- 1 Direct measurement of N₂O₅ heterogeneous uptake coefficients on ambient
- 2 aerosols via an aerosol flow tube system: design, characterization and
- 3 performance
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- 19 **Abstract.** An improved aerosol flow tube system coupled with detailed box model was
- developed to measure N_2O_5 heterogeneous uptake coefficients ($\gamma(N_2O_5)$) on ambient aerosols
- 21 directly. This system features sequential measurements of N₂O₅ concentration at the both
- 22 entrance and exit of the flow tube to ensure an accurate retrieval of N₂O₅ loss in the flow tube.
- 23 Simulation and laboratory tests demonstrate that this flow tube system is able to overcome the
- interference from side reactions led by varying reactants (e.g., NO₂, O₃ and NO) and improve
- 25 the robustness of results with the assistance of box model method. Factors related to $\gamma(N_2O_5)$
- derivation were extensively characterized, including particle transmission efficiency, mean
- 27 residence time in the flow tube and wall loss coefficient of N₂O₅, for normal operating

condition. The measured $\gamma(N_2O_5)$ on $(NH_4)_2SO_4$ model aerosols were in good agreement with literature values over a range of relative humidity (RH). The detection limit of $\gamma(N_2O_5)$ was estimated to be 0.0016 at low aerosol surface concentration (Sa) condition of 200 μm^2 cm⁻³. Given the instrument uncertainties and potential fluctuation of air mass between successive sampling modes, we estimate the overall uncertainty of $\gamma(N_2O_5)$ that ranges from 16 to 43% for different ambient conditions. This flow tube system was then successfully deployed for field observations at an urban site of Beijing influenced by anthropogenic emissions. The performance in field observation demonstrates that the current setup of this system is capable of obtaining robust $\gamma(N_2O_5)$ amid the switch of air mass.

1 Introduction

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38 Dinitrogen pentoxide (N₂O₅), forming from the reaction of nitrogen dioxide (NO₂) and nitrate 39 radical (NO₃), acts as an important reservoir of atmospheric nitrogen. The N₂O₅ can undergo 40 either thermal dissociation (back to NO₂ and NO₃; photolysis of NO₃ also generate NO₂) to 41 release NO₂ or hydrolysis (both homogeneous and heterogeneous) to remove nitrogen oxides 42 from the atmosphere (Brown and Stutz, 2012; Chang et al., 2011). Among the budgets of N₂O₅, 43 the uptake on aerosol particles is a highly efficient pathway to be responsible for production 44 of nitrate aerosol in some regions (Fu et al., 2020; Wang et al., 2019; Wang et al., 45 2017c; Baasandorj et al., 2017; McDuffie et al., 2019; Prabhakar et al., 2017; Wang et al., 46 2018a; Chen et al., 2020) and promote activation of chlorine via ClNO₂ formation (Bertram 47 and Thornton, 2009a; Osthoff et al., 2008; Tham et al., 2018; Thornton et al., 2010; Wang et al., 48 2017f;Riedel et al., 2012a;Riedel et al., 2013;Gaston and Thornton, 2016;Mitroo et al., 2019). 49 The N_2O_5 uptake coefficient ($\gamma(N_2O_5)$) is critical in determining the uptake reaction rate of 50 N₂O₅ on aerosol in addition to aerosol surface area (Sa). It represents the fraction of collisions 51 between gaseous N₂O₅ molecules and particle surfaces that resulted in a loss of N₂O₅. Model 52 simulation showed the variations in $\gamma(N_2O_5)$ can significantly influence the fate of NOx, O₃ and OH radical in a regional (Li et al., 2016; Sarwar et al., 2012; Lowe et al., 2015) and global 53 scale (Dentener and Crutzen, 1993; Evans and Jacob, 2005; Macintyre and Evans, 2010; Murray 54

et al., 2021). However, ambient data of direct observation on $\gamma(N_2O_5)$ is still scarce. It is thereby necessary to develop an accurate equipment or method to quantify this parameter on ambient aerosols.

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Extensive laboratory experiments have been conducted to derive the values of $\gamma(N_2O_5)$ on aerosols and understand the mechanism of N₂O₅ uptake by various methods, including aerosol flow reactor (Kane et al., 2001; Mozurkewich and Calvert, 1988; Hu and Abbatt, 1997; Thornton and Abbatt, 2005; Thornton et al., 2003; Tang et al., 2014; Bertram and Thornton, 2009a; Cosman et al., 2008; Escoreia et al., 2010; Gaston et al., 2014; Folkers et al., 2003), droplet train reactor (Van Doren et al., 1990; Schweitzer et al., 1998), Knudsen flow reactor (Karagulian et al., 2006) and smog chamber (Wahner et al., 1998; Wu et al., 2020). The γ (N₂O₅) was found to be highly variable and dependent on particle chemical composition, acidity, size, phase state and the presence of organic coating using these laboratory methods under controllable conditions (Badger et al., 2006; Bertram et al., 2011; Fried et al., 1994; Griffiths et al., 2009; Gross et al., 2009; Hallquist et al., 2000; McNeill et al., 2006; Mentel et al., 1999; Riemer et al., 2003; Gaston and Thornton, 2016; Escoreia et al., 2010; Gaston et al., 2014; Thornton et al., 2003). While laboratory results have contributed to recognize the mechanism of N_2O_5 uptake and develop $\gamma(N_2O_5)$ parameterizations (Anttila et al., 2006; Bertram and Thornton, 2009b; Davis et al., 2008; Griffiths et al., 2009; Riemer et al., 2009), issues might emerge when quantitatively extended to ambient conditions due to the discrepancy between laboratory conditions and real air mass. For example, much higher reactant and particle concentration usually used in laboratory experiments might induce surface saturation or secondary reactions in a short time period, which lead to the bias of reaction rate used in ambient conditions (Thornton et al., 2003). In addition, the physicochemical properties of ambient aerosol are much more complicated that the model aerosol used in laboratory studies, which led to the laboratory results on model aerosols are difficult to accurately represent what happens on the atmospheric aerosols (Royer et al., 2021; Mitroo et al., 2019).

There have been several methods implemented for field campaigns to indirectly derive $\gamma(N_2O_5)$, simply based on observation of ambient NO₃, N₂O₅, NO₂, O₃, ClNO₂, pNO₃⁻ and

other auxiliary parameters without special equipment to capture the decay of N₂O₅ like laboratory ways. These include (1) the linear fit between N₂O₅ (NO₃) lifetime and the product of NO₂ and Sa concentration according to steady state equations (Brown et al., 2002;Brown et al., 2009;Brown et al., 2006;Platt et al., 1984;Wang et al., 2017b;Wang et al., 2017d;Tham et al., 2016;Wang et al., 2017f;Brown et al., 2016), (2) the analysis of production rates of products (pNO₃⁻ and ClNO₂) resulting from N₂O₅ uptake under a stable condition (Mielke et al., 2013;Phillips et al., 2016;Wang et al., 2018b) and (3) box model simulations with an iterative approach to reproduce the evolutions of NO₃-N₂O₅ chemistry within each separate air mass after sunset (McDuffie et al., 2018;Wagner et al., 2013;Wang et al., 2020a;Yun et al., 2018). All these methods contain some specific assumptions and are only applicable in a few special cases.

To directly determine the $\gamma(N_2O_5)$ on ambient aerosols, Bertram et al. (2009a) firstly design an entrained aerosol flow reactor to adapt for low atmospheric Sa concentration with easy operation. By switching between filtered and bypass sampling mode, the N_2O_5 concentration at the exit of flow tube can be measured in the presence and absence of aerosols, respectively. The pseudo-first-order rate coefficients for N_2O_5 loss on aerosols is thereby derived from the ratio of measured N_2O_5 concentration in these two modes within a duty cycle according to Eq. 1:

$$k_{aerosols} = -\frac{1}{\Delta t} \ln \frac{[N_2 O_5]_{\Delta t}^{w/particles}}{[N_2 O_5]_{\Delta t}^{wo/particles}}$$
 Eq. 1

where the Δt is the mean residence time of the flow tube, and the $[N_2O_5]_{\Delta t}^{wo/particles}$ and $[N_2O_5]_{\Delta t}^{w/particles}$ are the measured N_2O_5 concentration at the exit of flow tube in filtered and bypass mode, respectively. Assuming the gas-phase diffusion effect is negligible for atmospheric particles and low reaction probability (γ <0.1) (Fuchs and Sutugin, 1970), γ (N_2O_5) can then be calculated from Eq. 2:

$$\gamma(N_2O_5) = \frac{4 \times k_{aerosols}}{c \times S_a}$$
 Eq. 2

This method was deployed to measure $\gamma(N_2O_5)$ on ambient particles during two field campaigns (Bertram et al., 2009b;Riedel et al., 2012b) and on aerosols generated in the laboratory (Ahern et al., 2018). While values of $\gamma(N_2O_5)$ were determined to be robust in laboratory experiments, most of data would be dropped under ambient conditions due to the variations of wall loss coefficients (dominated by RH), fresh NO emission, N_2O_5 regeneration and flow pattern inside the flow tube. Based on the above measurement system, Wang et al. (2018c) added NOx, O_3 and Sa measurement on the exit of flow tube and introduce an iterative box model to minimize the potential influences from changing air mass and non-linear response of interference reactions. With the assumption of the equilibrium between NO_3 and N_2O_5 , the box model runs backward and forward iteratively to obtain the N_2O_5 loss rate constant in the absence ($k_{het}^{wo/particles}$) and presence ($k_{het}^{w/particles}$) of aerosols respectively. The difference between these two parameters can finally derived the $\gamma(N_2O_5)$ according to Eq. 3, assuming the wall loss effect stays consistent.

