



# 1 **Field comparison of dry deposition samplers for collection of atmospheric** 2 **mineral dust: results from single-particle characterization**

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## 10 **Abstract**

11 Frequently, passive dry deposition collectors are used to sample atmospheric dust deposition. However,  
12 there exists a multitude of different instruments with different, usually not well-characterized sampling  
13 efficiencies. As result, the acquired data might be considerably biased with respect to their size  
14 representativity, and as consequence, also composition. In this study, individual particle analysis by  
15 automated scanning electron microscopy coupled with energy-dispersive X-ray was used to characterize  
16 different, commonly used passive samplers with respect to their size-resolved deposition flux and  
17 concentration. This study focuses on the microphysical properties. In addition, computational fluid  
18 dynamics modeling was used in parallel to achieve deposition velocities from a theoretical point of view.

19 Flux measurements made using different passive samplers show a disagreement between the samplers.  
20 Both MWAC and BSNE collect considerably more material than Flat plate and the Sigma-2. The  
21 collection efficiency of MWAC for large particles increases in comparison to Sigma-2 slightly with  
22 increasing wind speed, while there is barely such increase visible for the BSNE. A correlation analysis  
23 between dust flux, derived dust concentrations and wind speed reveals a positive correlation between  
24 dust flux and dust concentration and negative correlation between dust flux and wind speed. A very good  
25 correlation is found between derived concentrations and PM<sub>10</sub> concentration measurements by an optical  
26 particle spectrometer. The results also suggest that a Big Spring Number Eight as horizontal flux sampler  
27 and a Sigma-2 as vertical flux sampler can be good options for PM<sub>10</sub> measurement, whereas a Modified  
28 Wilson and Cooke sample is not a suitable choice. Furthermore, it is found that deposition velocities  
29 calculated from classical deposition models do not agree with deposition velocities estimated using  
30 computational fluid dynamics simulations. The deposition velocity from CFD was often higher than the



31 values derived from classical deposition velocity models. Comparatively, deposition velocity calculated  
32 using analytical approach better fits to the measurement data than deposition velocity from CFD.

33 **Key words:** Mineral dust particles, passive samplers, SEM-EDX, single particle analysis, computational  
34 fluid dynamics

## 35 1 Introduction

36 Mineral dust aerosol in the climate system has received considerable scientific attention mainly due to  
37 its direct effect on the radiative budget and indirect one on cloud microphysical properties (Arimoto,  
38 2001; Jickells et al., 2005). Mineral dust particles also play a key part with respect to gas phase chemistry  
39 by providing a reaction surface e.g. ozone depletion (Nicolas et al., 2009; Prospero et al., 1995).  
40 Moreover, dust aerosol also plays an important role in biogeochemical cycles by supplying important  
41 and limiting nutrients to Ocean surfaces. Mineral dust is emitted mainly from the arid and semi-arid  
42 regions of the world and believed to have a global source strength is ranging from 1000-3000Tgyr<sup>-1</sup>  
43 (Andreae, 1995). They form the single largest component of global atmospheric aerosol mass budget,  
44 contributing about one third of the total natural aerosol mass annually (Penner et al., 2001).

45 Deposition measurement data of mineral dust are useful to validate numerical simulation models and to  
46 improve our understanding of deposition processes. However, the scarcity and the limited  
47 representatively of the deposition measurement data for validation pose a major challenge to assess dust  
48 deposition at regional and global scales (Schulz et al., 2012; WMO, 2011). This is in part linked to the  
49 uncertainties evolving from the use of different and non-standardized measurement techniques.

50 Commonly, deposition is measured by passive techniques, which provide an acceptor area for the  
51 depositing atmospheric particles. The advantage of these passive samplers is that they operate passively,  
52 resulting in simple and thus cheaper instruments, so that many locations can be sampled at a reasonable  
53 cost (Goossens and Buck, 2012). Moreover, the usual lack of a power supply allows also for unattended  
54 remote setups. However, the most important disadvantage is that collection efficiency and deposition  
55 velocity is determined by the environmental conditions not under control (and frequently also unknown).  
56 That implies on addition, that the sampler shape can have a strong and variable impact of the collection  
57 properties. Also, they may need long sampling time necessary to collect sufficient particles.

58 While there are papers describing and modeling single samplers (Einstein et al., 2012; Wagner and Leith,  
59 2001a, b; Yamamoto et al., 2006) and a few comparison studies (Goossens and Buck, 2012; Mendez et  
60 al., 2016), nearly previous studies only compare on total mass, thereby neglecting size dependence and



61 potential comparison biases. Mendez et al. (2016) showed that efficiency of BSNE and MWAC samplers  
62 for collecting PM<sub>10</sub> varies with wind speed. Furthermore, Goossens and Buck (2012) found that for  
63 PM<sub>10</sub>, concentrations obtained from BSNE and DustTrak samplers have comparable values for wind  
64 speed in between 2–7 m/s.

65 The purpose of this study is to assess the particle collection properties of different deposition and other  
66 passive samplers based on single particle measurements and their agreement with theory. From the  
67 available data, also relations of the collected particle microphysics and composition homogeneity  
68 between the samplers will be presented, which can be used as estimators for the comparability of previous  
69 literature data based on the different techniques. To the best of our knowledge, this is the first study to  
70 analyze dry deposition measurements collected using passive samplers by means of a single-particle  
71 SEM-EDX Analysis approach (particularly in the size fraction larger than 10 μm).

## 72 2 Material and methods

### 73 2.1 Sampling location and time

74 Sahara and Sahel provide large quantities of soil dust, resulting in a westward flow of mineral dust  
75 particles over the North Atlantic Ocean accounting for up to 50% of global dust budget (Goudie and  
76 Middleton, 2001). Owing to proximity to the African continent, the Canary Islands are influenced by dust  
77 particles transported from Sahara and Sahel regions. Therefore, Tenerife is one of the best locations to  
78 study relevant dust aerosol in a natural environment.

79 For this study, we conducted a two month (July to August 2017) aerosol collection and dry deposition  
80 sampling campaign at Izaña Global Atmospheric Watch observatory (Bergamaschi et al., 2000;  
81 Rodríguez et al., 2015) (28.3085°N, 16.4995°W). Sampling was performed on top of a measurement  
82 installation, approximately 2m above the ground (including the inlet heights of the samplers). The  
83 installation was made on a 160m<sup>2</sup> flat concrete platform. The trade wind inversion, which is a typical  
84 meteorological feature of the station shields most of the time the observatory from local island emissions  
85 (García et al., 2016). Therefore, Izaña Global Atmospheric Watch observatory is an ideal choice for in-  
86 situ measurements under “free troposphere” conditions (Bergamaschi et al., 2000; García et al., 2016).

### 87 2.2 Wind measurements

88 An ultra-sonic anemometer (the young models 81000 was installed at approximately 2m height above  
89 the ground to obtain the 3-D wind velocity and direction and was operated with a time resolution of 10  
90 Hz to get basic information on turbulence structure.



### 91 **2.3 Particle sampling**

92 Samples were collected from different, commonly used samplers, namely Big Spring Number Eight  
93 (BSNE) (Fryrear, 1986), Modified Wilson and Cooke (MWAC) (Wilson and Cook, 1980), Sigma-2  
94 (VDI2119, 2013) and Flat-plate (UNC-derived)(Ott and Peters, 2008). In addition, the free-wing  
95 impactor (FWI) (Kandler et al., 2018) was also used to collect coarser particles. The BSNE, MWAC,  
96 FWI and Filter Sampler were mounted on wind vane to align to ambient wind direction. Samples were  
97 collected at interval of 24 hours (exposure time). The sampling duration for FWI (12mm Al-stub) was  
98 30min. The sampling duration for filter sampler was set to be one hour.

#### 99 2.3.1 Flat plate sampler

100 The flat plate sampler used in this work was taken from the original flat plate geometry used in Ott et al.  
101 (2008b). Briefly, the geometry contains two round brass plates (top plate diameter 203 mm, bottom plate  
102 127 mm, thickness 1 mm each) mounted in a distance of 16mm. Unlike the original design, the geometry  
103 of the current work has a cylindrical dip in the lower plate, which recedes the sampling substrate – a SEM  
104 stub with a thickness of 3.2 mm – from the airflow, reducing the flow disturbance. A preliminary study  
105 with identical setup in a rural environment had shown that this recession approximately doubles the  
106 collection efficiency for large particles. In this design, larger droplets (> 1 mm) are prevented by this  
107 setup from reaching the SEM stub surface at the local wind speeds (Ott et al., 2008b). As described in  
108 (Wagner and Leith, 2001a, b), the main triggers for particle deposition on the substrates for this sampler  
109 are diffusion, gravity settling, and turbulent inertial forces, of which only the latter two are relevant in  
110 our study.

#### 111 2.3.2 Sigma-2 sampler

112 The sigma-2 sampling device is described in (Dietze et al., 2006; Schultz, 1989; VDI2119, 2013). Briefly,  
113 the geometry consists of a cylindrical sedimentation tube with a height of about 27cm made of antistatic  
114 plastic, which is topped by a protective cap with diameter of 158mm. At its top, the cap has four  
115 rectangular inlet windows (measuring 40mm x 77mm, all at the same height) at its side providing away  
116 for passive entrance of particles to the collection surface. Once entered the tube, particles settle down to  
117 the collection surface due to gravitation (Stokes' law) (VDI2119, 2013). The samplers designed in a way  
118 that it prevents the sample from direct radiation, wind and precipitation.



119 2.3.3 The Modified Wilson and Cooke (MWAC) sampler

120 The MWAC sampler is based on an original design developed by Wilson and Cook (1980). The sampler  
121 consists of a closed polyethylene bottle, serving as settling chamber, to which an inlet tube and an outlet  
122 tube have been added. The MWAC sampling bottles are 95mm long with a diameter of 48mm. The two  
123 inlet and outlet plastic tubes with inner and outer diameter 8 and 10mm respectively, pass air through the  
124 cap into the bottle and then out again. The large volume of the bottle relative to the inlet diameter makes  
125 the dust particles entering the bottle to be deposited in the bottle due to the flow deceleration the total  
126 bottle area, and due to impaction below the exit of the inlet tube. The air then discharges from the bottle  
127 via the outlet tube. MWAC is one of the most commonly used samplers (Goossens and Offer, 2000) and  
128 has a high sampling efficiency for large particles (Mendez et al., 2016).

129 2.3.4 The Big Spring Number Eight (BSNE) sampler

130 The BSNE sampler originally designed by Fryrear (1986) is intended to collect airborne dust particles  
131 from the horizontal flux (Goossens and Offer, 2000). Briefly, the particle laden air passes through a  
132 rectangular inlet (21mm wide and 11mm high, with total area of 231mm<sup>2</sup>). Once inside the sampler, air  
133 speed is reduced by continuous cross section increase (angular walls) and the particles settle out in  
134 collection surface. Air discharges through a mesh screen.

