supplement).'

And we added the following section in the Supplement:

20 'Based on the findings from Vollmer et al. (2015) who identified several potential impurities in HFC-125 inherited from its production pathway, we have measured the presence of impurities in the permeator for HFC-125. We have done this test using the reference gas mixture for HFC-125 prepared at 85 nmol/mol (cylinder MP15-4020, see Fig. S1) as part of the METAS-2015 suite for HFC-125. These measurements have been performed by injecting 1 L of this mixture directly in the Medusa-GC-MS at Empa. The detection of the HFC-125 peak was disabled to avoid saturation of the detector. For HCFC-132b, there was no
25 chromatographic baseline excursion suggesting that the mole fraction was well below the detection limit (defined here as three times the noise level). As the amount of gas used for a measurement was 1 L, i.e. half the normal gas quantity of 2 L, we roughly estimate the detection limit for HCFC-132b as twice the detection limit for a normal measurement of 2 L, i.e. 0.03 pmol/mol (instead of 0.015 pmol/mol).

In addition, the measurements showed the presence of:

- 30
- CFC-115: 31 pmol/mol ($0.36 \cdot 10^{-3}$ mol per mol HFC-125)
 - HFC-143a: 51 pmol/mol ($0.6 \cdot 10^{-3}$ mol per mol HFC-125)
 - HFC-134a: 31 pmol/mol ($0.36 \cdot 10^{-3}$ mol per mol HFC-125)
 - HCFC-124: 11 pmol/mol ($0.13 \cdot 10^{-3}$ mol per mol HFC-125)

- SF₆: 0.2 pmol/mol with LOD = 0.03 pmol/mol ($2.5 \cdot 10^{-6}$ mol per mol HFC-125)
- HFO-1234yf: 0.06 pmol/mol with LOD = 0.02 pmol/mol, although we are not sure if this is a small impurity introduced potentially by contamination from a regulator
- CFC-13: no baseline disruption (LOD = 0.14 pmol/mol).

5 In cylinder MP-001 containing 32.027 pmol/mol HFC-125, the SF₆ impurities originating from the HFC-125 permeator correspond to a contribution of $2.5 \cdot 10^{-6} \cdot 32.027 = 0.00008$ pmol/mol SF₆. This can be neglected compared to the prepared 10.582 pmol/mol SF₆. The same conclusion applies to HFO-1234yf and to the other cylinders.'

Figure 6: I dont find this figure particularly helpful. It seems that the relevant information is in fig. 7 and Table S6.

10 We agree and Figure 6 is now removed. Table S6 is therefore now included in the main text, as Table 7.

P1, L1: replace "withing" with "within" The text was corrected accordingly.

15 **P1, L15: Perhaps be more specific, "... traceable to the SI-units, amount of substance, ..."** The final unit we generate using the presented method contains indeed the mole, one of the SI-units, but to generate this unit we use as well for example flows, that are traceable to the SI-units second and meter. Also, the balance measures a mass, traceable to the unit kilogram, and the conversion to unit mole is realised using molar masses of molecules. Thus the final quantity, even being mole/mole, is traceable not only to the mole but to other SI units as well. We therefore prefer to keep the sentence as it is.

20 **P1, L23: Consider rephrasing: "Such a combined system supports maximizing compatibility ..."** Suggestion implemented.

P2, L9: (minor) Consider using mixing ratio or molar fraction instead of concentration Text modified accordingly, 'concentration' being substituted by 'molar fraction' for all occurrences.

25

P2, L13: Change "Kigali agreement" to "Kigali Amendment" Text modified accordingly.

P2, L16: Should probably spell out "Non-Article 5" Corrected.

30 **P2, L16: "bottom-up"** Corrected.

P2, L31: "detect gradients between" Corrected.

P2, L32: "attribute" rather than "attributing" Text modified accordingly.

P2, L29: Consider; "... while assessments of climate forcing and stratospheric ozone rely on observations of atmospheric composition". Text modified according to suggestion.

5

P3, L11: No mention of what "compatibility target" is. Consider simplifying as "The calibration scale approach enables a high degree of consistency, but still requires" Text modified according to suggestion.

P3, L12; Consider replacing "consists in" with "includes" Text modified according to suggestion.

10

P5, L3: Consider re-phrasing. "The permeation rate depends exponentially on temperature; ..." Text modified according to suggestion.

P12: Im glad you included some possible reasons for some cylinders failing verification tests. Do you consider the possibility that some fraction of a component could be lost to the surface of the cylinder before the water is added? Maybe future experiments could be done in which the H2O is added earlier in the sequence?

15

Indeed, there is always the possibility that some compounds are partially lost to the surface of the cylinder, and adding water earlier in the sequence of fillings would be a judicious approach. In this study, the strategy we applied to evidence potential losses on cylinder surfaces was to use cylinders of different volumes, filled at different pressures, with different coating materials. In the literature, tests of adding water after filling cylinders with gas mixtures for CCl₄ showed a desorption of CCl₄, suggesting that adding water afterwards may be acceptable in certain cases (Yokohata et al., 1985).

20

Besides, for cylinders which failed the verification test and which showed anomalously low levels of e.g. HFO-1234yf, we still don't know if the loss occurred due to adsorption in the cylinder or previously, on other stainless steel surfaced of the preparation system. This is a point we plan to investigate in the future by comparing molar fraction measured in the gas coming out of cylinders to molar fraction measured in the gas stream coming directly from the second dilution step of the magnetic suspension balance (MSB). This system being physically only a few meters apart from a new APRECON-GC-MS installed at METAS, it will be possible to have the MSB system connect to one inlet port of the APRECON-GC-MS, a cylinder filled with this same mixture to another port, and compare if the two molar fractions are identical, within measurement uncertainty. This was not done in this paper as the APRECON-GC-MS system was not validated yet. We hope to include this in a future study.

25

We included a paragraph in Section 3.2.2 (Verification test and exclusion of outliers) of the manuscript to discuss this:

30

'Furthermore, we plan to investigate if the observed substance losses occurred by adsorption on cylinders walls or beforehand in the preparation system. To do so, a comparison of the molar fraction in the mixture exiting the magnetic suspension balance/dynamic dilution system with the same mixture filled in cylinders will be performed. The recent installation of a measurement system for halogenated gases at METAS in the same laboratory makes this possible. If the adsorption indeed oc-

curs in the cylinders, it will be tested if adding water vapour earlier in the sequence of fillings may help to limit this adsorption.’

P15, L14: change "apply for" to "applies to" Text corrected.

5 **P15, L27:** I think you have the NOAA/SIO ratio backwards. Rigby et al 2010 adjusted NOAA data by the factor 0.998, so that means that SIO/NOAA = 0.998, consequently NOAA/SIO would be 1.002. While the Rigby et al 2010 comparison is out of date (NOAA updated their SF6 scale from NOAA-2006 to NOAA-X2014), the ratio 1.002 is consistent, within uncertainties, with those calculated by P. Krummel (http://www.wmo.int/pages/prog/arep/gaw/documents/GGMT2017_T03_Krummel.pdf).

10 Thank you for this precise observation. We now use the ratio of 1.002 obtained by calculating the weighted mean of comparison ratios as presented by P. Krummel et al. (GGMT, 2017). Figure 7 was updated accordingly.

We also realised that on Figure 7, we show the known factor UB98/SIO for HFC-125 but it is not mentioned in the main text. We now added a small section:

15 **UB-98:** Before using the SIO-14 scale for HFC-125 within AGAGE, a primary calibration scale prepared by University of Bristol was in use (UB-98 O’Doherty et al., 2004, 2009). The known conversion factor UB-98/SIO-14 is 0.9237 (C.M. Harth and R.F. Weiss, pers. com., 2018).

20 **Fig. 1:** It would help if a box was drawn around the permeation chamber, similar to the box around MFM, MFC1, and MFC2. Figure 1 is now modified according to suggestion. The permeation chamber is now drawn by an orange box. Additionally another box is drawn around the ensemble ‘magnetic suspension balance’, made of the balance plate and its associated electromagnet, the permeator hooked to the permanent magnet, both in the permeation chamber.

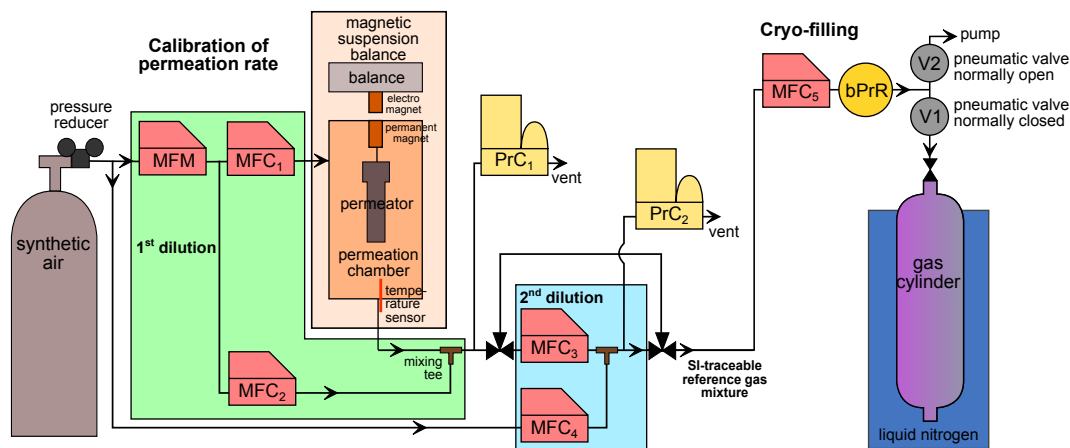


Figure 1. Schematic of the dynamic-gravimetric preparation method. MFM: thermal mass flow meter. MFC: thermal mass flow controller. PrC: pressure controller. bPrR: back (downstream) pressure regulator. V1 and V2: pneumatic valves.

Table 2: Is the entry for Permeation supposed to be ng/s instead of ng/min? The given value of 1654.77 for the permeation rate is correctly assigned a unit of ng/min. However there is indeed a mistake in Table 2, because the time values t_{1SF_6} and t_{2SF_6} should be in minutes, not in seconds. Table 2 is now corrected accordingly. Table S1 contained the same unit mistake and is now corrected as well. Note that all calculations are still valid, and the units in Figure 2 are correct. This mistake likely comes from the fact that $\Delta t_{i,j}$ are reported in seconds.

2 Response to comments from Reviewer 2

The manuscript by Guillevic et al. titled "Dynamic-gravimetric preparation of metrologically traceable primary calibration standards for halogenated greenhouse gases" describes the preparation of novel traceable gas standards containing SF₆, HCFC-132b, HFC-125, HFO-1234yf, and CFC-13 in air by dynamic means using a permeation device. Many of these compounds are atmospherically important and no traceable reference standards are well established, therefore this is an important publication. The authors discuss the need and uses for these gravimetric standards and compare them to previous calibration scales. On the whole, the article is well written, with a few minor typos that can easily be amended. Please see below for my comments and feedback.

We thank the reviewer for his/her time and constructive comments. Please find below a point-by-point answer to each comment.

Minor changes: For coverage factors and confidence intervals k values should be in italics.

The text was corrected accordingly.

P1, line 1 remove 'g' from within.

Text corrected.

P3, line 3 add an 'and'.

Text modified according to suggestion.

25

P3, line 12 replace 'in' with 'of'.

Text modified, also according to suggestion by R1: 'This QA/QC procedure includes regular intercomparisons [...]'.
25

P3, line 13 remove end 's' from flasks.

30 Text corrected accordingly.

P6, line 20 transferred 'into'.

Text corrected accordingly.

P7, line 2 'checking'.

Text corrected accordingly.

5

P10, line 1 why do you use $k = 1$?

We use $k = 1$ for $u_{R_{prep,i,j}}$ because this standard uncertainty is then used in the bivariate weighted linear fit, together with $u_{R_{meas,i,j}}$ to find the parameters a_i and b_i . The equations are detailed in the Supplement, Section S3.

10 **Comments: In the introduction there is discussion about calibration scales and static point source measurements. It may be worth briefly commenting on atmospheric measurement and sampling of these compounds to highlight the challenges and needs for reference standards.**

Thank you for this remark. Also in agreement with R1, we have now completed the third paragraph of the introduction, introducing atmospheric measurement and sampling:

15 'Atmospheric measurements of halogenated compounds are currently provided by several networks such as AGAGE (Advanced Global Atmospheric Gases Experiment), NOAA (National Oceanic and Atmospheric Administration), and GAW (Global Atmospheric Watch). Such measurements, used to precisely estimate atmospheric molar fraction of these halogenated substance together with associated trends, are crucial to understand and predict the evolution of stratospheric ozone and estimate their radiative forcing thereby refining future climatic projections. Furthermore based on these measurements and using
20 atmospheric transport modeling, emissions can be quantified ('top-down' estimation, e.g., Prinn et al., 2000; Rigby et al., 2010; Brunner et al., 2017). The comparison of top-down reconstructions with bottom-up inventories shows agreement for some gases but also discrepancies that can be considerable for others (Weiss and Prinn, 2011; Lunt et al., 2015; Hu et al., 2016; Simmonds et al., 2016; Sherry et al., 2017). The top-down approach thus is a complementing and independent way to review production/consumption/emission inventories and compliance with reduction targets, while assessments of climate forcing and
25 stratospheric ozone rely on observations of atmospheric composition'.

In the introduction you may want to refer to WMO data quality objectives.

Thank you for this comment. We did not mention WMO data quality objectives in this article for several reasons. First, WMO is only one of the several networks/groups measuring halocarbons (e.g., AGAGE, University of California, Goethe Universität
30 Frankfurt). To our knowledge, there are set DQO for SF₆ within WMO (Compatibility goal, 1 sigma: 0.02 pmol/mol and extended compatibility goal, 1 sigma: 0.05 pmol/mol), but not for the other halocarbons (see for example GAW Report No. 229, 18th WMO/IAEA Meeting on Carbon Dioxide, Other Greenhouse Gases and Related Tracers Measurement Techniques (GGMT-2015), Table 1 p. 3). The WMO DQO for SF₆ applies to the data produce within the WMO network, not to other networks, which may have different DQOs or different methods to measure data quality. As our suite of standards is meant to
35 be available to any group/network asking for it, we decided not to mention requirements of one specific network.

Second, the link between DQO as defined by WMO and expanded uncertainty of a produced reference gas mixture is not straightforward. It strongly depends on the method used to disseminate the primary standard to the end-users. Actually, within the scale system used by networks such as WMO for SF₆ or AGAGE for halocarbons, DQO becomes mostly relevant for the primary calibration scale propagation, not for its preparation. Within this framework, the best way to reach DQOs is to make the calibration chain between primary calibration scale and laboratory standard as short as possible as well as to improve measurement reproducibility. As the dissemination of the produced METAS-2017 primary calibration scales is beyond the scope of this paper, we think it is not very relevant to mention WMO DQOs for SF₆. The dissemination of the METAS-2017 scale for CFC-13 to the AGAGE network is described in Vollmer et al. (2018). Note that AGAGE does not use DQO as a measure of network data quality.

10

Emphasise the impact of HFCs etc. on climate forcing and why the dynamically prepared reference standards are so important. One interesting paper is Velders et al. 2009.

The impact of HFCs on climate forcing is mentioned in the first paragraph of the introduction, p. 2 l. 11-15. We thank Reviewer 2 for the suggested reference and have now modified the paragraph to include it: 'HFCs (hydrofluorocarbons) were introduced as replacement for CFCs and HCFCs. Their emissions, though not harmful to the ozone layer, are still increasing and contributing to global warming due to their high radiative forcing (Harris and Wuebbles, 2014, Velders et al., 2009). For this reason the recent Kigali Amendment (Oct. 2016) added these HFCs to the Montreal Protocol'.

The importance of dynamically prepared reference gas mixture for the mentioned gases was actually not well known before this study, therefore it is not mentioned in the introduction. However this finding is emphasised in Section 4.2, and especially when discussing the results for HFC-125 (Section 4.2.2) and HFO-1234yf (Section 4.2.3). It is mentioned again as the last sentence of the conclusion: 'Dynamic generation methods and/or minimisation of contact on surfaces should therefore be favoured when preparing primary reference gas mixtures for such reactive substances'.

Section 2.1 Please give the numeric calibration range.

We added to the first paragraph of Section 2.1 the following sentence: 'The resulting prepared molar fraction range covered by this suite varies between the five compounds, with a range of 0.9 – 1.5 pmol/mol for HFO-1234yf with the lowest molar fractions, to 26 – 42 pmol/mol for HFC-125 with the highest molar fraction (see details for each substance in Table 3)'.

Section 2.4 Describe how equivalent cylinders (e.g. 3 & 4 or 2 & 9) were prepared in parallel.

All cylinders were prepared in series, i.e. we use the same mixture exiting the MSB-dilution system to fill all cylinders, one after the other, as described in Section 2.4 p. 7: '[...] The cylinder valve is then manually closed, the cylinder disconnected and left standing vertically outside the building to warm up. A new cylinder is placed in the liquid nitrogen bath, connected to the filling system, and the filling procedure starts again'.