$$\gamma(N_2O_5) = \frac{4(k_{het}^{w/particles} - k_{het}^{wo/particles})}{c \times S_a}$$
 Eq. 3

This iterative approach was demonstrated to be able to buffer against certain fluctuations of air mass and measure $\gamma(N_2O_5)$ in the polluted atmosphere (Yu et al., 2020b).

Until now, only few direct measurements of $\gamma(N_2O_5)$ on ambient aerosols have been conducted during field campaigns (Bertram et al., 2009b;Riedel et al., 2012b;Yu et al., 2020a). Even though combining with dataset from indirect approaches (e.g. steady state approximations), it is still challenging to characterize the temporal and spatial distributions of $\gamma(N_2O_5)$ on ambient aerosols. To better investigate the reactive uptake of N_2O_5 on aerosols in different environments, we develop an aerosol flow tube system with newly designed gas circuit and data acquisition procedures to quantify $\gamma(N_2O_5)$ on ambient aerosols. In the following sections, the setup of this system and laboratory characterizations for each part are described in details. Procedures of acquiring and processing data are compared to previous methods and discussed with potential uncertainties. Laboratory tests on model aerosols and field observations are presented to demonstrate its performance under varying ambient

conditions.

2 The aerosol flow tube system

A schematic of the aerosol flow tube system is shown in Figure 1. The ambient air enters the system from the sampling manifold, mixes with gaseous N_2O_5 source in a Y-tee and flows to aerosol flow tube and detection instruments, as indicated by arrows in the figure. The design of sampling module and aerosol flow tube in this work follows previous work for measuring $\gamma(N_2O_5)$ on ambient aerosols (e.g. Bertram et al., 2009). The major improvement of this system from previous work are continuous monitor of NOx and O_3 concentration before the inlet of flow tube (after sampling air mixing with N_2O_5 source) and the sequential measurements of N_2O_5 concentration both at the inlet and the exit of flow tube within a duty cycle. To achieve the programmed cyclic measurement of these key parameters, we adopted a new design of Y-tee with a static mixer inside and cyclic measurement setup.

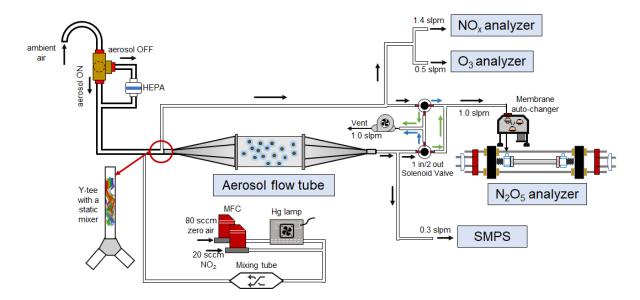


Figure 1. Overall schematic of aerosol flow tube system. The arrows alongside the tube show the flow directions. The black arrows indicate the flow directions consistent during the measurements, green arrows indicate the flow directions active in measuring the exit N_2O_5 and blue arrows indicate the flow directions active in measuring the inlet N_2O_5 .

2.1 Sampling manifold

The sampling tube is made of a 50 cm long and half inch outside diameter (OD) aluminum tubing, with a curve tip (10 cm radius of curvature) turning the inlet straight down in order to

avoid precipitation. The ambient air is then pass through a three-way stainless-base solenoid ball valve, which is controlled by a time relay to either allow the air to flow directly into a following Y-tee (filter bypass mode) or divert to a HEPA (high efficiency particulate air filter, Whatman) to remove particles (filter inline mode). The HEPA can retain particles at a high efficiency (>99.9%) with low pressure drop and RH difference between filter inline and bypass mode.

2.2 Gaseous N₂O₅ generation

A home-made temperature-controlled gas generator is used to generate gaseous N₂O₅ in-situ via the reaction of O₃ with NO₂ (R1) and the subsequent reaction of produced NO₃ with NO₂ (R2).

$$NO_2 + O_3 \rightarrow NO_3 + O_2$$
 R1

$$NO_2 + NO_3 + M \leftrightarrow N_2O_5 + M$$
 R2

 NO_2 is delivered from a compressed gas cylinder (20 ppmv in N_2 diluent gas, Jinghao Corp.). O_3 is generated from the photolysis of O_2 in compressed ultra-pure synthetic zero air at 254 nm, using a commercial mercury lamp (UVP, the USA) fixed inside the generator. The produced O_3 are then mixed with NO_2 in a Teflon chamber for about 2 min under the temperature of 15 °C, stabilized by a Peltier cooler controlled by proportion integration differentiation algorithm. A PFA tube with polyethylene foam was used to transmit the synthesized N_2O_5 to sampling stream and minimize the influence of ambient temperature variation on N_2O_5 level. The flow rate of NO_2 (20 sccm) and zero air (80 sccm) are controlled by mass flow controller separately at a total of 100 sccm. By changing the flow rate ratio between NO_2 and zero air, the generator can produce N_2O_5 concentration varying from 1 ppbv to 6 ppbv (after dilution in zero air at sampling flow rate of 4.5 slpm). Under the typical measurement condition, an excess of NO_2 concentration is applied to shift the equilibrium towards N_2O_5 production (R2) and suppress the NO_3 concentration to less than 30 pptv, which is expected to decrease the uncertainty of varying NO_3 reactivity (NO, VOCs and heterogeneous loss). The resulted initial N_2O_5 concentration was 4.0 ppbv at the inlet of

aerosol flow tube, together with around 50 ppbv of NO_2 and 15 ppbv of O_3 . A stability test on N_2O_5 source showed the variation was within 1% for a 24-h continuous operation, with ambient temperature ranging from 0 to 15 °C.

2.3 Aerosol flow tube

Air flow enters and exits the flow tube via two identical conical diffuser caps at a diffuser angle of 45° . A $35 \text{cm} \times 14$ cm inner diameter (ID) cylindrical tube is mounted in the middle of two caps, flanged with screws and nitrile rubber O-rings. All sections of this aerosol flow tube are made of stainless-steel with electro-polished and FEP-coated inside. The exterior of the flow tube is insulated with aluminum coated polyethylene foam 3 cm thick to minimize thermal eddies fluctuation of ambient temperature. The mechanic design of this flow tube follows that used in Bertram et al. (2009), with different length and diffuser angles particularly designed for our typical flow rate. Under the typical flow rate of 2.1 SLPM in the flow tube, the axial velocity in the cylindrical tube section is $0.23 \text{ cm} \cdot \text{s}^{-1}$ which produces a Reynolds numbers (Re) of 22, well below the threshold of laminar flow (Re<2100).

In front of the flow tube, the synthesized N₂O₅ source is introduced perpendicular to ambient air sampling stream and the mixture then enters a stainless-steel Y-tee for further mixing. The inner surface of Y-tee is electro-polished and coated with SilcoNert 2000 (Silotek Corp.), a technique commonly applied in semiconductor industry, to maintain the transmission efficiency of particles and minimize the loss of N₂O₅ in the meantime. A 10 cm long stainless-steel static mixer is mounted inside the Y-tee in order to swirl the flow and therefore facilitate the mixing between sampling stream and N₂O₅ source in a relatively short distance. The presence of static mixer in front of the inlet also help to improve the flow expansion after entering the flow tube by minimizing recirculation zone, which decreases the wall loss of N₂O₅ and particles (Huang et al., 2017). After passing through the static mixer, the mixture of ambient air and N₂O₅ source is split into two flows at the same flow rate, one of which straightly enters the aerosol flow tube and the other one is diverted to measurements of NOx, O₃ and N₂O₅. We measured the concentrations of NOx, O₃, N₂O₅ and Sa at the both exits of Y-tee under typical flow rate for three repeated experiments (Figure 2). Almost the same

gaseous concentrations and particle distributions at both exits of Y-tee demonstrate that the N_2O_5 source has been well mixed with the sampling flow.