135 2.3.5 Free-wing impactor (FWI)

136 A free rotating wing impactor (Jaenicke and Junge, 1967; Kandler et al., 2018; Kandler et al., 2009) was  
137 used to collect particles larger than approximately 5µm. A FWI has a sticky impaction surface attached  
138 to a rotating arm that moves through air; particles deposit on the moving plate. The rotating arm is moved  
139 at constant speed by a stepper motor, which is fixed on a wind vane, aligning the FWI to wind direction.  
140 The particle size cut-off is defined by the impaction parameter, i.e. by rotation speed, wind speed and  
141 sample substrate geometry. The details of working principle of FWI can be obtained from Kandler et al.  
142 (2018)

143 2.3.6 Filter sampler

144 A filter sampler with Nucleopore filters (Whatman® Nucleopore™ Track-Etched Membranes diam. 25  
145 mm, pore size 0.4µm, polycarbonate) mounted on a wind vane was used for iso-axial particle collection.  
146 An inlet nozzle of 6 mm was used to achieve pseudo-isokinetic conditions. Sample flow (0.75m<sup>3</sup>hr<sup>-1</sup>) was



147 measured by a mass flow meter (MASS-STREAM, M+W instruments). The filter sampler was operated  
148 at least two times a day.

#### 149 **2.4 Upward-downward flux sampler**

150 Following an approach by Noll and Fang (1989) – assuming that turbulent transport is the main  
151 mechanism for upward flux while turbulent transport and sedimentation are the mechanism of for  
152 downward deposition flux – a sampler with an upward- and a downward-facing substrate in analogy to  
153 the flat plate sampler was designed. Both substrates are aligned to face each other with the air passing in  
154 between.

#### 155 **2.5 Ancillary Aerosol Data**

156 Additional information regarding the aerosol particle size distributions has been obtained by using OPC  
157 (GRIMM) instruments available at Izaña Global Atmospheric Watch observatory (Bergamaschi et al.,  
158 2000; Rodríguez et al., 2015). The particle size ranging from 10nm to 496nm was measured with an  
159 SMPS while from 350nm to 20µm was measured with an OPC.

#### 160 **2.6 SEM-Analysis**

161 All aerosol samples were (except the filter sampler) collected on pure carbon adhesive substrate (Spectro  
162 Tabs, Plano GmbH, Wetzlar, Germany) mounted on standard SEM aluminum stubs (12 and 25mm).  
163 Individual particle analysis by automated scanning electron microscopy (SEM; FEI ESEM Quanta (400  
164 FEG, FEI, Eindhoven, The Netherlands; operated at 12.5 kV, lateral beam extension 3 nm approx., spatial  
165 resolution 160 nm)) was used to characterize particles for size and composition. A total of 315,000  
166 particles from six samplers was analyzed. 26 samples from BSNE (52882 particles), 23 samples from  
167 MWAC (48650 particles), 23 samples from SIGMA-2 (38506 particles), 18 samples from flat plate  
168 (12mm) (24340 particles), 22 samples from Flat plate (25mm) (20700), 13 samples from Filter (80000)  
169 and 12 samples from FWI-12mm (50000 particles) were analyzed. Each sample was characterized at  
170 randomly selected areas, until a total of 3,000 particles with projected area diameters greater than 1µm  
171 was reached. For particle identification, the backscattered electron image (BSE-image) has been used, as  
172 dust particles contain heavier elements than carbon and therefore appear as detectable bright spots in the  
173 BSE-image.

174 Chemical information was derived by energy-dispersive X-ray analysis (EDX; Oxford X-Max 120,  
175 Oxford Instruments, Abingdon, United Kingdom). The internal ZAF-correction of the software system –  
176 based on inter-peak background radiation absorption measurements used for correction – was used for  
177 obtaining quantitative results.



178 **2.7 Particle size determination**

179 The image analysis integrated into the SEM-EDX software determines the size of particles as a projected  
 180 area diameter.

$$181 \quad d_g = \sqrt{\frac{4B}{\pi}} \quad (1)$$

182 Where  $B$  and  $d_g$  are the area covered by the particle on the sample substrate and the projected area  
 183 diameter respectively.

184 Following Ott et al. (2008a), the volumetric shape factor,  $S_v$  is determined from the count data as:

$$185 \quad S_v = \frac{P^2}{4\pi A} \quad (2)$$

186 Where  $P$  and  $A$  are the perimeter and the projected area of the particle respectively.

187 The volume-equivalent diameter (sphere with the same volume as the irregular shaped particle) is then,  
 188 calculated from the projected area diameter via the volumetric shape factor (Ott et al., 2008a) and is  
 189 expressed by particle projected area and perimeter as

$$190 \quad d_v = \frac{4\pi B}{P^2} d_g = \frac{1}{P^2} \sqrt{64\pi B^3} \quad (3)$$

191 The aerodynamic diameter ( $d_a$ ) is calculated from projected area diameter through the use of a volumetric  
 192 shape factor and aerodynamic shape factor (Wagner and Leith, 2001b)

$$193 \quad d_a = \sqrt{[d_v (\rho_p / \rho_0) 1 / S_d]} \quad (4)$$

194 With  $S_d$  the aerodynamic shape factor,  $\rho_p$  and  $\rho_0$  are particle density and air density respectively. For  
 195 this work, a value of  $S_d = 1.41$  was used (Davies, 1979). Cunningham's slip correction was neglected in  
 196 this study, as all particles considered were super-micron size.

197 **2.8 Mass flux calculation**

198 The mass flux ( $M$ ) is calculated from deposited particle number per area, individual particle size and  
 199 density. The particle density was assumed to be equal the bulk material density of the dominating  
 200 identified compound for each particle (e.g., Kandler et al. 2007). A window correction (Kandler et al.,  
 201 2009) was applied to the particle flux as:

$$202 \quad C_w = \frac{w_x w_y}{(w_x - d_p)(w_y - d_p)} \quad (5)$$

203 Where  $w_x$  and  $w_y$  are the dimensions of the analysis rectangle.



204 The mass flux of the samples is then determined as

$$205 \quad M = \frac{1}{At} \sum_k \rho d_p^3 C_w(d_p, k) \quad (6)$$

206 With  $A$  is the total analyzed area,  $t$  is the sample collection time and  $k$  is index of the particle.

207 Size distributions for all properties were calculated for the logarithmic-equidistant intervals of 1-2 $\mu\text{m}$ , 2-  
208 4 $\mu\text{m}$ , 4-8 $\mu\text{m}$ , 8-16 $\mu\text{m}$ , 16-32 $\mu\text{m}$ , and 32-64 $\mu\text{m}$ .

## 209 **2.9 Modeling atmospheric mass concentrations and its size distribution from flux measurements**

210 Concentrations are calculated from the deposition flux using different deposition velocity models for  
211 different samples, namely the models of Stokes and Piskunov. The basic relationship between  
212 concentration and deposition rate was already given by Junge (1963), as the ratio of deposition flux to  
213 concentration:

$$214 \quad V_d = F/C \quad (7)$$

215 With  $F$  is deposition flux and  $C$  is concentration.

216 All different approaches now give different formulations for the deposition velocity, based on a set of  
217 assumptions and neglections.

### 218 2.9.1 Stokes settling

219 Terminal settling velocity ( $V_{ts}$ ) is calculated according to Stokes' law.

$$220 \quad V_{ts} = \frac{d_p^2 g (\rho_p - \rho_a)}{18\mu} \quad (8)$$

221 Where  $d_p$  is the particle size,  $g$  is the gravitational acceleration (9.81 $\text{ms}^{-2}$ );  $\rho_p$  the density of particle;  $\rho_a$   
222 the air density;  $\mu$  is the dynamic viscosity of air (1.8e-05 $\text{kgm}^{-1}\text{s}^{-1}$ ).

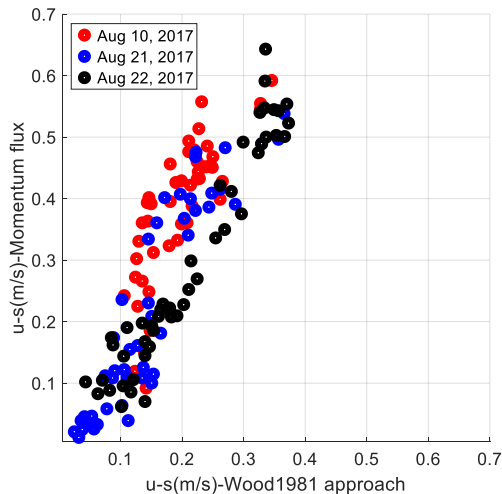
### 223 2.9.2 Turbulent deposition and more complex deposition models

224 To calculate the turbulent impaction velocity, which depends of the wind speed, the friction velocity is  
225 needed. Friction velocity ( $u_s$ ), which is a measure of wind generated turbulence is one most important  
226 variables affecting deposition velocity (Arya, 1977). Mainly two different approaches have been used to  
227 estimate  $u_s$ . On one hand the momentum flux or the eddy covariance (EC) approach (Ettling, 1996),  
228 which directly estimates friction velocity from the correlations between the measured horizontal and  
229 vertical wind velocity fluctuation, and on the other the law of the wall (LoW) approach (Shao et al.,  
230 2011), which estimates  $u_s$  from the wind profile. The latter can be approximated from free-stream  
231 velocity and roughness assumptions (Wood (1981)), where the flow inside the sampler is assumed to be





232 in the hydraulically smooth regime (Schlichting, 1968). **Figure 1** shows correlations between  $u_s$   
 233 estimated using Wood (1981) and Ettlting (1996) approaches. Obviously, the approaches lead to different  
 234 results, for which no clear explanation is available (Dupont et al., 2018).



235

236 **Figure 1:** Comparison of the friction velocities obtained from the momentum flux and the Wood1981  
 237 approaches for different days with different wind speeds (average wind speed =2.900m/s, 2.075m/s,  
 238 3.110m/s for Aug 10, 2017, Aug 21, 2017, Aug 22, 2017 respectively).

239 For the current work, the friction velocity is calculation is based on Wood (1981) approach:

$$240 \quad u_s = (u/\sqrt{2}) [(2\log_{10}(Re) - 0.65)^{-1.15}] \quad (9)$$

241 Where  $Re$  is the flow Reynolds number at the sampling stub location and is given as

$$242 \quad Re = uX/V \quad (10)$$

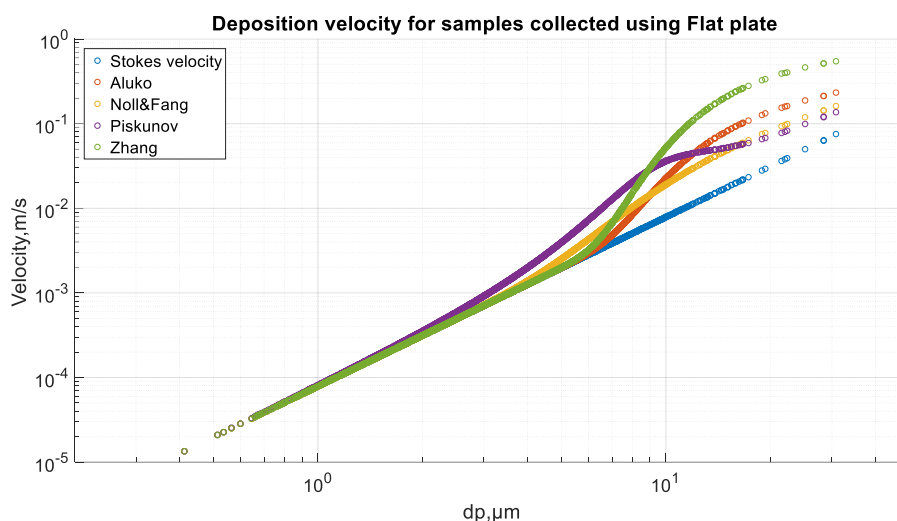
243  $X$  is the distance from the lower plate edge to the center of the sampling stub (6.3cm) and  $V$  is kinematic  
 244 viscosity.

