A comprehensive evaluation of enhanced temperature influence on gas and aerosol chemistry in the lamp-enclosed oxidation flow reactor (OFR) system

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Abstract. Oxidation flow reactors (OFRs) have been extensively utilized to examine the formation of secondary organic aerosol (SOA). However, the UV lamps typically employed to initiate the photochemistry in OFRs can result in **an** elevated reactor temperature with their implications not thoroughly evaluated. In this study, we conducted a comprehensive

35 investigation into the temperature distribution within an Aerodyne Potential Aerosol Mass OFR (PAM-OFR), and<u>then</u> examined the subsequent effects on flow and chemistry due to lamp heating. A lamp-induced temperature increase was observed, which was a function of lamp driving voltage, number of lamps, lamp types, OFR residence time, and positions within the PAM-OFR. Under typical PAM-OFR operational conditions (e.g., < 5 days of equivalent atmospheric OH exposure

under low-NOx conditions), the temperature increase typically ranged from 1-5 °C. Under extreme (but less frequently encountered) conditions, the heating could reach up to 15 °C. The influenceinfluences of the increased temperature over ambient conditions on the flow distribution, gas, and condensed phase chemistry within PAM-OFR waswere evaluated. Our findings indicate that the increase in temperature altered the flow field, resulting in a diminished tail on the residence time distribution and corresponding oxidant exposure due to faster recirculation. According to simulation results from a radical chemistry box model, the variation of absolute oxidant concentration within PAM-OFR due to temperature increase was

- 45 minimal (<5%). The temperature influences on existing and newly formed-seed_organic aerosol (OA) and newly formed secondary OA were also investigated, suggesting that an increase in temperature can impact the yield, size, and oxidation levels of representative biogenic and anthropogenic SOA types. Recommendations for temperature-dependent SOA yield corrections and PAM-OFR operating protocols that mitigate lamp-induced temperature enhancement and fluctuations are presented. We recommend blowing air around the reactor's exterior with fans during PAM-OFR experiments to minimize the
- 50 temperature increase within PAM-OFR. Temperature increases are substantially lower for OFRs utilizing less powerful lamps compared to the Aerodyne version.

1 Introduction

Secondary organic aerosol (SOA) constitutes 60-95% of organic aerosol (OA) and 10-75% of submicron particles (Jimenez et al., 2009), thus, strongly impacting air quality (Huang et al., 2014), climate (Myhre, 2013; Poschl, 2005) and

- human health (Nel, 2005; Feng et al., 2016; Nault et al., 2021). Elucidating the formation mechanism of SOA is crucial for clarifying its environmental impact (Ziemann and Atkinson, 2012; Hallquist et al., 2009; Klyta and Czaplicka, 2020). To investigate SOA formation, chambers (Hildebrandt et al., 2009; Cocker et al., 2001; Paulsen et al., 2005; Wang et al., 2014; Carter et al., 2005; Martin-Reviejo and Wirtz, 2005; Rollins et al., 2009; White et al., 2018; Zong et al., 2023) and flow tubes (Cooper and Abbatt, 1996; George et al., 2007; Hanson and Lovejoy, 1995; Robbins and Cadle, 2002; Katrib et al., 2005;
 Knopf et al., 2005; Ezell et al., 2010) have been commonly used in the laboratory for investigating secondary formation in the early periods of past several decades. In the last decade, due to rapid advancements in online measurement techniques, various types of oxidation flow reactors (OFRs), which are portable and suitable for field studies to explore SOA formation under ambient conditions, have been developed and widely deployed (Kang et al., 2007; Watne et al., 2018; George et al., 2007; Peng and Jimenez, 2020; Lambe et al., 2011b; Shah et al., 2020; Saha et al., 2018; Xu and Collins, 2021; Chu et al., 2016;
- 65 Simonen et al., 2017; Li et al., 2019; Keller et al., 2022 and references therein).

The potential aerosol mass (PAM) reactors, initially distributed by Prof. Bill Brune (the Penn State PAM) and later modified and commercialized by Aerodyne Research Inc., are the most extensively utilized OFRs for investigating SOA formation and evolution in ambient environments (Peng and Jimenez, 2020). The PAM reactor was first proposed and designed by Kang et al. (2007), leading to successful deployment across various field studies including forests (Hu et al., 2016; Palm et

70 al., 2016; Palm et al., 2017; Palm et al., 2018; Sumlin et al., 2021), urban areas (Ortega et al., 2016; Liu et al., 2018; Chen et

al., 2021; Hu et al., 2022; Sbai et al., 2021; Park and Kim, 2023; Xu et al., 2022; Park et al., 2019), rural sites (Ahlberg et al., 2019; Hodshire et al., 2018; Hu et al., 2016), tunnel/roadside studies (Liu et al., 2019; Liao et al., 2021; Tkacik et al., 2014; Saha et al., 2018), as well as numerous laboratory studies (Kang et al., 2007; Lambe et al., 2011b; Bahreini et al., 2012; Bruns et al., 2015; Sengupta et al., 2018; Kramer et al., 2019; Cheng et al., 2021; Lei et al., 2022; Srivastava et al., 2023 and references

therein). In the PAM, high concentrations of the OH radicals, which is the major oxidant for SOA formation in ambient air, can be generated quickly by initiating the photochemistry of O_3 and H_2O with UV lamps (185/254 nm) mounted inside of a flow tube (Lambe et al., 2011b; Li et al., 2015; Peng et al., 2015).

