



1 **Comparison of temperature dependent calibration methods**
2 **of an instrument to measure OH and HO₂ radicals using**
3 **laser-induced fluorescence spectroscopy**

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13

14 **Abstract**

15 Laser Induced Fluorescence (LIF) spectroscopy has been widely applied to fieldwork
16 measurements of OH radicals, and of HO₂, following conversion to OH, over a wide variety of
17 conditions, on different platforms, and in simulation chambers. Conventional calibration of
18 HO_x (OH + HO₂) instruments has mainly relied on a single method, generating known
19 concentrations of HO_x from H₂O vapour photolysis in a flow of zero air impinging just outside
20 the sample inlet ($S_{HO_x} = C_{HO_x} \cdot [HO_x]$, where S_{HO_x} is the observed signal and C_{HO_x} is the
21 calibration factor). The FAGE (Fluorescence Assay by Gaseous Expansion) apparatus
22 designed for HO_x measurements in the Highly Instrumented Reactor for Atmospheric
23 Chemistry (HIRAC) at the University of Leeds has been used to examine the sensitivity of
24 FAGE to external gas temperatures (266 – 348 K).

25 The conventional calibration methods give the temperature dependence of C_{OH} (relative to the
26 value at 293 K) of $(0.0059 \pm 0.0015) \text{ K}^{-1}$ and C_{HO_2} of $(0.014 \pm 0.013) \text{ K}^{-1}$. Errors are 2σ . C_{OH}
27 was also determined by observing the decay of hydrocarbons (typically cyclohexane) caused
28 by OH reactions giving C_{OH} (again, relative to the value at 293 K) of $(0.0038 \pm 0.0007) \text{ K}^{-1}$.
29 Additionally, C_{HO_2} was determined based on the second order kinetics of HO₂ recombination
30 with the temperature dependence of C_{HO_2} , relative to 293 K being $(0.0064 \pm 0.0034) \text{ K}^{-1}$.



1 The temperature dependence of C_{HOx} depends on HOx number density, quenching, relative
2 population of the probed OH rotational level and HOx transmission from inlet to detection axis.
3 The first three terms can be calculated and, in combination with the measured values of C_{HOx} ,
4 show that HOx transmission increases with temperature. Comparisons with other instruments
5 and the implications of this work are discussed.

6

7 **1 Introduction**

8 Hydroxyl radicals (OH) play a key role in our atmosphere, oxidising a broad range of species.
9 OH is the main daytime oxidant in the troposphere and the main sink for methane, a potent
10 greenhouse gas. The OH radical is linked to the HO₂ radical through the oxidation of most
11 other non-methane hydrocarbons (NMHCs) and CO in the troposphere and, through reaction
12 with NO₂, in the upper troposphere/lower stratosphere. Due to the high reactivity of OH
13 (lifetime ~1 s even in clean air), these radicals undergo minimal transport and local
14 concentrations depend only on the *in situ* chemistry. Measurements of HOx concentrations, in
15 conjunction with measurements of their sources and sinks are a sensitive test of chemical
16 models. Accurate measurement of [HOx] is therefore paramount, not only for field
17 measurements, (Stone et al., 2012; Heard and Pilling, 2003; Gligorovski et al., 2015), but also
18 for atmospheric simulation chambers where OH/HO₂ instruments have been deployed (Karl et
19 al., 2004; Glowacki et al., 2007).

20 Sensitive detection techniques with high temporal resolution are required for HOx detection
21 and techniques have been reviewed in Stone et al. (2012) and Wang et al. (2021). Fluorescence
22 Assay by Gaseous Expansion (FAGE) (e.g. Hard et al. (1984)) is the most common method
23 used for both field and chamber studies. Here, the sample is expanded to low pressures and OH
24 detected by resonance fluorescence at ~308 nm. The low pressures are required to temporally
25 separate fluorescence from the excitation laser pulse. HO₂ is converted to OH by reaction with
26 NO and detected in a separate cell. Both techniques require calibration which is conventionally
27 based on the generation of OH and HO₂ from water vapour photolysis at 185 nm at atmospheric
28 temperature and pressure.

29 Recent studies have demonstrated potential interferences for measurements of both OH and
30 HO₂ radicals using the FAGE technique, with the magnitude dependent upon instrument design
31 (Mao et al., 2012; Novelli et al., 2014; Novelli et al., 2017; Fuchs et al., 2011; Whalley et al.,
32 2013; Fuchs et al., 2016). Considerable effort has been made to minimize, understand and



1 mitigate any interference, with many groups now fitting an external OH scavenger injector to
2 measure OH concentrations using an alternative background signal, OH_{CHEM} , alongside the
3 conventional method of measuring OH using a background signal determined by tuning the
4 laser wavelength off-resonant to the transition, OH_{WAVE} (Woodward-Massey et al.,
5 2020; Novelli et al., 2014; Mao et al., 2012). Intercomparison campaigns (e.g. Schlosser et al.
6 (2009), Onel et al. (2017a)) in the controlled environment of an atmospheric chamber are useful
7 to identify systematic errors in different approaches, but if both methods require calibration,
8 the accuracy of the measurements is still compromised by uncertainties in the calibration
9 methods.

10 In an earlier paper (Winiberg et al., 2015), accurate calibration of a FAGE instrument over
11 a range of external inlet pressures (440 – 1000 mbar) was performed in the Leeds HIRAC
12 (Highly Instrumented Reactor for Atmospheric Chemistry (Glowacki et al., 2007)) chamber.
13 The instrument sensitivity to OH and HO_2 agreed well for the conventional water vapour
14 calibration method (where the external pressure is always 1 bar, and external pressure effects
15 were simulated by altering the pressure in the FAGE detection cell) and alternative methods
16 based on the temporal decay of a hydrocarbon (for OH) or the temporal decay of HO_2 via its
17 second-order self-reaction (for HO_2) over an external pressure range of 300 – 1000 mbar. For
18 OH, the calibration factor, C_{OH} , (where $S_{\text{HO}_x} = C_{\text{HO}_x}[\text{HO}_x]$ and S_{HO_x} is the FAGE signal)
19 increased by 17% and for HO_2 a slightly greater increase in C_{HO_2} of 32% was determined as
20 the pressure increased from 350 to 1000 mbar. There was good agreement between the absolute
21 values and their pressure dependence for both calibration methods. Such comparisons are
22 particularly relevant to aircraft operation where external pressures will vary considerably
23 during the flight or for evacuable chambers such as the Leeds HIRAC chamber which can
24 operate from 50 – 1000 mbar. Marno et al. (2020) have also developed the All Pressure
25 Altitude-based Calibrator of HO_x Experimentation (APACHE) to allow calibration of their
26 FAGE instrument HORUS (HydrOxyl Radical measurement Unit based on fluorescence
27 Spectroscopy) as a function of pressure, but not temperature.

28 Little is known on the effect of gas temperature at the inlet upon instrument sensitivity for
29 LIF instruments, despite field instruments being used at extremes of temperature, from day to
30 night, from deserts to the polar regions, and in aircraft, where temperatures change rapidly with
31 altitude. Additionally, ambient conditions influence not only the inlet temperature, but the
32 whole apparatus. For example in the FAGE system associated with HIRAC, based on a design
33 for aircraft use (Commane et al., 2010), the whole inlet tube (~30 cm) is located inside the



1 HIRAC chamber and so wall loss rates of HO_x in the inlet tube will be influenced by the
2 temperature of the HIRAC chamber. The long inlet is required either to locate the pinhole
3 outside of the aircraft for the airborne instrument, or to allow sampling across the diameter of
4 the HIRAC chamber. To date, the only study investigating the effect of inlet temperature on
5 instrument sensitivity to HO_x radicals has been performed by Regelin et al. (2013), who
6 reported a minor positive dependence of the OH sensitivity (*C*_{OH}) as a function of decreasing
7 inlet temperature for the HORUS instrument (possibly due to a cooling effect on the
8 instrumentation). There was a more marked decrease in the instrument sensitivity to HO₂ with
9 decreasing temperature, most probably due to enhanced wall losses at lower temperatures.

10 In this paper, instrument sensitivity as a function of external inlet temperature has been
11 determined for the HIRAC FAGE instrument for both OH and HO₂, using the water vapour
12 photolysis calibration method in an external flowtube (termed ‘conventional method’) and
13 alternative calibration methods using chemical reactions in the HIRAC chamber (Winiberg et
14 al., 2015) at varying temperatures. Alternative OH calibrations used the inferred [OH] from the
15 measured decay of a hydrocarbon (HC), typically cyclohexane, reacting with OH (R1) (termed
16 ‘HC decay method’). The rate of loss of HC is then given by equation (E1).



$$18 \quad \frac{-d[\text{HC}]}{dt} = k_{\text{bi}}[\text{OH}][\text{HC}] \quad (\text{E1})$$

19 In E(1), *k*_{bi} is the well-established literature value for the bimolecular rate coefficient between
20 OH and the monitored hydrocarbon and $\frac{-d[\text{HC}]}{dt}$ can be measured from the HC time series so
21 that [OH] is the only unknown parameter and can be calculated and compared with the [OH]
22 predicted via the conventional calibration method.

23 HO₂ was also calibrated by monitoring the HO₂ kinetic decay during the recombination
24 following generation by HCHO photolysis in the presence of O₂ (termed ‘HO₂ self-reaction
25 method’).