Equivalent cylinders are not filled in parallel but one after the other. For one given substance, equivalent cylinders are therefore not more correlated than any other couple of cylinders.

Section 3.1 State detection limits (LODs).

5 We have completed Section 3.1 as follow: 'Detection limits, defined here as three times the noise level, are 0.015 pmol/mol for SF₆, 0.02 pmol/mol for HFC-125, 0.01 pmol/mol for HFO-1234yf, 0.015 pmol/mol for HCFC-132b and 0.07 pmol/mol for CFC-13'.

Regarding the stability of the permeation temperature, how critical is this? How can you tell if a sufficiently long stabilisation time has been reached to achieve equilibrium for the permeation device?

The sensitivity of the permeation rate to temperature is discussed in Section 2.5.1, p. 8, paragraph 'Permeation chamber temperature stability': 'Once carrier gas flow and pressure are kept constant, the permeation rate varies only with temperature. The stability of the permeation chamber temperature is 0.02 °C over 20 min ($k = 2$). Based on our experience measuring temperature sensitivity of permeation rate, this corresponds to approx. 0.1 % change in permeation rate'.

15 The estimation of the needed stabilisation time is explained in Section 2.2, p. 5, l. 22-24 : 'After inserting a permeation device, a stabilisation period is required mainly depending on chamber temperature, pressure and permeator membrane properties, before the mass loss becomes linear over time. This linear mass loss vs time is then determined for at least 8000 min to minimise the standard deviation of the measured mass loss due to balance noise.' We completed this information as follow: 'The time window $t_{2,i} - t_{1,i}$ during which the mass data are used is determined so that the residuals of the fit to the mass loss over time are centered around zero and randomly distributed (see example for CFC-13 on Fig. 2 and Section S1 in the Supplement)'. We also modified the legend of Fig. 2 accordingly.

Does the pressure of the cylinder have an influence? The authors suggest not, however the lower pressure cylinders seem to be more problematic, could this be attributed to wall effects? Surface reactions are mentioned for HFO-1234yf – was performance better in the treated cylinders? Why use stainless steel if dynamically produced standards often show lower values than statically prepared standards for reactive substances?

25 We discussed potential wall effects in Section 3.2.2, p. 12 l. 28-32: 'We however observe that most outliers are cases of substance loss (Fig. 5) and affect cylinders having the smallest total amount of gas filled and the highest surface/volume ratio (i.e. Essex cylinder 4.5 L, 24 bars). We would therefore in the future favour filling in cylinders of larger volume and pressure, as well as a further automatising the cryo-filling process to limit human intervention as much as possible as well as to increase the safety of the procedure.'

35 Following as well suggestion from R1, we added the following information: 'Furthermore, we plan to investigate if the observed substance losses occurred by adsorption on cylinders walls or beforehand in the preparation system. To do so, a comparison of the molar fraction in the mixture exiting the magnetic suspension balance/dynamic dilution system with the same mixture filled in cylinders will be performed. The recent installation of a measurement system for halogenated gases at

METAS in the same laboratory makes this possible. If the adsorption indeed occurs in the cylinders, it will be tested if adding water vapour earlier in the sequence of fillings may help to limit this adsorption.’.

Yes, it seems performance was better in the cylinders passivated with SilcoNert2000 coating, as cylinders MP-003 to MP-006 show no outliers presenting a substance loss. All other cylinders are made of stainless steel passivated by electropolishing of extremely high quality (Essex Industries), with two different volumes and associated maximum pressures (see main text, Table 1). The larger type of cylinder has been used for decades by the AGAGE network and is moreover the container of choice for the Cape Grim Air Archive, showing excellent stability over time for most halogenated compounds (e.g., Prinn et al., 2000).

Is your system not Silco treated?

Thank you for this remark, indeed the preparation system is almost entirely SilcoNert2000-treated but this was not mentioned. The text is now modified in Section 2.3 according to this suggestion: ‘Note that most metal surfaces in contact with the carrier gas and the produced gas mixture are passivated by applying SilcoNert2000 coating. This includes all metal tubing, all metal surfaces of the MFCs and MFM in contact with the gas, and most of the permeation chamber’.

Figure 6 is unclear and I recommend removal or overhauling it. We agree and Figure 6 is now removed.

3 Additional corrections and changes

The affiliation for Dr. Daiana Leuenberger has been updated.

In the Introduction p. 3 l. 4, the uncertainty range stated for NOAA primary standard preparation was for SF₆ only (0.6 to 0.9 %, Lim et al., 2017). However NOAA prepares primary reference gas mixtures for many other halocarbons, with usually higher uncertainties. The text is now modified to : ‘[...] 0.6 to <2 % for NOAA (Hall et al., 2007; Montzka et al., 2015; Lim et al., 2017)’.

It was not mentioned that molar fractions for halogenated compounds are calculated in dry synthetic air, i.e. the added water molar fraction is not included for the calculation of the halocarbon molar fraction. This is due to the fact that the Medusa-GC-MS used for analysis is equipped with a drying system. This is now mentioned in the text (Sect. 2.4), in Table 3 and Table 6.

There was a permutation mistake in Equations 1 and 2: the first denominator should be $(t_{2,i} - t_{1,i})$, otherwise the obtained mass loss is negative. This is now corrected. This has no influence on the results as permeation rate values were already correctly used as positive values in all calculations.

It is now mentioned in the abstract that the METAS-2017 scale for CFC-13 presented in this paper has been adopted by the AGAGE network: ‘Finally, for CFC-13 the METAS-2017 primary calibration scale is 5% higher than the interim calibra-

tion scale (Interim-98) that was in use within the Advanced Global Atmospheric Gases Experiment (AGAGE) network before adopting the scale established in the present work’.

5 Figure 4 has been updated: it includes now results not only for SF₆ and CFC-13 but for all five halogenated compounds. To fit on one page the figure is therefore now shifted to landscape position.

Tables 4 and 5 in the discussion version have been merged into one Table to facilitate the layout for the final version (now Table 4).

10 The new Table 6 (before Table S6) was completed with a last section: now we give for documentation purpose the ratios METAS-2017/NOAA-2014 for SF₆ of 1.000 and METAS-2017/NOAA-2008 for HFC-125 of 0.982. These ratios are calculated using the measured METAS-2017/SIO-05 and METAS-2017/SIO-14 ratios for SF₆ and HFC-125 respectively (this study) as well as the know conversion factors between SIO and NOAA for these two compounds (see main text for references).

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Dynamic-gravimetric preparation of metrologically traceable primary calibration standards for halogenated greenhouse gases

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Abstract. For many years, the comparability of measurements obtained with various instruments within a global-scale air quality monitoring network has been ensured by anchoring all results to a unique suite of reference gas mixtures, also called 'primary calibration scale'. Such suites of reference gas mixtures are usually prepared and then stored over decades in pressurised cylinders by a designated laboratory. For the halogenated gases which have been measured over the last forty years, this anchoring method is highly relevant as measurement reproducibility is currently much better ($< 1\%$, $k = 2$ or 95 % confidence interval) than the expanded uncertainty of a reference gas mixture (usually $> 2\%$). Meanwhile, newly emitted halogenated gases are already measured in the atmosphere at sub-pmol/mol levels, while still lacking an established reference standard. For compounds prone to adsorption on material surfaces, it is difficult to evaluate mixture stability and thus variations in the molar fractions over time in cylinders at pmol/mol levels.

To support atmospheric monitoring of halogenated gases, we create new primary calibration scales for SF₆ (sulfur hexafluoride), HFC-125 (pentafluoroethane), HFO-1234yf (or HFC-1234yf, 2,3,3,3-tetrafluoroprop-1-ene), HCFC-132b (1,2-dichloro-1,1-difluoroethane) and CFC-13 (chlorotrifluoromethane). The preparation method, newly applied to halocarbons, is dynamic and gravimetric: it is based on the permeation principle followed by dynamic dilution and cryo-filling of the mixture in cylinders. The obtained METAS-2017 primary calibration scales are made of 11 cylinders containing these five substances at near ambient and slightly varying molar fractions. Each prepared molar fraction is traceable to the realisation of SI units (Système International d'Unités) and is assigned an uncertainty estimate following international guidelines (JCGM 100:2008), ranging from 0.6 % for SF₆ to 1.3 % ($k = 2$) for all other substances. The smallest uncertainty obtained for SF₆ is mostly explained by the high substance purity level in the permeator as well as low SF₆ contamination of the matrix gas. The measured internal consistency of the suite ranges from 0.23 % for SF₆ to 1.1 % for HFO-1234yf ($k=1$). The expanded uncertainty after verification (i.e. measurement of the cylinders vs each others) ranges from 1 % to 2 % ($k = 2$).

This work combines the advantages of SI-traceable reference gas mixture preparation with a calibration scale system for its use as anchor by a monitoring network. Such a combined system supports maximising compatibility within the network while linking all reference values to the SI and assigning carefully estimated uncertainties.

For SF₆, comparison of the METAS-2017 calibration scale with the scale prepared by SIO (Scripps Institution of Oceanography, SIO-05) shows excellent concordance, the ratio METAS-2017/SIO-05 being 1.002. For HFC-125, the METAS-2017 calibration scale is measured as 7 % lower than SIO-14, and for HFO-1234yf 9 % lower than Empa-2013. No other scale for HCFC-132b was available for comparison. Finally, for CFC-13 the METAS-2017 primary calibration scale is 5% higher than the interim calibration scale (Interim-98) that was in use within the Advanced Global Atmospheric Gases Experiment (AGAGE) network, before adopting the scale established in the present work.

1 Introduction

Since the 1970s, atmospheric measurements of CFCs (chlorofluorocarbons) and HCFCs (hydrochlorofluorocarbons), used as refrigerants and blowing agents, have evidenced their role in stratospheric ozone layer depletion (Molina and Rowland, 1974; WMO, 1981). The reduction of CFC use (and later HCFCs) has been under strict regulations of the Montreal Protocol on Substances that Deplete the Ozone Layer since its entering into force in 1989 (WMO, 2014). While the molar fractions of major CFCs are now declining in the atmosphere, some longer-lived minor CFCs are still increasing (WMO, 2014; Laube et al., 2014; Vollmer et al., 2018). HFCs (hydrofluorocarbons) were introduced as replacement for CFCs and HCFCs. Their emissions, though not harmful to the ozone layer, are still increasing and contributing to global warming due to their high radiative forcing (Harris and Wuebbles, 2014; Velders et al., 2009). For this reason the recent Kigali Amendment (Oct. 2016) added these HFCs to the Montreal Protocol. As a consequence and in compliance with European Directive 2006/40/EC, replacement compounds were introduced, foremost the HFOs (hydrofluoroolefins, Vollmer et al., 2015).

Non-Article 5 (developed) countries of the Montreal Protocol are bound to report their CFCs/HCFCs/HFCs production and consumption based on so called 'bottom-up' inventories. Within the Kyoto Protocol aiming at limiting climate change, Annex-1 (developed) countries report inventories of greenhouse gas emissions to the atmosphere, for which reduction targets are set. Reviews of the success of such reduction targets and projections of future developments are so far still based on those inventories, while ozone layer recovery and climate change depend on real atmospheric molar fractions.

Atmospheric measurements of halogenated compounds are currently provided by several networks such as AGAGE (Advanced Global Atmospheric Gases Experiment), NOAA (National Oceanic and Atmospheric Administration), and GAW (Global Atmospheric Watch). Such measurements, used to precisely estimate atmospheric molar fraction of these halogenated substance together with associated trends, are crucial to understand and predict the evolution of stratospheric ozone and estimate their radiative forcing thereby refining future climatic projections. Furthermore based on these measurements and using atmospheric transport modeling, emissions can be quantified ('top-down' estimation, e.g., Prinn et al., 2000; Rigby et al., 2010; Brunner et al., 2017). The comparison of top-down reconstructions with bottom-up inventories shows agreement for some gases but also discrepancies that can be considerable for others (Weiss and Prinn, 2011; Lunt et al., 2015; Hu et al., 2016; Simmonds et al., 2016; Sherry et al., 2017). The top-down approach thus is a complementing and independent way to review production/consumption/emission inventories and compliance with reduction targets, while assessments of climate forcing and stratospheric ozone rely on observations of atmospheric composition.

To quantify atmospheric molar fractions at specific sites, detect **gradients between** monitoring stations, evaluate data consistency and lack of biases and thereby **attribute** emissions to specific geographical areas, results have to be linked to accurate calibration scales. Currently for most monitored halogenated gases, measurement precision is as low as 0.4 % ($k = 2$ or 95 % confidence interval, Miller et al., 2008). This is much better than the expanded uncertainty of reference gas mixtures, estimated to be in the order of e.g. 2 to 4 % for SIO standards (Scripps Institution of Oceanography, e.g., Prinn et al., 2000), 0.3 to 3 % for NIST (National Institute of Standard and Technology, Rhoderick et al., 2015), and 0.6 to <2 % for NOAA (Hall et al., 2007; Montzka et al., 2015; Lim et al., 2017). Given this technical state of the art, monitoring networks have developed a so called 'primary calibration scale' system, in which all stations of a specific network are anchored to the same suite of primary reference gas mixtures with a calibration chain as short as possible. To ensure long term continuity of atmospheric composition data, such calibration scales have to be maintained over years and only replaced if substantial necessity arises, with a scheme to properly back-calibrate all past measurements if a new calibration scale is defined. Accurate and stable calibration scales directly impact the quality of emission quantification, trend estimation and the calculation of values relevant for future climate projections, such as radiative forcing which is derived from atmospheric composition.

The calibration scale approach enables a high degree of consistency, but still requires detecting and documenting systematic offsets as an indicator for potentially existing systematic biases. This QA/QC procedure includes regular intercomparisons between instruments installed at the same sites and reference gas mixtures or air sample flask exchanges (Hall et al., 2014; Rhoderick et al., 2015). In addition, geographically close monitoring stations anchored to different calibration scales regularly assess the potential development of a bias over time, that can dependent on the molar fraction (e.g., O'Doherty et al., 2004; Rigby et al., 2010; Vollmer et al., 2016; Simmonds et al., 2017).

The production of a robust and accurate primary calibration scale at low molar fraction level, which is usually created through a set of reference gas mixtures, is a major task (Prinn et al., 2000; Zhao et al., 1997; Dlugokencky et al., 2005; Zhao and Tans, 2006; Hall et al., 2007). In particular for compounds prone to adsorption on material surfaces, it is difficult to evaluate mixture stability and thus variations of molar fractions over time in cylinders. As a consequence, some halogenated gases are measured in the atmosphere against reference standards that lack conventional calibration (relative calibration scales) or with only limited sets of primary reference standards (e.g., Vollmer et al., 2015).

To support atmospheric monitoring of halogenated gases, we present here a method to produce reference gas mixtures at near atmospheric molar fractions for SF₆ (sulfur hexafluoride), HFC-125 (pentafluoroethane), HFO-1234yf (HFC-1234yf, 2,3,3,3-tetrafluoroprop-1-ene, newly emitted compound), HCFC-132b (1,2-dichloro-1,1-difluoroethane) and CFC-13 (chlorotrifluoromethane). While SF₆ and HFC-125 have already widely used calibration scales (see Sect. 4.1), HCFC-132b and CFC-13 have been measured for many years in AGAGE yet not reported on a conventional calibration scale (Vollmer et al., 2018). We apply a preparation technique combining dynamic gravimetry (ISO 6145-10, 2002) and dynamic dilution (ISO 6145-7, 2009), followed by cryo-filling in cylinders. This is an alternative to the prevailing preparation method for such compounds which is by static gravimetry (Prinn et al., 2000; Hall et al., 2007; Rhoderick et al., 2015; Lim et al., 2017). The produced suite of reference gas mixtures is SI-traceable, i.e. all measured/relevant quantities of each preparation step are linked to the realisation of SI units (the International System of units) through an unbroken chain of calibrations. Finally, the prepared suite

of mixtures is assigned a carefully quantified expanded uncertainty taking into account all known relevant potential sources of uncertainties, following international recommendations (JCGM, 2008). The aim is to provide independent calibration scales and compare them to other available scales. This would provide existing calibration scales, which have so far been used on a relative basis, with a link to the SI.

5 In this paper, we present in detail the method developed to prepare SI-traceable reference gas mixtures for the mentioned halogenated gases at near atmospheric background levels, i.e. as low as 1 pmol/mol (Sect. 2). The calculations to assign prepared values are described together with the method. The associated uncertainty budgets, established following JCGM:2008, are presented and discussed in Sect. 2.5. The internal consistencies of the calibration scales are determined in Sect. 3.2. These SI-traceable primary standards are then compared to other standards currently in use in the AGAGE network, as reported in
10 Sect. 4. In addition, we determine conversion factors which compare the METAS-2017 suite to other primary calibration scales.