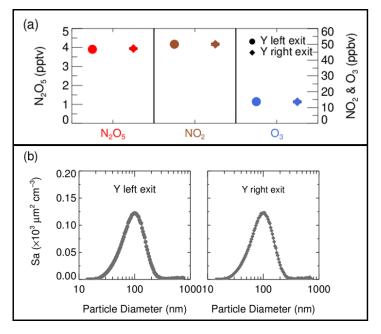


Figure 2. (a) The concentration of N_2O_5 , NO_2 and O_3 in the mixture of N_2O_5 source and sampling aerosols measured at each exit of Y-tee; (b) The size distribution of Sa concentration in the mixture of N_2O_5 gas source and sampling aerosols measured at each exit of Y-tee.

2.4 Detection instruments

Instruments used in this system are listed in Table 1. A portable cavity-enhanced absorption spectrometer (CEAS) is used to measure N₂O₅ concentration (Wang et al., 2017a) at both inlet and exit of the aerosol flow tube by automatically switching the flow directions (see details in section 2.5). Briefly, the N₂O₅ is thermally decomposed to NO₃ by heating up to 130°C and then quantified according to the extinction coefficient caused by NO₃ absorption in the wavelength window from 640 to 680 nm. A Teflon polytetrafluoroethylene (PTFE) membrane is placed in front of the CEAS to remove particles, which will be replaced with a new one every two hours by a self-designed membrane auto-changer. Laboratory tests have been conducted to quantified the transmission efficiency of N₂O₅ over the membrane (92±3%), sampling tube of CEAS (99.7%) and the inside of CEAS (93.6%). The use of a filter upstream of the CEAS and the procedures of membrane changing have been successfully applied in many field campaigns to measure ambient N₂O₅ (Brown et al., 2016;Kennedy et al.,

2011; Wang et al., 2017a; Wang et al., 2017b; Wang et al., 2018a). The loss of N_2O_5 on membrane filter, sampling tube and the detection chamber inside the CEAS were corrected according to transmission efficiency. The detection limit of N_2O_5 was determined to be 2.7 pptv (1 σ , 60 s) with the measurement uncertainty of 19%. The CEAS has been successfully applied to measure ambient N_2O_5 concentration in several field campaigns and laboratory studies (Chen et al., 2020; Wang et al., 2020a; Wang et al., 2017b; Wang et al., 2020b; Wang et al., 2018b; Wang et al., 2022).

Table 1. Performance of related instruments incorporated in the flow tube system.

Parameter	Technique	Time resolution	Detection Limit(1σ)	Accuracy
NO	Chemiluminescence ^a	1 min	200 pptv	±10%
NO_2	Chemiluminescence	1 min	300 pptv	±10%
O_3	UV photometry	1 min	500 pptv	±5%
VOCs	GC-MS/FID ^b	60 min	20-300 pptv	±15%
N_2O_5	CEAS	1 min	2.7 pptv	±19%
Sa	SMPS	5 min	-	±10%
RH&T	Sensor	1 min	-	±0.1%&±0.1K

^a Photolytic conversion to NO through blue light before detection; ^b Gas chromatography equipped with a mass spectrometer and a flame ionization detector;

At the inlet of flow tube, NOx concentration is measured via chemiluminescence method equipped with a blue-light photolytic converter (Thermo, Model 42i) and O₃ concentration is also measured via chemiluminescence method by adding excessive NO (Teledyne API, Model T265). Both NOx and O₃ concentration are averaged to 1 min time-resolution. The size distribution of particle number density is measured at the exit of flow tube using a scanning mobility particle sizer (SMPS, TSI 3776), which determines the total Sa concentration covering the range from 13 to 730 nm. Particles larger than this range usually contributed less than 5% of total Sa according to our previous field measurements (Chen et al., 2020) and it is included in the uncertainty analysis (see section 5). A cycle of size scanning is set to around 5 min and the derived Sa concentration is then interpolated into 1 min for further calculation. Aerosols pass through a Nafion tubing (MD-700) before entering into SMPS to reduce RH to less than 30%. The dry-state Sa is therefore corrected to wet-state at the RH inside the flow

tube for particle hygroscopicity. The growth factor, $f(RH)=1+8.77\times(RH/100)^{9.74}$, used for correction is valid only when RH is within the range from 30 to 90% (Liu et al., 2013). The RH and temperature of flow are continuously measured both before entering and after leaving the flow tube by commercial sensors (Rotronic, Model HC2A-S). The averages of the values obtained at both locations are used to represent the RH and temperature inside the flow tube. In addition, ambient volatile organic compounds (VOCs) are measured in-situ alongside the aerosol flow tube system using an online gas chromatograph mass spectrometer coupled with a flame ionization detector (GCMS-FID) to derive the NO₃ reactivity to VOCs ($k_{NO3-VOCs}$) in the flow tube.

2.5 Procedures of data acquisition

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The N₂O₅ concentration is acquired at both inlet and exit of the flow tube within a duty cycle via a CEAS instrument, which is different from that only at the exit of the flow tube in previous studies (Bertram et al., 2009a; Wang et al., 2018c). Each duty cycle consists of once HEPA inline mode for measuring k_{wall} of N_2O_5 and once HEPA bypass mode for retrieving the N_2O_5 loss on aerosols. The procedure that measuring N₂O₅ at the inlet of flow tube first and then at the exit is executed within each mode. An exemplary case obtained during a field campaign is shown in Figure 3 to explain this procedure. Within the mode of HEPA inline, N₂O₅ data is firstly acquired at the inlet of the flow tube and then switch to the exit of the flow tube. The $k_{het}^{wo/particles}$, which is the k_{wall} of N_2O_5 , can be derived from a box model constrained by these N₂O₅ data (see section 3 for the model description and data processing). The same procedures are executed in the mode of HEPA bypass, except the $\gamma(N_2O_5)$ is derived according to Eq 2. Two three-way valves controlled by a time relay were implemented to realize this procedure in order to avoid the changes of flow condition in the flow tube that could have been caused. As indicated in Figure 1, the blue arrows show the flow directions when measuring the N₂O₅ concentration at the inlet of flow tube, while the green arrows shows that for the exit of flow tube. It should be noted that the concentration of NOx and O₃ are always acquired at the inlet of the flow tube and the Sa concentration always at the exit of the flow tube during the operation.

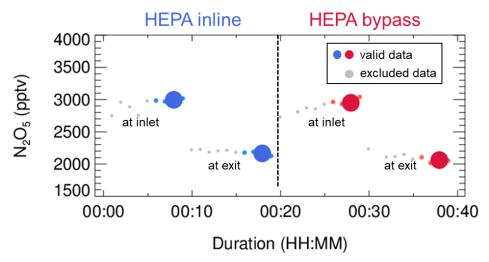


Figure 3. An exemplary case of measured N_2O_5 concentration within a duty cycle. This case was observed on the night of 13 December 2020, with average ambient Sa of 320 μ m² cm⁻³. The derived k_{wall} of N_2O_5 and $\gamma(N_2O_5)$ were 0.0023 s⁻¹ and 0.035, respectively. The blue dots indicate N_2O_5 concentration measured under the mode of HEPA inline either at the inlet or exit of the flow tube (denoted as texts); the respective averages (blue dots of larger size) are used for deriving k_{wall} (blue square). The red dots indicate N_2O_5 concentration measured under the mode of HEPA bypass either at the inlet or exit of the flow tube; the respective averages (red dots of larger size) are used for deriving the overall rate constant of N_2O_5 loss on the wall and aerosols. The data points in gray are excluded from calculation due to unstable conditions in the flow tube.

In addition, laboratory tests were conducted to determine a suited duration for each duty cycle. During a duty cycle, the duration for each mode should last long enough to develop a stable flow condition for particles or empty particles, while a much longer duration could decrease the measurement time-resolution and leads to large uncertainty due to the fluctuations within a long time period. We measured Sa and N₂O₅ concentration continuously at the exit of flow tube when sampling (NH₄)₂SO₄ aerosols. As shown in Figure 4, it took about 15 minutes for particles to rise to a stable level from none or to decrease from a certain level to none, when our system underwent mode switches. The periodical variation of N₂O₅ concentration was consistent with particles. The residence time distribution (RTD) profiles (see in section 4.2) also demonstrated that a pulse injection of NO₂ requires 10~15 minutes to be fully drained out of the flow tube, which to some extent supports the 15-minute time required for complete mixing of N₂O₅. As a result, a typical duration of duty cycle is composed of 40 minutes with

20 minutes for each mode, which is similar to that in Bertram et al. (2009). The N_2O_5 measurement at the exit of the flow tube in the last 5 minutes of each mode is able to represent valid decays of N_2O_5 under this mode and satisfy the requirements of further data processing.