1 The time dependence of the $[\text{HO}_2]$ in the second-order decay depends on the initial
2 concentration of HO_2 allowing for calibration.

3

4 **2 Experimental**

5 **2.1 The HIRAC chamber**

6 The alternative calibration methods of monitoring hydrocarbon or HO_2 decays were conducted
7 in HIRAC using very similar methods and conditions as described in Winiberg et al. (2015).
8 HIRAC is a stainless steel chamber with a total volume of 2.25 m^3 and can operate over a wide
9 range of pressures (50 – 1000 mbar) and temperatures (227 – 343 K). Multiple access ports are
10 available to connect an array of instrumentation and monitoring equipment (pressure gauges,
11 thermocouples etc.). The chamber has been described previously in detail in Glowacki et al.
12 (2007), Malkin et al. (2010) and (Bejan et al., 2018). More recently a temperature control
13 system was installed to further enhance the capabilities of the HIRAC chamber (Section 2.1.1).
14 Details on the temperature characteristics of HIRAC can be found in Section S1 of the SI.

15 The photolysis lamps, housed in eight quartz tubes mounted radially inside the reactive
16 volume, were used to initiate photochemistry. The lamps were interchangeable depending on
17 the target molecules; lamps, with primary emissions centred at 254 and 310 nm (GE Optica,
18 GE55T8/HO and Philips, TL40W/12 RS respectively), were used for the alternative OH and
19 HO_2 calibration methods respectively (sections 3.2 and 3.3). The housings were flushed with
20 dry N_2 ($\sim 3 \text{ slm}$ per housing) to help regulate the temperature and remove photolabile species
21 and water, which could condense or freeze around the lamps at lower temperatures. A
22 photolysis lamp induced chamber temperature increase of $\sim 2 - 5 \text{ K}$ was seen over the course
23 of a typical experiment ($< 40 \text{ mins}$), but this variation was reduced if the chamber was
24 temperature controlled. Temperatures were monitored using a series of K-type thermocouples
25 inside the lamp housings (one per lamp) as well as distributed around the inside of the chamber.
26 Thermocouples were placed strategically to allow the temperature to be measured close to the
27 chamber walls, inlets, flanges and in the chamber.

28 **2.1.1 Temperature Control System**

29 During manufacture, square cross section steel tubing (volume $\sim 50 \text{ L}$) was welded directly to
30 the outer skin of HIRAC, allowing a cooling/heating liquid to flow around the chamber,



1 controlling the temperature inside. The square tubing enabled the temperature control liquid to
2 transfer heat more efficiently to the chamber by offering a larger contact surface area compared
3 to cylindrical tubing. A Huber thermostat unit (model 690W) was used to circulate ~60 L of
4 thermofluid (Huber DW-THERM, 183 - 473 K) around the chamber. Further details are given
5 in the SI (Section S1).

6 HIRAC was able to sustain a steady temperature (± 2 K) across the chamber at any
7 temperature between 227 and 343 K and example temperature profiles are given in the SI
8 (Figure S2). A negligible temperature gradient was observed across the central portion of the
9 chamber, in both the horizontal and vertical axes. Close to the walls of the chamber, however,
10 a change of ~1 K was observed. The flanges around the HIRAC chamber were insulated with
11 ~40 mm of neoprene, however there was no direct temperature control of the flanges or access
12 ports, which was likely responsible for the change in temperature at the large 600 mm access
13 flanges.

14 2.1.2 HO_x Instrumentation

15 The OH and HO₂ radicals were detected using a FAGE instrument based in the HIRAC
16 chamber with a 5 kHz pulse repetition frequency (PRF) laser light source, as described in
17 Winiberg et al. (2015); Winiberg et al. (2016) and Glowacki et al. (2007). Air was sampled at
18 ~6 slm through a 1.0 mm diameter pinhole nozzle and passed down the inlet (length 280 mm,
19 50 mm diameter) into the OH detection axis maintained at low pressure (typically ~3.85 mbar)
20 using a high-capacity rotary-backed roots blower pumping system (Leybold, Trivac D40B and
21 Ruvac WAU251). The long inlet was used to draw a sample away from the chamber walls
22 where radical losses increase (a maximum of 15% decrease at <10 mm from the chamber wall)
23 and to probe any radical gradients occurring due to spatially inhomogeneous production
24 (Winiberg et al., 2015). The FAGE instrument was coupled to the HIRAC chamber using ISO-
25 K160 flanges, ensuring the pinhole is kept >200 mm from the chamber walls.

26 Concentrations of HO₂ were measured simultaneously in a second detection axis ~300 mm
27 downstream of the OH detection axis. High purity NO (BOC, N2.5 Nitric Oxide) was added
28 ~20 mm before the HO₂ detection axis into the centre of the FAGE cell in the direction of gas
29 flow through 1/8" stainless steel tubing at a rate of 5 sccm (Brooks 5850S) converting HO₂ to
30 OH. Conversion of some types of RO₂ radicals (in particular β -hydroxyperoxy radicals) to OH
31 upon reaction with NO has been reported in other FAGE instruments (Whalley et al.,
32 2013; Fuchs et al., 2011). However, during the alternative HO₂ calibrations (based on HCHO



1 photolysis) presented here no β -hydroxyperoxy radicals were generated hence any interference
2 was assumed to be negligible.

3 A JDSU Nd:YAG pumped Sirah Cobra Stretch system (PRF = 5 kHz) was used to generate
4 the frequency doubled \sim 308 nm (307.99 nm to excite the $Q_1(2)$ rotational state) light for the
5 fluorescence of OH radicals. Light was directed from the output of the laser and focussed into
6 fibre optic cables (10 m, Oz Optics) which were then attached directly to the FAGE cell arms
7 *via* collimators (Oz Optics). Fluctuations in laser power were accounted for using a linear
8 response UV sensitive photodiode (UDT-555UV, Laser Components UK) at the exit arm of
9 the OH and HO₂ detection axes to normalise the LIF signal. The laser system provided between
10 5 – 7 and 2 – 3 mW of 308 nm light to the OH and HO₂ detection axes, respectively.

11 The OH fluorescence was collected orthogonal to the gas flow onto electronically gated
12 Channeltron PhotoMultiplier tubes (CPM, Perkin Elmer, C943P) *via* a series of imaging lenses
13 and a narrow bandpass filter (Barr Associates, 308.8 ± 5.0 nm). A spherical concave back
14 reflector was positioned underneath the cell, opposite the detection optics, to optimise light
15 collection onto the CPM. To avoid detector saturation, the CPM was gated (i.e. switched off)
16 for the duration of the laser pulse using a modified gating unit based on the original design by
17 Creasey et al. (1997a). Signals from the CPM were analysed using PC-based photon counting
18 cards (Becker and Hickl PMS-400A).

19 2.1.3 Other instrumentation

20 As with the previously published work (Winiberg et al., 2015), a chemiluminescence NO_x
21 analyser (TEC 42C, limit of detection = 50 pptv at 60 s averaging) was used to determine that
22 levels of NO_x (NO + NO₂) in the HIRAC chamber were typically below the detection limit of
23 the apparatus.

24 Most of the OH calibration experiments using the hydrocarbon decay method were
25 performed monitoring HC decays using a chemical ionization time of flight mass spectrometer
26 (Kore custom build) operating with N₂⁺ ionization. Gas was sampled from HIRAC via \sim 7 m of
27 1/8" Teflon tubing with the inlet being located close (within 70 cm) to the FAGE inlet. A
28 majority of the experiments were carried out with cyclohexane as the HC (monitored at $m/z =$
29 84.15), although other compounds were used. The mass spectrometer signal was calibrated by
30 introducing known HC concentrations into HIRAC. An example of the resulting calibration
31 plot can be found in the SI (Section S2, Figure S3).

32



1 **2.2 General Chamber preparation**

2 Calibration experiments were conducted at 1000 mbar in an Ultra-High Purity (UHP) 1:4
3 synthetic air mix of O₂ (BOC, zero-grade, >99.999%) and N₂ (BOC, zero-grade, >99.998%) to
4 match the range of pressures from the water vapour calibration method (section 3.1). Thorough
5 mixing of reaction mixtures within HIRAC was achieved in ≤ 70 s by four circulation fans
6 mounted in pairs at each end of the chamber. The chamber was evacuated to ~ 0.05 mbar for
7 $\sim 60 - 120$ min following each experiment using the rotary pump backed roots blower to ensure
8 removal of all reactants/products. The combined sampling rate of ~ 9 slm from the chamber
9 required a counter flow of synthetic air to maintain the desired pressure and resulted in a first
10 order dilution term of $(4.5 \pm 0.2) \times 10^{-5} \text{ s}^{-1}$. The dilution flow was regulated using two Brooks
11 mass flow controllers (N₂ and O₂) and the dilution was taken in account in all analyses.

12

13 **2.3 Chemical reagents**

14 Known concentrations of precursors (except H₂O₂) and reagents were introduced to the
15 chamber in the vapour phase through a 0.97 L stainless steel delivery vessel. Hydrogen
16 peroxide (50% wt solution, Merck, used as supplied) was directly injected via a syringe.
17 Multiple injections could be made in each run to ensure a wide range of [OH] was covered.

18 For the hydrocarbon based OH calibration method, cyclohexane (99%, Fischer Scientific),
19 methylcyclohexane (>99.9%, Sigma Aldrich) and heptane (99%, Fischer Scientific) were
20 purified using freeze-pump-thaw cycles before being introduced into the HIRAC chamber.