245 The reason why we opted to use the Wood (1981) over the Ettlting (1996) approach is a) its simplicity, as  
 246 it requires only average wind speeds instead of 3D high resolution ones, and therefore will be more  
 247 commonly applicable; and b) the fact that the momentum approach yields sometimes uninterpretable  
 248 data, in particular in case of buoyancy-driven flow.

249 There are a variety of models estimating the particles deposition speed (Aluko and Noll, 2006; Noll and  
 250 Fang, 1989; Noll et al., 2001; Piskunov, 2009; Slinn and Slinn, 1980; Wagner and Leith, 2001a) (see



251 **Figure 2).** The formalism of Piskunov (2009) deposition speed model was selected for calculation of  
252 concentration in this work. Unless otherwise stated, the particle density used in deposition velocity  
253 calculation is  $2600\text{kgm}^{-3}$ .



254

255 **Figure 2:** Deposition velocities for single particles to a smooth surface calculated by using set of  
256 different classical deposition models for Tenerife samples (Aug 9, 2017; average wind speed  
257  $\approx 3.045\text{m/s}$ ).

258 2.9.3 Deposition models applied to the samplers

259 The Piskunov deposition velocity model was used for flat plate and BSNE samplers, as in both a  
260 horizontal flow deposits particles onto a horizontal flat substrate. , For the sigma-2 sampler, it is assumed  
261 that each particle settles with the terminal settling velocity (Tian et al., 2017) and therefore, Stokes'  
262 velocity was used for calculation of mass concentrations. In the case of MWAC, a different approach  
263 was required due to its semi-impaction geometry. We derived a velocity model based on wind speed (or  
264 a reduced wind speed) and calculated the collection efficiency assuming the MWAC to act as impactor  
265 for particles in the range of the cut-off diameter and larger. For smaller particles, we assumed that flow  
266 is like a flow over a smooth surface, so the Piskunov deposition velocity model was applied. I.e. as soon  
267 as the deposition velocity from impactor considerations becomes smaller than the Piskunov one, the latter  
268 was used.



269 **2.10 Determining the size distributions for mass concentration from the free-wing impactor**  
270 **measurements**

271 Considering the windows correction and the collection efficiency dependence on the impaction speed  
272 and geometry, the overall collection efficiency is calculated according to Kandler et al. (2018).

273 After calculating the collection efficiency, the atmospheric concentration is calculated from flux and  
274 deposition velocity as

$$275 \quad C = \frac{M}{V_d} \quad (11)$$

276 With  $V_d = E \cdot v_{imp}$ ,  $E$  being the collection efficiency and  $v_{imp}$  the impaction velocity, calculated from  
277 ambient wind speed and rotation speed.

278 **2.11 Determining the size distributions for mass concentration from the filter sampler**  
279 **measurements**

280 Apparent number concentrations are determined from the particle deposition rate and the volumetric flow  
281 rate calculated from the mass flow for ambient conditions. The inlet efficiency ( $Eff_{in}$ ) – accounting for  
282 the difference in wind speed and inlet velocity - is calculated as a function of Stokes number ( $Stk$ ). The  
283 ambient concentration finally ( $N_{out}$ ) is calculated by weighting the measured number concentration  
284 with the calculated inlet efficiency correction.

285 **2.12 Statistical uncertainty**

286 Owing to the discrete nature of the particle size measurement, the uncertainty coming from counting can  
287 pose a significant contribution to the uncertainty of mass flux measurement (Kandler et al., 2018). It is,  
288 therefore, important to assess the uncertainties in our mass flux measurements, which is done in  
289 accordance to the previous work (Kandler et al. 2018). For the mass flux calculations, the statistical  
290 uncertainty is assessed by a bootstrap simulation approach using Monte Carlo approximation (Efron,  
291 1979).

292 In this work, the bootstrap simulations and the two-sided 95 % confidence intervals calculation were  
293 performed by using Matlab's bootstrap function (MATLAB R2016a (MathWorks, Inc). Here, MATLAB  
294 function uses a non-parametric bootstrap algorithm (Neto, 2015) to compute the 95% bootstrap  
295 confidence interval.



### 296 3 Computational fluid dynamics (CFD) simulation

297 Computational fluid dynamics (CFD) simulations were conducted to predict the deposition of particles  
298 on to different passive samplers (MWAC, Sigma-2 and Flat-plate). A discrete phase model without  
299 interaction with continuous phase was used to calculate the trajectories of the particles. The CFD software  
300 ANSYS-FLUENT 18.2 was used for performing the numerical simulations.

#### 301 3.1 Evaluating the mean flow field

302 In a first step the geometry of samplers was created using ANSYS DesignModeler. In a second step, an  
303 enclosure around the geometry was generated. To ensure that there are no large gradients normal to the  
304 boundaries at the domain boundary, the domain was created depending on the width, the height and the  
305 length of the geometries. The space in front of the geometry is two times the height of the sampler, the  
306 space behind the sampler is ten times the height, the space left and right of the geometry is five times the  
307 width of the geometry and the space below and above the sampler is five times the height.

308 Afterwards a mesh was created using the ANSYS Meshing program. For the enhanced wall treatment  
309 the first near-wall node should be placed at the dimensionless wall distance of  $y^+ \approx 1$ . The dimensionless  
310 wall distance is given by

$$311 \quad y^+ = \frac{u_* y}{\nu} \quad (12)$$

312 With  $y$  the distance to the wall,  $\nu$  the kinematic viscosity of the fluid and  $u_*$  the friction velocity which  
313 is defined for this purpose by

$$314 \quad u_* = \sqrt{\tau_w / \rho} \quad (13)$$

315 With  $\tau_w$  the wall, shear stress and  $\rho$  the fluid density at the wall. The wall is then subdivided into a  
316 viscosity-affected region and a fully turbulent region depending on the turbulent Reynolds number  $Re_y$

$$317 \quad Re_y = \frac{\rho y \sqrt{k}}{\mu} \quad (14)$$

318 With  $y$  the wall-normal distance from the wall to the cell centers,  $k$  the turbulence kinetic energy and  $\mu$   
319 the dynamic viscosity of the fluid. If  $Re_y > 200$  the k-epsilon model is used.  $Re_y < 200$  the one-equation  
320 of Wolfstein is employed (Chmielewski and Gieras, 2013; Fluent, 2015). The flow field was calculated  
321 by solving the Reynolds Averaged Navier Stokes's equations with the software ANSYS Fluent. Standard  
322 k-epsilon model was used to calculate the Reynolds-stresses. The boundary conditions at the sides of the  
323 domain were set to symmetric. The inlet boundary condition was set to 2, 4 or 8 m/s with air as fluid



324 (Density:  $1.225\text{kgm}^{-3}$ , viscosity:  $1.7849\text{e-}05\text{kgm}^{-1}\text{s}^{-1}$ ). The outlet boundary condition was set to pressure  
325 outlet.

326 In the last step, particles were injected into the velocity field. Different particle sizes (1, 2.5, 5, 10, 20  
327 and  $50\ \mu\text{m}$ , Stokes' diameter) for three different wind speeds (2, 4, 8 m/s) were investigated. The particles  
328 density was set to a value of  $2600\ \text{kg/m}^3$  to match an approximate dust bulk density. The number of  
329 particles trapped in the deposition area was determined. The deposition velocity  $V_d$  was calculated by

$$330 \quad V_d = \frac{N_{pt}v}{A_d C_p} \quad (15)$$

331 with  $N_{pt}$  the number of trapped particle at the deposition area,  $v$  the velocity of the air at the inlet  
332 boundary of the domain,  $A_d$  the deposition area and  $C_p$  the particle concentration at the particle injection  
333 area (Sajjadi et al., 2016). The particle concentration was  $4 \cdot 10^8\ \text{m}^{-2}$  in all cases, while the injection area  
334 was adjusted to the geometries. The areas are shown in **Figure 3** with 10 exemplare particle trajectories  
335 along with the sampler geometry.

336 The turbulence intensity  $T_i$  was calculated and plotted from

$$337 \quad T_i = \frac{\left(\frac{2}{3}k\right)^{1/2}}{v} \quad (16)$$

338 With  $k$  the turbulence intensity and  $v$  the velocity at the inlet of the domain.

### 339 **3.2 Sampler geometries**

340 Detail of the sampler construction are found in the electronic supplement (see **Figure S 4**, **Figure S 5**,  
341 **Figure S 6**).

#### 342 **3.2.1 Flat plate sampler**

343 Two different cases were calculated for the flat plate sampler (**Figure 3**), a deposition area diameter of  
344  $12\ \text{mm}$  and another of  $25\ \text{mm}$ .