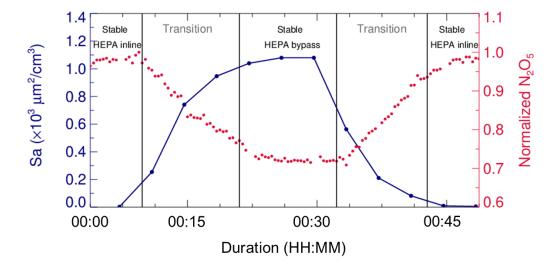


Figure 4. Variations of Sa and N₂O₅ concentration (normalized to peak values) measured at the exit of flow tube when switching the sampling mode. The phases of species concentrations in the flow tube approaching stable after a mode switch are denoted as the transition phases.

3 Box model for determination of loss rate coefficients of N₂O₅

3.1 Method description

Large uncertainties were found in retrieving $\gamma(N_2O_5)$ on ambient particles according to Eq. 1 in a previous flow tube study (Bertram et al., 2009a), due to the dependence of homogeneous reaction rates on sampling modes and the atmospheric variations of parameters related to NO_3 - N_2O_5 chemistry (e.g. NO, NO_2 , O_3 , VOCs, and RH). To minimize these influences, a time-dependent box model constrained by the measurements of N_2O_5 concentration and other auxiliary parameters is applied to calculate loss rate coefficients of N_2O_5 under the mode of HEPA inline and bypass, respectively. The model is able to simulate the reactions related to budgets of NO_3 - N_2O_5 chemistry in a dark condition, including R1, R2 and the follows:

$$NO_3 + NO \rightarrow 2 NO_2$$
 R3
 $NO_3 + VOCs \rightarrow products$ R4

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The rate constants for reactions R1 to R3 are referenced to IUPAC database. The reaction of VOCs and NO₃ is treated as pseudo-first-order with a rate constant of $k_{\text{NO3-VOCs}}$, which is the sum of rate constants for reactions of NO₃ with each VOCs scaled by the concentration of VOCs measured by GC-FID. In this work, there are 30 kinds of measured VOCs having known reaction rate constants with NO₃ included in the model (Table A1). Due to low time-resolution of VOCs measurements (1 h), the $k_{\text{NO3-VOCs}}$ is kept constant for each derivation of $\gamma(\text{N}_2\text{O}_5)$. The suppressed NO₃ concentration is expected to attenuate the influence resulted from the uncertainty of $k_{\text{NO3-VOCs}}$ (see discussion in section 5). The reaction R5 represents the loss of N₂O₅ only on the wall in the mode of HEPA inline or on the both wall and particles in the mode of HEPA bypass. The rate constant of R5 is also treated as pseudo-first-order and it is adjustable among different runs.

The same procedures of data screening and model operation are applied to both sampling and bypass modes, as shown in Figure 5. For example, in the mode of HEPA inline, the average of NO concentration less than 6 ppbv and the variation of N₂O₅ measured at the inlet of flow tube less than 10% should be validated prior to the following model operation. Under typical concentration of N₂O₅ source we used in this flow tube system, the exit concentration of N₂O₅ is detected to be under triple detection limit with initial NO large than 6 ppbv according to our laboratory tests. In ambient condition, high level of NO is usually also accompanied by rapid variation due to fresh emission, which disturbs the decay of N₂O₅ in the flow tube and leads to large uncertainty in deriving its loss rate coefficient. Excluding the cases that N₂O₅ measured at the inlet of flow tube varies exceeding 10% can further minimize the uncertainty of N₂O₅ loss rate coefficient resulted from rapid change of NO₃ reactants (NO, VOCs). If the measured data within the duration of a sampling mode satisfies the criteria for data screening described above, the model can therefore simulate the reactions starting from the entrance of flow tube and lasting for 156 s (mean residence time) based on these data. The initial concentrations of $[NO]_{t=0}$, $[NO_2]_{t=0}$, $[O_3]_{t=0}$ and $[N_2O_5]_{t=0}$ are the averages of last-5-min values measured at the inlet of flow tube. The RH and temperature are constrained by the mean values

during this sampling mode. By tuning the loss rate coefficient of N_2O_5 (k_{N2O5}) in the way of binary search, we optimized an appropriate k_{N2O5} to ensure that the N_2O_5 concentration output from the simulation is consistent with last-5-min average of N_2O_5 concentration measured at the exit of flow tube within 1 pptv. As a result, this derived k_{N2O5} (aka. $k_{het}^{wo/particles}$) is expected to be the k_{wall} of N_2O_5 . The same procedures above are then applied to the data obtained in the mode of HEPA bypass, except that the derived k_{N2O5} (aka. $k_{het}^{w/particles}$) contains the loss rate coefficients of N_2O_5 on the both wall and particles. It should be noted that the above calculation for obtained data is only valid under the variation of RH less than 2% within a duty cycle and the k_{wall} of N_2O_5 can then be reasonably assumed to be constant between two successive sampling modes. Therefore, the $\gamma(N_2O_5)$ can be retrieved by the Eq 3, where the last-5-min averages of Sa concentration in the mode of HEPA bypass is used.

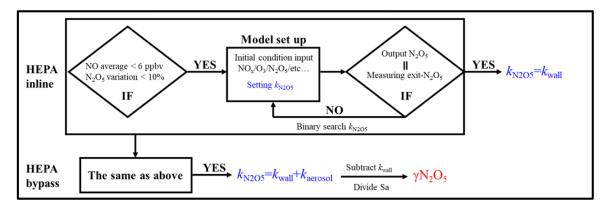


Figure 5. Flow diagram of $\gamma(N_2O_5)$ derivation through box model method.

3.2 Evaluation of the box model method

The box model method is introduced to our flow tube system to overcome the influence from homogeneous reactions and variations of air mass on γ(N₂O₅) retrieval. A series of scenarios were provided to evaluate the performance of box model method by both simulations and laboratory experiments. We allow NO, NO₂ and O₃ in the mixture of sampling air at the entrance of the flow tube to vary in a reasonable range, in order to develop the scenarios of different gradients of NO concentration and NO₃ production rates (PNO₃). The levels of PNO₃ was adjusted by NO₂ and O₃ concentrations (O₃ ranging from 10 to 80 ppbv and NO₂ ranging from 50 to 160 ppbv) under the temperature of 283 K and RH of 30%. In simulation studies,

the exit concentration of N_2O_5 would be obtained from the simulated N_2O_5 evolutions with and without particles in the flow tube. To corroborate the results estimated by simulations, laboratory tests were performed on $(NH_4)_2SO_4$ aerosols to measure the exit concentration of N_2O_5 under varying NO concentration. The $\gamma(N_2O_5)$ on particles are then calculated according to Eq 1&2 or by box model method described above.

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As shown in Figure 6(a), the exit concentration method ($\gamma(N_2O_5)$) exit-conc., derived directly by Eqs. 1-2) underestimates $\gamma(N_2O_5)$ and the extent of underestimation increases with PNO₃ levels in simulation tests. Similarly, the exit concentration method underestimates $\gamma(N_2O_5)$ by 50 to 60% with PNO₃ of 1.0 ppbv h⁻¹ in the laboratory tests (Figure 6(b)). Noted that the $\gamma(N_2O_5)$ was determined to be at around 0.01 by box model method over the NO range from 0 to 6 ppbv, which agrees well with previous laboratory observation of $\gamma(N_2O_5)$ on (NH₄)₂SO₄ aerosols within uncertainty (Badger et al., 2006; Hallquist et al., 2003; Kane et al., 2001). The cause of $\gamma(N_2O_5)$ exit-conc. underestimation is mainly due to the in situ N_2O_5 production in the flow tube. With a continuous production of NO₃ via the reaction of NO₂ and O₃ and rapid heterogeneous loss of N₂O₅ in the flow tube, the equilibrium between NO₃ and N_2O_5 always shifts to the production of N_2O_5 , and masking the actual amount of N_2O_5 removal. In the mode of HEPA bypass, the N₂O₅ consumes faster than the other mode due to the addition of particles, which further facilitates the N₂O₅ formation through the equilibrium. Previous studies also found similar impacts from N_2O_5 production on retrieving $\gamma(N_2O_5)$ in the aerosol flow tube (Bertram et al., 2009a; Wang et al., 2018c). However, the discrepancy of $\gamma(N_2O_5)$ derived by two methods is much less dependent on the NO concentration, at least within the prescribed range, due to relatively small ratio of NO₃/N₂O₅ in the N₂O₅ source. The absence of dependence between NO concentration and $\gamma(N_2O_5)$ also indicates that this aerosol flow tube system can buffer against NO within the range from 0 to 6 ppbv under typical operating condition. However, this is not always the case when there is a rapid fluctuation of NO in a real atmosphere, which might lead to intractable uncertainty and is therefore excluded from further analysis according to the criteria of data screening.