21 For the second-order HO₂ calibration method, formaldehyde (HCHO) was produced in the
22 gas phase by gently heating paraformaldehyde (99.9%, Sigma Aldrich) into the evacuated
23 delivery vessel. This method was sufficient for producing the 2 – 3 ppmv concentrations of
24 HCHO in the HIRAC chamber that were required.

25

26 **3 Calibration methods**

27 **3.1 Flowtube/Water Photolysis Calibration Method**

28 The flowtube calibration method relies on the photolysis of H₂O vapour at 184.9 nm in a fast
29 flow (40 slm) of synthetic air. A mercury penray lamp (LOT-Oriel, Hg-Ar) was used as the
30 photolysis source, placed at the end of a square cross section flow tube ($12.7 \times 12.7 \times 300$ mm).
31 Air was humidified by passing a fraction of the bulk air flow through a bubbler containing

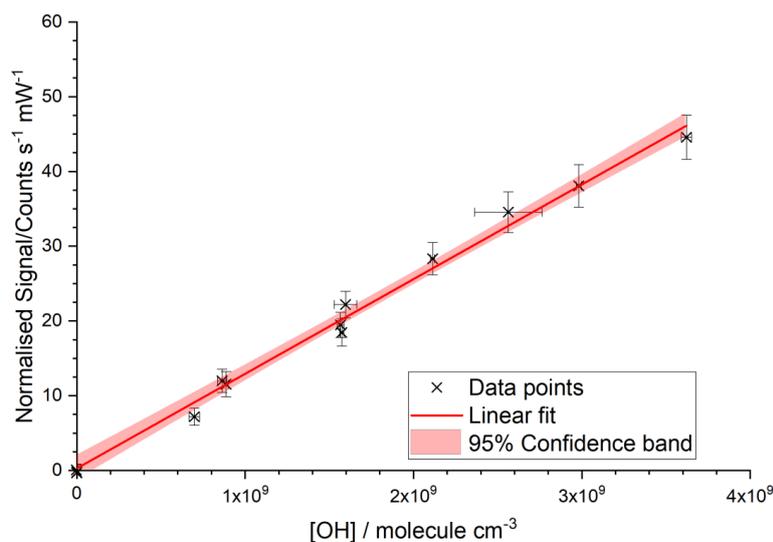


1 deionised water. The $[\text{H}_2\text{O}]$ was measured using a dew-point hygrometer (CR4, Buck Research
2 Instrument) prior to the flow tube and the resulting OH and HO_2 concentrations from photolysis
3 can be calculated from equation (E2):

$$4 \quad [\text{OH}] = [\text{HO}_2] = [\text{H}_2\text{O}] \sigma_{\text{H}_2\text{O}, 184.9 \text{ nm}} \Phi_{\text{OH}} F_{184.9 \text{ nm}} \Delta t \quad (\text{E2})$$

5 where $\sigma_{\text{H}_2\text{O}, 184.9 \text{ nm}}$ is the known absorption cross-section of H_2O vapour at 184.9 nm
6 $((7.22 \pm 0.22) \times 10^{-20} \text{ cm}^2 \text{ molecule}^{-1})$ (Cantrell et al., 1997; Creasey et al., 2000; Hofzumahaus
7 et al., 1997), $\Phi_{\text{OH}} (= \Phi_{\text{HO}_2} = 1)$ is the photodissociation quantum yield of OH and HO_2 (Fuchs
8 et al., 2011), $F_{184.9 \text{ nm}}$ is the photon flux of 184.9 nm light and Δt is the exposure time of the air
9 to the Hg lamp output. The exposure time of the air to the 184.9 nm light, Δt , was calculated
10 as a function of the known velocity of the air and the cross section of the photolysis region.
11 The product $F_{184.9 \text{ nm}} \times \Delta t$ was determined for lamp supply currents between 0.2 and 3.0 mA
12 using the N_2O actinometry method described in detail in a number of publications (Edwards et
13 al., 2003; Heard and Pilling, 2003; Faloon et al., 2004; Whalley et al., 2007; Glowacki et al.,
14 2007).

15 The gas output from the flow tube was directed towards the FAGE sampling inlet, where
16 the overflow of the FAGE sample volume from the flow tube stopped the impingement of
17 ambient air. A range of HO_x concentrations ($10^8 - 10^{10} \text{ molecule cm}^{-3}$) were produced by
18 changing the mercury lamp photon flux whilst keeping a constant $[\text{H}_2\text{O}]$ (typically 2000 - 3000
19 ppmv). The average calculated $[\text{HO}_x]$ values are compared to their concurrent OH/ HO_2 signals
20 observed during the same time period, the linear regression of which gives the instrument
21 sensitivity to OH/ HO_2 . A typical calibration plot is shown in Figure 1. Potential systematic
22 errors in the flowtube calibration method have been discussed previously (Winiberg et al. 2015)
23 and are summarized for the current instrument in Table 4 and discussed further in the SI,
24 Section S3, which also contains a schematic of the flowtube calibration apparatus (Figure S4).



1

2 **Figure 1:** Typical room temperature calibration plot from the conventional water photolysis, flow tube
3 method. The total flow rate was 40 slm, with [H₂O] = 1600 ppmv, the laser power was 9.65 mW and
4 the OH cell was at a pressure of 2.6 Torr. Gradient = $(1.266 \pm 0.034) \times 10^{-8}$ counts s⁻¹ mW⁻¹ cm³
5 molecule⁻¹, intercept = 0.28 ± 0.74 counts s⁻¹ mW⁻¹. Errors are 2σ.

6

7 3.1.1 Calibration for External Inlet Temperature

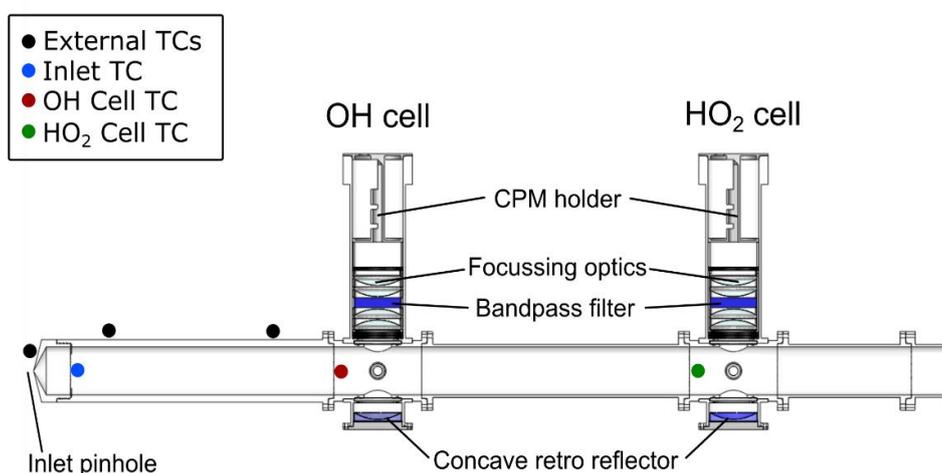
8 The FAGE inlet was wrapped with ¼” copper tubing (~ 5 cm between coils) and covered in
9 two layers of aluminium foil to aid thermal contact. A final layer of 10 mm thick neoprene was
10 added to the outside of the foil to aid insulation. The Huber temperature control unit was used
11 to flow DW-THERM thermofluid through the tubing to vary the temperature of the inlet.
12 Temperatures were monitored externally using three K-type thermocouples; two positioned on
13 the inlet and one on the conical pinhole nozzle during the calibration procedure (see Figure
14 2(a)).

15 Calibrations were conducted at five external inlet temperatures from 263 – 343 K,
16 representative of the operating temperature range for the HIRAC chamber. During the bulk of
17 the experiments, gases from the flowtube calibration source were maintained at room
18 temperature. However, an additional range of calibration experiments were performed with
19 flowtube gas maintained to within ±5 K of the measured external inlet temperature. This effect
20 was achieved by passing the humidified bulk flow through a 2 m long coil of ¼” copper tubing
21 held at the desired set point using a thermostat controlled water bath (Thermo Fischer Science).



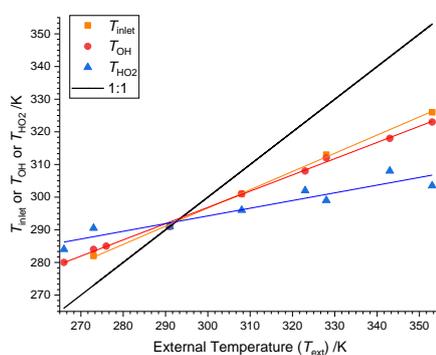
1 The $[H_2O]_{vap}$ was determined just before the calibration flowtube, with the temperature
 2 monitored both before and at the exit of the flowtube. Short gas lines were used between the
 3 water bath and the flow tube, which was covered in a thin layer of neoprene to insulate and
 4 reduce temperature gradients.