2 Method

2.1 Method overview: Dynamic-gravimetric generation process

The suite is designed to consist of one master cylinder (hereafter MP-001, for METAS Primary cylinder n. 001) containing all components at near ambient molar fractions but none below 1 pmol/mol, in order to not exceed preparation uncertainties of
15 2 %. Ten additional cylinders are filled with molar fractions bracketing those filled in cylinder MP-001 over the range from 20 % less to 30 % more. [The resulting prepared molar fraction range covered by this suite varies between the five compounds, with a range of 0.9 – 1.5 pmol/mol for HFO-1234yf with the lowest molar fractions, to 26 – 42 pmol/mol for HFC-125 with the highest molar fraction \(see details for each substance in Table 3\).](#) This allows the later determination of the internal consistency of the suite.

20 The generation process consists of three successive steps, starting from pure halocarbon substances diluted to [molar](#) fractions as low as pmol/mol in synthetic air. In a first step a matrix gas is spiked with one pure halocarbon substance using a permeation device (Sect. 2.2). In a second step, the high [molar fraction](#) mixture is dynamically diluted to pmol/mol level mixture using thermal mass flow controllers (MFCs, Sect. 2.3). In the final step the mixture is successively transferred into the 11 cylinders by cryo-filling (Sect. 2.4). In order to generate multi-component mixtures, the permeation device is changed and all steps are
25 repeated with the mixture containing a new substance being added to the same suite of cylinders.

2.2 Permeation

Reference gas generation by applying the permeation method combined with dynamic dilution is an established, standardised technique, particularly for reactive gases (e.g., O’Keeffe and Ortman, 1966; Scaringelli et al., 1970; Brewer et al., 2011; Flores et al., 2012; Haerri et al., 2017). It is routinely used at METAS following a procedure in compliance with international standards
30 (ISO 6145-10, 2002; ISO 6145-7, 2009). The permeation method is based on constant transfer of the substance of interest from a permeation device (or permeator), resulting in a mass loss which can be continuously monitored. Permeation devices are

placed in a permeation chamber, i.e. a controlled atmosphere in terms of temperature and pressure, continuously flushed by a carrier gas stream. Permeators [used here](#) consist of a stainless steel reservoir containing the pure substance as a liquid, sealed with a cap containing a polymer membrane permeable for the specific substance. All permeators used in this study (Fine Metrology, Italy) were filled with substances of purity 99 % or higher (Synquest Laboratories, Florida, USA). Substance purity levels were determined by the manufacturer using flame ionisation detector analysis. Permeators are filled under laminar flow to avoid potential contamination.

The permeation rate [depends exponentially on temperature](#); secondary influences are carrier gas composition and pressure (Lucero, 1971; Moosbach and Hartkamp, 1993; Jost, 2004; Brito and Zahn, 2011; Haerri et al., 2017). For mass loss determination, each permeator is placed individually in our magnetic suspension balance (MSB) 'Violetta' (hereafter MSB-Violetta, model FLUIDIFF MP, installed in 2014, Rubotherm, Germany, Fig. 1). A MSB system allows for continuous and unperturbed mass measurements as the temperature-controlled chamber, where the permeator is suspended, is physically decoupled from the balance itself. The stainless-steel permeation chamber of MSB-Violetta allows for precisely controlling temperature ($\pm 0.02^\circ\text{C}$, measured with a Pt100 sensor), pressure (± 0.1 hPa, Bronkhorst El-Press, the Netherlands) and carrier gas flow (± 0.1 % of the flow, Red-y series, Vögtlin, Switzerland). In this study, permeation typically occurs at 45°C and 3500 hPa. Inside the chamber, the permeator is coupled to a permanent magnet also placed in the chamber. On the outside of the chamber, an electromagnet connected to the balance (Sartorius ME66S) exerts a force over the permanent magnet thus coupling the permeation unit to the balance. To minimise balance noise, total weight and position of the permeation device are adjusted, as well as the vertical position of the electromagnet. The absolute mass of the permeation unit is measured in three-minute intervals. To correct for balance drift, after every 3 measurement points a calibration mass (CM1) is automatically placed on the balance plate. Additionally, a second calibration mass (CM2) of same volume but different mass is measured every 6 calibration points, to correct for any potential buoyancy change affecting the measurement of CM1. The masses of CM1 and CM2 are traceable to the Swiss realisation of the kilogramm (Fuchs et al., 2012; Marti et al., 2015; Marti, 2017, and references therein). All weight measurements and associated corrections realised with MSB-Violetta are fully automated. After each opening and closing of the permeation chamber, its tightness is checked by closing the input gas from the synthetic air cylinder as well as all exits and checking the absence of pressure decrease over time.

After inserting a permeation device, a stabilisation period is required mainly depending on chamber temperature, pressure and permeator membrane properties, before the mass loss becomes linear over time. This linear mass loss vs time is then determined for at least 8000 min to minimise the standard deviation of the measured mass loss due to balance noise. [The time window \$t_{2,i} - t_{1,i}\$ during which the mass data are used is determined so that the residuals of the fit to the mass loss over time are centered around zero and randomly distributed](#) (see example for CFC-13 on Fig. 2 and Section S1 in the Supplement). For each substance i , the molar fraction $x_{permeation,i}$ of the mixture exiting the permeation chamber can be calculated as:

$$x_{permeation,i} = \frac{m_{1,i} - m_{2,i}}{t_{2,i} - t_{1,i}} \cdot \text{purity}_i \cdot \frac{1}{M_i} \cdot \frac{V_{m,carrier}}{qV_{1,i}} + x_{residual,i} \quad (1)$$

with $m_{1,i} - m_{2,i}$, mass difference in between beginning and end of linear mass loss (g);

$t_{2,i} - t_{1,i}$, corresponding time difference (min);

M_i , molar molecular mass of substance i , calculated using average natural isotopic abundance (Meija et al., 2016, g/mol);

$pur_{i,i}$, purity fraction of the substance filled in permeator (mol/mol);

$V_{m,carrier}$, molar volume of carrier gas, here synthetic air, (L/mol). All volumes in this work are given at standard temperature and pressure (STP), i.e. 0°C and 1013.25 hPa. [Values are from the NIST Chemistry WebBook, assuming real gas;](#)

5 $q_{V1,i}$, volumetric flow of carrier gas regulated by MFC1 (Fig. 1, L/min);

$x_{residual,i}$, molar fraction of substance i in carrier gas (pmol/mol).

Permeation rates were determined at 3500 hPa and temperatures between 36°C and 45°C. We observed a particularly long stabilisation time (i.e., 6000 min) for the permeator containing CFC-13 (Fig. 2). The low mass loss for HFO-1234yf (88.5 ng/min) required a continuous measurement during 22 days to reach the required standard deviation (<0.4% for $Stab_{balance,i}$).

10 2.3 Dynamic dilution

The mixture exiting the permeation chamber, at $\mu\text{mol/mol}$ level, is diluted to pmol/mol levels over two successive, dynamic dilution steps (Fig. 1). The flows are piloted by thermal MFCs (in compliance with ISO 6145-7, 2009). First, the mixture exiting the permeation chamber is diluted with a first dilution flow (Fig. 1 MFC2, up to 5 L/min). The total flow $q_{V,MFM,i}$ passing through the permeation chamber (MFC1) and diluting this flow (MFC2) is measured by a mass flow meter (MFM on Fig. 1, Vögtlin, Switzerland), so that only this MFM needs calibration to calculate the resulting molar fraction. After this first dilution step, $x_{permeation,i}$ can be rewritten as:

$$x_{permeation,i} = \frac{m_{1,i} - m_{2,i}}{t_{2,i} - t_{1,i}} \cdot pur_{i,i} \cdot \frac{1}{M_i} \cdot \frac{V_{m,carrier}}{q_{V,MFM,i}} + x_{residual,i} \quad (2)$$

Second, a small flow of this resulting mixture is sampled by MFC3 (10 mL/min) and is diluted by another larger flow (MFC4, up to 5 L/min). The dilution factor $f_{dilution,i}$ to obtain the second dilution step is calculated as:

$$20 \quad f_{dilution,i} = \frac{q_{V3,i}}{q_{V3,i} + q_{V4,i}} \quad (3)$$

with $q_{Vn,i}$, volumetric flow of MFC $_n$ (L/min) set for substance i .

After this second dilution step, the prepared molar fraction $x_{filled,i}$ that will be filled in all cylinders can be calculated as:

$$x_{filled,i} = x_{permeation,i} \cdot f_{dilution,i} + (1 - f_{dilution,i}) \cdot x_{residual,i} \quad (4)$$

At this stage, the generated mixture has a molar fraction approximately 10 times higher than atmospheric levels. [Note that most metal surfaces in contact with the carrier gas and the produced gas mixture are passivated by applying SilcoNert2000 coating. This includes all metal tubing, all metal surfaces of the MFCs and MFM in contact with the gas, and most of the permeation chamber.](#)

2.4 Cryo-filling

The generated mixture after the second dilution step is then transferred [into](#) 11 cylinders, named MP-001 to MP-011. The technical characteristics of these cylinders are summarised in Table 1. In brief, we used 7 cylinders made of electropolished

stainless steel (Essex Industries, USA) and 4 cylinders made of Silconert2000-coated stainless steel (Swagelok). To detect potential systematic biases due to adsorption on cylinder surfaces, this set of cylinders presents four different surface/volume ratios (see details in Table 1).

5 A set flow of the reference gas mixture ($q_{V5,j}$, 3 L/min for the 34 L Essex cylinders, 0.5 L/min for all other smaller volume cylinders) is sampled by MFC5 (CMOSsens series, Sensirion, Switzerland, Fig. 1) and then directed to a tee. The two exiting paths of this tee are piloted by pneumatic valves (Swagelok), one being normally closed (to the cylinder, V1), the other one being normally open (to the pump, V2).

10 All cylinders are cleaned beforehand, being evacuated to approx. 6 Pa and filled with nitrogen at 2000 hPa (purity grade 99.999% or better), 3 times. Each cylinder was then evacuated one last time to 6 Pa or lower just before being connected to the filling system.

After being connected, the tubing between the cylinder valve and the pneumatic valve V1 (Fig. 1) is evacuated to 1 hPa and filled with synthetic air, 3 times. After leak checking, it is filled with synthetic air at a pressure of 800 hPa \pm 20 hPa, because it is the residual pressure that is lost after each filling, when the cylinder valve is manually closed (see Supplement Sect. S2).

15 After this preparation step, the bath is (re)filled with liquid nitrogen. Once the cylinder content is re-liquified, its valve is manually opened, and, piloted by a Labview program the pneumatic valve positions are switched for a precisely set duration, in order to fill a precisely controlled volume of the reference gas mixture in each cylinder. The filling periods last from 17 min to 6 hours depending on substance and target molar fraction. To avoid freezing the cylinder valve is intermittently heated with a heat gun during filling. Once the pneumatic valves are back at their default setting, the cylinder valve is kept open for one minute, while the tubing between the cylinder valve and V1 is heated to force all potential remaining substance of interest to
20 be cryo-trapped in the cylinder still in liquid nitrogen. The cylinder valve is then manually closed, the cylinder disconnected and left standing vertically outside the building to warm up. A new cylinder is placed in the liquid nitrogen bath, connected to the filling system, and the filling procedure starts again. The state of the filling system is checked at least every 30 min during filling. Once the filling of each cylinder with one given mixture is completed, the permeation chamber of the balance is opened, a new permeator installed, the chamber closed, and a new mass loss measurement starts.

25 After the fillings of all five substances of interest are completed, additional precisely determined volumes of synthetic air are cryo-filled into the cylinders in order to dilute the mixtures to atmospheric molar fractions. For this special filling, synthetic air is also directed through the permeation chamber where a glass reaction tube filled with deionised water is placed, evaporating water, in order to slightly humidify each cylinder. The resulting water vapour molar fraction ranges from 20 to 70 μ mol/mol. Note that this added water is not included in the calculations of molar fractions for the halogenated compounds, which are
30 therefore expressed in dry synthetic air. Adding water vapour to each cylinder was motivated by the fact that losses due to adsorption are known to occur for some halogenated compounds (Prinn et al., 2000). This has been evidenced by Yokohata et al. (1985) for CCl₄ and CH₃CCl₃ in very dry mixtures (i.e., likely less than 750 nmol/mol of water vapour), who also experimentally showed that adding water vapour to the cylinder annulled this adsorption, water vapour being an excellent competitor for adsorption sites on a metal surface (Vaitinen et al., 2013; Pogány et al., 2016).

Reference gas mixtures for each of the five compounds were filled in this order: SF₆, HFC-125, HFO-1234yf, HCFC-132b and CFC-13. All cylinders are homogenised for a minimum of 6 hours each before measurement using an automated rolling system, with cylinders lying horizontally, and alternating directions. A minimum of one week elapsed between the final cylinder fillings and the measurements.

- 5 Filling different mixtures successively in each cylinder j with different filling duration results in an additional dilution factor for each substance i . The durations are chosen in order to attain the same dilution factor for all substances in one given cylinder. The resulting molar fraction $x_{prep,i,j}$ for substance i in cylinder j is:

$$x_{prep,i,j} = \frac{x_{filled,i} \cdot q_{V5,j} \cdot \Delta t_{i,j} + x_{residual,i} \cdot q_{V5,j} \cdot (\Delta t_{total,j} - \Delta t_{i,j})}{\Delta t_{total,j} \cdot q_{V5,j}} \quad (5)$$

with the total filling duration in each cylinder j being:

$$10 \Delta t_{total,j} = \Delta t_{SF_6,j} + \Delta t_{HFC-125,j} + \Delta t_{HFO-1234yf,j} + \Delta t_{HCFC-132b,j} + \Delta t_{CFC-13,j} + \Delta t_{carrier,j} \quad (6)$$

with $\Delta t_{i,j}$, filling duration of mixture containing substance i in cylinder j ;

$q_{V5,j}$, flow of MFC5 used to regulate the flow into the cylinder during cryo-filling. Equ. 5 can be simplified by removing $q_{V5,j}$, and re-arranging to:

$$x_{prep,i,j} = x_{filled,i} \cdot \frac{\Delta t_{i,j}}{\Delta t_{total,j}} + x_{residual,i} \cdot \left(1 - \frac{\Delta t_{i,j}}{\Delta t_{total,j}}\right) \quad (7)$$

- 15 However, the stability component of the flow $Stab_{q_{V5,j}}$ has to be taken into account in the uncertainty budget (see Equ. 9).

Note that for a given substance, the molar fractions in cylinders vary only due to varying filling durations. This is designed to maximise the correlation between cylinders and therefore improve the resulting internal consistency (defined in Sect. 3.2.3) of the prepared suite of reference gas mixtures. Correlation coefficients between cylinders for one given substance therefore range from 0.96 to 0.99. This set constitutes the METAS-2017 primary calibration scale for SF₆, HFC-125, HFO-1234yf,

- 20 HCFC-132b and CFC-13. All computed prepared values are reported in Table 3.

2.5 Uncertainty of preparation

2.5.1 Uncertainty of prepared values in pmol/mol

- We estimate the uncertainty of the assigned molar fraction, for each substance in each cylinder, following JCGM:2008 by measuring (type A uncertainty) or assigning (type B uncertainty) an uncertainty estimate to each input quantity used in the equations presented in the Method. Expanded uncertainties, noted U, are then calculated with $k = 2$ for a coverage probability of approximately 95 %. All uncertainty computations for the prepared molar fractions are made using the GUMWorkBench program. We describe hereafter the most important contributions to the uncertainty.

- Balance measurement:** The uncertainty of the weighing is estimated by fitting a linear function through the measured masses over time, and using the standard deviation between this linear fit and the residuals for each point as uncertainty estimate ($k = 1$, e.g. Fig. 2). This measurement noise level, noted $Stab_{balance,i}$ in Equ. 8, is in the order of 0.2 % of the

mass loss (for SF₆, whose mass loss was higher and therefore the associated balance noise relatively smaller) to 0.6 %. In addition, we take into account potential biases due to mass calibration of the two used calibration masses (CM1, CM2) and time uncertainty, even if these two contributions are extremely small (see also Sect. S1 in the Supplement).

Permeation chamber temperature stability $Stab_T$: Once carrier gas flow and pressure are kept constant, the permeation rate varies only with temperature. The stability of the permeation chamber temperature is 0.02°C over 20 min ($k = 2$). Based on our experience measuring temperature sensitivity of permeation rate, this corresponds to approx. 0.1 % change in permeation rate. $Stab_{balance,i}$ and $Stab_T$ are given a value of one and included as follow to Equ. 2 in order to take into account their uncertainty contributions:

$$x_{permeation,i} = \frac{m_{1,i} - m_{2,i}}{t_{2,i} - t_{1,i}} \cdot Stab_{balance,i} \cdot Stab_T \cdot purity_i \cdot \frac{1}{M_i} \cdot \frac{V_{m,carrier}}{q_{V,MFM,i}} + x_{residual,i} \quad (8)$$

Substance purity $purity_i$: We use the certificate provided by the substance manufacturer, i.e. $p = 0.999$ for SF₆ and $p = 0.99$ for all other substances. As uncertainty we choose a triangular distribution with 1 as upper boundary, and $1 - 2 \cdot (1 - p)$ as lower boundary. This is a conservative approach.