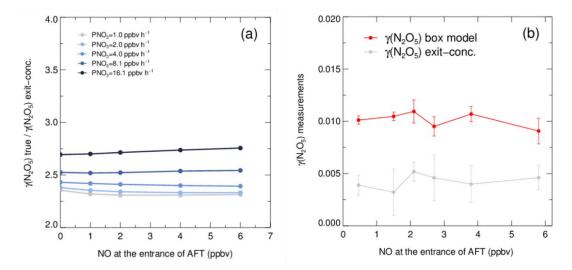


Figure 6. Simulated and laboratory tests on performance of box model method and exit concentration method for $\gamma(N_2O_5)$ derivation. (a) The ratios of given $\gamma(N_2O_5)$ ($\gamma(N_2O_5)$ true) over exit concentration derived $\gamma(N_2O_5)$ ($\gamma(N_2O_5)$ exit-conc.) determined from simulated scenarios. The $\gamma(N_2O_5)$ derived by box model method is exactly the same as $\gamma(N_2O_5)$ true. The ratios vary with NO concentration and the lines are color coded by PNO₃ values. Both NO concentration and PNO₃ represent the values at the entrance of aerosol flow tube. (b) $\gamma(N_2O_5)$ measurements on lab-generated (NH₄)₂SO₄ aerosols under different gradients of NO with constant RH of 50% and PNO₃ typically generated from our N₂O₅ source. The red line shows the $\gamma(N_2O_5)$ derived by box model method and gray line shows the $\gamma(N_2O_5)$ derived by exit concentration method. The NO concentrations are measured at the entrance of aerosol flow tube.

In comparison to the work by Bertram et al. (2009) and Wang et al. (2018), the combination of above box model method and the improved flow tube system in this study has progress in the following aspects. First, the dynamic quantification of k_{wall} of N_2O_5 within each duty cycle based on the constraint of sequentially measured N_2O_5 source is helpful to provide accurate data for both k_{wall} and $\gamma(N_2O_5)$ retrieval. The k_{wall} in ambient conditions could deviate from the results from laboratory tests (Figure B1) due to temperature variation and particles adsorption, which leads to large uncertainty when calculating $\gamma(N_2O_5)$ without the frequent determination of k_{wall} . While the k_{wall} was also determined frequently in the flow tube of Wang et al. (2018), the N_2O_5 source they used for k_{wall} and $\gamma(N_2O_5)$ retrieval is an assumed stable value instead of an observed one. Second, the concentrations of initial NO, NO₂, O₃ and N₂O₅ at the entrance of the flow tube, and exit N_2O_5 are obtained through programed cyclic

measurements in this work, which can reduce the uncertainties by adding the model constraints. It is different from the iterative box model used in Wang et al. (2018) as we enable a straightforward simulation of NO₃-N₂O₅ chemistry occurring in the flow tube, instead of estimating the initial NO₂ and O₃ with assumed NO profile and stable N₂O₅ source based on backward simulations. In ambient conditions, the initial N₂O₅ concentration can be largely influenced by air mass conditions (especially NO concentration and temperature). Figure B2(a) presents box whisker plot of N₂O₅ and NO concentration at the flow tube entrance during a field campaign, which shows a much larger variation of N₂O₅ than in lab condition (<1%). As a result, the box model would underestimate γ (N₂O₅) by using a fixed initial N₂O₅ concentration under certain circumstances (Figure B2(b)). Third, we simulate NO₃-N₂O₅ relationship via specific reactions rather than approximating it in equilibrium and introducing the equilibrium coefficient (*K*eq) into calculation. Calculating NO₃ or N₂O₅ concentration by *K*eq could induce large bias (up to 90%) under the high aerosol loading and low temperature (Chen et al., 2021).

4 Laboratory characterizations

4.1 Particle transmission efficiency

The transmission efficiency of particles in the sampling module and flow tube are estimated respectively in Figure 7. In the laboratory, pure ammonia nitrate ((NH₄)₂SO₄) aerosols were generated from an atomizer loading with 0.1 M (NH₄)₂SO₄ solution. The RH and concentration of produced aerosols flow was conditioned in a glass bottle (~2 L) by introducing a humidified dilution flow of ultrahigh-purity N₂. As a result, aerosols in different concentrations (1000~4500 µm² cm⁻³) and under a range of RH (20~70%) were applied to test the transmission efficiency. Figure 7(a) shows the loss of total Sa concentration in the sampling module and flow tube are 8±1% and 10±2% on average, respectively. We found that the fraction of particles loss is mainly caused by particles smaller than 100 nm. This is most likely due to the turbulence generated by static mixer and the recirculation in the flow tube. Large particles are prone to stay within the main flow direction, whereas small particles readily

adsorb on the walls by the entrainment of turbulence or recirculation. In addition, the particles distribution measured at the exit of flow tube with HEPA inline (gray line in Figure 7(a)) demonstrated its capability of removing almost all particles (>99.5%) at the typical flow rate. The same transmission efficiency was also found on ambient aerosols (Figure 7(b)) as that on laboratory-generated aerosols. The results we obtained from above particle transmission experiments are similar to the findings of Bertram et al. (2009).

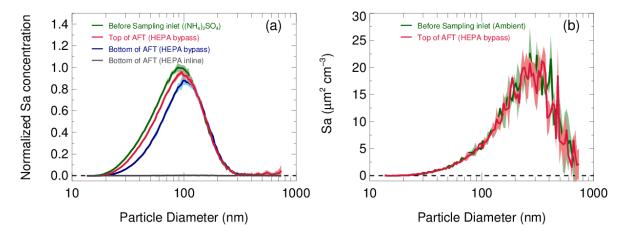


Figure 7. (a) Particles transmission determined by sampling laboratory-generated (NH₄)₂SO₄ aerosols. Aerosols at different concentrations and RH levels are used in experiments and the size distribution of Sa concentration are normalized to the peak values. The normalized size distribution of Sa concentration measured before sampling inlet (green line), at the inlet of flow tube with HEPA bypass (red line) and at the bottom of flow tube with HEPA bypass (blue line) are shown respectively. Under the mode of HEPA inline, the Sa concentration was almost zero at the bottom of flow tube (gray line). The shadows indicate the standard deviations of the normalized Sa concentration for all experiments. (b) Particles transmission determined by sampling ambient particles.

4.2 Residence time in the flow tube

The method of residence time distribution (RTD) was applied to estimate the average reaction time of the gas species in the flow tube (residence time). In comparison to ideal plug flow, the RTD method can better describe actual behavior of the flow in practice and determine the mean residence time more accurately (Danckwerts, 1953). Several studies have also used this RTD method to determine the residence time in the flow tube (Huang et al., 2017; Wang et al., 2018c; Lambe et al., 2011).

The RTD profiles were obtained by introducing a 2 s pulse of NO₂ gas diluted in N₂ into the flow tube under RH less than 1%. NO₂ is relatively inert against the flow tube wall coated with FEP and was measured at the exit of the flow tube by a CEAS (Li et al., 2021) at high time-resolution (2 Hz). A three-way solenoid valve combined with a time relay was implemented to control the pulse in order to avoid the disturbance on flow condition from the injection. Experiments were performed under typical operation. The mean residence time (t_{ave}) can be derived from the each RTD profile according to Eq. 4,

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$$t_{ave} = \frac{\sum_{i=0}^{\infty} C_i \times t_i}{\sum_{i=0}^{\infty} C_i},$$
 Eq. 4

where the C_i is the concentration of NO₂ recorded at the time step t_i. From the RTD profiles of NO₂ injection experiments in Figure 8, the determined t_{ave} was 156±3 s. This value is 19% less than the space time (τ_{space} , flow tube volume divided by operation flow rate, 192.6 s). It has also been found that the assumption of ideal plug flow overestimated the residence time in previous flow tube experiments (Lambe et al., 2011; Huang et al., 2017; Wang et al., 2018c), which could lead to underestimation of the derived k_{N2O5} . The residence time of current set up is designed for investigating $\gamma(N_2O_5)$ in typical episode days with medium to high aerosol loadings (the Sa concentration usually larger than 500 um² cm⁻³) in polluted regions. As shown in Section 5, the detection limit of this system is 6.4×10^{-4} with Sa of 500 um² cm⁻³, which is well below the most of previous ambient $\gamma(N_2O_5)$ results ranging from 1×10^{-3} to >0.1 in polluted regions of China (Wang et al., 2020a; Wang et al., 2017d; Wang et al., 2017e; Xia et al., 2019). The residence time determined in this work is also slightly higher than 149 s that reported in a previous work focusing on investigating $\gamma(N_2O_5)$ in polluted regions (Wang et al., 2018c). In addition, the residence time for this flow tube can be extended to over 300 s to satisfy the $\gamma(N_2O_5)$ measurement requirements under low Sa by reducing the flow rate of air passing through, which is controlled by an extra pump.