5 (a)

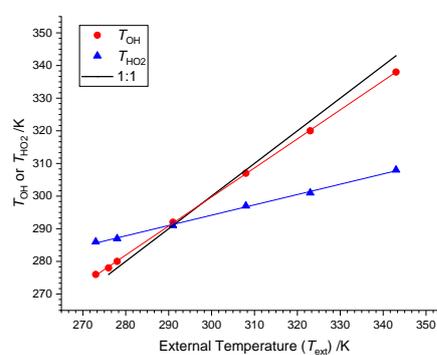


6

7 (b)



(c)



8 **Figure 2:** (a) Schematic of FAGE Cell showing locations of thermocouples. (b) Internal cell
 9 temperatures (T_{OH} or T_{HO_2}) and inlet temperatures (T_{inlet}) plotted as a function of the external temperature
 10 (T_{ext}), when sampling air at 293 K from the calibration flowtube. (c) Internal temperatures as a function
 11 of the external temperature when either sampling temperature controlled air from the calibration
 12 flowtube or sampling from the HIRAC chamber.

13

14



1 Prior to the calibration, the internal cell temperatures were measured using three K-type
2 thermocouples positioned in the centre of the gas flow inside the inlet (just after the inlet
3 pinhole), OH and HO₂ fluorescence cells, details of which are discussed in the results section
4 (4.1.1). The thermocouples were inserted into the cell using a 1/4" compression fitting port, seal;
5 this allowed the cell to be operated at normal operating pressure during the temperature profile
6 measurements. Thermocouples were held in place temporarily using electrical tape, and
7 OH/HO₂ calibrations were not performed with the thermocouples in place.

8

9 3.2 Hydrocarbon decay method

10 A majority of the hydrocarbon decay OH measurements were made with cyclohexane as the
11 monitored hydrocarbon (HC) (monitored via the $m/z = 84.15$ peak) and hydrogen peroxide
12 photolysis at 254 nm as the OH source.

13 The principle of the hydrocarbon decay method was outlined in the introduction; the rate of
14 loss of the HC by OH is given by:

$$15 \quad -\frac{d[\text{HC}]}{dt} = k_{bi}[\text{OH}][\text{HC}] \quad (\text{E1})$$

16 The rate coefficient for cyclohexane, c-C₆H₁₂, has received much attention in the literature over
17 the 273 – 343 K temperature range used in this study, and so we use the IUPAC recommended
18 rate expression (Atkinson et al., 2006):

$$19 \quad k_{\text{OH}+\text{c-C}_6\text{H}_{12}} = 3.26 \times 10^{-17} T^2 e^{(262 \pm 66)/T} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \quad (\text{E3})$$

20 The calculated [OH] from the hydrocarbon decay can be compared to the corresponding FAGE
21 signal, corrected for the difference in [H₂O] used in the calibration and that present in the
22 HIRAC chamber, to determine the C_{OH}. In practice, the total HC decay is a combination of
23 reaction with OH and other first order loss processes, primarily dilution (as sampled gas is
24 replenished with air). Therefore

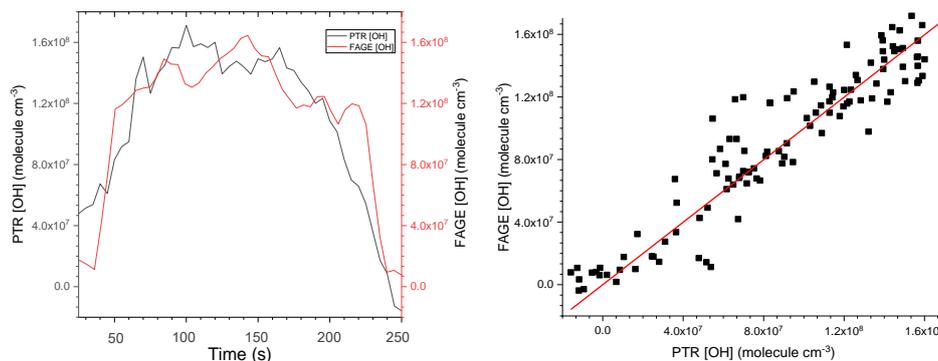
$$25 \quad -\frac{d[\text{HC}]}{dt} = k_{1st}[\text{HC}] + k_{bi}[\text{OH}][\text{HC}] \quad (\text{E4})$$

26 where k_{1st} represents the rate coefficient for the sum of all non-OH first order loss processes.
27 Gradients were obtained from analysis within the Origin software package. A second order
28 polynomial was fitted to 10 – 40 points (with the separation of each point being 10 s); the
29 number of points depending on the rate of change of the [HC] and the data points were
30 smoothed via the method of Savitzky-Golay (Savitzky and Golay, 1964).



1 k_{1st} was determined from the HC decays in the absence of OH (either with no lamps on, or
2 no OH precursor present). For each injection of HC (typical initial concentration of $3 - 5 \times$
3 10^{13} molecule cm^{-3}) there were multiple H_2O_2 injections (~ 1 ml). FAGE measurements were
4 typically averaged over 30 s (30 data points, with each data point corresponding to accumulated
5 signal over ~ 1 s) to counteract the noise arising in fluorescence counts. During rapid changes
6 in the observed signal, for example immediately after initial photolysis of hydrogen peroxide
7 in the chamber (see Figure 3(a)), a reduced averaging period was used.

8 Figure 3(a) shows a typical time series of OH with the black line giving the [OH] derived
9 from the mass spectrometer measurements and the brown line giving [OH] derived from the
10 FAGE signal and converted to [OH] using the conventional flow tube water vapour photolysis
11 calibration at 293 K. Figure 3(b) shows the resultant scatter plot. The slope of the scatter plot
12 gives the correction to be applied to $C_{293\text{ K}}$ from the conventional calibration to match the [OH]
13 derived from the mass spectrometric measurements.



14 **Figure 3:** a) Time series of [OH] derived from FAGE measurements and from mass spectrometric
15 measurements of cyclohexane removal recorded following H_2O_2 photolysis at 293 K and 1000 mbar
16 air. b) Resultant scatter plot where the gradient, 0.998 ± 0.016 (2σ) gives C_{rel} for the FAGE apparatus
17 at 293 K for this experiment. The average gradient at 293 K is 1.034 ± 0.0068 from five experiments.

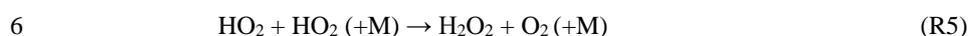
18

19 3.3 Calibration of HO_2 detection via HO_2 recombination kinetics

20 The HCHO photolysis/ HO_2 recombination kinetics method of HO_2 cell calibration was used
21 as described in Winiberg et al. (2015). Formaldehyde was introduced in a flow of nitrogen into
22 the chamber (containing synthetic air at 1000 mbar) at concentrations of
23 $\sim 2 \times 10^{13}$ molecule cm^{-3} . The chamber was irradiated (lamps: Philips TL40W/12 RS) resulting
24 in an almost instantaneous HO_2 signal (reactions R2 – R4). Once a steady state HO_2



1 concentration was achieved, the photolysis lamps were turned off and the decay of HO₂ was
2 monitored by FAGE for ~120 s (Figure 4). The decay of HO₂ was primarily controlled by the
3 self-reaction (R5), but there was a small first-order contribution from loss to the walls (R6).
4 The measurement of HO₂ decays was repeated up to six times before the laser wavelength was
5 scanned to the offline position.



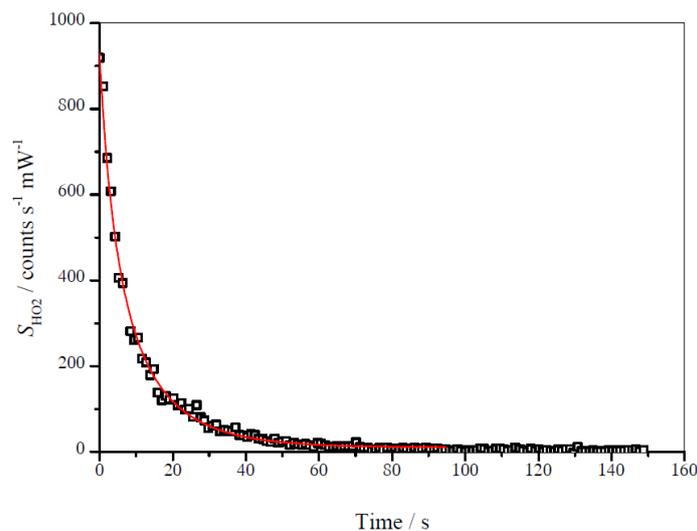
8 The chamber mixing fans were used for the first three calibration decays, representative of
9 a typical experimental homogeneous gas mixture. The second series of three calibration decays
10 were conducted without the mixing fans to probe the HO₂ recombination and wall loss kinetics
11 in the absence of effective mixing.

12 When the fans are on, the loss of HO₂ was characterised by bimolecular self-reactions and
13 a first order wall loss parameter. The solution to this mixed order decay is given by:

14
$$(S_{\text{HO}_2})_t = \left(\left(\frac{1}{(S_{\text{HO}_2})_0} + \frac{2 \cdot k_{\text{HO}_2+\text{HO}_2}}{k_{\text{loss}} \cdot C_{\text{HO}_2}} \right) \cdot e^{(k_{\text{loss}} t)} - \left(\frac{2 \cdot k_{\text{HO}_2+\text{HO}_2}}{k_{\text{loss}} \cdot C_{\text{HO}_2}} \right) \right)^{-1} \quad (\text{E5})$$

15 where $(S_{\text{HO}_2})_t$ and $(S_{\text{HO}_2})_0$ are the HO₂ signal at time t and $t = 0$ respectively, (C_{HO_2}) is the
16 instrument sensitivity, $k_{\text{HO}_2+\text{HO}_2}$ is the HO₂ recombination rate coefficient and k_{loss} represents
17 the wall loss parameter. Both k_{loss} and C_{HO_2} were determined by data fitting the S_{HO_2} decay
18 using equation (E5) with a Levenburg-Marquardt non-linear least squares algorithm, fixing the
19 initial signal and $k_{\text{HO}_2+\text{HO}_2}$. The first ~100 s of data were used, ensuring analysis after an almost
20 complete decay of S_{HO_2} . Figure 4 shows an example of a typical decay and the resulting fit to
21 equation (E5).