Impurity in the carrier gas $x_{residual,i}$: For all fillings, a total of three 50 L cylinders of the same type of synthetic air (Pangas synthetic air 5.6) have been used. Absolute impurity levels in one cylinder were measured at Empa on the Medusa-GC-MS system (Miller et al., 2008). The similarity of the impurity level in the other cylinders was checked at METAS on a similar preconcentration-GC-MS system, by trapping a total of 6 litres of synthetic air. For each measured impurity molar fraction $x_{residual,i}$ (ranging from 6 to 30 fmol/mol), we use a triangular distribution centred in $x_{residual,i}$, with zero as lower boundary and $x_{residual,i} \cdot 2$ as upper boundary (see Table S4).

Calibrated values of volumetric flows: $q_{V,MFM,i}$, $q_{V3,i}$ and $q_{V4,i}$ (MFM, MFC3 and MFC4 in Fig. 1) were calibrated using a SI-traceable primary reference standard applying a system of pistons with known volume (Niederhauser and Barbe, 2002). All flows are given at standard temperature and pressure (0°C, 1013.25 hPa). The actual flow has been calibrated using the same gas type, at the same input parameter values (pressure set points before and after each MFM/MFC, MFC set points). A minimum of 4 replicate measurements for each flow set point have been made and the average was taken as best estimate. The stability of each flow over the measurement duration (1-5 minutes) is better than 1 permil. The obtained, relative expanded uncertainty ($k = 2$) for each flow is $U = 0.3 \%$ for MFC3 (due to smaller flows) and $U = 0.2 \%$ for MFM and MFC4.

Filling durations Δt_i : Individual filling durations range from 1060 s to 24110 s (18 min to 6.7 hours, see Supplement Table S3). The associated uncertainty is fixed at $U = 1.8$ s and takes into account the response time of each pneumatic valve as well as the computer time clock uncertainty. In percentage this uncertainty therefore decreases with increasing filling duration.

Stability of filling flow $Stab_{q_{V5,j}}$: The flow stability of MFC5 was challenged due to the relatively small pressure gradient of approx. 800 hPa. We therefore take into account a flow stability component in the uncertainty of $U = 0.1 \%$. This stability component plays a role to explain the internal consistency between cylinders (Sect. 3.2.3).

The resulting, combined uncertainty is then expanded using a coverage factor $k = 2$ (representing a 95 % confidence interval for a Gaussian distribution). The obtained values are documented in Table 3. As an example for cylinder MP-001, we present in Fig. 3 the uncertainty contribution for the most important contributors as pie charts, for each substance. Expanded uncertainties

range from 0.6 % (for SF₆) to 1.3 %. The smallest uncertainty obtained for SF₆ is mostly explained by the high substance purity level inside the permeator (0.999 pure, ten times better than for the other substances), as well as low SF₆ contamination of the carrier gas.

2.5.2 Uncertainty of prepared ratios

5 To calculate the expected internal consistency of the prepared suite of mixtures, we also calculate ratios of assigned values, using cylinder MP-001 as master cylinder. The assigned value of a ratio for substance *i* between cylinder *j* and cylinder MP-001 (marked by subscript 1 hereafter) can be calculated with a very good approximation by:

$$R_{prep,i,j} = \frac{Stab_{T,i,j}}{Stab_{T,i,1}} \cdot \frac{Stab_{qV5,j}}{Stab_{qV5,1}} \cdot \frac{\Delta t_{total,1}}{\Delta t_{total,j}} \cdot \frac{\Delta t_{i,j}}{\Delta t_{i,1}} \quad (9)$$

The terms 'Stab' represent the stability of each filling temperature and each filling flow of MFC5, respectively. Each 'Stab' term is assigned a value of 1 and an expanded uncertainty of $Stab_{T,i,j} = 0.1 \%$ for the temperature stability and $Stab_{qV5,j} = 0.05 \%$ for the flow stability (as discussed in Sect. 2.5.1). The standard uncertainty ($k = 1$) of $R_{prep,i,j}$, calculated using Equ. 9, is hereafter noted $u_{R_{prep,i,j}}$.

Ratio values range from 0.8 to 1.3 and the corresponding expanded uncertainty has an actually constant value of 0.3 % over this limited ratio range (Table 3). Due to the elimination of many common factors when working in such a ratio space, the correlation coefficient between ratios is approximately 0.4.

3 Measurement results and discussion

3.1 Measurement method

The relative molar fractions of the five compounds in the eleven samples MP-001 – MP-011 were determined using Medusa gas chromatography mass-spectrometry (GC-MS) methods (Miller et al., 2008; Arnold et al., 2012). Medusa GC-MS systems have been in use in AGAGE for hourly field and laboratory measurements of more than 50 halogenated compounds. In brief, it consists of a multi-port inlet, a sample drying system (nafion driers), a custom-designed preconcentration system, a capillary GC column (CP-PoraBOND Q, 0.32 mm ID x 25 m, 5 μm film thickness, Varian Chrompack) and a quadrupole mass spectrometer (Agilent Technologies, 5975).

Measurements were conducted on the Empa laboratory Medusa GC-MS and consisted of 2 L samples measured alternately with a reference gas measurement. MP-001 was used as the reference sample. Hence all results of the MP-002 – MP-011 samples are expressed as ratios by dividing the area of the sample by the mean of the chromatographic peak area of the bracketing MP-001 measurements. Minor analytical modifications compared to the routine field measurements were adopted. In particular, to enhance precision of the measurements, compounds, which chromatographically elute near those of interest, were omitted from acquisitions, and the electron multiplier was elevated to enhance the signal size. Integration of the chromatographic peaks was done using commercial software (GCWerks). Detection limits, defined here as three times the noise level, are 0.015 pmol/mol for SF₆, 0.02 pmol/mol for HFC-125, 0.01 pmol/mol for HFO-1234yf, 0.015 pmol/mol for HCFC-132b

and 0.07 pmol/mol for CFC-13. All results are expressed as dry-air molar fraction. The system was shown to be free of blanks and linear in the range of molar fractions of our samples (see e.g. Vollmer et al., 2015). The repeatability of the measurements was calculated as the standard deviation (1σ) of the area-ratios. The standard deviation of the mean was obtained by dividing by the square root of n , n being the number of measurements.

5 3.2 Measurement results

Quantifying analyser response, correcting results and identifying potential outliers is done in an iterative manner. First, all measurement results with their standard deviation are used to calculate a first analyser response function. Using this function, all measurements results are corrected. The corrected values are then compared to the assigned value. Based on the results of this test, potential outliers are excluded, and an adjusted analyser response is calculated, etc. Details of the calculations are presented hereafter.

3.2.1 Analyser response calibration

Following the approach already developed at SIO, and similar to methods already used for isotopic studies (e.g., Dansgaard, 1953; Craig, 1957), we compare measured and assigned values in the ratio space, for three reasons. First, the mass spectrometer used for analysis is naturally drifting over time and to correct for this effect, measured areas are expressed as area ratios relative to the bracketing mixture used as standard, here MP-001. The most precise measurement result given by the MS is therefore a ratio of areas. Second, due to the preparation design made to maximise correlation between cylinders for one given substance, here again the prepared ratio $R_{prep,i,j}$ has an uncertainty much smaller than each molar fraction separately, because when calculating these ratios many constant factors cancel out (Equ. 9). The uncertainty components that still have to be taken into account are mostly those related to the stability over time of the preparation system, i.e. the stability of the permeation temperature, the stability of each MFC flow (negligible, except for MFC5), and the filling duration uncertainty. Expanded uncertainties in ratio space are therefore 0.3 %, compared to expanded uncertainties of 0.6 % to 1.3 % in the molar fraction space (Table 3). Third, the correlation between values of assigned ratios is much smaller (in the order of 0.4) than the correlation between assigned molar fraction values, and therefore using ratios is again better indicated to estimate the fit between assigned values and instrument response (Sect. 5.4.2 in ISO 6143, 2001).

To calibrate the measured value, we therefore determine the analyser response function in ratio space, i.e. measured ratio vs assigned ratio. We therefore can compare a maximum of 10 ratio values, using 11 cylinders. An example is given in Fig. 4.

The analyser response is calculated using a linear fit due to the relatively small number of measured values as well as the good linear response of the MS over this limited range:

$$R_{meas,i,j} = a_i \cdot R_{prep,i,j} + b_i \tag{10}$$

with $R_{meas,i,j}$, the measured area ratio for substance i in cylinder j .

The fit coefficients a_i and b_i are computed using a bivariate weighted linear fit, following the York algorithm (York et al., 2004) as described in Cantrell (2008) (Supplement, Sect. S3), coded in Octave (results in Table 4). As an additional test we

ran the same fitting algorithm forcing $b_i=0$. Interestingly, for each substance the obtained slope can then not be distinguished from a slope of 1 within uncertainties (Table 4). This suggests that the analyser response is linear within the tested range and within stated uncertainties. The deviation in the corrected values for cylinder MP-001 is no more than 0.2 %, but varies up to 0.5 % for MP-005 and 1 % for MP-006, which are at the upper and lower end of the scale. We also calculated a_i and b_i using a simpler weighted linear fit considering only weights associated with the measured values, giving very similar results (difference < 0.03 %).

The measured & corrected ratios $R_{meas,corr,i,j}$ and values in pmol/mol $x_{meas,corr,i,j}$ are calculated using:

$$R_{meas,corr,i,j} = \frac{R_{meas,i,j} - b_i}{a_i} \quad (11)$$

$$x_{meas,corr,i,j} = R_{meas,corr,i,j} \cdot x_{prep,i,1} \quad (12)$$

with $x_{prep,i,1}$, the prepared value in pmol/mol for substance i in cylinder MP-001.

Hereafter we refer to $R_{meas,corr,i,j}$ as measured ratios and to $x_{meas,corr,i,j}$ as measured molar fractions.

3.2.2 Verification test and exclusion of outliers

To compare the measured results to the prepared results, we use the measured ratios $R_{meas,corr,i,j}$ and their associated uncertainties $u_{R_{meas,corr,i,j}}$ calculated according to Equ. 11 (Supplement, Table S5). We then calculate the verification criteria (Sect. 5.2.2 in ISO 6143, 2001):

$$d_{i,j} = |R_{meas,corr,i,j} - R_{prep,i,j}| - \left(2 \cdot \sqrt{u_{R_{meas,corr,i,j}}^2 + u_{R_{prep,i,j}}^2} \right) \leq 0 \quad (13)$$

Using this procedure, after the first iteration cylinder MP-008 is excluded as outlier for SF₆, HFC-125 and HFO-1234yf, the measured value being systematically too low. Because this represents already the majority of all substances, we decided to exclude this cylinder for HCFC-132b and CFC-13 as well. After the second iteration cylinder MP-002 is excluded for HFC-125, MP-010 for HFO-1234yf and MP-003 for HCFC-132b. After the third iteration, cylinder MP-010 is identified as an outlier for HCFC-132b.

For cylinder MP-008 (a 4.5 L Essex cylinder filled at 24 bar, Table 1), we note that the difference between measured value and assigned value is large for SF₆ (the first filled substance) and more or less decreases until showing no particular offset for CFC-13 (being filled last). An explanation for such a time varying offset could be a potential leak over time, affecting more the substance that was filled first.

During filling of cylinder MP-002 for HFC-125, we noted that the mass flow controller sampling the flow into the cylinder (MFC5, Fig. 1) was suffering from large instability during the 15 s towards the end of the filling period. This particularly high instability was very likely due to both the small pressure gradient over MFC5, and additionally the small flow from MFC4 (4 L/min) compared to the flow sampled by MFC5 (3 L/min), making the pressure control before MFC5 (done by PrC2) to be particularly challenging. To improve the pressure regulation by PrR2 and therefore limit MFC5 instability, an additional

buffer volume (approx. 1 L, stainless steel) was added on the flow path just before PrC2. This instability did not occur during subsequent fillings.

We tentatively explain cylinder MP-003 being an outlier for HCFC-132b by the fact that this cylinder was filled first after a synthetic air cylinder exchange. Additional tests showed that HCFC-132b is affected by regulator contamination and takes 5 time to clear out. The regulator was purged three times before using the synthetic air but perhaps this was not sufficient. The system being then continuously running, the purge was already sufficient for the second filling not to be affected.

We unfortunately do not have a specific explanation for cylinder MP-010 being an outlier for HCFC-132b and HFO-1234yf, potentially pointing towards operator error, and highlighting the need of a verification step. We however observe that most outliers are cases of substance loss (Fig. 5) and affect cylinders having the smallest total amount of gas filled and the highest 10 surface/volume ratio (i.e. Essex cylinder 4.5 L, 24 bar). We would therefore in the future favour filling in cylinders of larger volume and pressure, as well as a further automatising the cryo-filling process to limit human intervention as much as possible as well as to increase the safety of the procedure. Furthermore, we plan to investigate if the observed substance losses occurred by adsorption on cylinders walls or beforehand in the preparation system. To do so, a comparison of the molar fraction in the mixture exiting the magnetic suspension balance/dynamic dilution system with the same mixture filled in cylinders will be 15 performed. The recent installation of a measurement system for halogenated gases at METAS in the same laboratory makes this possible. If the adsorption indeed occurs in the cylinders, it will be tested if adding water vapour earlier in the sequence of fillings may help to limit this adsorption.

After excluding the outliers, we can observe no systematic bias between mixtures filled in electro-polished cylinders from those filled in SilcoNert-coated cylinders. This result gives us confidence that there is also no identifiable loss of the halogenated 20 substances on cylinder surfaces.

3.2.3 Internal consistency of the suite

To give an estimation of the preparation reproducibility, we calculate the so-called 'internal consistency' of the suite of mixture (e.g., Prinn et al., 2000). This parameter quantifies the difference between assigned values and measured values, for each substance.

25 First, we calculate the difference d for each substance, in each cylinder:

$$d_{i,j}[\%] = \frac{x_{meas,corr,i,j} - x_{prep,i,j}}{0.5 \cdot (x_{meas,corr,i,j} + x_{prep,i,j})} \cdot 100 \quad (14)$$

and the associated uncertainty:

$$u_{d_{i,j}}[\%] = \frac{\sqrt{u_{x_{meas,corr,i,j}}^2 + u_{x_{prep,i,j}}^2}}{0.5 \cdot (x_{meas,corr,i,j} + x_{prep,i,j})} \cdot 100 \quad (15)$$

We then calculate the weighted mean difference for each substance, over the set of cylinders (without outliers):

$$30 \quad d_{W,i}[\%] = \frac{\sum W_{d_{i,j}} \cdot d_{i,j}}{\sum W_{d_{i,j}}} \quad \text{with} \quad W_{d_{i,j}} = \frac{1}{u_{d_{i,j}}^2} \quad (16)$$

We use the corresponding weighted standard deviation $u_{d_{W,i}}$ of $d_{W,i}$ as estimator of the internal consistency:

$$u_{d_{W,i}} [\%] = \sqrt{\frac{\sum_{j=1}^N W_{d_{i,j}} (d_{i,j} - d_{W,i})^2}{\frac{N-1}{N} \cdot \sum_{j=1}^N W_{d_{i,j}}}} \quad (17)$$

The calculated internal consistencies for each substance are reported in Table 4. This measured internal consistency is due to measurement reproducibility of the Medusa-GC-MS system as well as how stable the preparation system is (i.e., including all potential sources of random noise in the preparation system, any systematic bias being on the contrary canceled out when working in ratio space).

3.3 Final assigned uncertainties

3.3.1 According to ISO-6142-1:2015

According to ISO 6142-1 (2015), the expanded uncertainty ($k = 2$) of the final molar fraction after the verification step can be calculated as:

$$U_{x_{meas,corr,i,j},ISO} = \sqrt{u_{prep,i,j}^2 + u_{meas,corr,i,j}^2 + (x_{prep,i,j} - x_{meas,corr,i,j})^2} \quad (18)$$

This formula includes the uncertainty of the preparation as well as the uncertainty of the verification, with equal weights. The resulting uncertainties range from 0.7 % for SF₆ to 1.5 % for HFO-1234yf (excluding outliers). In particular, here the uncertainties for HFC-125 and HCFC-132b become smaller (1 %) than the prepared uncertainty (1.3 %), because in this formula uncertainties from preparation and measurement are arbitrarily given equal weights.

3.3.2 According to preparation and measurement equations

We calculate the uncertainty of $x_{meas,corr,i,j}$ using the uncertainty of each component defining it, according to Equ. 12. This method therefore includes both the preparation uncertainty (through $x_{prep,i,1}$) and the measurement uncertainty (through $R_{meas,corr,i,j}$). The expanded uncertainty ($k = 2$) ranges from 1 % for SF₆ to 2 % for HCFC-132b and CFC-13 (Table 5). The disadvantage of using this method is that $u_{R_{prep,i,j}}$ is included twice, once in $u_{R_{meas,corr,i,j}}$ through a_i and b_i , and once in $u_{x_{prep,i,1}}$ that includes the same stability factors as in $u_{R_{prep,i,j}}$ (Equ. 2 and 7). To correct for this effect we would need to remove the stability factors in $u_{x_{prep,i,1}}$. However, the uncertainty budgets of the prepared mixtures (Fig. 3) suggest that this contribution is overall minor (from less than 1 % to 5 % of the total), and removing one occurrence of $u_{R_{prep,i,1}}$ would be a marginal change.