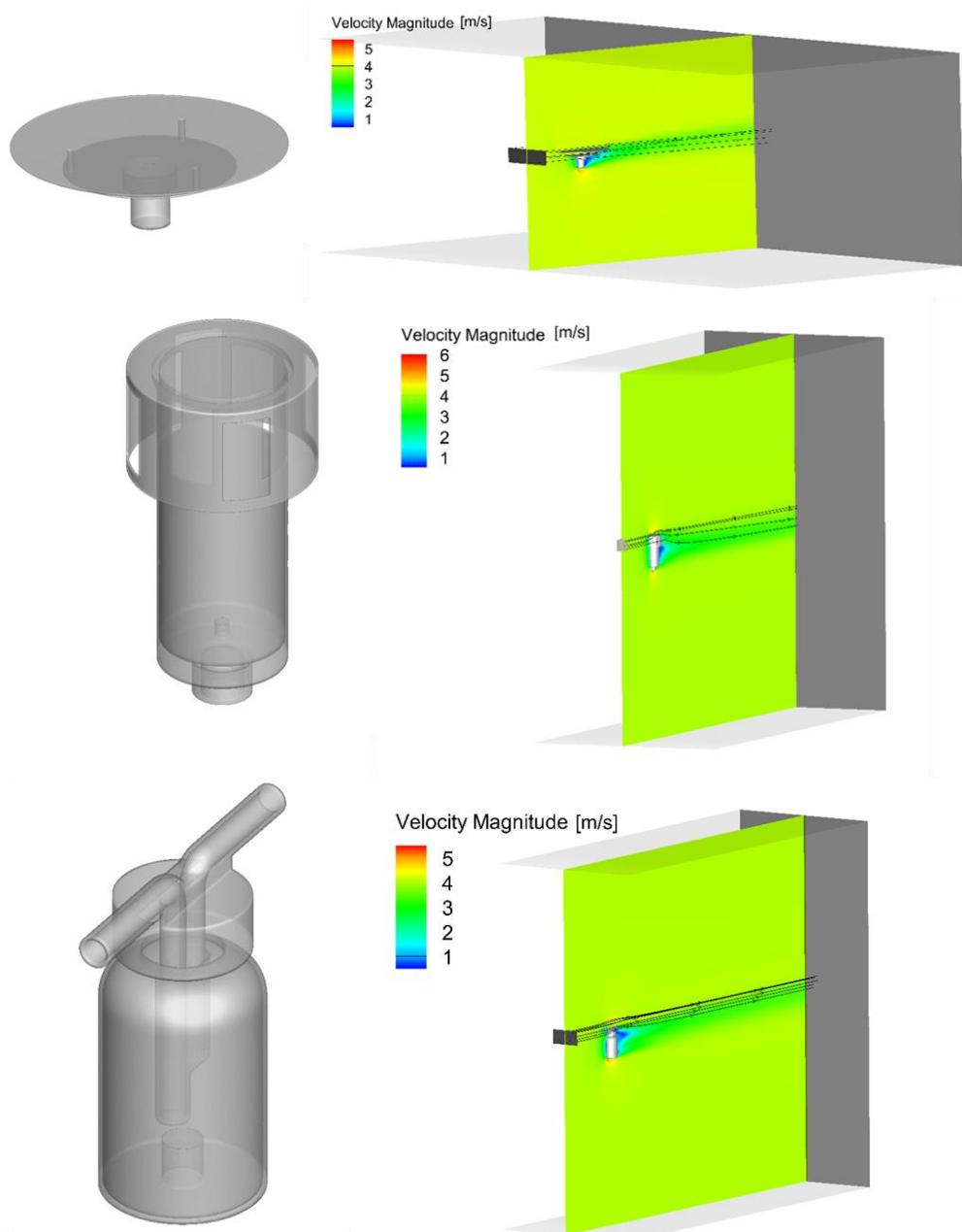
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351 **Figure 3:** Geometries of Flat plate sampler (top), Sigma-2 sampler (middle), MWAC sampler (bottom)  
352 CFD modeling domain and velocity magnitude, inlet velocity: 4m/s (right); in addition, the injection  
353 area is shown in black (Flat plate sampler: width 0.2 m, height 0.05 m; Sigma-2-sampler: width 0.2 m,  
354 height 0.1 m; Bottle sampler: width 0.1 m, height 0.05 m) along with exemplary streamtraces.



355 A mesh with 3920000 cells was generated and the flow field was calculated. In **Figure 3**, the velocity  
356 magnitude in the middle of the domain is shown for a velocity of 4 m/s at the inlet. 4000000 particles  
357 were injected. The deposition area boundary condition for DPM was set to “trap” and the walls were  
358 defined as reflecting boundaries.

### 359 3.2.2 Sigma-2 sampler

360 The geometry of the Sigma-2 sampler is given in **Figure 3**. A mesh with 7600000 cells was generated  
361 and the flow field was calculated. All wall boundary conditions were set to “trap” for the DPM model.

### 362 3.2.3 MWAC sampler

363 In **Figure 3** the geometry of the MWAC sampler is shown. A mesh with 4620000 cells was generated  
364 and the flow field was calculated. All wall boundary conditions were set to “trap” for the DPM model.

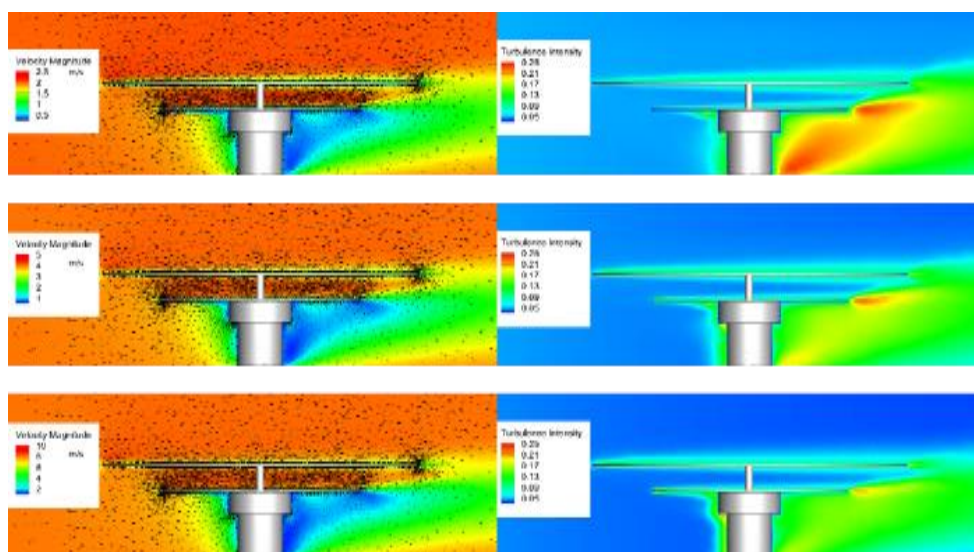
## 365 3.3 Velocity contours and vectors for the samplers

### 366 3.3.1 Flat Plate Sampler

367 The results in the cross section of the domain are shown in **Figure 4**. The formation of the boundary layer  
368 at the wall of the sampler is clearly visible at all velocities. At the central sampling location, the flow  
369 between the plates has the same velocity as the free stream, so for the analytical deposition models, the  
370 lower plate can be treated as single surface. The highest velocity is found at the sharp edge at the bottom  
371 of the sampler. Due to the high velocity gradients in this part there is also the highest turbulence intensity  
372 in the domain. As expected, the turbulent wake becomes smaller with increasing wind speed.

373

374

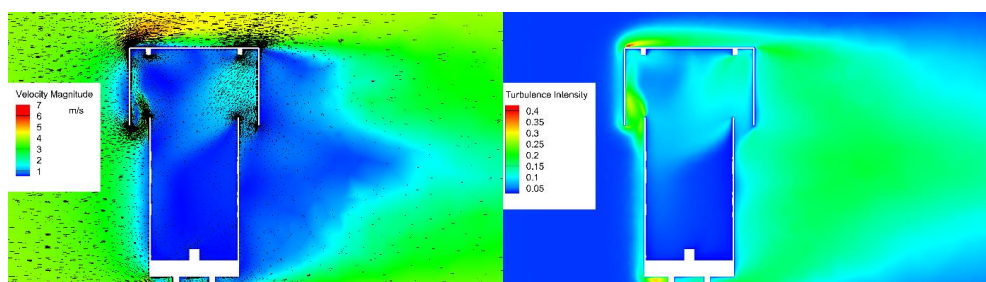


375

376 **Figure 4:** Flat Plate Sampler: Velocity magnitude and turbulence intensity at wind speed 2 m/s (top),  
377 Flat Plate Sampler: Velocity magnitude and turbulence intensity at wind speed 4 m/s (middle), Flat  
378 Plate Sampler: Velocity magnitude and turbulence intensity at wind speed 8 m/s (bottom).

379 3.3.2 Sigma 2 Sampler

380 The results in the cross section of the domain are shown for the 4 m/s case in **Figure 5**. Apparently the  
381 velocity magnitude inside the sampler is much smaller than outside. In the vertical settling tube, the  
382 turbulence intensity is low, justifying the idea of Stokes settling inside. Owing to the open, but bulky  
383 geometry, there is a flow into the interior at the back. The highest velocities and turbulence intensities  
384 are found at the sharp edges at the top and bottom of the sampler.



385

386 **Figure 5:** Sigma-2 Sampler: Velocity magnitude and turbulence intensity at wind speed 4 m/s.



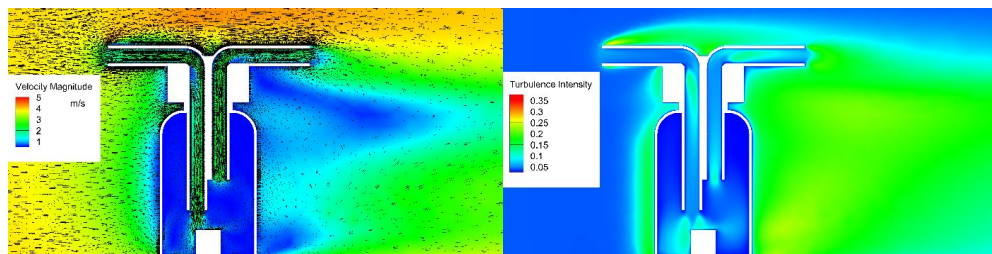


387 3.3.3 MWAC Sampler

388 The results in the cross section of the domain are shown for the 4 m/s case in **Figure 6**. Furthermore, the  
389 velocity field and the velocity vectors in the cross sections across and along the inlet tube are shown in  
390 **Figure 7**. In the tubes the typical pipe flow is formed. In the figures showing the cross sections along the  
391 inlet tube a symmetrical flow over the pipe cross section is visible.

392 In **Figure 8** the mean flow velocity in the MWAC tube is shown as a function of the outside velocity for  
393 the three cases. The fitting curve shows that the mean velocity in the pipe increases linearly with the  
394 external velocity.

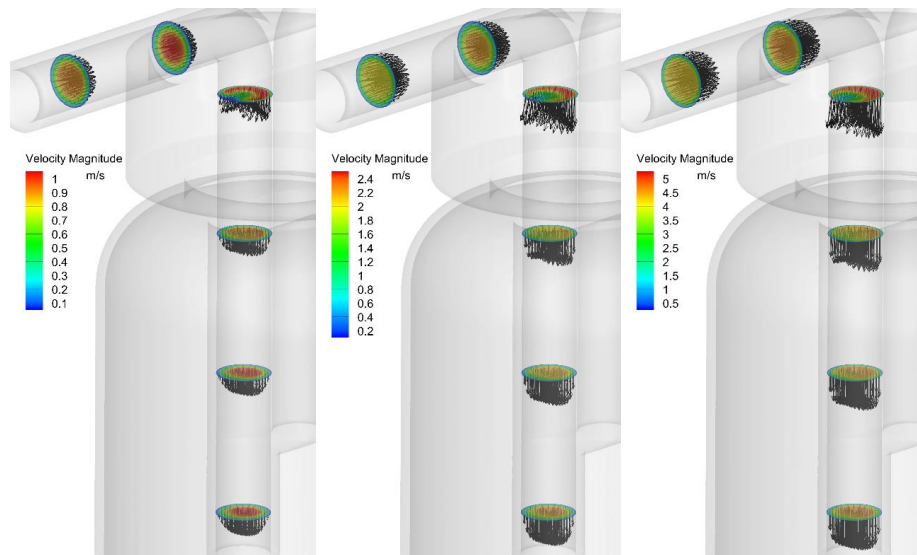
395 In comparison to the other geometries, the turbulent wake related to the geometry size is much bigger for  
396 the MWAC sampler.