22 For the experimental temperature range (275 – 345 K), $k_{\text{HO}_2+\text{HO}_2}$ has values between
23 $(2.00 - 2.85) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ according to the recommendation given by IUPAC
24 (2007). The chamber was operated under dry conditions ($< 10 \text{ ppmv } [\text{H}_2\text{O}]_{\text{vap}}$), and so the
25 enhancement of $k_{\text{HO}_2+\text{HO}_2}$ by formation of a pre-reactive complex with H₂O was ignored for
26 these analyses. The wall loss rate, k_{loss} , was dependent on daily chamber conditions and was
27 therefore determined as part of the fitting procedure along with C_{HO_2} , typically between
28 $0.032 - 0.073 \text{ s}^{-1}$ with an uncertainty of $\pm 10 \% (2\sigma)$.



1

2 **Figure 4:** Typical HO₂ decay recorded at 293 K and 1000 mbar air. The red line is the fit to
3 the data from equation (E5) giving $C_{\text{HO}_2, 293 \text{ K}} = (4.17 \pm 1.66) \times 10^{-8} \text{ counts cm}^3 \text{ molecule}^{-1}$
4 $\text{mW}^{-1} \text{ s}^{-1}$

5

6 **4 Results and Discussion**

7 **4.1 Conventional Calibration method**

8 4.1.1 Temperature profiles in the FAGE instrument

9 Temperatures within the FAGE instrument as a function of external temperatures are shown in
10 Figures 2(b) and (c) and tabulated in Table 1. For Figure 2(b) and the first part of Table 1, the
11 temperatures were recorded with FAGE sampling air at 293 K from the calibration flow tube
12 as the FAGE inlet was cooled or heated. Temperatures became closer to ambient (293 K) from
13 the inlet (T_{inlet}) to the OH observation cell (T_{OH}) and finally to the HO₂ observation cell (T_{HO_2}).
14 In Figure 2(c) and the second part of Table 1, the sampled air (either from the calibration flow
15 tube or from HIRAC) matched the external temperature of the inlet tube. For these experiments,
16 there was no thermocouple located inside the inlet to give T_{inlet} . The temperature in the OH cell
17 was very close to the external temperature of the sampled air. The transmission process through
18 the FAGE inlet following sampling through the pinhole should be similar to when FAGE is in
19 HIRAC, however, even with the temperature controlled air in the wand calibration, it is still
20 difficult to determine the actual temperature and conditions at the pinhole itself.



1 The gap between the OH and HO₂ cells means that the sampled air was closer to ambient
 2 room temperatures when reaching the HO₂ cell. HO₂ was predominantly be exposed to a
 3 temperature environment similar to that for OH as it passed through the inlet, which may
 4 influence wall loss rates. The variation in T_{OH} and T_{HO_2} under different calibration regimes
 5 means that care has to be taken in comparing C_{HO_x} values, as a number of processes within
 6 FAGE are temperature dependent. Nevertheless, the different calibration methods do yield
 7 important insights into the processes in the FAGE apparatus.

8

9 **Table 1:** Temperature Calibration of the FAGE instrument with a) constant temperature (293
 10 K) calibration gas b) with calibration gas at the external temperature.

External Temperature/K (T_{ext})	Inlet Temperature /K, (T_{inlet})	OH FAGE Cell Temperature /K, (T_{OH})	HO ₂ FAGE Cell Temperature /K, (T_{HO_2})
<i>Ambient Calibration Air at 293 K</i>			
266 ^a		280	284
273	282	284	290.5
276		285	
293	293	293	293
308	301	301	296
323		308	302
328	313	312	299
343		318	308
353	326	323	313.5
<i>Calibration Air Matched to FAGE Inlet Tube Temperature</i>			
273		276	286
276		278	
278		280	287
293		293	293
308		307	297
323		320	301
343		338	308

11 a – All temperature measurements have uncertainty of ± 0.5 K.

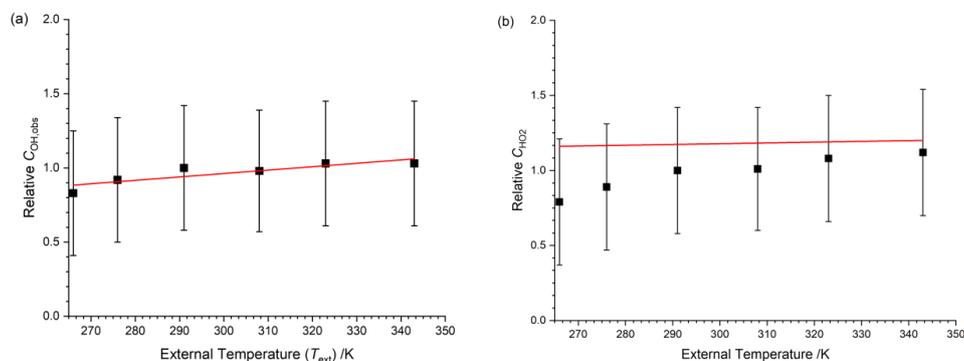
12 Figures 2(b) and (c) show the linear relationship between the internally measured
 13 temperature at the pinhole, OH cell and HO₂ cell. For Figure 2(b), the linear regression of the
 14 data gives ratios of 0.556 ± 0.002 , 0.510 ± 0.002 and 0.195 ± 0.002 for the inlet thermocouple
 15 (close to the pinhole), OH cell and HO₂ cell. The temperature in the OH cell is controlled by
 16 the external temperature. In contrast, in field instruments which have a very different design
 17 and where OH is probed very close to the pinhole, there is a significant cooling effect due to



1 the expansion (Creasey et al., 1997b). This is lost in the HIRAC FAGE due to the long inlet
2 prior to probing the OH.

3 4.1.2 Temperature Dependent Flow Tube Calibration with Air at 293 K

4 Figure 5 displays the relative C_{OH} and C_{HO_2} for the HIRAC FAGE instrument as a function of
5 external temperature between 266 – 343 K, with the data points listed in the top half of Table
6 2. In these experiments the FAGE inlet was cooled or warmed to give the external temperature
7 (T_{ext}). The air from the calibration flow tube was at a constant 293 K and therefore the
8 temperature in the observation cells (OH or HO₂) was varying compared to the inlet air. This
9 method of investigating the temperature dependence of C_{HO_x} therefore operates under different
10 conditions from the subsequent methods (Sections 4.1.3 and 4.2). Data for C_{HO_x} are presented
11 relative to the calibration factor at room temperature (293 K).



12 **Figure 5:** Temperature dependence of the calibration factors (C_{HO_x}) as a function of the external
13 temperature with HO_x being delivered from the calibration flow tube at a constant temperature. (a)
14 $C_{\text{OH,obs}}$, slope = $(0.0023 \pm 0.0007) \text{ K}^{-1}$. (b) $C_{\text{HO}_2,obs}$, slope = $(0.0005 \pm 0.0031) \text{ K}^{-1}$. Errors are 2σ .

15

16 $C_{\text{OH,obs}}$ shows a positive temperature dependence ($0.0023 \pm 0.0007 \text{ K}^{-1}$), for $C_{\text{HO}_2,obs}$, the data
17 appear to be more scattered and no systematic trend is observable. The overall temperature
18 dependence of both HO_x calibration factors are small compared to the overall uncertainty in
19 the calibration (40%); the relative calibration factor for OH changes by about 20% from 266 –
20 343 K. However, the error bars in Figure 5 represent the total error in the calibration, much of
21 which will be temperature independent. A full discussion on the temperature dependence of
22 the calibration factors is presented in Section 4.3.

23

24



1 **Table 2:** Instrument sensitivity to OH, C_{OH} , and HO₂, C_{HO_2} , determined using the
 2 conventional water vapour calibration method.