We favour this method to calculate the uncertainty, where the sensitivity of the final value to the preparation and verification uncertainties are taken into account, through Equ. 12, and where the resulting uncertainty is the largest – it is also the most conservative approach.

4 Comparison to other existing reference gas mixtures

Cylinder MP-001 was used to compare the METAS-2017 calibration scale to other scales, using Empas Medusa-GC-MS as comparator. We report hereafter a brief description of each calibration scale followed by the results of the comparisons, for SF₆, HFC-125, HFO-1234yf and CFC-13. For HCFC-132b, there was no other scale available for comparison.

5 4.1 Description of calibration scales

4.1.1 SF₆

SIO-05: SIO developed in the 1990s a preparation method using a bootstrap technique to make a suite of standards for halogenated compounds at pmol/mol levels (Prinn et al., 2000; Weiss et al., 1981). This technique relies on the preparation of a first primary standard for CO₂ at ppm levels (work of C. D. Keeling at SIO). CO₂ is then used as bootstrap gas to prepare a second mixture containing CO₂ and N₂O with a known prepared N₂O/CO₂ ratio, close to atmospheric conditions. The CO₂/N₂O ratio is prepared gravimetrically, by filling pure CO₂ and N₂O in individual glass vials, flame-sealing the vials, weighing them, and mixing their content into an aliquot. In this second standard the N₂O molar fraction is assigned using this known, gravimetrically prepared N₂O/CO₂ ratio, and a CO₂ molar fraction calibration vs the CO₂ calibration scale. In a third step N₂O is used as bootstrap gas to produce a new mixture containing N₂O and halogenated gases, again with ratios close to ambient conditions. Knowing these halogen/N₂O ratios and by measuring the N₂O molar fraction against the N₂O primary standard, each halogen molar fraction is determined. This preparation system therefore combines gravimetric preparation of ratios and measurement of one of them vs another suite of standards.

For comparison with the METAS-2017 calibration scale, we use so-called 'tertiary tanks' filled with real air at SIO and calibrated vs an SIO 'secondary standard', itself calibrated vs the suite of gravimetrically prepared, primary reference gas mixture defining the calibration scale for each compound. It is therefore necessary to take into account the uncertainty due to scale propagation, i.e. the measurement repeatability of the secondary vs the primary tank, and of the tertiary vs the secondary tank. The same principle applies to all other substances on a SIO calibration scale measured from a tertiary tank vs the METAS-2017 scale.

When preparing the primary calibration scales for halogenated gases, SIO did not assign an uncertainty following JCGM:2008, but still the internal consistency of the scale was precisely determined as being $u = 0.4 \%$ for SF₆ (R.F. Weiss, pers. com. Oct. 2017). Regular comparison with NOAA, comparing results at co-located monitoring stations (Rigby et al., 2010) or through cylinder exchanges (Hall et al., 2014), show agreement within 0.998 % or better for SF₆. NOAA recently determined the uncertainty of its SF₆ reference gas mixtures following JCGM:2008 as 0.062 pmol/mol ($k = 2$) for molar fractions in the range 7–10 pmol/mol, equivalent to 0.6 % to 0.9 % (Lim et al., 2017). The preparation method followed by NOAA has similarities with to the one developed at SIO, being based on static gravimetry as well. We therefore conservatively use an uncertainty for the SIO-05 assigned molar fraction of 1 % ($k = 2$).

METAS-2016: A set of two primary standards was prepared at METAS in 2016 (METAS-2016 calibration scale) to participate in an intercomparison for SF₆ in air at atmospheric molar fractions organised by the World Calibration Centre for SF₆

(Lee et al., 2017). These two standards were prepared using a similar method as for the METAS-2017 scale using permeation, dynamic dilution and cryo-filling of a nmol/mol molar fraction mixture containing SF₆ only in synthetic air (for more details see Lee et al., 2017). After homogenisation this mother mixture was dynamically diluted into two daughter mixtures at 8 and 10 pmol/mol, themselves transferred in cylinders by cryo-filling. The expanded uncertainty of the prepared standards is
5 U = 1.3 %.

NOAA-2014: We use for comparison the known SF₆ conversion factor between the NOAA-2014 and SIO-05 calibration scales of NOAA-2014/SIO-05 = 1.002 ± 0.002 (Krummel et al., 2017), based on measurements at co-located stations and tank exchanges. This conversion factor is depicted by a green dashed line on Fig. 6.

4.1.2 HFC-125

10 **SIO-14:** We use the SIO calibration scale for HFC-125 prepared in 2014 following the same method as the SIO scale for SF₆. The estimated uncertainty for this scale is 4 % (Prinn et al., 2000).

METAS-2015: A first HFC-125 reference gas mixture was produced by METAS in 2015, with expanded uncertainty U = 2%. The preparation method consisted of a permeation step using MSB-Violetta, generating a mixture at approx. 85 nmol/mol, transferred to SilcoNert-coated cylinder by cryo-filling. This mother mixture was then diluted into two daughter mixtures both
15 at 17 pmol/mol, using dynamic dilution steps. Diluted daughter mixtures were then directly injected into the Medusa-GC-MS (Supplement, Sect. S4 and Fig. S1, S2 and S3).

NOAA-2008: We use the published conversion factor NOAA-2008/SIO-14 of 0.946 ± 0.008 (Supplement of Simmonds et al., 2017, p. 11). This factor was determined by comparing AGAGE continuous measurements by Medusa-GC-MS and NOAA flask samples taken from 3 co-located sites.

20 **UB-98:** Before using the SIO-14 scale for HFC-125 within AGAGE, a primary calibration scale prepared by University of Bristol was in use (UB-98, O'Doherty et al., 2004, 2009). The known conversion factor UB-98/SIO-14 is 0.9237 (C.M. Harth and R.F. Weiss, pers. com., 2018).

4.1.3 HFO-1234yf

Empa-2013: In 2013 Empa prepared a first calibration scale for a set of newly emitted compounds, including HFO-1234yf at
25 ≈2 pmol/mol, using volumetric dilution (Supplement of Vollmer et al., 2015). The molar fraction uncertainty is likely no more than U ≤ 30 %.

METAS-2015: Two reference gas mixtures for HFO-1234yf were produced in 2015 at 2 pmol/mol following the same method as for the METAS-2015 standards for HFC-125 (Supplement, Sect. S4). The resulting expanded uncertainty was U = 2.5%.

4.1.4 CFC-13

Interim-98: For CFC-13, a preliminary calibration scale was developed at the University of Bristol based on dilution of a high molar fraction reference gas mixture purchased from a commercial manufacturer (Linde Gas, hereafter Interim-98 scale, O’Doherty et al., 2004). This preliminary scale has been used within AGAGE until 2017. It would be very difficult to assign an uncertainty to this mixture, and it should be noted that the aim of this Interim-98 standard was to serve as intermediate anchor in order to be able to report CFC-13 internally within AGAGE. We tentatively assign an uncertainty of 5 %. The Interim-98 scale was transferred to the SIO suite of secondary standards by measurement comparisons, and therefore the tertiary standards used at Empa have a CFC-13 assigned value on the Interim-98 scale. We provide comparison to this calibration scale to contribute to the documentation of the scale transfer from Interim-98 to METAS-2017 for CFC-13, rather than to realise a new intercomparison. Additional details on the scale transfer are given in Vollmer et al. (2018).

4.2 Results of comparisons

We express the results as ratio values, i.e. the value expressed on the METAS calibration scale divided by the value expressed on the historical calibration scale (SIO-05, SIO-14, Empa-2013 and Interim-98). A ratio of one would correspond to a perfect agreement between the two compared scales.

4.2.1 SF₆

The average ratio METAS-2017/SIO-05 using all available results is 1.002, i.e. the deviation from 1 is clearly within the ratio uncertainty (Fig. 6). This demonstrates that the two calibration scales are concordant with each other. SF₆ is also the substance for which the NOAA/SIO ratio is closest to 1 (NOAA-2014/SIO-05 ratio of 1.002). Combining these two ratios, one obtains a METAS-2017/NOAA-2014 ratio for SF₆ of 1.000. Such excellent agreements, in particular between standards produced by dynamic and static methods, can in addition to the reliability of both preparation methods be explained by the stability and non-reactivity (for instance low adsorptivity) of this substance.

4.2.2 HFC-125

The METAS-2017 calibration scale for HFC-125 is 7 % lower than the SIO-14 scale (METAS-2017/SIO-14 = 0.929). For HFC-125, the value assigned on the SIO-14 scale is not corrected for potential impurities in the pure HFC-125 substance used for the preparation (C.M. Harth, pers. com. 2017), while a 1 % correction is used for the METAS-2017 scale. Assuming HFC-125 sources were similar, and would both scales apply the same procedure, the disagreement would be reduced to 6 %. We plan for future reference gas mixture preparation to check the presence of substance impurities in permeators in a systematic way, to get a better estimate of the purity fraction as well as to quantify any potential cross-contamination, if any. For the METAS-2017 scale, we checked in particular the absence of HFC-132b as impurity in the HFC-125 permeator (see Section S5 in Supplement).

Comparison of the METAS-2015 and SIO-14 calibration scales showed as well a METAS value lower than the SIO value, by 4 % (METAS-2015/SIO-14 = 0.963). The ratio NOAA-2008/SIO-14 for HFC-125 is 0.946, one of the largest discrepancies observed between SIO and NOAA for halogenated gases (pers. comm. P.B. Krummel and B.D. Hall, Jan. 2018). Thus, comparing the SIO-14 calibration scale for HFC-125 to these three other scales (NOAA-08, METAS-2015, METAS-2017) points to a probable overestimation of the SIO-14 value (due e.g. to substance losses by adsorption) or that the values on the other calibration scales are underestimated (due to e.g. unaccounted for contamination). Cases of gas standards produced by dynamic methods yielding results lower than those produced by static method have already been observed several times with reactive substances prone to adsorption on surfaces, such as ammonia on stainless steel (van der Veen et al., 2010). This is due to the fact that when applying dynamic methods, potential losses by adsorption on surfaces can be canceled out when the generation process reaches equilibrium, after a sufficiently long stabilisation time. Interestingly, the METAS-2017 calibration scale is even lower than the METAS-2015 scale, by 3 %. Significant improvements in the generation process were made for the METAS-2017 scale to considerably minimise the total exposition to metal surfaces, compared to the METAS-2015 scale. This improvement is potentially the cause of the observed 3 % shift towards lower values.

4.2.3 HFO-1234yf

For HFO-1234yf, the two METAS calibration scales are lower than the Empa-2013 scale with in average METAS-2017/Empa-2013 = 0.910 and METAS-2015/Empa-2013 = 0.971. METAS-2017 is thus lower than METAS-2015 by 6 %. As with HFC-125, this latter ratio is significantly lower than 1. Within all halogenated substances studied here, this is the largest discrepancy observed between static (Empa-2013) and dynamic (METAS-2017) preparation methods, as well as the largest offset between different METAS scales. In addition, within the METAS-2017 suite of cylinders the largest offsets for outliers are also observed for HFO-1234yf (Fig.5, HFO-1234yf in MP-010 and MP-008 is ≈ 5.5 % too low). All these observations suggest that preparing primary reference gas mixtures for HFO-1234yf with $U \leq 2$ % may require dynamic generation methods, with additional minimisation of contact with surfaces.

4.2.4 CFC-13

Three cylinders on the Interim-98 calibration scale for CFC-13 have been compared to cylinder MP-001 on the METAS-2017 scale. For documentation purposes, we report the average ratio METAS-2017/Interim-98 measured as 1.055 (Fig. 6). The comparison was extended to additional cylinders in Vollmer et al. (2018) to ensure a reliable scale transfer from Interim-98 to METAS-2017 [within the AGAGE network](#).

5 Conclusions

We have developed a suite of primary, SI-traceable reference gas mixtures in 11 pressurised cylinders for SF₆, HFC-125, HFO-1234yf, HCFC-132b and CFC-13 in synthetic air, at atmospheric molar fractions. This suite constitutes the METAS-2017 primary calibration scales for these 5 halogenated compounds. This work therefore combines the advantages of SI-traceable

reference gas mixture preparation with a primary calibration scale system for its use as anchor by a monitoring network. Such a combined system allows to maximise the compatibility (as defined by GAW) within the network while linking all reference values to the international system of units (SI) and assigning carefully estimated uncertainties following international guidelines (JCGM 100:2008).

5 Expanded uncertainties of the METAS-2017 calibration scale after verification ranges from 1 % to 2 % at a 95 % confidence interval. Such **molar** fractions at the pmol/mol level with associated expanded uncertainties of no more than 2 % clearly mark a step beyond the state of the art for dynamic methods. We have demonstrated the applicability of dynamic gravimetric generation methods coupled to cryo-filling in cylinders to prepare primary reference gas mixtures for halogenated compounds as low as 1 pmol/mol. For stable compounds for which static gravimetric methods are also applicable (e.g., SF₆), these latter
10 methods perform better in terms of expanded uncertainties (e.g., Lim et al., 2017), but we emphasise that using a completely independent preparation method may always help to detect potential systematic biases affecting one method or the other. From a metrological point of view, this preparation exercise is therefore highly valuable, ensuring comparability and redundancy of prepared reference gas mixtures.

Comparison of the METAS-2017 calibration scale for SF₆ with the scale prepared by SIO (SIO-05) leads to a conversion
15 factor METAS-2017/SIO-05 of 1.002, illustrating the concordance of the two scales within uncertainties. An indirect comparison with the NOAA calibration scale also yields agreeing results. The excellent concordance obtained for SF₆ gives confidence in the reliability of the presented dynamic-gravimetric method to prepare standards for other, more reactive compounds, e.g. HFC-125.

For HFC-125, known as more reactive than SF₆, the METAS-2017 calibration scale is measured as 7 % lower than SIO-14. In
20 addition the METAS-2017 scale for HFO-1234yf is measured 9 % lower than Empa-2013. Such an offset towards lower values for standards prepared using dynamic generation methods by contrast to methods using static gravimetry or static volumetry has been previously observed for other reactive compounds such as ammonia. This underlines the risk of substance losses by e.g. adsorption on surfaces for HFC-125 and HFO-1234yf (and potentially other reactive substances). Dynamic generation methods and/or minimisation of contact on surfaces should therefore be favoured when preparing primary reference gas mixtures for
25 such reactive substances.

Data availability. All data used to prepare the METAS-2017 suite and results of cylinder measurements within the suite are available in this article and its Supplement.

Competing interests. The authors declare no competing interest.

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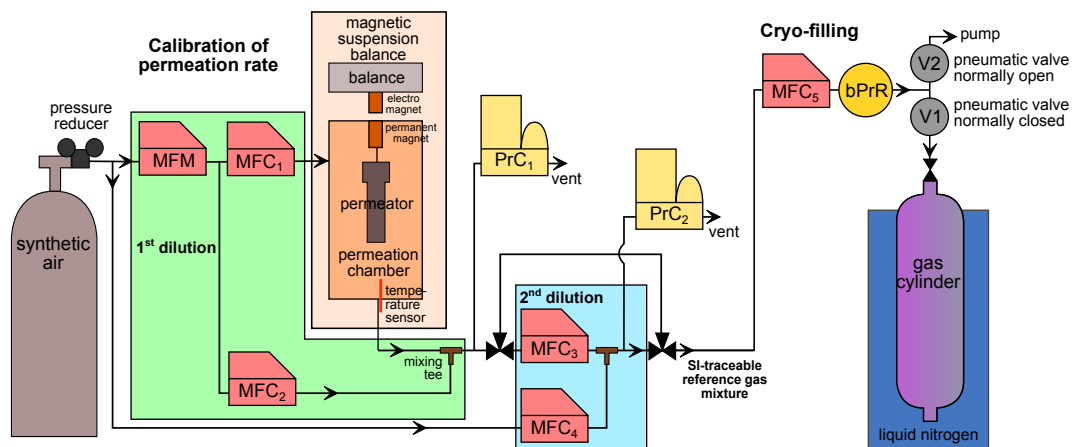


Figure 1. Schematic of the dynamic-gravimetric preparation method. MFM: thermal mass flow meter. MFC: thermal mass flow controller. PrC: pressure controller. bPrR: back (downstream) pressure regulator. V1 and V2: pneumatic valves.

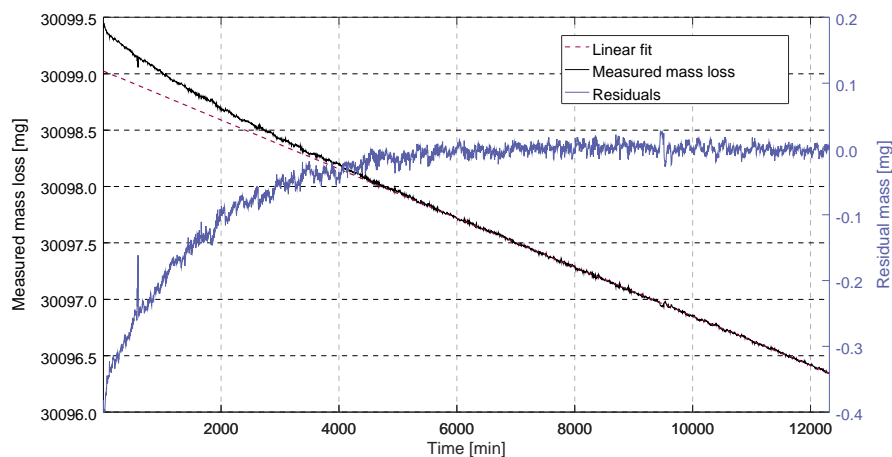


Figure 2. Example of measured mass loss rate for CFC-13 with magnetic suspension balance Violetta. After stabilisation of the permeation rate (first 6000 min), the mass loss becomes linear - the measured mass loss (6000 min to 12000 min) can be fitted to a linear function, yielding a mass loss rate of 217.44 ng/min. The residuals of the fit (blue line, right axis) are centered around zero and randomly distributed.