397

398 **Figure 6:** MWAC Sampler: Velocity magnitude and turbulence intensity at wind speed 4 m/s.

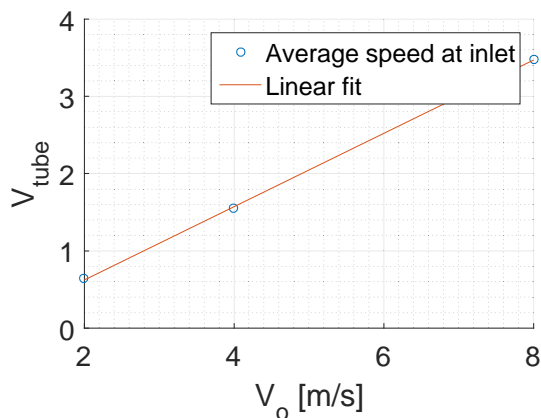
399



400



401 **Figure 7:** Velocity vectors at 2, 4 and 8 m/s (cross sections across and along the inlet tube).



402

403 **Figure 8:** Mean flow velocity ( $V_{tube}$ ) in the MWAC tube as a function of the outside velocity ( $V_o$ ).

404

Fitting curve:  $V_{tube} = 0.47V_o - 0.33$  for the range 2 – 8 m/s

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## 420 4 Results and Discussion

### 421 4.1 Methodical aspects (Field Measurements)

#### 422 4.1.1 Mass flux comparison between the samplers

423 Mineral dust was found to be the dominating particle type during this campaign, consisting of different  
424 silicates, quartz, calcite, dolomite, gypsum as reported previously for this location (e.g (Kandler et al.,  
425 2007)). Therefore, hygroscopicity was not taken into account, as due to the mostly non-hygroscopic  
426 compounds and the moderate humidities their impact was rated low. Details on the composition will be  
427 reported in a companion paper.

428 The mass and number fluxes (given per unit time and sample surface area) along with daily average  
429 temperature and wind speed are presented as daily values. Details for all days and all samplers can be  
430 found in the electronic supplement (see **Table S1, S2, S3, and S4 in the electronic supplement**).

431 **Figure 9** shows as example mass fluxes for different samplers during a dust event and a non-dust event  
432 day. For all samplers, the mass flux size distributions peaked in the 16-32 $\mu$ m interval. This result is in  
433 support of the conclusion that atmospheric dry deposition is dominated by coarse particles owing to their  
434 high deposition velocities (Davidson et al., 1985; Holsen et al., 1991). There is a considerable difference  
435 among different samplers, in particular for the size range with the highest mass deposition fluxes, whereas  
436 the difference is small for smaller particles. MWAC and BSNE – both horizontal flux samplers - collect  
437 more coarse material than Flat plate and Sigma-2 samplers, which in contrary measure the vertical flux.  
438 In particular, the MWAC sampler collects considerably higher coarse particle mass fluxes, probably  
439 owing to its impactor-like design.

440 **Table 1.** The campaign maximum and minimum fluxes measured by the samplers

Samplers	Maximum flux (mg/ (m <sup>2</sup> d))	Minimum flux (mg/ (m <sup>2</sup> d))
MWAC	1240	0.6
BSNE	310	0.2
Flat plate	80	2.0
Sigma-2	117	1.9

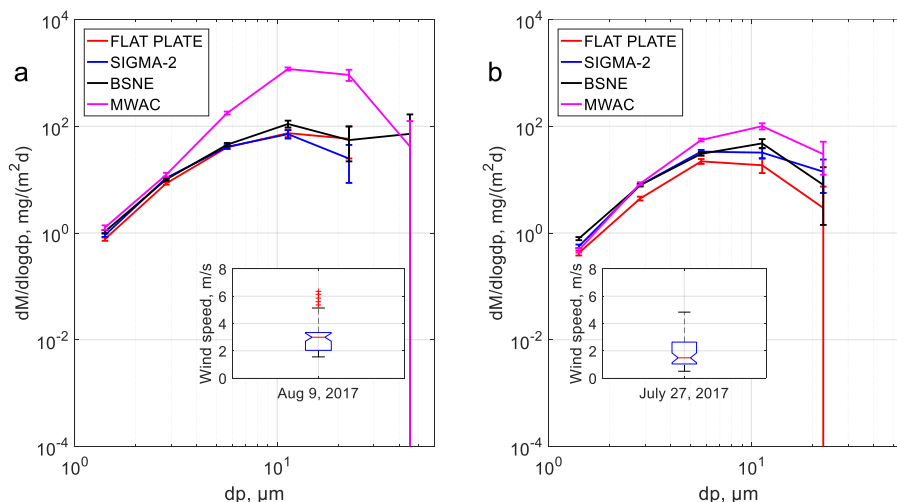
441

442 From **Table 1** it becomes obvious that the vertical flux instruments collect much less than material than  
443 the horizontal flux ones, in accordance with previous findings (Goossens, 2008). In the present study,  
444 horizontal to vertical flux ratio as function of particle size is approximately in between 2 and 50, while



445 Goossens (2008) reported it to be in between 50 and 160. This difference in the ratio might come from  
 446 the different approaches. Goossens (2008) used water as a deposition surface while in our study we used  
 447 a sampling substrate – a SEM stub suited inside a Flat plate geometry as deposition surface. MWAC  
 448 sampler is used a horizontal dust flux sampler in both studies. Furthermore, from **Figure 9**, we can clearly  
 449 see that that there is high temporal variation in deposition flux between dust event days and non-dust  
 450 event days. Generally, the temporal variation is much higher than difference between samplers.

451



452

453 **Figure 9:** Size resolved mass flux measured by different passive samplers: a) dust event day; b) non-  
 454 dust event day. Error bars show bootstrapped 95% confidence interval. The inserts show box plots for  
 455 the wind speed distribution based on 30-min intervals.

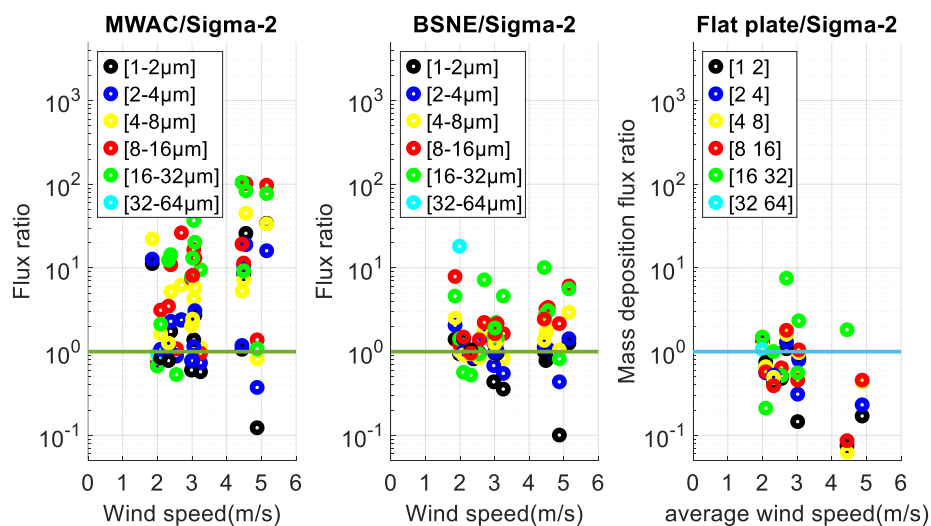
#### 456 4.1.1.1 Comparison in terms as function of wind speed and particle size

457 The daily box-plots of 30-min averaged wind speed at Izaña is shown in **Figure 13**. The average wind  
 458 speed during the campaign was about 3.5 m/s with the lowest daily median around 1.5 m/s and the highest  
 459 7 m/s.

460 **Figure 10** show the mass flux ratio of MWAC, BSNE and Flat plate to Sigma-2 as function of wind  
 461 speed. The collection efficiency of MWAC for large particles increases in comparison to Sigma-2 slightly  
 462 with increasing wind speed, while there is barely such increase visible for the BSNE. Both – being  
 463 horizontal sampler – collect considerably more material than the Sigma-2.

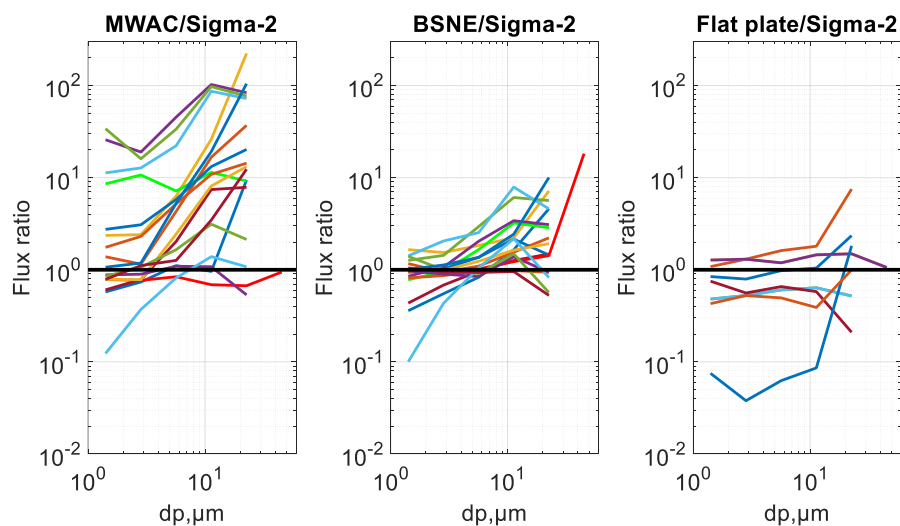


464 Similarly, **Figure 11** shows the deposition flux ratio of MWAC, BSNE and Flat plate to Sigma-2 against  
 465 particle size. On average, the mass flux ratio of Flat plate to Sigma-2 against wind speed and particle size  
 466 is less than one. This indicates that, on average at a given wind speed and particle size, Sigma-2 sampler  
 467 collects more particles than flat plate.



468

469 **Figure 10:** Flux ratio as function of wind speed for different days (MWAC/SIGMA-2 and  
 470 BSNE/SIGMA-2). Different colors represent different size intervals.