T_{ext}/K	T_{OH} / K	T_{HO_2} / K	$C_{OH,obs}$	$C_{HO_2,obs}$
<i>Ambient Calibration Air at 293 K</i>				
266	280	284	0.83 ± 0.42	1.11 ± 0.26
276	285	-	0.92 ± 0.42	- ^a
293	293	293	1.00 ± 0.42	1.00 ± 0.50
308	301	297	0.98 ± 0.41	1.36 ± 0.31
323	308	302	1.03 ± 0.42	1.40 ± 0.38
343	318	308	1.03 ± 0.42	1.01 ± 0.32
<i>Calibration Air Matched to FAGE Inlet Temperature (T_{in})</i>				
276	278	-	1.06 ± 0.39	- ^a
278	280	287	0.91 ± 0.50	1.43 ± 0.54
293	293	293	1.00 ± 0.40	1.00 ± 0.45
323	320	301	1.18 ± 0.39	1.91 ± 0.38
343	338	-	1.45 ± 0.39	- ^a

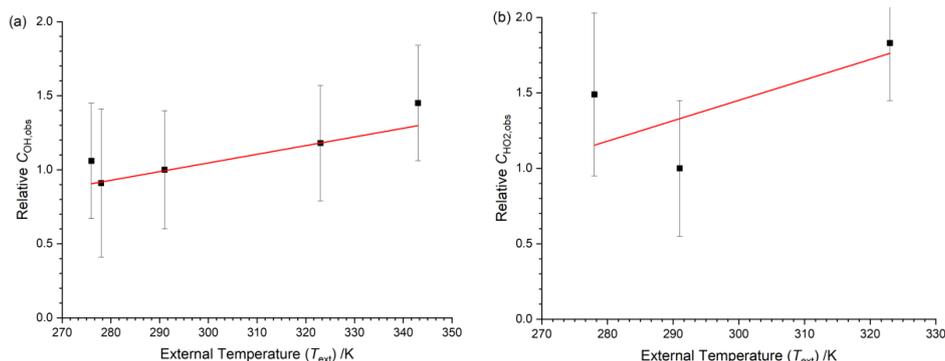
3 The internal temperatures (± 0.5 K) for the OH and HO₂ fluorescence cells are represented by T_{OH} and
 4 T_{HO_2} respectively. a – determination of C_{HO_2} was precluded by a malfunctioning NO mass flow
 5 controller.

6

7 4.1.3 Temperature Dependent Flow Tube Calibration with Air at Varying Inlet 8 Temperatures

9 A similar procedure to Section 4.1.2 was carried out, but in this case, the air flowing into the
 10 calibration flow tube had been cooled/heated to match the external temperature of the FAGE
 11 inlet. This method will give conditions that are more closely matched to those when the FAGE
 12 instrument is located in the HIRAC chamber, where the FAGE inlet is at the same temperature
 13 as the gas being sampled from HIRAC. The water vapour concentration was measured at a
 14 fixed temperature in the dew-point hydrometer and therefore the [HO_x] emitted from the wand
 15 needed to be corrected for the change in [H₂O] and additionally, for the change in Δt in equation
 16 (E2).

17 In this calibration arrangement the temperature of the OH cell (T_{OH}) was virtually identical
 18 to the external temperature (T_{ext}). The HO₂ FAGE cell was closer to ambient room temperature.
 19 The temperature dependence of $C_{HO_x,obs}$ relative to 293 K is shown in Figure 6. The calibrations
 20 were taken at different times from those in Section 4.1.2, but the absolute C_{HO_x} factors at 293
 21 K were in good agreement, within 5%. For OH, the slope of Figure 6(a) is again positive. For
 22 HO₂ (Fig 6(b)) there are only three datum points and they are somewhat scattered.



1 **Figure 6:** Temperature dependence of the calibration factors ($C_{HO_x,obs}$) as a function of the external
2 temperature with HOx being delivered from the calibration flow tube at the external temperature. (a)
3 $C_{OH,obs}$, slope = $(0.0059 \pm 0.0015) K^{-1}$. (b) $C_{HO_2,obs}$, slope = $(0.014 \pm 0.013) K^{-1}$.
4

5 4.2 Alternative Calibration Methods

6 4.2.1 Hydrocarbon Decay Calibration of OH Sensitivity

7 The ratio of the conventional water vapour flowtube calibration to the HC decay method
8 derived from scatter plots such as Figure 3 at 293 K was 1.034 ± 0.068 , where the errors are
9 the statistical errors in the gradient of the scatter plots at the 2σ level. The two methods are
10 therefore in excellent agreement as has been observed in our previous study conducted solely
11 at room temperature (Winiberg et al. (2015), 1.19 ± 0.26). The increased number of data points
12 available for the HC analysis using PTR monitoring increases the precision of this work
13 compared to our earlier studies where [HC] was measured at much lower time resolution by
14 FTIR or gas chromatography.

15 A potential source of error in the HC decay method is quantifying the removal of the HC by
16 non-OH sources. The effects of dilution and wall loss can be accounted for by suitable blank
17 experiments, however, it is harder to account for any other chemically induced removal by
18 photolytically generated radicals other than OH in such blank experiments. The hydrocarbons
19 chosen for this analysis are simple alkanes with well-established chemistry that should
20 minimize such possibilities i.e., very slow reactions with any photolytically generated O_3 or
21 NO_3 . In addition, when both cyclohexane (CH) and heptane (HEP) were used as the HC, the
22 gradient of the resulting relative rate plot ($\ln([HEP]_0/[HEP]_t)$ vs $\ln([CH]_0/[CH]_t)$, slope = 0.923
23 ± 0.010) was in good agreement the ratio of the literature rate coefficients for OH reactions



1 ($k_{\text{HEP}}/k_{\text{CH}} = 0.97 \pm 0.14$ at 298 K (Atkinson, 2003)). This confirms that OH was the dominant
2 route for chemical removal (see SI, Section S4).

3

4 **Table 3:** Temperature Dependence of $C_{\text{OH,obs}}$ Determined via the Hydrocarbon Decay Method

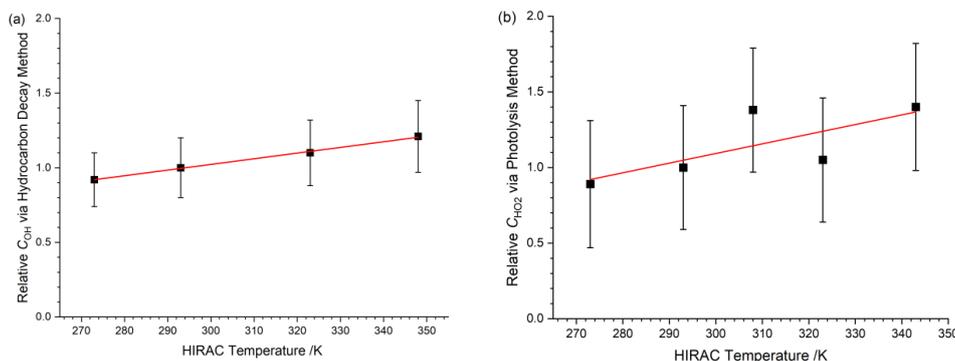
Temperature/K (± 0.5 K)	$C_{\text{OH,obs}}$ relative to the HC decay method at 293 K
273	$0.92 \pm 0.17^{\text{a}}$
293	1.00 ± 0.18
323	1.10 ± 0.20
348	1.21 ± 0.22

5

a – errors represent the total uncertainty in C_{OH} , see Table 4.

6

7 Displayed in Table 3 is the instrument sensitivity to OH radicals, $C_{\text{OH,obs}}$, measured between
8 273 and 348 K at 1000 mbar HIRAC chamber pressure using the hydrocarbon decay method
9 and Figure 7(a) shows these data as a function of the HIRAC temperature. An increase in C_{OH}
10 is observed. As with the experiments carried out in Section 4.1.2, the temperature of the OH
11 cell (T_{OH}) is very close to that of the gas being sampled at the inlet.



12 **Figure 7:** Temperature dependence of $C_{\text{HOx,obs}}$ relative to values at 293 K. (a) Relative $C_{\text{OH,obs}}$ from the
13 HC decay method. Slope = $(0.0038 \pm 0.0007) \text{ K}^{-1}$ (b) Relative $C_{\text{HO}_2,obs}$ from the HCHO photolysis
14 method. Slope = $(0.0064 \pm 0.0034) \text{ K}^{-1}$. Errors are 2σ .

15



1 **Table 4:** The systematic uncertainties in the various parameters that determine the accuracy in
 2 the OH and HO₂ calibration factors for the conventional and alternative calibration methods.

Conventional Flowtube		Hydrocarbon Decay		HCHO + <i>hν</i>	
Parameter	Uncertainty	Parameter	Uncertainty	Parameter	Uncertainty
$F_{184.9\text{ nm}} \times t$	20%	$k_{\text{OH} - \text{c-C}_6\text{H}_{12}}$	12% ^a	$k_{\text{HO}_2 + \text{HO}_2}$	38% ^e
[H ₂ O]	1%	k_{Dil}	2% ^b	S_{HO_2} initial	10% ^f
$\sigma_{\text{H}_2\text{O}}$	3%	[c-C ₆ H ₁₂]	5%	Laser power	6%
Laser power	6%	Gradient	10%	Online Position	4% ^c
Online Position	4% ^c	Laser power	6%		
		Online Position	4% ^c		
Error	22%^d	Error	18%^d	Error	40%^d

3 a – Error estimated from literature review. Five recent determinations (NIST Kinetics) of the 298 K rate coefficient
 4 give ~5% spread, added some additional uncertainty to account for temperature dependence.

5 b – Dilution determined from flow controller measurements.

6 c – The online position error is the approximate error in the maximum line intensity that is achieved when
 7 positioning the laser wavelength at the centre of the OH transition.

8 d – Total accuracy is taken as the sum in quadrature of the individual uncertainties.

9 e – Error in rate coefficient from the IUPAC evaluation.

10 f – Uncertainties in the fitting parameters.

11

12 Table 4 summarizes the errors associated with the alternative calibration methods. For the
 13 hydrocarbon decay method, the major uncertainties are in the rate coefficient of the
 14 hydrocarbon (~12% for OH + cyclohexane), determination of cyclohexane concentration (5%)
 15 and the gradient of the cyclohexane decay (10%). Other uncertainties are drifts in the laser
 16 power (~6%, determined from monitoring a photodiode) and wavelength position (~4%).