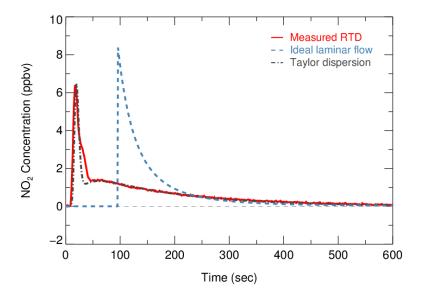


Figure 8. Residence time distribution derived by sampling NO₂ gas. Red solid line indicates the measured RTD profiles. The calculated RTD of ideal laminar flow (without dispersions) and the Taylor dispersion model fitted to measurements are shown as blue dash line and dot-dash line, respectively.

Two theoretical RTDs were calculated, namely ideal laminar flow and Taylor diffusion, besides the measured RTD, intending to reflect the fluid field inside the flow tube. The ideal laminar flow describes the flow without dispersion. The velocity profile of ideal laminar flow is parabolic, with the fluid in the center of the tube moving the fastest. According to the following Eq. 5, the RTD of ideal laminar flow is scaled by the integrated concentration of NO₂ and presented as the blue dash line in Figure 8.

$$\begin{cases} 0, & t < 0.5\tau_{space} \\ \frac{\tau_{space}^2}{2t^3}, t \ge 0.5\tau_{space} \end{cases}$$
 Eq. 5

While the determined *Re* is well within the laminar flow threshold, the measured RTD occurs earlier than theoretical laminar flow condition and exhibits a broaden distribution. The discrepancy between them indicates that the dispersions or potential secondary flows could dominate the flow regime. Instead, an improved Taylor dispersion model (shown as the gray dot-dash line in Figure 8) is able to reproduce the measured RTD, which was previously implemented in the characterization of photooxidation flow reactors (Lambe et al., 2011). Two flow patterns with distinct effective diffusivities (0.02 and 0.51 derived from best fit) were considered in this dispersion model. An implication from the characteristics of the model is

that two flow components consist of the flow regime: a direct flow path through the flow tube with less diffusion and a secondary flow path representing the recirculation in the dead zone that induced by temperature gradient and significant diffusions (Huang et al., 2017).

4.3 N₂O₅ wall loss

Laboratory tests were conducted to quantify the k_{wall} of N₂O₅ under different levels of RH with HEPA inline. As shown in Figure 9, the k_{wall} of N₂O₅ gradually increase from 0.002 s⁻¹ in a dry condition to 0.006 s⁻¹ when RH is 70%. The level of k_{wall} is less than the result of Wang et al. (2018c) but higher than Bertram et al. (2009a) as indicated in Table 2. In addition, the flow tube was rinsed with deionized water every week during the field campaigns to remove the build-up of particles, which might increase the hygroscopicity of the internal surface and thus the k_{wall} of N₂O₅ in a wet condition. Uncertainty in γ (N₂O₅) derivation resulted from the variation of k_{wall} related to RH is discussed in section 5.

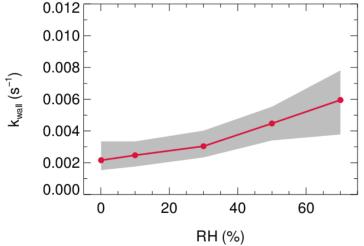


Figure 9. The dependence of pseudo-first-order wall loss coefficient (k_{wall}) of N₂O₅ in the

FEP-coated aerosol flow tube.

Table 2. Summary of the k_{wall} of N₂O₅ for the existing aerosol flow tube deployed in field campaigns.

RH range	k_{wall} range (×10 ⁻³ s ⁻¹)	References
5~50%	0.5~3	Bertram et al., 2009
20~70%	4~9	Wang et al., 2018
0~70%	2~6	This work

4.4 Demonstration of $\gamma(N_2O_5)$ measurements on model particles

 $\gamma(N_2O_5)$ measurements by current aerosol flow tube system equipped with box model method were performed on lab-generated (NH₄)₂SO₄ aerosols over a range of RH. The system was operated at room temperature of 295K with N₂O₅ concentration of 4.0 ppbv at the entrance of flow tube. We conditioned the RH of generated aerosols by introducing dry N₂ gas dilution, which could decrease the RH level down to $10\sim55\%$, starting from over 95% where (NH₄)₂SO₄ aerosols are expected to be in aqueous state. The resulting Sa concentrations of aerosols were around 600 μ m²·cm⁻³. As shown in Figure 10, the observed $\gamma(N_2O_5)$ values were below 0.01 when RH was within 40% and significantly rose up to 0.02 with higher RH. The dependence of $\gamma(N_2O_5)$ on RH and the exact values are well consistent with previous laboratory results on (NH₄)₂SO₄ aerosols (Badger et al., 2006;Hallquist et al., 2003;Hu and Abbatt, 1997;Kane et al., 2001;Mozurkewich and Calvert, 1988), which shows that the setup of our instrument has good practicability. A large standard deviation of $\gamma(N_2O_5)$ found at RH of 39% is possibly due to the unstable phase transition of (NH₄)₂SO₄ particles, as its efflorescence RH is reportedly from 35 to 48% (Martin, 2000).

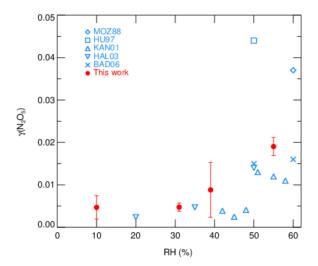


Figure 10. The dependence of $\gamma(N_2O_5)$ on RH for laboratory-generated $(NH_4)_2SO_4$ aerosols. The red points with standard deviations represent the values measured by current aerosol flow tube system in this work. Previously reported values are indicated in blue marks.

5 Uncertainty analysis and detection limit

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The uncertainty of $\gamma(N_2O_5)$ is in relevance to the measurement uncertainties of each instrument and rapid fluctuations of various parameters. As outlined before, the 5-min averages of N₂O₅ concentration measured at the inlet and exit of the flow tube were used for calculating $\gamma(N_2O_5)$ via the box model method. The potential variations within these selected time periods would therefore lead to relative errors. For example, the variations of N₂O₅ concentration is resulted majorly from the rapid changes of ambient NO and less from variations of VOCs, NO₂, O₃ as well as N₂O₅ gas source itself (1% in 24 hours). A cutoff of 10% for N₂O₅ variation was implemented to filter out the air mass that was too unstable for valid analysis, according to our prescribed criteria of data screening. It consequently leads to 10% uncertainty in the average of N_2O_5 and can translate into a deviation of 2% in $\gamma(N_2O_5)$ with the $\gamma(N_2O_5)$ at 0.02, Sa at 800 μm²·cm⁻³ and other parameters (shown in Table 3) representing the typical inlet values measured during the field campaign (described in section 6). Similarly, cases that over 2% variation in RH exists between the HEPA inline and bypass mode are excluded from analysis, owing to its significant influence on k_{wall} of N_2O_5 in the flow tube. By assuming a consistent k_{wall} in successive sampling modes, the potential variations in RH could lead to uncertainty in $\gamma(N_2O_5)$ from $\pm 8 \times 10^{-4}$ at RH of 20% to $\pm 2 \times 10^{-3}$ at RH of 70%, respectively, with the Sa at 800 μ m² cm⁻³. In addition, the $k_{NO3-VOCs}$ is treated as constant in a duty cycle due to the limit of time resolution of VOCs measurements. A variation of $\pm 0.01 \text{ s}^{-1}$ in $k_{\text{NO3-VOCs}}$ only induces less than $\pm 1\%$ uncertainty in $\gamma(N_2O_5)$ for more than 95% cases obtained during the field campaign. All the impacts from inherent instruments uncertainties and variations of different parameters are thereby considered in Monte Carlo simulations to assess the overall uncertainty of $\gamma(N_2O_5)$. The basic simulation is initialized with the typical conditions measured at the inlet of the flow tube during the field campaign and repeatedly performs the procedures of determining $\gamma(N_2O_5)$ via the box model method 1000 times. In each run, all parameters were allowed to vary independently within a prescribed range. The basic simulation condition and variation range are presented in Table 3.