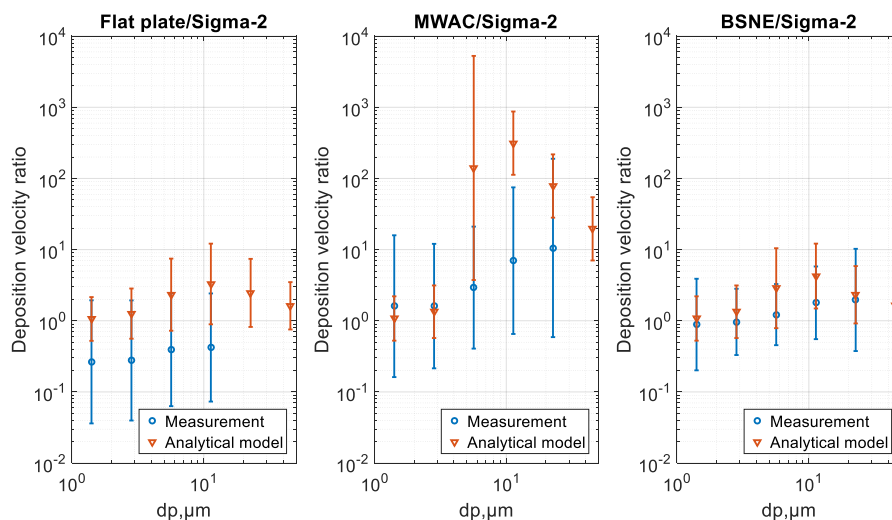
471



472 **Figure 11:** Flux ratio as function of particle size (MWAC/Sigma-2, BSNE/Sigma-2 and Flat plate/  
 473 Sigma-2). Different colors represent different measurement days.

474 In connection to this, the ratios of dry deposition flux (number) and deposition velocity from models are  
 475 shown in the **Figure 12**. The deposition velocity ratio from models is often higher than the ratios derived  
 476 from the mass and number (greater than factor of 2) due to reasons that are yet to be fully understood and  
 477 clarified.

478 The deposition velocity ratio from models also shows in increase with particle size, but up to some size  
 479 limit and then starts decreasing. The increase in flux ratio with particle size confirms that particle size,  
 480 among others, strongly affects the deposition velocity for particles.



481 **Figure 12:** Comparing geometric mean ratio of fluxes (Flat plate/Sigma-2 , MWAC/Sigma-2 ,  
 482 BSNE/Sigma-2 ) of measurements to geometric mean ratio of deposition velocity calculated using  
 483 models (Flat plate; Piskunov, MWAC; Piskunov & Sigma-2; Stokes). Error bars show geometric  
 484 standard deviations.  
 485

486 4.1.2 Dependence of small particle dust deposition on atmospheric PM<sub>10</sub> concentration and wind speed

487 **Figure S 2** (in the electronic supplement) and **Table 2** display the correlation between deposition number  
 488 fluxes, atmospheric number concentration by the OPC and the wind speed for different samples. It is  
 489 evident (**Figure S 2**) that there is generally a positive correlation between concentration and number flux,  
 490 which can be expected from the high variation in concentration compared to the lower variation in wind



491 speed. However, deposition rate and wind speed are even anti-correlated, indicating a cross-influence of  
 492 wind speed and concentration. Such a behavior was observed by different techniques for a dust transport  
 493 region (Kandler et al., 2011). Also, an ambiguous wind-dependency has been reported for other places  
 494 (Xu et al., 2016). The main driver of the deposition rate during this study is obviously the dust  
 495 concentration.

496 **Table 2:** Summary of regression analysis for correlation between dust deposition flux vs atmospheric  
 497 concentration and deposition flux vs wind speed. Significant relationships are shown in bold.

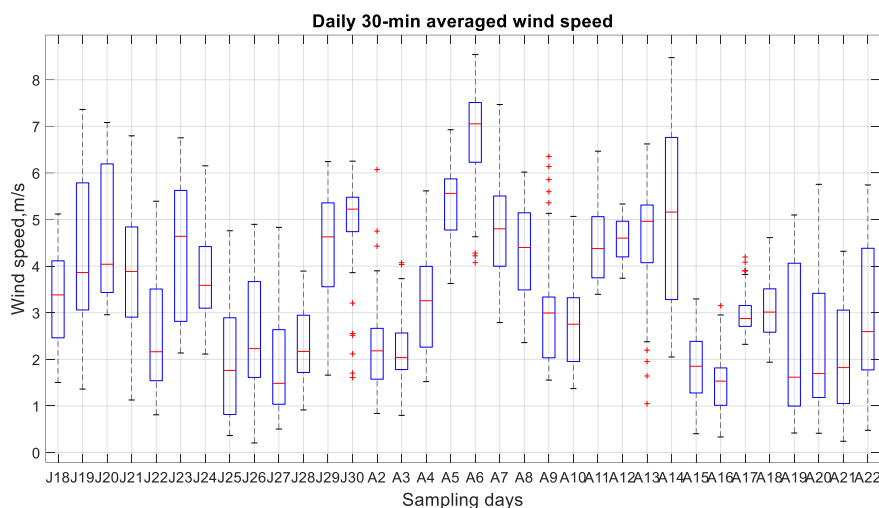
	Flux vs concentration			Flux vs wind speed		
	r <sup>2</sup>	p-value	slope (m/d)	r <sup>2</sup>	p-value	Slope (1.16*10 <sup>5</sup> /(m <sup>3</sup> ))
Flat plate	0.606	0.005	0.58	0.315	0.0726	-0.28
MWAC	0.287	0.171	0.21	0.391	0.0974	-0.17
BSNE	<b>0.975</b>	<b>1.5 * 10<sup>-8</sup></b>	<b>0.87</b>	0.014	0.729	-0.05
Sigma-2	<b>0.877</b>	<b>0.0002</b>	<b>0.78</b>	0.0128	0.772	-0.07

498

499 In a second step the correlation between modeled dust concentration from different samplers and the  
 500 corresponding OPC-measured concentration was assessed **Table 2**. However, no increase in correlation  
 501 is observed, indicating that – like already observed from the ratio calculations above – the deposition  
 502 models fail to describe the deposition behavior in detail.

503 From the correlation relations it can be learned that MWAC is least suitable for estimating PM<sub>10</sub>, which  
 504 fully agrees well with previous studies (Mendez et al., 2016). However, the correlation analysis here  
 505 shows that BSNE is actually a suitable instrument for a PM<sub>10</sub> estimation, which is in contrast to the wind-  
 506 tunnel observation of (Mendez et al., 2016). This discrepancy might be derived from the different  
 507 approaches. While in the referred previous work the loss of concentration from the passing aerosol was  
 508 measured, here a gain of deposition was investigated. As result, for lower deposition velocities (discussed  
 509 below), the former approach will yield high uncertainties. Similar to BSNE, flat plate and Sigma-2 appear  
 510 good estimators for PM<sub>10</sub>, which is also in accordance with previous studies (Dietze et al., 2006).

511



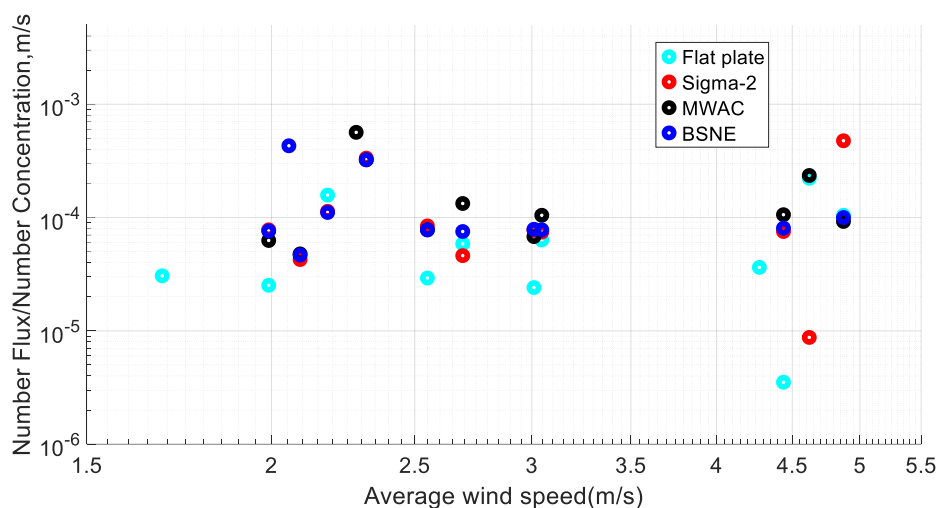
512

513 **Figure 13:** Daily box-plots of 30-min averaged wind speed observed at Izaña Atmospheric  
514 Observatorio from 18/July/2017 to 23/August/2017. The black vertical lines show the standard  
515 deviation (J=July, A=August).

#### 516 4.1.2.1 Small particle apparent deposition velocity (PM<sub>10</sub> size range: 1-2µm, 2-4µm, 4-8µm)

517 **Figure 14** displays the apparent deposition velocity (the ratio of the number flux to the concentration of  
518 the OPC, for each particle size class) as function of wind speed for different samplers. Obviously, there  
519 is not clear trend for the small particles. The effective deposition velocities range between  $3.5 \cdot 10^{-6}$ -  
520  $5.7 \cdot 10^{-4}$  m/s. As can be clearly seen from the plot, the effect of wind speed on deposition velocity is  
521 negligible.





522

523 **Figure 14:** Apparent deposition velocity: ratio of number flux (approximately **PM<sub>10</sub>** size range) to  
524 number concentration (OPC; approximately **PM<sub>10</sub>** size range) as function wind speed.

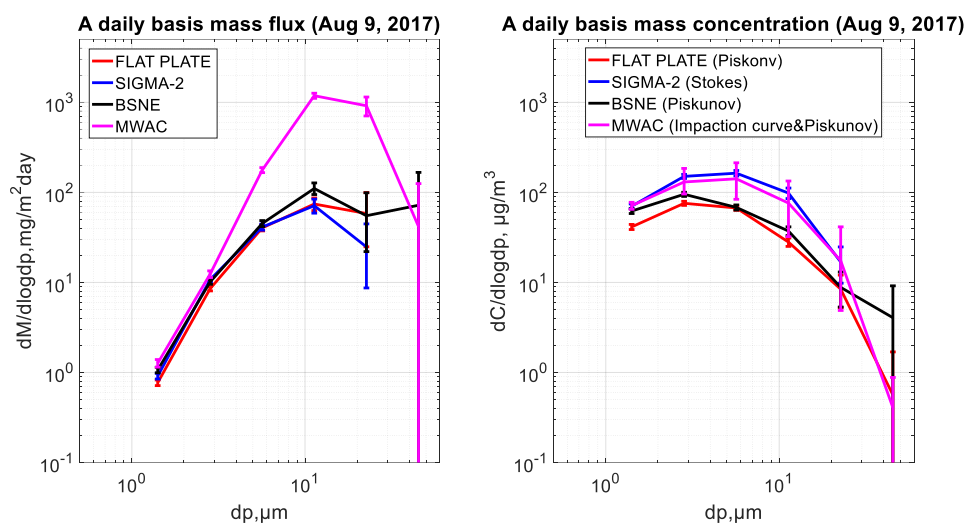
525 4.1.3 Atmospheric mass concentration calculation from deposition flux

#### 526 4.1.3.1 Consistency between samplers

527 **Figure 15** compares a mass flux size distribution with the according concentrations derived by the  
528 modeled deposition velocities. Mass concentrations calculated from different passive samplers agree  
529 generally well with respect to the statistical uncertainties, which is the case for most of the days (**see also**  
530 **Figure S1 in the electronic supplement**). This indicates that the deposition velocity models selected for  
531 the samplers are generally suitable, despite the deviations in single cases.