17 4.2.2 Calibration via HO₂ recombination kinetics

18 Displayed in Table 5 is the instrument sensitivity to HO₂, $C_{\text{HO}_2, \text{obs}}$, determined using the
 19 alternative calibration method between 273 and 343 K at 1000 mbar chamber pressure. Figure
 20 7(b) shows C_{HO_2} as a function of temperature relative to the instrument sensitivity at 293 K.
 21 Each measurement point represents the weighted average of at least five experimental data sets
 22 and the error bars represent the total uncertainty in the instrument sensitivity to $\pm 2\sigma$. As with
 23 the hydrocarbon decay method, the overall uncertainty is calculated as the sum in quadrature
 24 of fit precision to the decay and the systematic uncertainties listed in Table 4. The largest
 25 uncertainty was in the HO₂ self-reaction rate coefficient, dependent on the temperature used
 26 (38%). The slope of the linear fit to the C_{HO_2} values is $(0.0064 \pm 0.0034) \text{ K}^{-1}$. The absolute



1 agreement between the conventional and HCHO photolysis methods at 293 K is good with
2 $C_{\text{HO}_2, \text{conventional}} = (3.38 \pm 1.08) \times 10^{-8}$ counts cm^3 molecule $^{-1}$ mW^{-1} s^{-1} and $C_{\text{HO}_2, \text{HCHO photolysis}} =$
3 $(3.69 \pm 1.48) \times 10^{-8}$ counts cm^3 molecule $^{-1}$ mW^{-1} s^{-1} .

4

5 **Table 5:** Instrument sensitivity to HO₂, C_{HO₂}, determined using the HCHO photolysis method
6 over the 273 – 343 K external inlet temperature range.

$T_{\text{HIRAC}} / \text{K}^{\text{a}}$	$T_{\text{HO}_2} / \text{K}^{\text{a}}$	$C_{\text{HO}_2} (\text{rel. } 293 \text{ K})^{\text{b}}$
273	286	$0.89 \pm 0.36^{\text{c}}$
293	293	1.00 ± 0.40
308	297	1.38 ± 0.55
323	302	1.05 ± 0.42
343	308	1.40 ± 0.56

7

a – Error in temperature ± 0.5 K.

8

b – Values are relative to $C_{\text{HO}_2, 293 \text{ K}}$ of $(3.69 \pm 1.48) \times 10^{-8}$ counts cm^3
molecule $^{-1}$ mW^{-1} s^{-1} .

9

10

c – Each C_{HO_2} represents the weighted average of at least 5 individual
determinations. All experiments were conducted in 1000 mbar synthetic
air mixture.

11

12

13

14 4.3 Discussion of calibration methods and temperature dependence

15 4.3.1 Comparison of calibration methods

16 For room temperature, there is excellent agreement between the wand calibration and that for
17 OH based on hydrocarbon decays ($[\text{OH}]_{\text{wand}}:[\text{OH}]_{\text{HC}} = 1.00:0.97$) and HO₂ based on HCHO
18 photolysis and the kinetics of the HO₂ recombination reaction ($[\text{HO}_2]_{\text{wand}}:[\text{HO}_2]_{\text{kinetics}} =$
19 $1.00:1.09$). This is consistent with our earlier study (Winiberg et al. 2015) and has also been
20 confirmed in an intercomparison in the HIRAC chamber of the FAGE and NIR – CRDS (near
21 infrared cavity ring down spectroscopy) for HO₂ (Onel et al., 2017a) and CH₃O₂ (Onel et al.,
22 2020;Onel et al., 2017b).

23 For the hydrocarbon decay method there are several advantages compared to the
24 conventional wand calibration:

25 1) The [OH] is much closer to the conditions typically used in a chamber experiment (10^6 –
26 10^8 molecule cm^{-3}) whereas the lowest [OH] used in the wand calibration performed here is
27 typically 10^8 molecule cm^{-3} . Ideally one should calibrate over the same range as used in an
28 experiment.

29 2) This work has shown that there is a temperature dependence to the calibration factors.
30 Calibrating via the hydrocarbon decay method provides identical conditions (temperature



1 and pressure) to that of a real experiment in the HIRAC chamber. Temperature variation
2 can be simulated using the conventional wand device, but this introduces additional
3 uncertainty.

4 3) Conventional calibrations always take place with a significant water concentration, whereas
5 the water concentration in the hydrocarbon decay can be set at any value.

6 4) Calibration can be achieved without removing the FAGE apparatus from the HIRAC
7 chamber decreasing the time taken for calibration.

8 There are some disadvantages too. The calibration for OH is strongly dependent on the
9 accuracy of the HC rate coefficient. It is therefore important to use a hydrocarbon with a well-
10 characterised rate coefficient; realistically, even the best-characterised rate coefficient is likely
11 to have an uncertainty of 5 – 10%. Several HC can be used to give multiple independent
12 determinations of $[\text{OH}]_{\text{HC}}$, but this may increase the complexity of the analysis (e.g. coincident
13 mass spectral peaks, or overlapping FTIR spectra) and reduce the absolute concentration of
14 OH. Determination of $[\text{OH}]_{\text{HC}}$ also relies on an accurate and precise determination of the
15 concentration gradient and the $[\text{HC}]$ at that time. PTR measurements provide a near continuous
16 output, but if the $[\text{HC}]$ is measured using systems with lower sampling rates (e.g. FTIR or GC),
17 there can be a significant loss in precision of the gradient measurement.

18 Many of the advantages and disadvantages of the hydrocarbon decay method also apply to
19 HO_2 kinetics method for HO_2 calibration. The rate coefficient for HO_2 recombination has a
20 higher degree of uncertainty than many OH + hydrocarbon rate coefficients and is dependent
21 on the amount of water present. In the HIRAC chamber the humidity can be kept very low, but
22 that may not be possible in all chambers; in these circumstances the humidity would need to
23 be measured and the rate coefficient adjusted.

24 All calibration methods are subject to systematic uncertainties, the magnitude of which may
25 vary with conditions and therefore it is sensible to use a range of calibration methods.

26 4.3.2 Temperature dependence of C_{HO_x}

27 Table 6 compares the relative observed $C_{\text{HO}_x, \text{obs}}$ calibration factors for the three different
28 calibration methods. In all cases, a positive temperature dependence is observed, but for C_{HO_2} ,
29 only the alternative calibration method displays a statistically significant positive slope.

30 The C_{HO_x} factors can be broken down into temperature independent components (laser
31 power, solid angle of fluorescence collection, detector efficiency etc) and temperature



1 dependent terms. Four temperature dependent terms are relevant for C_{HOx} : the number density
2 of OH in the cell, the quenching efficiency of the fluorescence, the population of the probed
3 quantum state of OH and the transmission efficiency through the pinhole and inlet tube
4 (Creasey et al., 1997b). The first three terms can be calculated and hence accounted for. Any
5 residual temperature dependence of C_{HOx} should then relate to the transmission coefficient
6 through the apparatus.

7 *HOx number density* – The calculated [HOx] delivered to the FAGE apparatus depends on the
8 temperature of the HOx source, either the wand (operating at a fixed $T = 293$ K (Method 1) or
9 at T_{ext} (Method 2) or the HIRAC chamber. If the temperature of the HOx cells are different
10 from this temperature, then there will be a change in the number density of HOx, over and
11 above that caused by the pressure changes between the HOx source (1 bar) and the HOx cell
12 (typically 3.6 mbar). As the temperatures of the HOx cells have been measured it is
13 straightforward to correct for the different number density in the observation cells and the
14 resulting contribution to the temperature dependence of C_{HOx} as summarized in Tables S2-4.

15 *Quenching* – As shown in Faloon et al. (2004), the quenching parameter, $Q(T)$, is defined by
16 integrating the OH fluorescence decay over the defined sample time, or gated region. The
17 quenching rate coefficients for N_2 , O_2 and H_2O have been shown to be dependent on
18 temperature (Copeland and Crosley (1986) and (Bailey et al., 1997) for N_2 and O_2 , and Bailey
19 et al. (1999) for H_2O). The total decay intensity is defined by: $[\text{OH}(A^2\Sigma^+, v' = 0)]_0 \exp(-\Gamma t)$,
20 where Γ , the total OH lifetime, is defined approximately as the sum total of the radiative
21 lifetime for OH, γ , and the non-radiative lifetime due to quenching by the aforementioned bath
22 gases. Bailey et al. (1997) have calculated the impact of temperature on quenching accounting
23 for both the change in the quenching rate coefficients and the change in the number density of
24 the quenchers. Both the rate coefficient for quenching and the quencher number density
25 decrease with increasing temperature and hence quenching overall decreases with increasing
26 temperature (summarized in Table S5), enhancing the fluorescence quantum yield.

27 *Rotational population* – The rotational population of the probed state in the $Q_1(2)$ transition
28 will vary with temperature. The $Q_1(2)$ is the transition giving the largest signal between 280 –
29 340 K, the limits of T_{OH} explored in the study. Relative to ambient temperature, the rotational
30 population probed by $Q_1(2)$ increases by 3.5% at 280 K and decreases by 9.0% at the highest
31 T_{OH} of 340 K (Table S6).