Table 3. Parameters involved in the Monte Carlo simulations.

Parameters	Value ^a	Variation range ^b
NO	1 ppbv	±10%
NO_2	70 ppbv	$\pm 10\%$
O_3	10 ppbv	±5%
Inlet N ₂ O ₅	4 ppbv	±19%
Exit N ₂ O ₅ ^c	2.2 ppbv	±19%
Temperature	273 K	±0.1 K
RH ^d	30 %	±1%
$k_{ m NO3\text{-}VOCs}$	0.01 s^{-1}	$\pm 0.01 \text{ s}^{-1}$

^a Values used for initializing Monte Carlo simulations in a basic scenario; ^b Ranges within which each parameter can vary independently; ^c Determined from the case that $\gamma(N_2O_5)$ is at 0.02, Sa is at 800 μ m²·cm⁻³ and other parameters are shown in this table; ^d The RH and its variation can be transformed into values in k_{wall} of N_2O_5 via the fitting function derived from Figure 9.

The resulting $\gamma(N_2O_5)$ values from Monte Carlo simulations under the basic scenario are shown as frequency distributions in Figure 11(a). This distribution can be fitted by a Gaussian function and the standard deviation (1 σ) of Gaussian distribution is regarded as the overall uncertainty of $\gamma(N_2O_5)$, which is $\pm 9 \times 10^{-4}$ (4.5% relative to true $\gamma(N_2O_5)$). The uncertainty of Sa measurements and unmeasured particles larger than 730 nm (usually less than 5% of total Sa) would together introduce an extra 16% uncertainty to $\gamma(N_2O_5)$.

We further found that the uncertainty of $\gamma(N_2O_5)$ could be sensitive to the measurement conditions. With higher O₃, potential variations of NO and $k_{NO3\text{-}VOCs}$ will induce larger uncertainty of $\gamma(N_2O_5)$ (Figure 11(b)), as it enhances the abundance of NO₃ and N₂O₅. In comparison, the low O₃ in the basic scenario suppressed the side formation of NO₃ in the flow tube, limiting the aggravation of $\gamma(N_2O_5)$ uncertainty from the increase of NO and NO₂. The $\gamma(N_2O_5)$ uncertainty is also positive correlated with RH and T. As is discussed before, the k_{wall} of N₂O₅ increases with RH level, which can amplify the potential bias of k_{wall} at a higher RH level. The equilibrium between NO₃ and N₂O₅ shifts towards the decomposition of N₂O₅ at higher T, leading to larger uncertainty of $\gamma(N_2O_5)$ caused by potential variations of NO and

 $k_{\text{NO3-VOCs}}$. The overall uncertainty of $\gamma(\text{N}_2\text{O}_5)$ therefore rises to 8.2% at the RH of 70% and to 14.4% at the temperature of 293K (Figure 11(c)), with NO, NO₂, O₃, $\gamma(\text{N}_2\text{O}_5)$ and Sa keeping the same as the basic scenario. In addition, Monte Carlo simulations were also performed for different $\gamma(\text{N}_2\text{O}_5)$ values ranging from 0.01 to 0.08. The uncertainty of $\gamma(\text{N}_2\text{O}_5)$ clearly decreased with the $\gamma(\text{N}_2\text{O}_5)$ (Figure 11(d)). A lower $\gamma(\text{N}_2\text{O}_5)$ weaken the impacts N₂O₅ uptakes has on the budgets of NO₃ and N₂O₅, which causes the $\gamma(\text{N}_2\text{O}_5)$ derivation to be more susceptible to uncertainties of other parameters and then increases the uncertainty of $\gamma(\text{N}_2\text{O}_5)$.

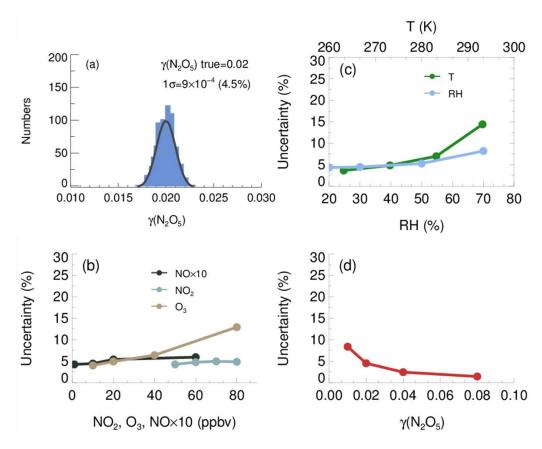


Figure 11. The uncertainty of $\gamma(N_2O_5)$ determined from the Monte Carlo simulations. (a) Histogram distribution of $\gamma(N_2O_5)$ generated from a Monte Carlo simulation (1000 single runs) in the basic scenario (shown as Table 3), where the overall uncertainty of $\gamma(N_2O_5)$ was determined to be $\pm 9 \times 10^{-4}$; (b) dependence of the uncertainty of $\gamma(N_2O_5)$ on NO, NO₂ as well as O₃; (c) dependence of the uncertainty of $\gamma(N_2O_5)$ on RH and T; (d) dependence of the $\gamma(N_2O_5)$ uncertainty on $\gamma(N_2O_5)$ level.

In addition, the mean residence time used in the box model method could bias the retrieved $\gamma(N_2O_5)$ due to the non-normal distribution of residence time with a discernable tail. The reactants entrained by those slower streamlines close to the wall will take much longer time to

reach the exit of the flow tube than that by the centerline. In order to evaluate the uncertainty caused by the distribution of residence time, we first performed simulations of N_2O_5 decay in the flow tube under the basic scenarios and calculate the exit N_2O_5 concentration according to the probability distribution function derived from RTD profile. Then the $\gamma(N_2O_5)$ can be retrieved from the box model method running for the duration of mean residence time, constrained by this calculated exit N_2O_5 concentration. The result shows that the use of mean residence time produces 32% underestimation of $\gamma(N_2O_5)$ in the basic scenario. The extent of underestimation is most sensitive to the level of $\gamma(N_2O_5)$ and RH. In short, when taking all the factors and their corresponding varying ranges discussed above into consideration, the overall uncertainty of $\gamma(N_2O_5)$ determined from Monte Carlo simulations is in the range of 16-43%. To directly compare with previous studies, at 0.03 $\gamma(N_2O_5)$ with 1000 μ m² cm⁻³ Sa, the uncertainty is calculated to be 19% which is lower than that ~24% in Bertram et al (2009) and that ranging 37%~40% in Wang et al (2018).

In order to determine the detection limit of the current aerosol tube system, the continuous blank measurements in zero air were performed with settled operation procedures. Within per duty cycle (40 minutes), one k_{wall} of N_2O_5 and one $\gamma(N_2O_5)$ can be derived in pair. In total, we obtained 56 sets of result. The detection limit of k_{N2O5} on aerosols is 2.1×10^{-5} s⁻¹, derived from 1σ of the Gaussian function fitted to this distribution. It is equivalent to 0.0016 for the detection limit of $\gamma(N_2O_5)$ with a low Sa condition of 200 μ m² cm⁻³ (Figure 12(a)), and 0.00064 for the detection limit of $\gamma(N_2O_5)$ with a moderate Sa condition of 500 μ m² cm⁻³ (Figure 12(b)). This result indicates that the flow tube system has capability of quantifying $\gamma(N_2O_5)$ for most cases even under a low aerosol-loading environment.

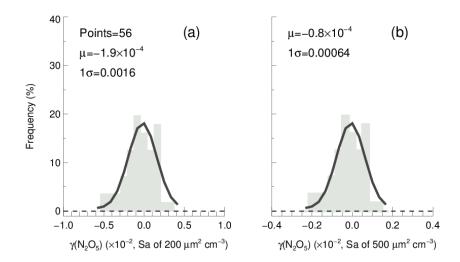


Figure 12. The γ (N₂O₅) derived from blank measurements in histogram distribution plot. The γ (N₂O₅) was calculated from $k_{\rm N2O5}$ by Eq 2 with Sa of (a) 200 μm² cm⁻³ and (b) 500 μm² cm⁻³, respectively, under the temperature of 293K. The Gaussian function is fitted to the distribution and plotted in black line. The 1σ from Gaussian fit is regarded as the detection limit.