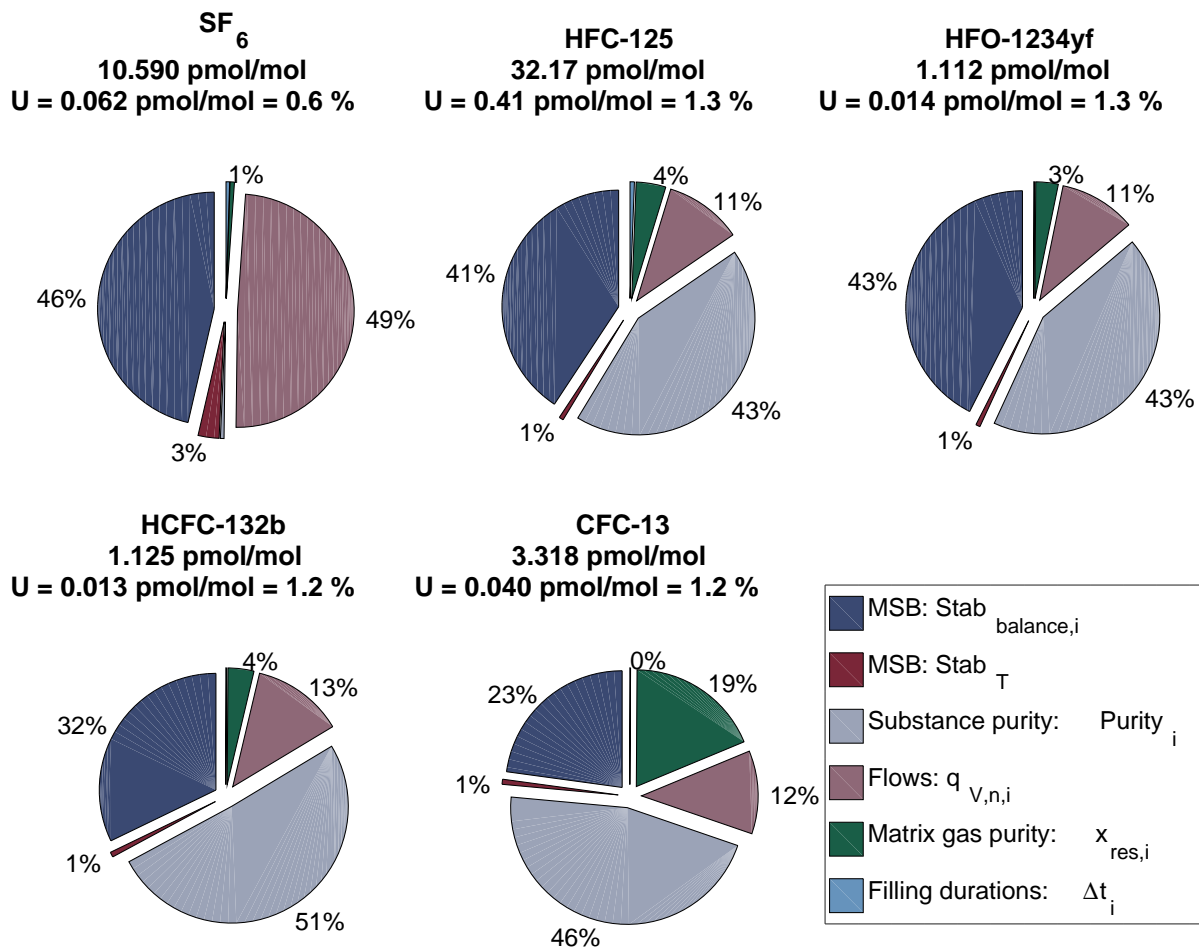


Figure 3. Uncertainty budget of the preparation for cylinder MP-001. The pie charts depict the most important sources of uncertainties, in percent, for each substance (see also Sect. 2.5.1). U is the relative expanded uncertainty of the preparation ($k = 2$). All input values used to calculate the budget for SF₆ in MP-001 are detailed in Table 2.

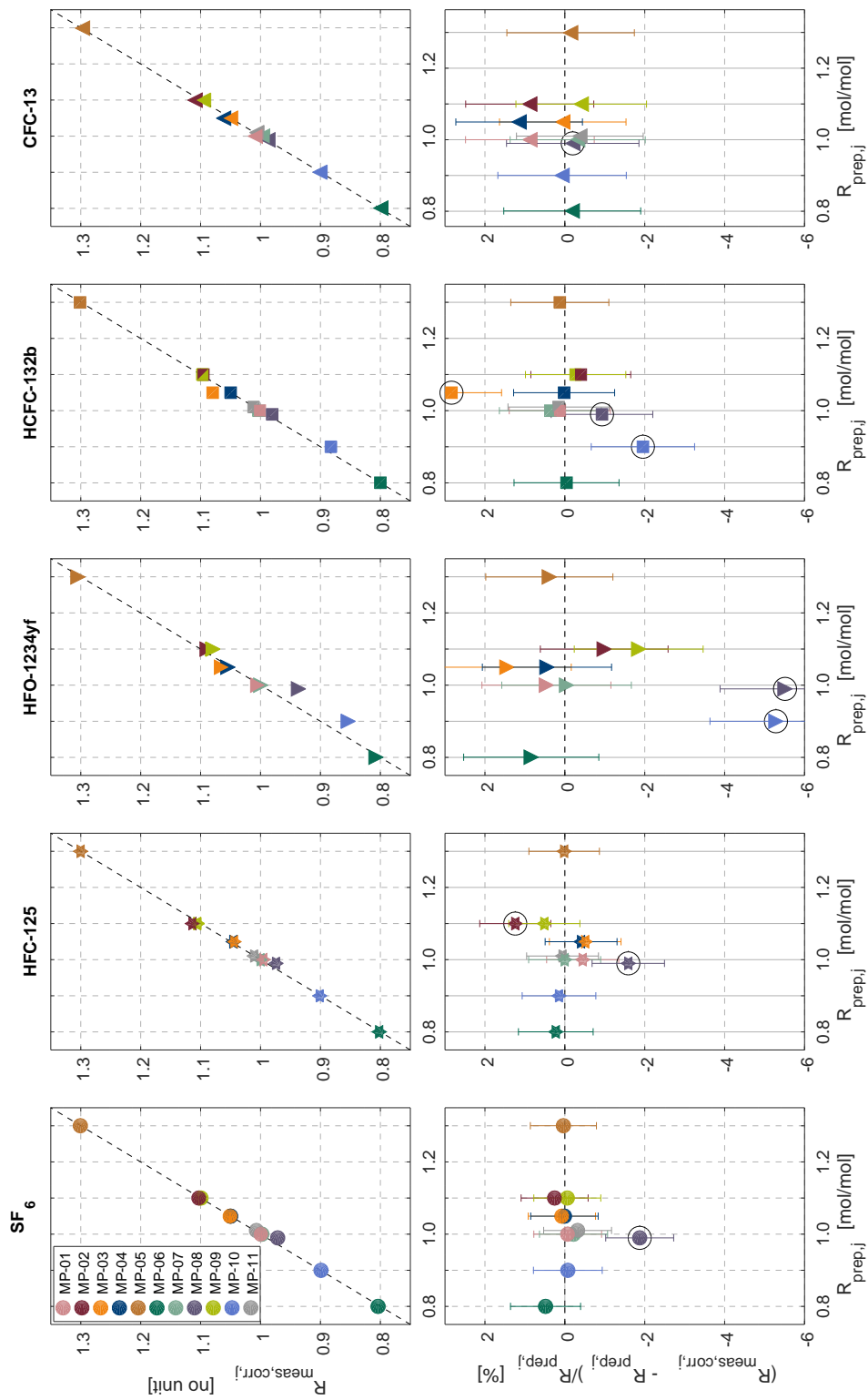


Figure 4. Internal consistency estimates for the METAS-2017 primary calibration scales. Top: Measured ratios $R_{meas,corr,i,j}$ vs prepared ratios $R_{prep,i,j}$. $R_{prep,i,j}$ represents the prepared molar fraction in cylinder j divided by the corresponding prepared molar fraction in cylinder MP-001 (Equ. 9). The unit of $R_{prep,i,j}$ is therefore mol/mol. $R_{meas,corr,i,j}$ is a signal ratio and unit-less. Bottom: Difference, in percent, between prepared and measured ratios. The error bars take into account the uncertainty of $R_{prep,i,j}$ as well as the measurement standard deviation of the mean and represent a 95% confidence interval. Outliers excluded from the calculation of the analyser response function are highlighted by black open circles.

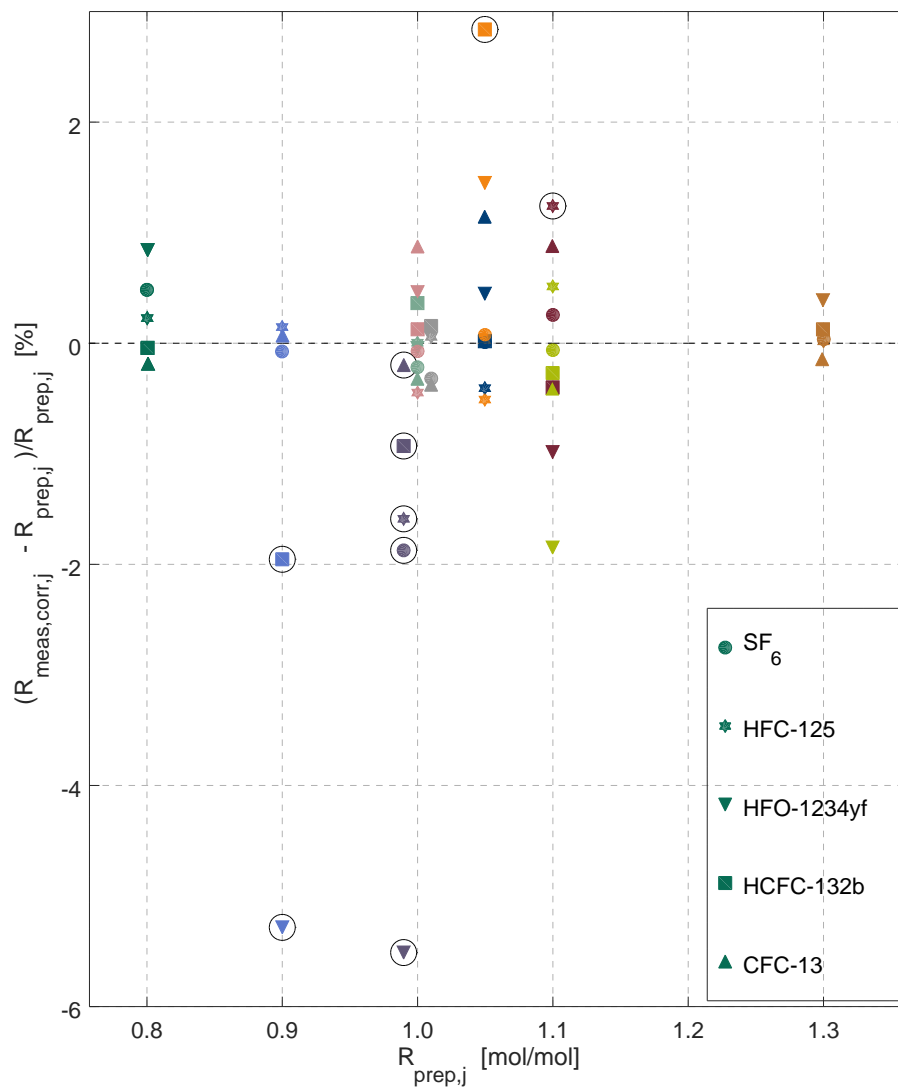


Figure 5. Overview of internal consistency estimates for the METAS-2017 calibration scales. Prepared and measured ratios of molar fractions for each substances (shown by different marker types) in each cylinder (shown using different colors, see color legend in Fig. 4). Outliers are highlighted by black open circles (see main text Sect. 3.2.2).

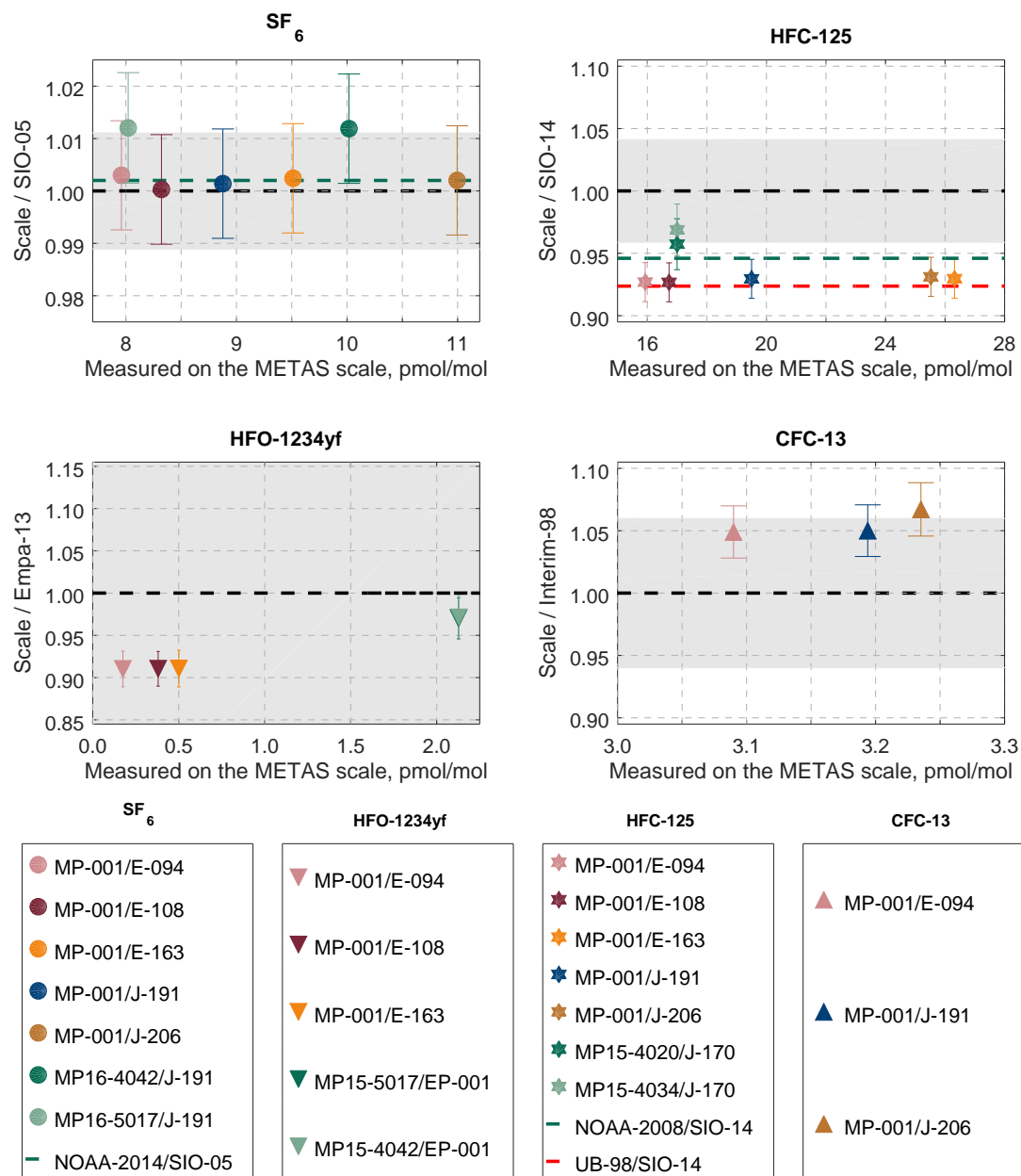


Figure 6. Comparison to existing calibration scales. Results are shown as ratios of values on the METAS scale divided by values on the historical scale. Results where both scales are in perfect agreement would line on the 1:1 line (dashed, black line). The grey area represents the uncertainty associated with the historical scale plus the scale transfer uncertainty (see description in Sect. 4.1). Markers represent measurement results of cylinder comparisons. Error bars on the markers take into account uncertainty of the METAS scales as well as the measurement reproducibility. Results on METAS and historical scales are in agreement within uncertainties as soon as the error bars touch the grey area. Additional dashed lines represent published conversion factors between SIO scales and other scales, i.e. NOAA (green) and University of Bristol (UB-98, red). An overview of results from this work and used conversion factors can also be found in Table 6.