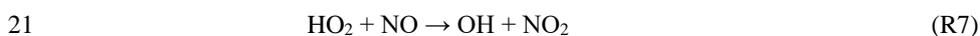


1 It is therefore possible to calculate the expected variation in C_{HO_x} for the different calibration
2 methods dependent on OH number density, quenching and rotational population; these can be
3 compared with the observed variation in C_{HO_x} summarized in Table 6. Full details on the
4 temperature dependences of the above components, which vary slightly with the calibration
5 method used are presented in Section S5 of the SI.

6 The difference between the observed C_{HO_x} and the calculated C_{HO_x} due to the above
7 parameters is attributed to increased transmission of HO_x through the pinhole and inlet tube
8 and is given in Table 6. The HO_x transmission, to the fluorescence region will depend on the
9 magnitude of heterogeneous loss of radicals to the walls of the FAGE inlet. The wall loss
10 process is a combination of diffusion and uptake at the wall and the actual temperature
11 dependence will depend on the radical, conditions and wall composition (Howard, 1979).

12 For the OH calibrations, there is an increase in OH transmission with temperature across all
13 three calibration methods, consistent with a decrease in OH loss to the walls which has been
14 observed in previous flow tube studies. OH wall loss rate in the inlet tube is usually
15 approximated to a first order process with a rate coefficient, k_w , and decreasing values of k_w
16 with temperature have been reported for flow tube studies of OH reactions (Howard, 1979), for
17 example Brown et al. (1990) report k_w decreasing from 35 s^{-1} at 227 K to 5 s^{-1} at room
18 temperature.

19 For HO₂ measurements, there is potentially a further temperature dependent component, the
20 conversion of HO₂ into OH via R7:



22 The rate coefficient for this reaction has a negative temperature dependence and the increased
23 number density of NO would further enhance the rate of reaction at lower temperatures. The
24 experiments reported in this work operated with excess NO such that the small variations in
25 the rate of reaction over the range of T_{HO_2} (284 – 313 K) will not alter the conversion of HO₂
26 to OH. However, if one were working at lower HO₂ conversions to mitigate against RO₂ to OH
27 conversion (Whalley et al. 2013), then variations in the conversion efficiency could change
28 C_{HO_2} as a function of temperature.

29 Temperature dependent HO₂ calibrations based on the conventional wand method give
30 significant scatter, but a positive increase in HO₂ transmission is observed for the alternative
31 calibration method based on HO₂ kinetics, the magnitude of which is similar to that for OH,
32 albeit with significant error bars. In general, HO₂ and RO₂ radicals exhibit lower wall loss rate



1

Table 6: Summary of the temperature dependence of C_{HO_x} with different calibration methods

Method	Observed slope of relative $C_{OH,obs}$ with temperature	Calculated contribution ^a	Difference (relative OH transmission)	Observed slope of relative $C_{HO_x,obs}$ with temperature	Calculated contribution ^a	Difference (relative HO ₂ transmission)
Heated FAGE inlet, ambient air at 293 K	$(0.0023 \pm 0.0007) \text{ K}^{-1}$	$(0.0001 \pm 0.0010) \text{ K}^{-1}$	$(0.0022 \pm 0.0012) \text{ K}^{-1}$	$(0.0005 \pm 0.0031) \text{ K}^{-1}$	$(0.0000 \pm 0.0010) \text{ K}^{-1}$	$(0.0000 \pm 0.0032) \text{ K}^{-1}$
Heated FAGE inlet, match air	$(0.0059 \pm 0.0015) \text{ K}^{-1}$	$(0.0029 \pm 0.0010) \text{ K}^{-1}$	$(0.0030 \pm 0.0018) \text{ K}^{-1}$	$(0.014 \pm 0.013) \text{ K}^{-1}$	$(0.0033 \pm 0.0010) \text{ K}^{-1}$	$(0.0029 \pm 0.0016) \text{ K}^{-1}$
Alternative kinetics based methods	$(0.0038 \pm 0.0007) \text{ K}^{-1}$	$(0.0027 \pm 0.0010) \text{ K}^{-1}$	$(0.0011 \pm 0.0012) \text{ K}^{-1}$	$(0.0064 \pm 0.0034) \text{ K}^{-1}$	$(0.0032 \pm 0.0010) \text{ K}^{-1}$	$(0.0032 \pm 0.0035) \text{ K}^{-1}$

^a - Contribution from the change in number density, quenching and relative rotation population in the probed state.



1 coefficients, but in our FAGE system, HO₂ molecules have to travel further to reach the
2 titration region where reaction occurs with NO to convert HO₂ to OH. Therefore, there is also
3 potential for OH loss from the titration point to the second detection cell.

4 4.3.3 Comparison with other instruments

5 The temperature dependence of the calibration factors will be strongly dependent on the design
6 of the FAGE apparatus. Our instrument was designed with a long (~ 1 m) inlet such that we
7 can probe across the diameter of the HIRAC chamber to check for radial distributions of
8 radicals (Malkin et al., 2010). Hence, we would expect HO_x transmission to play a significant
9 role in the temperature dependence of the calibration factor which is observed. Any similarly
10 designed instrument would have a contribution from HO_x transmission, the magnitude of
11 which would depend on inlet length/residence time and construction material. Heating the inlet
12 should reduce transmission losses. The aircraft based instrument, from the Juelich research
13 group, uses a PID controlled heater to maintain their FAGE inlet at ~300 K, mitigating any
14 possible temperature effects. They have an in-field calibration system, also, which has shown
15 negligible deviation from the expected behaviour at 300 K, based on the sample gas altitude
16 temperature (Marno et al., 2020).

17 Regelin et al. (2013) have reported a similar temperature dependence study of C_{OH} and C_{HO₂}
18 as the current flowtube study with the aircraft based HORUS instrument. Cooling lines were
19 wound around the inlet to simulate the measured temperature profile and ambient air was
20 sampled from a calibration flow tube. In contrast to our slight increase in C_{OH} with temperature
21 in the flow tube experiment, Regelin et al. observed a slight negative dependence of the OH
22 signal. Regelin et al. report that their calculations have shown that the sample forms a jet
23 between the pinhole and the OH cell such that there is insignificant interaction with the walls
24 and therefore transmission will not be a problem.

25 In contrast, a significant decrease in HO₂ signal, S_{HO₂}, (50%) was observed as the
26 temperature was decreased from ~295 to ~262 K (slope = 0.017 K⁻¹ normalised to S_{HO₂,293 K}),
27 i.e. the same qualitative behaviour as we observed, approximately a factor two greater than
28 measured in our work, based on HO₂ recombination kinetics. Beyond the OH cell in the
29 HORUS experiment, the jet breaks up and Regelin et al. suggest that temperature dependent
30 wall losses are responsible for the change in S_{HO₂}. Quantitative comparisons cannot be made
31 due to the differences in construction. The observed temperature dependence of C_{OH} and C_{HO₂}



1 for the HORUS and HIRAC experiments emphasise the important of performing calibrations
2 for each instrument under conditions as close as possible to those used in measurements.

3 **5 Conclusions**

4 The effect of temperature of the incoming sample on the sensitivity of the HIRAC FAGE
5 instrument to OH and HO₂ has been investigated between 266 and 348 K using a combination
6 of conventional water vapour photolysis/flow tube method (Faloona et al.) and alternative
7 calibration methods based on hydrocarbon decays for OH and the HO₂ self-reaction for HO₂.
8 In all cases, a positive increase in sensitivity was observed (Table 6) although with large error
9 bars in the case of HO₂ with conventional calibration.

10 The temperature dependence of the calibration factor can be broken down to four
11 components. Variations in three parameters: number density, quenching and rotational
12 population of the probed level, can be accounted for if the temperature and pressure in the LIF
13 cells are monitored. The difference between the observed and calculated temperature
14 dependence for the above parameters, has been attributed to HO_x transmission from the pinhole
15 to the relevant detection chamber.

16 The temperature dependence of C_{HO_x} will depend on the design and construction materials
17 of the FAGE apparatus. It is therefore difficult to utilise the results of this study to predict
18 results in other systems. However, for any systems with significant sampling inlet residence
19 times, such as the HIRAC FAGE described in this work, increased HO_x transmission with
20 increasing temperature should be expected. Therefore, maintaining the inlet at a relatively high
21 temperature should improve sensitivity in low temperature applications.

22 The *in situ* calibration methods (hydrocarbon decay and HO₂ recombination kinetics) offer
23 important advantages in that the FAGE apparatus is calibrated under the physical conditions
24 and [HO_x] that more closely correspond to real experiments. All calibration methods are
25 subject to significant uncertainty, however, the origins of these uncertainties are different and
26 hence good agreement between calibration methods should provide confidence that significant
27 systematic errors are not present.

28

29 **Supplementary Information**

30 Supplementary information; HIRAC temperature profiles, calibrations, further discussions on
31 calibration uncertainties, relative rate plots to confirm OH as the key species in hydrocarbon



1 removal and further discussion on the temperature dependence of the FAGE signal can be
2 found at *****.

3

4 **Author Contributions**

5 FAFW and IGB led the initial work on OH temperature dependence performing all experiments
6 with external calibration, WJW, THS and GB completed the experiments with HC decays in
7 HIRAC, CAB and IGB completed experiments on HO₂ temperature dependence. PWS, DEH
8 and DS planned and supervised the experiments and wrote the manuscript with contributions
9 from all co-authors.

10

11 **Competing Interests**

12 DEH is a member of the editorial board of AMT, otherwise the authors declare that they have
13 no conflict of interest.

14

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