6 Performance in the field campaign

The aerosol flow tube system was successfully deployed to measure $\gamma(N_2O_5)$ on ambient aerosols in Beijing lasting for 20 days during the December of 2020. The sampling site was at the campus of Peking University, which is located in the city center of Beijing surrounded by major roads with heavy traffic. Therefore, this site represents an area with large amount of fresh emission of NOx and other anthropogenic sources. The system was mounted in the top floor of a building, about 15 m height above the ground. The sampling manifold was placed in open air and the ambient aerosols could directly enter the inlet of the manifold without additional sampling tubes. During the period of measurement, the averages of ambient temperature, RH, NO, NO₂, O₃ and Sa were 273 ± 3 K, 25 ± 12 %, 23 ± 36 ppbv, 23 ± 12 ppbv, 16 ± 15 ppbv and 409 ± 249 μ m² cm⁻³, respectively. The NO and Sa levels could vary by 2 orders of magnitude due to the periodical switch between clean air mass from the north and pollutants accumulated by local emission.

A total of 99 valid $\gamma(N_2O_5)$ values were determined from the measurements based on the criteria of data screening described in section 3.1. We found that $\gamma(N_2O_5)$ was 0.042 ± 0.026 on average with a median of 0.035, ranging from 0.0045 to 0.12 (Figure 13). These results are

comparable to that previously determined in the North of China using various different methods (Wang et al., 2017b; Wang et al., 2018b; Wang et al., 2017d; Wang et al., 2017e; Xia et al., 2019; Yu et al., 2020a). The k_{wall} of N₂O₅ corresponding to valid γ (N₂O₅) measurements was rather stable at an average of 0.0021±0.0007 s⁻¹, which was consistent with the values determined at similar RH levels in the laboratory tests. It somehow reflected the robustness of the status of the flow tube system and the derived results.

In the current system, the N_2O_5 concentrations measured at both entrance and exit of the flow tube are sensitive to the NO fluctuations within the timescale of one sampling mode, which can induce large uncertainty on calculating $\gamma(N_2O_5)$. With our stringent criteria of data screening, the cases of drastic NO fluctuations were excluded from the analysis. Hence, the majority of valid $\gamma(N_2O_5)$ for this campaign were obtained during the periods of the NO below 2 ppbv, when the clean air mass was dominant at this urban site. Meanwhile, the Sa concentration within clean episodes were also lower than other periods, with an average of 159 μ m² cm⁻³. The derived k_{N2O5} ranged from 2.1×10^{-5} to 1.6×10^{-3} s⁻¹ well above the detection limit, which demonstrated the robustness of results even subject to low ambient Sa conditions. In order to improve the applicability of $\gamma(N_2O_5)$ measurements, future development is suggested to prioritize the reduction or removal of NO level (at least the fluctuation of NO) in the sampling system before the entrance of flow tube without the cost of particles transmission efficiency.

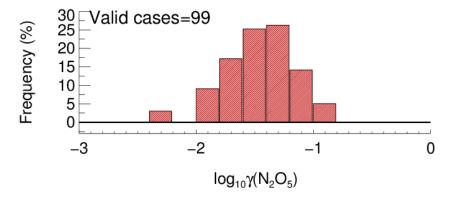


Figure 13. The histogram distribution of measured $\gamma(N_2O_5)$ for valid cases.

7 Summary and conclusion

We report a new development of an aerosol flow tube system coupled with detailed box model to derive $\gamma(N_2O_5)$ directly on ambient aerosols. The unique feature of this system is that the sequential N_2O_5 measurement at the both ends of flow tube was applied to improve the accuracy in quantifying $\gamma(N_2O_5)$, by taking it as a constraint for the box model to reproduce the decay of introduced N_2O_5 gas source in the flow tube. With the consideration of detailed chemistry related to N_2O_5 , the proposed approach was testified to refrain from the interference of side reactions, induced by the additional N_2O_5 generation, NO titration in the flow tube and variations of air masses between successive sampling modes.

A series of laboratory tests were performed to characterize factors affecting $\gamma(N_2O_5)$ derivation and demonstrate its applicability on $(NH_4)_2SO_4$ aerosols. The uncertainties associated with instruments used in the system and potential fluctuations of various parameters were thoroughly discussed in the uncertainty analysis, and we estimated the overall uncertainty of $\gamma(N_2O_5)$ to be 16-43% which is subject to NO, NO_2 , O_3 , meteorological parameters, residence time and $\gamma(N_2O_5)$ value itself. The detection limit of $\gamma(N_2O_5)$ was quantified to be 0.0016 at the aerosol surface concentration (Sa) of 200 μm^2 cm⁻³. We deployed this system for field observations of $\gamma(N_2O_5)$ at an urban site in Beijing, where strong anthropogenic emission and frequent switch of air mass were encountered. The obtained $\gamma(N_2O_5)$ was in comparable level to previously reported values in northern China and demonstrated the robustness of this system during low NO episodes. Further investigations on N_2O_5 heterogeneous chemistry for both laboratory-generated and ambient particles are also available by the introduced approach.

Appendix A: Measured VOCs used to calculate NO3 reactivity in the box model method

A total of 59 kinds of VOCs were measured by GC-FID-MS in this work, half of which had known rate constants that can be used to parameterize the reaction of NO3 with VOCs (mainly compose of alkenes and aromatics) in γ(N₂O₅) retrieval by box model method (see also section 3). Their rate constants were obtained from MCM331 or IUPAC and the values at 298K are listed in Table A1.

Table A1. VOCs used to calculate NO₃ reactivity (k_{NO3}) in the box model method

Species	k _{NO3} (298 K)	Species	k _{NO3} (298 K)
METHANE	1D-18 ^b	TRANS-2-PENTENE	3.70D-13 ^a
ETHANE	1D-17 ^b	1-HEXENE	1.20D-14 a
PROPANE	7D-17 ^b	1-3 BUTADIENE	1.03D-13 ^a
N-BUTANE	4.6D-17 ^b	ISOPRENE	7.0D-13 ^b
I-BUTANE	1.1D-16 ^b	STYRENE	1.50D-12 a
ETHYLENE	2.1D-16 ^b	ETHYNE	1D-16 ^b
PROPYLENE	9.5D-15 ^b	BENZENE	3D-17 ^b
1-BUTENE	1.3D-14 ^b	TOLUENE	7.8D-17 ^b
CIS-2-BUTENE	3.50D-13 ^a	O-XYLENE	4.10D-16 a
TRANS-2-BUTENE	3.90D-13 ^a	M-XYLENE	2.60D-16 a
I-BUTENE	3.4D-13 ^b	P-XYLENE	5.00D-16 a
1-PENTENE	1.20D-14 ^a	ETHYL BENZENE	1.20D-16 a
CIS-2-PENTENE	3.70D-13 ^a	N-PROPYL BENZENE	1.40D-16 a

Note: a. MCM; b. IUPAC

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Appendix B: Evaluations of box model method by ambient data.

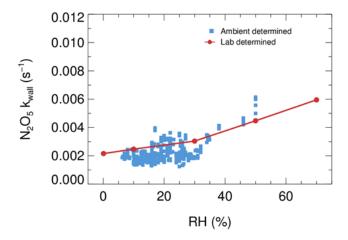


Figure B1. The derived dependence of N_2O_5 wall loss on RH at laboratory condition (red dots) and field measurement (blue square)

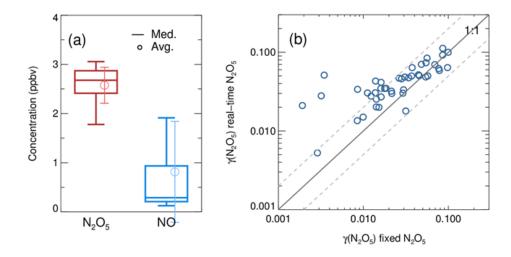


Figure B2. (a) the box whisker of N_2O_5 source and NO measured before the entrance; (b) the inter-comparison of derived N_2O_5 uptake coefficient by using a fixed initial N_2O_5 and a dynamic measured N_2O_5 at the flow tube entrance in the iterative box model.

- 715 Code/Data availability. The datasets used in this study are available from the corresponding
- author upon request (wanghch27@mail.sysu.edu.cn; k.lu@pku.edu.cn).

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- 718 **Author contributions.** K.D.L. and H.C.W. designed the study. X.R.C and H.C.W. analyzed
- 719 the data and wrote the paper with input from K.D.L.

720

721 **Competing interests.** The authors declare that they have no conflicts of interest.

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