Table 1. Overview of cylinders used to store the reference gas mixtures.

Cylinder reference	MP-003 to MP-006	MP-001	MP-002	MP-007 to MP-011
Manufacturer	Swagelok	Essex Industries, MO, USA		
Material	Stainless steel 304L	Stainless steel 304L		
Treatment	SilcoNert2000 coating	Electropolishing		
Volume	2.25 L	34 L	34 L	4.5 L
Pressure	60 bar	65 bar	30 bar	20 bar
Volume filled, L @ STP	135	2210	1020	90
Surface/volume, m ⁻¹	1	0.4	0.8	2.5

Table 2: Primary reference gas mixtures for SF₆ filled in cylinder MP-001: List of variables taken into account in the uncertainty budget. Variables and corresponding numbers in *italic* are intermediate results. To fill SF₆ in the other cylinders, only the filling durations were modified (i.e. last section in this Table), all other input values remained unchanged. Input values used to calculate molar fractions and expanded uncertainties for the other substances can be found in the Supplement, Tables S1, S2 and S3.

Quantity	Value	Standard uncertainty ($k = 1$)	Unit	Distribution	Sensitivity coefficient	Uncertainty contribution pmol/mol	%
Weighing of SF ₆ permeation device							
m_{1,SF_6}	28.44957646	0.00000289	g	rectangular	790	2.30E-004	0
m_{2,SF_6}	28.43612094	0.00000289	g	rectangular	-790	-2.30E-004	0
t_{1,SF_6}	5999.45	0.025	<i>min</i>	normal	1.30E-003	3.30E-005	0
t_{2,SF_6}	14130.8	0.025	<i>min</i>	normal	-1.30E-003	-3.30E-005	0
$Stab_{balance,SF_6}$	1	0.002	-	normal	11	0.021	46.3
$Permeation_{SF_6}$	<i>1654.77</i>	<i>3.31</i>	<i>ng/min</i>				
$Stab_T$	1	0.0005	-	normal	11	5.30E-003	2.9
$Purity_{SF_6}$	0.9995	0.000204	-	triangular	11	2.20E-003	0.5
Molar volume of carrier gas							
$fraction_{O_2}$	0.2	0.005	-	normal	-6.10E-003	-3.10E-005	0
d_{O_2}	1.4287	0.00015	kg/m ³	normal	-1.6	-2.50E-004	0
d_{N_2}	1.2501	0.00015	kg/m ³	normal	-6.6	-9.90E-004	0.1
M_O	15.9994	0.000151	g/mol	triangular	0.15	2.20E-005	0
M_N	14.006855	0.000174	g/mol	triangular	0.59	1.00E-004	0
$V_{m,carrier}$	<i>28.8107</i>	<i>0.0199</i>	<i>L/mol</i>				

Table 2: Continued.

Quantity	Value	Standard uncertainty ($k = 1$)	Unit	Distribution	Sensitivity coefficient	Uncertainty contribution pmol/mol	%
Molar mass of SF ₆							
M_S	32.0675	0.00347	g/mol	triangular	-0.072	-2.50E-004	0
M_F	18.998403163	0.000000003	g/mol	normal	-0.43	-1.30E-009	0
M_{SF_6}	<i>146.05792</i>	<i>0.00347</i>	<i>g/mol</i>				
Dynamic dilution							
$q_{V,carrier,SF_6}$	4594.97	4.59	mL/min	normal	-2.30E-003	-0.011	11.6
q_{V3,SF_6}	10.809	0.0162	mL/min	normal	0.98	0.016	25.9
q_{V4,SF_6}	5115.46	5.12	mL/min	normal	-2.10E-003	-0.011	11.5
f_{SF_6}	<i>2.11E-003</i>	<i>3.79E-006</i>	-				
$x_{residual,SF_6}$	6.00E-003	2.45E-003	pmol/mol	triangular	1	2.40E-003	0.6
x_{filled,SF_6}	<i>116.438</i>	<i>0.34</i>	<i>pmol/mol</i>				
Cryo-filling in cylinder MP-001							
$\Delta t_{SF_6,1}$	4018	0.9	s	normal	2.40E-003	2.20E-003	0.5
$\Delta t_{HFC125,1}$	4018	0.9	s	normal	-2.40E-004	-2.20E-004	0
$\Delta t_{HFC1234yf,1}$	4018	0.9	s	normal	-2.40E-004	-2.20E-004	0
$\Delta t_{HFC132b,1}$	4018	0.9	s	normal	-2.40E-004	-2.20E-004	0
$\Delta t_{CFC13,1}$	4018	0.9	s	normal	-2.40E-004	-2.20E-004	0
$\Delta t_{water,1}$	24110	0.9	s	normal	-2.40E-004	-2.20E-004	0
$\Delta t_{total,1}$	<i>44200</i>	<i>4.58</i>	<i>s</i>				
$Stab_{MFC5}$	1	0.001	-	normal	-0.96	-9.60E-004	0
$x_{prep,SF_6,1}$	<i>10.590</i>	<i>0.032</i>	<i>pmol/mol</i>				

Table 3. METAS-2017 suite of reference gas mixtures: prepared ratios and molar fractions and associated uncertainty with a 95% confidence interval. **Molar fractions for halogenated compounds are expressed in dry synthetic air.** Ratios represent the number of moles of substance i in cylinder j divided by the number of moles of the same substance in cylinder MP-001. $R_{prep,i,j}$ is therefore a molar ratio. Prepared ratios are identical for all substances within a given cylinder and thus only one value per cylinder is reported here. Note: HFO-1234yf was not filled in cylinder MP-011.

Cylinder	6	10	8	1 & 7	11	3 & 4	2 & 9	5
SF₆								
Molar fraction, pmol/mol	8.47	9.53	10.48	10.59	10.70	11.12	11.65	13.77
U, pmol/mol	0.05	0.06	0.07	0.06	0.07	0.07	0.07	0.08
U, %	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6
HFC-125								
Molar fraction, pmol/mol	25.74	28.95	31.84	32.17	32.49	33.77	35.38	41.82
U, pmol/mol	0.33	0.37	0.40	0.41	0.41	0.43	0.44	0.52
U, %	1.3	1.3	1.3	1.3	1.3	1.3	1.2	1.2
HFO-1234yf								
Molar fraction, pmol/mol	0.890	1.001	1.101	1.112	-	1.167	1.223	1.445
U, pmol/mol	0.011	0.013	0.014	0.014	-	0.015	0.015	0.018
U, %	1.2	1.3	1.3	1.3	-	1.3	1.2	1.2
HCFC-132b								
Molar fraction, pmol/mol	0.900	1.012	1.113	1.125	1.136	1.181	1.237	1.462
U, pmol/mol	0.011	0.012	0.013	0.013	0.013	0.014	0.014	0.017
U, %	1.2	1.2	1.2	1.2	1.1	1.2	1.1	1.2
CFC-13								
Molar fraction, pmol/mol	2.657	2.987	3.284	3.318	3.351	3.482	3.648	4.310
U, pmol/mol	0.034	0.037	0.040	0.040	0.041	0.042	0.044	0.051
U, %	1.3	1.2	1.2	1.2	1.2	1.2	1.2	1.2
Ratio								
Prepared ratio, mol/mol	0.800	0.900	0.990	1.000	1.010	1.050	1.100	1.300
U, mol/mol	0.002	0.003	0.003	0.003	0.003	0.003	0.003	0.004
U, %	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3

Table 4. Correcting the measured ratio: results of weighted linear fitting and calculated internal consistency within the METAS-2017 suite of reference gas mixtures, for each substance. Values correspond to calculations done after exclusion of the outliers.

	SF ₆	HFC-125	HFO-1234yf	HCFC-132b	CFC-13
Fitting $R_{meas,i,j} = a_i \cdot R_{prep,i,j} + b_i$					
a_i	1.0217	1.0123	1.0182	1.0013	1.0204
u_{a_i}	0.0040	0.0042	0.0074	0.0058	0.0075
b_i	-0.0210	-0.0078	-0.0229	-0.0026	-0.0293
u_{b_i}	0.0015	0.0017	0.0032	0.0025	0.0029
Internal consistency, 1 σ , %	0.23	0.35	1.1	0.24	0.6
Fitting $R_{meas,i,j} = a_i \cdot R_{prep,i,j}$					
a_i	1.0019	1.0050	0.9974	0.9989	0.9931
u_{a_i}	0.0039	0.0042	0.0073	0.0058	0.0073

Table 5. METAS-2017 suite of reference gas mixtures: final molar fraction values $x_{meas,corr,i,j}$ expressed in dry synthetic air and associated uncertainties at a 95% confidence interval.

Cylinder	6	10	8	1	7	11	3	4	2	9	5
SF₆											
Molar fraction, pmol/mol	8.513	9.522	10.286	10.582	10.566	10.663	11.126	11.119	11.679	11.642	13.774
U, pmol/mol	0.084	0.094	0.101	0.104	0.105	0.105	0.110	0.110	0.115	0.115	0.136
U, %	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
HFC-125											
Molar fraction, pmol/mol	25.801	28.992	31.337	32.027	32.168	32.514	33.597	33.632	35.826	35.566	41.828
U, pmol/mol	0.392	0.442	0.477	0.488	0.490	0.495	0.512	0.513	0.546	0.541	0.639
U, %	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5
HFO-1234yf											
Molar fraction, pmol/mol	0.898	0.949	1.042	1.117	1.111	-	1.184	1.173	1.211	1.201	1.451
U, pmol/mol	0.018	0.018	0.020	0.022	0.022	-	0.023	0.023	0.024	0.024	0.029
U, %	2.0	1.9	1.9	2.0	2.0	-	2.0	2.0	2.0	2.0	2.0
HCFC-132b											
Molar fraction, pmol/mol	0.900	0.993	1.103	1.126	1.129	1.138	1.215	1.181	1.232	1.234	1.464
U, pmol/mol	0.015	0.016	0.018	0.018	0.019	0.019	0.020	0.019	0.020	0.020	0.024
U, %	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6
CFC-13											
Molar fraction, pmol/mol	2.652	2.989	3.278	3.347	3.307	3.339	3.484	3.523	3.681	3.634	4.304
U, pmol/mol	0.052	0.057	0.065	0.065	0.067	0.064	0.067	0.068	0.072	0.072	0.085
U, %	2.0	1.9	2.0	1.9	2.0	1.9	1.9	1.9	2.0	2.0	2.0

Table 6. Scale comparison: individual cylinder measurement results and calculated average scale ratios. All measurements have been performed by Medusa-GC-MS at Empa Laboratories (see main text). We provide as well for documentation the known scale conversion factors used in this study: (a) Krummel et al. (2017), (b) Simmonds et al. (2017), (c) C.M. Harth and R.F. Weiss, pers. com., 2018.

	SF₆	HFC-125	HFO-1234yf	CFC-13
Individual cylinder measurements				
MP15-4020/J-170	-	0.957	-	-
MP15-4034/J-170	-	0.969	-	-
MP15-5017/EP-001	-	-	0.970	-
MP15-4042/EP-001	-	-	0.971	-
MP16-4042/J-191	1.012	-	-	-
MP16-5017/J-191	1.012	-	-	-
MP-001/E-094	1.003	0.927	0.910	1.049
MP-001/E-108	1.000	0.927	0.910	-
MP-001/E-163	1.002	0.930	0.911	-
MP-001/J-191	1.001	0.930	-	1.050
MP-001/J-206	1.002	0.931	-	1.067
Calculated average scale ratios				
METAS-2016/SIO-05	1.012	-	-	-
METAS-2015/SIO-14	-	0.963	-	-
METAS-2015/Empa-2013	-	-	0.971	-
METAS-2017/SIO-05	1.002	-	-	-
METAS-2017/SIO-14	-	0.929	-	-
METAS-2017/Empa-2013	-	-	0.910	-
METAS-2017/Interim-98	-	-	-	1.055
METAS-2017/METAS-2015	-	0.964	0.938	-
METAS-2017/METAS-2016	0.990	-	-	-
Known scale conversion factors used in this study				
NOAA-2014/SIO-05	1.002 ^(a)	-	-	-
NOAA-2008/SIO-14	-	0.946 ^(b)	-	-
UB-98/SIO-14	-	0.9237 ^(c)	-	-
Additionally calculated scale conversion factors				
METAS-2017/NOAA-2014	1.000	-	-	-
METAS-2017/NOAA-2008	-	0.982	-	-

Supplement for: Dynamic-gravimetric preparation of primary, metrologically traceable calibration standards for halogenated greenhouse gases

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S1 Determination of mass loss rate of permeation devices

The mass loss q_m in ng/min due to permeation through the membrane of the permeation device is calculated using a linear fit based on multiple data of mass and time as measured by our magnetic suspension balance. This linear fit gives directly q_m and the associated standard deviation used in the uncertainty budget as $Stab_{balance}$. However, to calculate the expanded uncertainty of the mass loss it is needed to take into account the reading resolution of the balance. To include this in the uncertainty we decompose q_m into the first data point (m_1, t_1) and the final data point (m_2, t_2) . (m_1, t_1) is directly taken as the first data from the set used to calculate the linear fit. t_2 is taken from the last data point of the set. m_2 is re-calculated using the values of m_1 , t_1 , t_2 and q_m so that is it consistent:

$$m_2 = m_1 - q_m \cdot (t_2 - t_1)$$

10 It is now possible to associate to each variable m_1 , m_2 , t_1 and t_2 the uncertainty of the reading resolution (respectively 0.0000005 g and 0.05 s, as reported in Table 2 of the main text).

S2 Cryo-filling: dead volume correction

When filling a cylinder, at the end of the filling routine the nitrogen gas present in between the pneumatic valve V1 and the valve of the cylinder is lost. This is due to the saturation vapour pressure of nitrogen in equilibrium with the liquid nitrogen.

15 This pressure is a function of liquid nitrogen temperature. Before doing any of the filling, we therefore determined how much gas is exactly lost, by measuring the residual pressure in this volume when the cylinder is filled with some air and placed in the filled liquid nitrogen bath.

For this test, the pressure gauge was placed directly in between the cylinder and V1. Synthetic air was filled in the cylinder placed in liquid nitrogen, V1 was closed, and the pressure was measured in this closed system. The pressure was at 800 hPa, in agreement with a liquid nitrogen temperature of $-200\text{ }^{\circ}\text{C}$.

To compensate for this loss, before switching valves V1 and V2 to start filling the cylinder, the interval in between V1 and the cylinder valve is flushed with the carrier gas three times and then filled at 800 hPa. This volume of gas is then trapped in the cylinder when the valves are switched at the beginning of the filling. This volume compensates for the approximately equivalent volume lost at the end.

S3 Weighted linear fit: York algorithm

To calculate the weighted linear fit taking into account the standard uncertainties $u_{R_{prep,i,j}}$ and $u_{R_{meas,i,j}}$ of both $R_{prep,i,j}$ and $R_{meas,i,j}$, we apply the York algorithm (York et al., 2004) as written in Cantrell (2008). $u_{R_{prep,i,j}}$ are calculated according to Eq. 8 in the main text. $u_{R_{meas,i,j}}$ are the standard deviation of the mean of $R_{meas,i,j}$ and documented in Table S5.

First, input values are initialised. For a given substance j , and with i representing all accepted cylinder values (i.e. all values except outliers), we set:

$$\begin{aligned}
 x_i &= R_{prep,i,j} \\
 y_i &= R_{meas,i,j} \\
 w_{x_i} &= (1/u_{R_{prep,i,j}}^2) \\
 w_{y_i} &= (1/u_{R_{meas,i,j}}^2) \\
 a &= 1 \\
 r_i &= 0 \\
 \alpha_i &= \sqrt{w_{x_i} \cdot w_{y_i}}
 \end{aligned}$$

The following algorithm is then ran 10 times:

$$\begin{aligned}
 W_i &= \frac{w_{x_i} \cdot w_{y_i}}{w_{x_i} + a^2 \cdot w_{y_i} - 2 \cdot a \cdot r_i \cdot \alpha_i} \\
 \bar{x} &= \frac{\sum W_i \cdot x_i}{\sum W_i} \\
 \bar{y} &= \frac{\sum W_i \cdot y_i}{\sum W_i} \\
 U_i &= x_i - \bar{x} \\
 V_i &= y_i - \bar{y} \\
 B_i &= W_i \cdot \left(\frac{U_i}{w_{y_i}} + \frac{a \cdot V_i}{w_{x_i}} - (a \cdot U_i + V_i) \cdot \frac{r_i}{\alpha_i} \right)
 \end{aligned}$$

$$a = \frac{\sum W_i \cdot B_i \cdot V_i}{\sum W_i \cdot B_i \cdot U_i}$$

After these ten runs (which are in this case more than necessary to reach convergence of a), the final value for b is computed:

$$b = \bar{y} - a \cdot \bar{x}$$

5 The standard uncertainty ($k = 1$) for the obtained parameters is calculated as follow:

$$\bar{B} = \frac{\sum W_i \cdot B_i}{\sum W_i}$$

$$\sigma_a = \sqrt{\frac{1}{\sum W_i \cdot (B_i - \bar{B})^2} \cdot \frac{1}{\sqrt{\text{length}(x_i)}}$$

10
$$\sigma_b = \sqrt{\frac{1}{\sum W_i} + (\bar{x} + \bar{B})^2 \cdot \sigma_a^2} \cdot \frac{1}{\sqrt{\text{length}(x_i)}}$$

S4 METAS-2015 scales for HFC-125 and HFO-1234yf

Diagrams presenting the experimental setup used to prepare reference gas mixtures for HFC-125 and HFO-1234yf are presented in Fig. S2 (permeation and cryo-filling) and Fig. S3 (additional dynamic dilution).