532



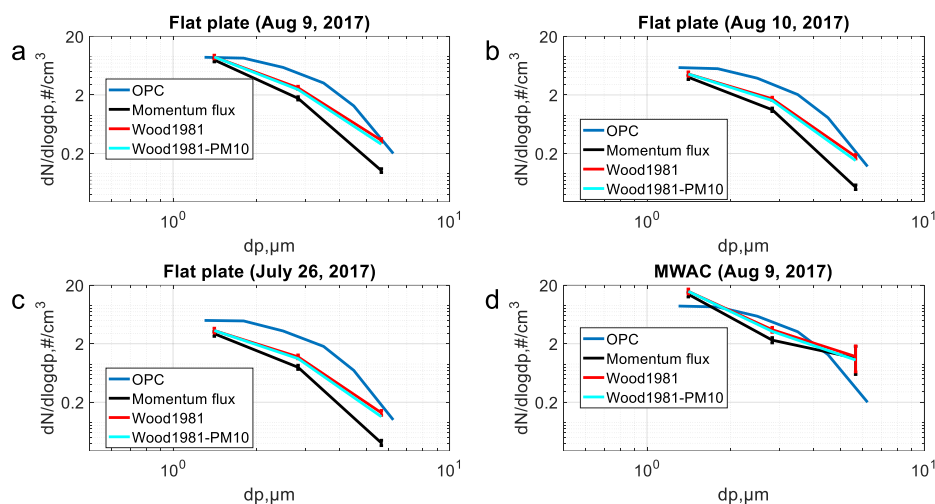
533

534 **Figure 15:** Comparing dust mass flux and dust mass concentration. Bars show 95% confidence  
 535 interval.

536 **4.1.3.2 Size-resolved comparison with active samplers**

537 The calculated number concentration in size interval between 1–10µm is validated through a comparison  
 538 with concentration measured using OPC (Grimm). Similarly, the mass concentration size distribution  
 539 above PM<sub>10</sub> size range is validated using the FWI measurements.

540 **Figure 16** shows the comparisons of number size distributions calculated from flux measurements of the  
 541 flat plate and MWAC sampler with ones measured using the OPC for different days. Overall number  
 542 concentrations obtained from OPC measurement are slightly higher than the ones from the fluxes. To the  
 543 contrary, for low-dust days they are slightly smaller.



544

545 **Figure 16:** Comparing number concentration from measurement with number concentration by OPC  
546 measurement (Flat plate sampler (a), (c), (d), and MWAC (b); daily average wind speed=3.05m/s,  
547 2.69m/s, 2.28m/s and 2.55m/s for Aug 9, 2017, Aug 10, 2017, Aug 2, 2017 and July 2017  
548 respectively). The light blue curve shows the concentration curve calculated using (Piskunov – Wood  
549 approach) with PM<sub>10</sub> inlet correction (atmospheric concentration), the red curve shows the  
550 concentration curve calculated using (Piskunov – Wood approach); The green curve shows the  
551 concentration curve calculated using (Piskunov – Momentum flux approach); The dark blue curve  
552 shows the concentration measurement by OPC. Bars show the central 95 % confidence interval

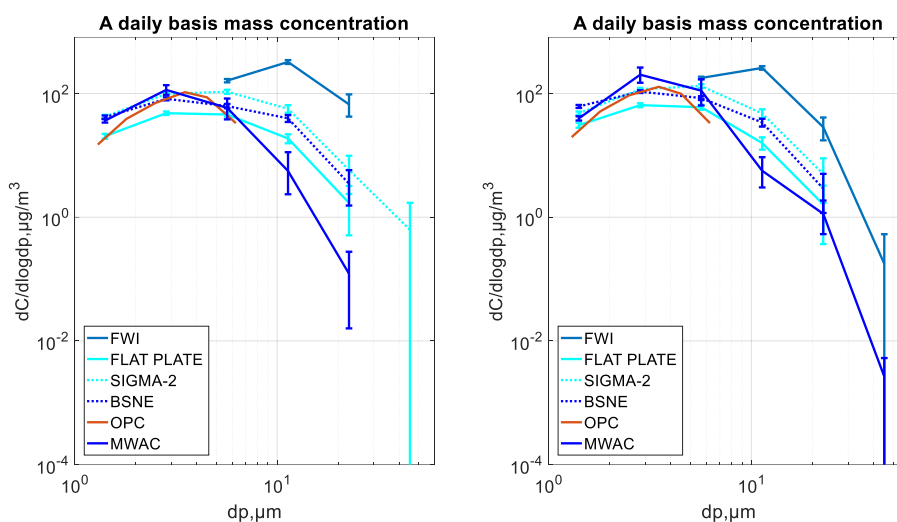
553 In general, **Figure 16** show that the deviation of calculated values from OPC measured values is  
554 significant.

555 In this connection, the above figure (**Figure 16**) also show the comparison of the mass concentration  
556 size distribution measurement obtained by eddy covariance method of u-s estimation (Ettling, 1996)  
557 and the size distribution measurement obtained with friction velocity estimated using Wood (1981)  
558 approach. As shown in the figures, the mass concentration deduced using friction velocity estimated  
559 from Wood (1981) formulation appear larger than the ones deduced from the momentum flux and  
560 therefore agree in our case better with OPC data.

561 For a comparison with large particles, measurements of FWI are used (**Figure 17**).



562



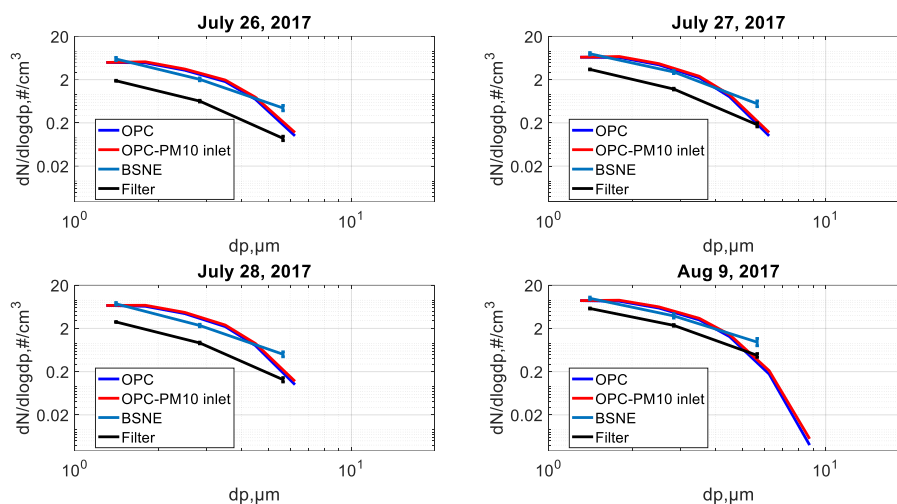
563

564 **Figure 17:** a daily basis mass concentration measured with passive-sampler method, in comparison to  
565 active samplers (FWI). Error bars show the central 95% confidence interval.

566 Here, a large inconsistency occurs between mass size distribution by passive samplers and by FWI. In  
567 particular, the size range larger than 10 µm seems to be largely underestimated by the passive samplers.  
568 While for particles around 10 µm, this could be partly to a badly-defined collection efficiency curve of  
569 the FWI (Kandler et al. 2018; 50 % cut-off at 11 µm) and the according correction, this can't be the  
570 reason for the large particles, where this efficiency approaches unity. Here, either the deposition velocity  
571 for the samplers is apparently overestimated.

572 A further comparison of deposition-derived concentrations with these determined from the iso-axial filter  
573 sampler (**Figure 18**) shows that, while the calculated size distributions are in good agreement with the  
574 OPC ones, the filter-derived seem to relatively underestimate the concentrations.

575 Moreover, a correlation analysis (R-squared: 0.947, p-value = 0.0053 and slope = 2.0733) suggests that  
576 there is a positive correlation between calculated number concentration from filter samples and the OPC  
577 measured concentration.

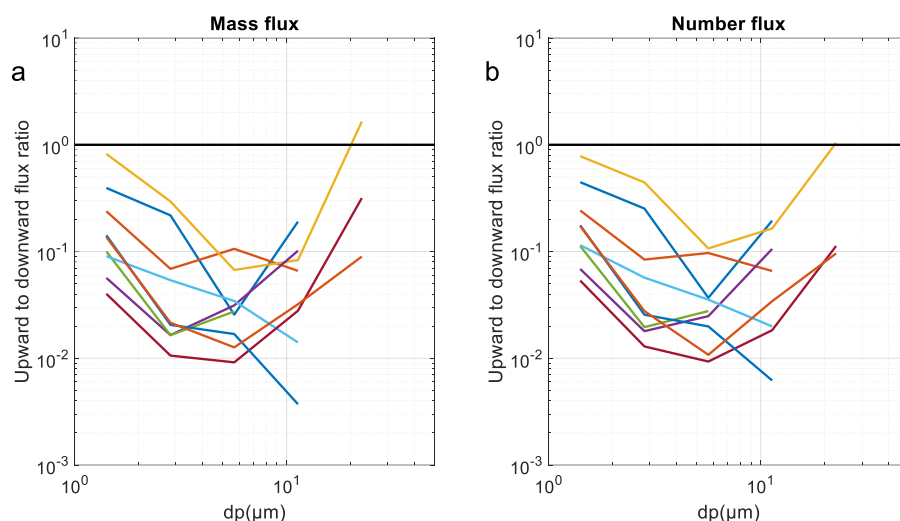


578

579 **Figure 18:** Number concentration measured with Filter-sampler method, in comparison to BSNE and  
580 OPC. The red curve shows OPC with **PM<sub>10</sub>** inlet efficiency correction.

581 4.1.4 Estimating the turbulent versus gravitational transport fraction by upward-/downward-facing  
582 measurements

583 Details of size resolved mass and number flux measurements along with daily average temperature and  
584 wind speed for up-ward and down-ward flux is given in the electronic supplement (see **table S5 and S6**).  
585 The upward flux is always less than the downward flux. This is expected because the upward facing  
586 substrate (for the downward flux) collects particles deposited by gravitational settling and turbulent  
587 inertial impaction, while the downward facing substrate (for the upward flux) collects particles only by  
588 means of turbulent impaction. **Figure 19** shows the mass and number flux ratio of upward flux to  
589 downward flux as function of particle size. The deviation is greatest for the particle size range around 8  
590  $\mu\text{m}$ , which are strongly affected by turbulence (Noll and Fang, 1989). However, only a very weak trend  
591 of increasing ratio with increasing wind speed can be found here (see **Figure S 3** in the electronic  
592 supplement). Besides the wind speed magnitude, different properties were calculated (e.g, turbulent  
593 intensity, Monin-Obukhov length, relative standard deviation of wind speed, average vertical  
594 component), but none of them was able to explain the observed variations in the flux ratio.