The main technical differences with the METAS-2017 preparation method are:

- 15
- the carrier gas is additionally purified at the beginning of the preparation, using a commercially available purification cartridge (Microtorr, SAES Getters).
 - only one dilution step is used after the permeation chamber (MFC1, MFC2);
 - only one cryo-filling routine is done for each cylinder (there are no multiple fillings). As a result each cylinder contains a reference gas mixture for only one substance.
- 20
- the reference gas mixture in the produced cylinder is at nmol/mol (ppb) level and therefore needs additional dilution. This is done dynamically using a setup called 'METAS 2-step-dilutor' already existing at METAS, based on two successive dynamic dilution steps (Fig. S3).
 - the mixture exiting the '2-step-dilutor' is directly injected into the Medusa-GC-MS system in operation at Empa for measurement.

25 S5 Measurement of impurities in the permeation device for HFC-125

Based on the findings from Vollmer et al. (2015) who identified several potential impurities in HFC-125 inherited from its production pathway, we have measured the presence of impurities in the permeator for HFC-125. We have done this test using

the reference gas mixture for HFC-125 prepared at 85 nmol/mol (cylinder MP15-4020, see Fig. S1) as part of the METAS-2015 suite for HFC-125. These measurements have been performed by injecting 1 L of this mixture directly in the Medusa-GC-MS at Empa. The detection of the HFC-125 peak was disabled to avoid saturation of the detector. For HCFC-132b, there was no chromatographic baseline excursion suggesting that the mole fraction was well below the detection limit (defined here as three times the noise level). As the amount of gas used for a measurement was 1 L, i.e. half the normal gas quantity of 2 L, we roughly estimate the detection limit for HCFC-132b as twice the detection limit for a normal measurement of 2 L, i.e. 0.03 pmol/mol (instead of 0.015 pmol/mol).

In addition, the measurements showed the presence of:

- CFC-115: 31 pmol/mol ($0.36 \cdot 10^{-3}$ mol per mol HFC-125)
- 10 – HFC-143a: 51 pmol/mol ($0.6 \cdot 10^{-3}$ mol per mol HFC-125)
- HFC-134a: 31 pmol/mol ($0.36 \cdot 10^{-3}$ mol per mol HFC-125)
- HCFC-124: 11 pmol/mol ($0.13 \cdot 10^{-3}$ mol per mol HFC-125)
- SF₆: 0.2 pmol/mol with LOD = 0.03 pmol/mol ($2.5 \cdot 10^{-6}$ mol per mol HFC-125)
- HFO-1234yf: 0.06 pmol/mol with LOD = 0.02 pmol/mol, although we are not sure if this is a small impurity introduced potentially by contamination from a regulator
- 15 – CFC-13: no baseline disruption (LOD = 0.14 pmol/mol).

In cylinder MP-001 containing 32.027 pmol/mol HFC-125, the SF₆ impurities originating from the HFC-125 permeator correspond to a contribution of $2.5 \cdot 10^{-6} \cdot 32.027 = 0.00008$ pmol/mol SF₆. This can be neglected compared to the prepared 10.582 pmol/mol SF₆. The same conclusion applies to HFO-1234yf and to the other cylinders.

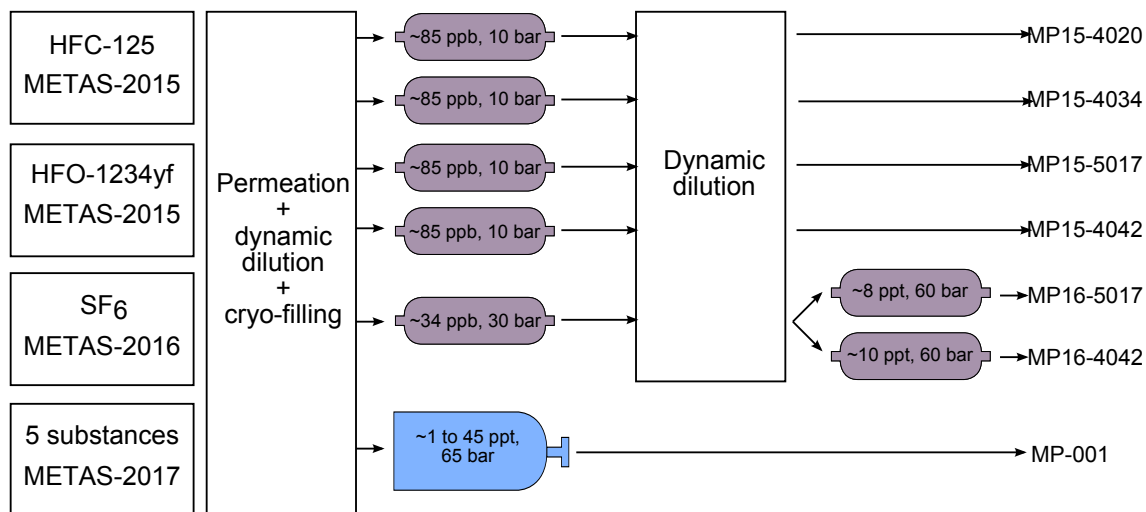


Figure S1. Overview of preparation steps for the 3 successive generations of scales prepared at METAS: METAS-2015, METAS-2016 and METAS-2017. The METAS-2017 scale is the most advanced scale in terms of minimisation of exposition to metal surfaces. ppb: nmol/mol. ppt: pmol/mol.

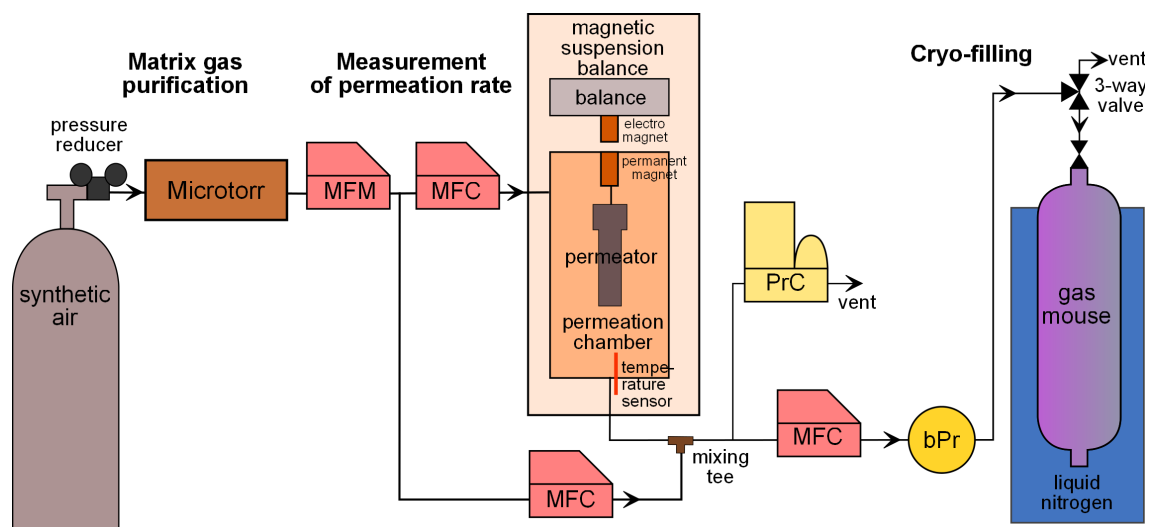


Figure S2. Preparation setup used to produce high concentration mixtures for HFC-125 and HFO-1234yf in cylinders.

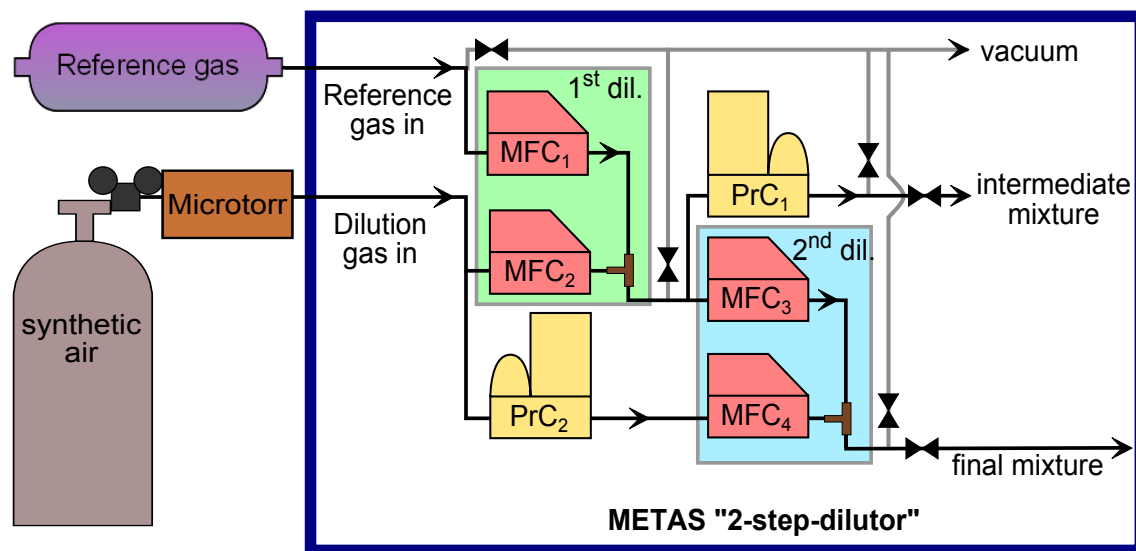


Figure S3. Schematic of METAS '2-step-dilutor', a two-stage dynamic dilutor based on thermal mass flow controllers. This setup is used to dilute the high concentration cylinders for HFC-125, HFO-1234yf and SF₆ (see preparation overview in Fig. S1). The final mixtures are at pmol/mol levels.

Table S1. Mass loss rate determination for each permeation device.

	m_1 , g	m_2 , g	t_1 , min	t_2 , min	q_m , ng/min	$Stab_{balance}$, % ($k = 1$)
SF ₆	28.44957646	28.43612094	5999.45	14130.80	1654.77	0.20
HFC-125	28.56911448	28.56634188	1505.17	7128.32	493.07	0.40
HFO-1234yf	30.40242526	30.39984672	998.70	30205.77	88.28	0.41
HCFC-132b	29.46146154	29.46037128	89.83	10068.25	109.26	0.64
CFC-13	30.09772063	30.09634635	5999.55	12319.95	217.44	0.57

Table S2. Flows used for the first and second dynamic dilution steps, in mL/min @ STP. MFM measures the total flow MFC1 + MFC2. MFC1 and MFC2 therefore do not need individual calibration.

	MFC1	MFC2	MFM	MFC3	MFC4
Set points					
SF ₆	167	4500	-	10	5000
HFC-125	167	500	-	10	4000
HFO-1234yf	167	3500	-	10	4000
HCFC-132b	300	3500	-	10	4000
CFC-13	300	3000	-	10	4000
water vapour	300	1200	-	not used	not used
Calibrated values					
SF ₆	-	-	4594.968	10.809	5115.463
HFC-125	-	-	676.333	10.809	4109.936
HFO-1234yf	-	-	3691.690	10.809	4109.936
HCFC-132b	-	-	3817.535	10.809	4109.936
CFC-13	-	-	3333.618	10.809	4109.936
water vapour	-	-	not calibrated	not used	not used

Table S3. Filling durations, in seconds.

Cylinder	MP-001	MP-002	MP-003	MP-004	MP-005	MP-006	MP-007	MP-008	MP-009	MP-010	MP-011
SF ₆	4018	2040	1546	1546	1915	1178	1178	1166	1296	1060	1190
HFC-125	4018	2040	1546	1546	1915	1178	1178	1166	1296	1060	1190
HFO-1234yf	4018	2040	1546	1546	1915	1178	1178	1166	1296	1060	0
HCFC-132b	4018	2040	1546	1546	1915	1178	1178	1166	1296	1060	1190
CFC-13	4018	2040	1546	1546	1915	1178	1178	1166	1296	1060	1190
water vapour	24110	10200	8470	8470	6625	10310	7070	7130	6480	7660	8200

Table S4. Matrix gas impurity content: results of measurement by Medusa-GC-MS (molar fraction, pmol/mol). For the uncertainty budget we use a triangular distribution centered in this measured molar fraction, with the same value as half width of limit.

	SF ₆	HFC-125	HFO-1234yf	HCFC-132b	CFC-13
Molar fraction, pmol/mol	0.006	0.04	0.003	0.003	0.015
Half width of limit, pmol/mol	0.006	0.04	0.003	0.003	0.015

Table S5. Results of measured ratios without correction of analyser response. n is the number of replicate measurements. For cylinder MP-001, by default the ratio is set to 1, and we apply as standard deviation the average standard deviation over the set of cylinders, for each given substance. $u_{R_{meas}}$ is the standard deviation of the mean.

Cylinder	MP-006	MP-010	MP-008	MP-001	MP-007	MP-011	MP-003	MP-004	MP-002	MP-009	MP-005
SF₆											
R_{meas}	0.800	0.898	0.971	1.000	0.998	1.008	1.052	1.052	1.106	1.102	1.308
n	20	9	19	12	9	10	9	10	18	10	12
$u_{R_{meas}}$	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001
HFC-125											
R_{meas}	0.804	0.905	0.978	1.000	1.004	1.015	1.049	1.051	1.120	1.111	1.308
n	20	10	17	12	9	9	10	10	18	10	12
$u_{R_{meas}}$	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.002
HFO-1234yf											
R_{meas}	0.799	0.846	0.931	1.000	0.995	-	1.062	1.051	1.086	1.076	1.305
n	20	9	18	11	9	-	10	10	19	10	12
$u_{R_{meas}}$	0.003	0.002	0.003	0.003	0.003	-	0.004	0.004	0.004	0.004	0.006
HCFC-132b											
R_{meas}	0.799	0.881	0.979	1.000	1.002	1.010	1.079	1.049	1.094	1.096	1.300
n	19	9	18	12	9	10	10	10	19	10	12
$u_{R_{meas}}$	0.001	0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002
CFC-13											
R_{meas}	0.786	0.890	0.979	1.000	0.988	0.997	1.042	1.054	1.103	1.088	1.294
n	20	8	19	12	9	8	9	9	19	10	12
$u_{R_{meas}}$	0.004	0.002	0.005	0.004	0.006	0.003	0.003	0.003	0.005	0.006	0.006

Table S6. Measured & corrected ratios using a linear fit.

Cylinder	MP-006	MP-010	MP-008	MP-001	MP-007	MP-011	MP-003	MP-004	MP-002	MP-009	MP-005
R_{prep}	0.800	0.900	0.990	1.000	1.000	1.010	1.050	1.050	1.100	1.100	1.300
U	0.002	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.004
U, %	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3
SF₆											
$R_{meas,corr}$	0.804	0.899	0.971	0.999	0.998	1.007	1.051	1.050	1.103	1.099	1.301
U	0.007	0.008	0.008	0.008	0.009	0.009	0.009	0.009	0.009	0.009	0.011
U, %	0.9	0.9	0.9	0.8	0.9	0.8	0.8	0.8	0.8	0.8	0.8
HFC-125											
$R_{meas,corr}$	0.802	0.901	0.974	0.996	1.000	1.011	1.044	1.045	1.114	1.106	1.300
U	0.007	0.008	0.009	0.009	0.009	0.009	0.009	0.009	0.010	0.010	0.011
U, %	0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9
HFO-1234yf											
$R_{meas,corr}$	0.807	0.854	0.937	1.005	0.999	NaN	1.065	1.054	1.089	1.080	1.305
U	0.014	0.014	0.015	0.016	0.016	NaN	0.017	0.017	0.017	0.017	0.021
U, %	1.7	1.7	1.6	1.6	1.6	NaN	1.6	1.6	1.6	1.6	1.6
HCFC-132b											
$R_{meas,corr}$	0.800	0.883	0.981	1.001	1.004	1.012	1.080	1.050	1.095	1.097	1.301
U	0.011	0.011	0.012	0.013	0.013	0.013	0.014	0.013	0.014	0.014	0.016
U, %	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.2
CFC-13											
$R_{meas,corr}$	0.799	0.901	0.988	1.009	0.997	1.006	1.050	1.062	1.109	1.095	1.297
U	0.014	0.014	0.016	0.016	0.017	0.016	0.017	0.017	0.018	0.018	0.021
U, %	1.7	1.6	1.7	1.6	1.7	1.6	1.6	1.6	1.6	1.6	1.6

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