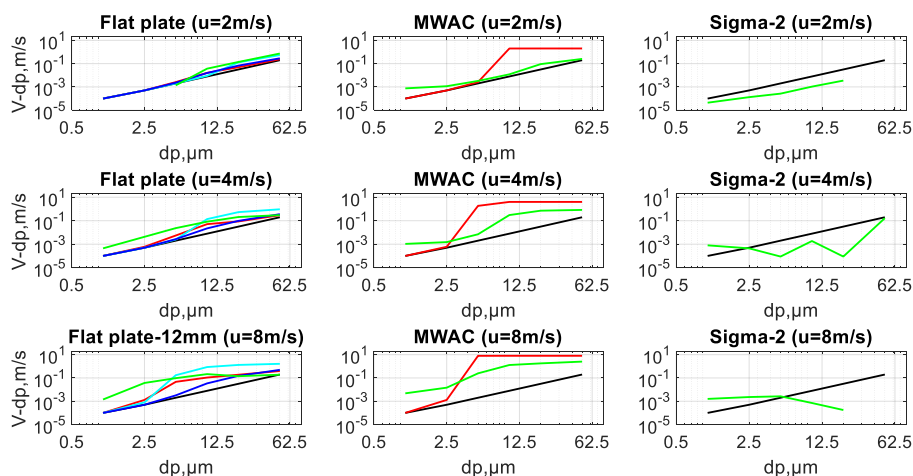


595

596 **Figure 19:** Upward to downward flux ratio vs particle size. The flux is measured using flat plate  
 597 sampler (with 25mm stub), Mass flux (a) and number flux (b). Different colours represent different  
 598 measurement days.

599 **4.2 Computational fluid dynamics (CFD) simulation**

600 Using computational fluid dynamics (CFD), deposition velocities of particles for different passive  
 601 samplers were predicted and compared to the analytical deposition velocity models used for the different  
 602 samplers (see **Figure 20**).



603

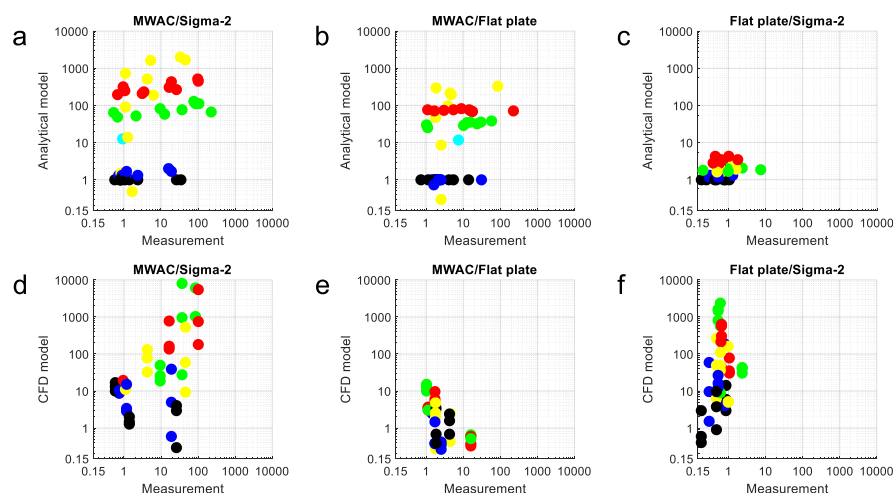


604 **Figure 20:** The red curve shows deposition velocity calculated using Piskunov deposition velocity  
605 model, the black curve shows deposition velocity calculated using Stokes's velocity, the blue curve  
606 shows deposition velocity calculated using Noll and Fang deposition velocity model, the cyan curve  
607 shows deposition velocity calculated using Zhang deposition velocity model, the green curve shows  
608 deposition velocity from CFD.

609 While for the flat plate and MWAC sampler the curves agree qualitatively, for the Sigma-2 except for  
610 the lowest wind velocity, they are largely contrary. The latter might be owed to the fact that in a flow  
611 model the non-omnidirectional construction of the Sigma-2 might lead to preferred airflows, which are  
612 not relevant in a more variable and turbulent atmosphere. However, also for the former ones, the  
613 deposition velocity curves are quantitatively different. **Figure S 7** in the electronic supplement shows  
614 comparison of the CFD-derived particle deposition velocities at different wind speed values for different  
615 samplers.

#### 616 **4.3 Comparison of measured deposition flux ratios to analytically and CFD modeled ones**

617 **Figure 21** shows comparison of correlations of the deposition velocity ratios derived from the analytical  
618 models (left column) with the according measured deposition velocity (taken as according flux ratio)  
619 with the correlation of the ratios derived from CFD modeling with the measurement. As the CFD models  
620 could only be calculated for a limited number of flow velocities, deposition velocity values were  
621 interpolated between the calculated cases. Generally, the agreement is very low. Practically no variation  
622 observed in the measurement data can be explained by model variation, independent of the type of model.  
623 While this might be explained to a smaller extent by the propagating measurement uncertainties for the  
624 largest particles with low counting statistics, for the smaller ones this systematic deviation must have  
625 other reasons.



626

627 **Figure 21:** Comparison of deposition velocity ratios (MWAC/Sigma-2; measurement to analytical  
628 model (a); measurements to model, MWAC/Flat plate; measurement to analytical model (b), Flat  
629 plate/Sigma-2; measurement to analytical model (c), MWAC/Sigma-2; measurement to CFD model  
630 (d), MWAC/Flat plate; measurement to CFD model (e), Flat plate/Sigma-2; measurement to CFD  
631 model (f) plate/Sigma-2). Different colors represent different size intervals of different measurement  
632 days; 1-2 $\mu\text{m}$ : Black, 2-4 $\mu\text{m}$ : Blue, 4-8 $\mu\text{m}$ : Yellow, 8-16 $\mu\text{m}$ : Red, 16-32 $\mu\text{m}$ : Green, 32-64 $\mu\text{m}$ : Cyan.

## 633 5 Summary and Conclusions

634 Dust aerosol deposition measurements by means of deposition and other passive samplers were  
635 conducted at Izaña Global Atmospheric Watch observatory continuously from 14th of July to 24th of  
636 August 2017. In addition, active aerosol collection was done with a free-wing impactor and an iso-axial  
637 filter sampler. Additional information regarding the aerosol particle size distributions has been obtained  
638 by an OPC Izaña. The single-particle data of size, flux and concentration of over 315,000 particles from  
639 6 different samplers were obtained by applying a SEM-EDX technique. Different samplers are compared  
640 based on size-resolved measurements, which makes our work unique when compared to previous works.

641 As known from previous studies, the total deposition flux was dominated by coarse particles (16-32  $\mu\text{m}$ ).  
642 A high temporal variability in dust flux was observed on a daily basis.

643 The size resolved flux measurements of different passive samplers varied significantly between the  
644 samplers under the same conditions. This is to be expected from the different sampler construction.  
645 Applying suitable deposition velocity models, atmospheric concentrations can be calculated from





646 different sampler deposition fluxes, which are more in agreement. However, discrepancies beyond the  
647 measurement uncertainty remain unexplained by the deposition models.

648 In particular when considering the size-resolved deposition velocities and flux ratios, great discrepancies  
649 show up. While for an integrated bulk measurement or the PM<sub>10</sub> size range at least a qualitative agreement  
650 can be reached, no model – analytical nor CFD – is able to explain the observed variations in deposition  
651 flux between the samplers. Clearly, a better physical understanding is needed here.

652 The deposition velocity calculated from different models and flux measured from different samplers are  
653 then used to calculate size resolved concentration. Nevertheless, the estimation of an appropriate  
654 deposition velocity from different models is one of the main challenge of this work. The deposition  
655 velocity model we applied in the calculation for concentration contains the gravitational and inertial  
656 components of particle deposition.

657 We found also that the mass concentrations size distribution calculated from different passive samplers  
658 have approximately the same values, which further confirms that the deposition velocity models selected  
659 for this work are the appropriate ones to calculate mass concentration from mass flux. In this connection,  
660 a comparison of friction velocity estimated from different approaches demonstrates that one approach  
661 for some days is more pronounced than other measurement days, which could mean that the concentration  
662 estimation from deposition flux might work better for a particular day with one approach than with the  
663 other approach.

664 A very good agreement is found between the calculated concentration for samples from different passive  
665 and active samplers and the concentration measured using OPC (Grimm) (this is particularly for particles  
666 approximately in PM<sub>10</sub> size range). For particle sizes above PM<sub>10</sub>, comparison of size distribution is made  
667 to a novel FWI and comparison shows the results does not agree.

668 A deposition velocity results from different classical deposition models for different samplers are  
669 compared to the deposition velocity calculated using a computational fluid dynamics simulations. The  
670 comparison shows two methods do not agree. The deposition velocity calculated from computational  
671 fluid dynamics looks more extreme in comparison to the one calculated from classical deposition models.

672 The correlation analysis between dust flux, dust concentrations and wind speed reveals that the change  
673 in flux is mainly controlled by changes in concentration; variation of wind speed play a minor role for  
674 wind speeds lower than 6 m/s. Situation might be different for higher wind speeds (e.g., Kandler et al.  
675 2018). In connection to this, correlation analysis on number concentration calculated for samples from  
676 different samplers yielded diverging results. It demonstrated that BSNE can be a good option for PM<sub>10</sub>



677 measurement while MWAC as a horizontal flux sampler is not a suitable option for  $PM_{10}$  measurement.  
678 The analysis also showed that Flat plate and Sigma-2 geometries can also be a good option for measuring  
679  $PM_{10}$  (Sigma-2 is better than Flat plate).

680 This data set provides the size-resolved information on deposition rate and concentration of mineral  
681 aerosol particles which will help to assess special and temporal variability. A hypothesis of our study was  
682 that the passive samplers could be capable of measuring size resolved particle concentration above the  
683  $PM_{10}$  size range. However the results show that the samplers are not capable of producing measurements  
684 consistent between the samplers or versus active collection techniques. Therefore, a recommendation  
685 must be that if a certain sampler type is chosen for a study, it should not be modified or replaced by  
686 another one for consistency of results. In a broader context, the results show nevertheless that passive  
687 sampling techniques coupled with an automated single particle analysis provides insights into the  
688 variation of size distribution, flux and concentration of atmospheric particles.

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710 7 Author contribution

711 A. W. conducted the field measurements and the data evaluation. K. S. helped with the field  
712 measurements, carried out the SEM analyses and did data processing. J. M. and B. E. executed the CFD  
713 model setup and calculations. S. R. operated the OPC including the data processing and the  
714 meteorological base measurements. K. K. designed the experiment, designed and prepared the sampling  
715 equipment and did data processing and interpretation. All authors contributed to the data discussion and  
716 manuscript preparation.

717 8 Data availability

718 The data sets used for this publication are available from the Pangaea repository free of charge (Waza et  
719 al., doi: tbd.)

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