Previous research utilizing the Penn State PAM reported a temperature elevation of 2 °C. However, several recent studies using the PAM have demonstrated that the UV lamps can augment the internal temperature of that reactor by 0-15 °C (up

- 80 values are under extremely high voltage conditions) above ambient temperature (Lambe et al., 2011a; Chen et al., 2013; Tkacik et al., 2014; Lambe et al., 2019; Charnawskas et al., 2017). Despite this, a comprehensive investigation of the lamp heating effect on the temperature distribution within PAM-OFR and an elucidation of its influences on the flow distribution within PAM-OFR remain unreported. The temperature is a key parameter for gas diffusion and gas/aerosol partitioning (Pankow, 1994; Donahue et al., 2006). The increase in the temperature gradient caused by lamp heating inside an OFR can result in the
- 85 formation or deepening of recirculating flow, leading to a shorter residence time and a broader residence time distribution (Huang et al., 2017; Lambe et al., 2019). Numerous chamber studies have determined that elevated temperatures can substantially reduce the SOA yield (Gao et al., 2022; Lamkaddam et al., 2017; Boyd et al., 2017; Price et al., 2016; Clark et al., 2016; Tillmann et al., 2010; Pathak et al., 2007) and influence SOA chemical composition (Jensen et al., 2021; Gao et al., 2022; Simon et al., 2020; Li et al., 2020a; Kristensen et al., 2020; Quéléver et al., 2019; Denjean et al., 2015). Consequently,
- 90 the increase of temperature within PAM-OFR, which could lead to extra uncertainty for SOA simulations and studies, should be further assessed and clarified.

In this study, we systemically investigate the effects of lamp-induced heating on PAM-OFR measurements. Based on computational fluid dynamics (CFD) simulation, we show how the temperature affects the flow and average OH exposure within the PAM-OFR. Two box models were applied to illustrate the influence of increased temperature on the chemistry of

95 gas-phase reactions and SOA formation within the PAM-OFR. The model results can serve as a preliminary reference for correcting the related experimental results due to increased temperature. Finally, we suggest utilizing fans to cool the PAM-OFR and implementing an online sampling strategy that alternates between high and low driving voltages at varied lamp settings to reduce the uncertainty caused by the varied heating effect.

2 Methods

100 **2.1 Oxidation flow reactor (OFR)**

The PAM-OFR (Aerodyne Research, Inc., abbreviated as ARI) used in this study is a 13 L horizontal aluminum cylindrical chamber (46 cm long \times 22 cm ID). Four low-pressure germicidal mercury (Hg) lamps are isolated from the sample

flow by type 214 quartz tubes (Fig. S1). The Hg UV fluorescent lamps used in this study are commercial products (GPH436T5VH/4 or GPH436T5L/4, Light Sources, Inc.), which are the default light bulbs selected by ARI for the OFR (Fig.

- 105 S2). Additionally, the temperature within an OFR with the Penn State low-pressure Hg UV lamps (model no. 82-9304-03, BHK Inc.), which are also widely utilized in PAM-OFR (Khalaj et al., 2021; Xu and Collins, 2021; Lambe et al., 2011b; Siemens et al., 2022; Hu et al., 2016; Ortega et al., 2013; Link et al., 2016; Palm et al., 2016; Kang et al., 2018; Mitroo et al., 2018; Kang et al., 2007), are measured as well. For the Light Sources lamps, the light intensity of each lamp was adjusted via the AC voltage input to the lamp ballast, controlled by a computer with settings ranging from 0 V (minimum) to 10 V
- 110 (maximum, full AC output). For BHK lamps, the maximum setting voltage is 5 V (full AC output). At maximum voltage, the optimal estimation of supply power is 8.9 W (see sect. S1 for details) to each lamp for the Light Source lamp and 6.3 W for the BHK lamp. When the lamps are turned on, a pure nitrogen purge gas is introduced into the lamp sleeve at a flow rate of 0.2-0.3 L min⁻¹. The lamp sleeve is defined as the space between the lamps and the quartz tube wall to prevent oxidation products from accumulating on the lamp surface and to slightly cool the UV lamps (minor effect, as discussed below). On the
- 115 inner surface of the front plate of the PAM-OFR, a hexagon nut is attached to the center inlet. The side of the nut is drilled with holes to promote axial mixing of the sample flow and is hereafter referred to as an inlet diffuser (Fig. S1c) (Mitroo et al., 2018). Two mesh screens are installed inside the front and back plates to block debris and insects and to improve air flow uniformity (helping to break up eddies from outside) (Fig. S1b). A detailed schematic plot of the PAM-OFR used in this study is shown in Fig. 1.

120 2.2 Measurement of OFR temperature

The temperature distribution inside the PAM-OFR was measured with multiple temperature sensors. The types and models of temperature sensors used are listed in Table S1. To evaluate the accuracy of temperatures measured by different temperature sensors, a comparative experiment was conducted under different ambient environments. We observed a good agreement (within 2 °C) among the different temperature sensors, supporting the robustness of the temperatures measured in this study (Fig. S3). Detailed information on experimental settings for temperature measurements inside the PAM-OFR is summarized in Fig. 1 and Table S2. Briefly, we measured the air temperature inside PAM-OFR at varied positions (vertical and horizontal directions, as well as different depths from inlet (Fig. 1b)) under different lamp configurations (e.g., number of lamps, types of lamps, intensity of lamps) and flow rates. For this purpose, an external temperature sensor was placed directly inside the PAM-OFR and was moved manually from outside. The values reported in this study were obtained after the internal

- 130 temperature of the PAM-OFR stabilized for 20 min after switching the PAM-OFR configuration. During measurement, the inlet diffuser and the mesh screen on the front plate or backplate of the PAM-OFR needed to be removed to extend the thermocouple inside the PAM-OFR. We tested whether removing the mesh screen would affect the temperature field inside the PAM-OFR and found negligible effects as shown in Fig. S4 (removed the back plate mesh screen) vs. Fig. 5 (removed the inlet diffuser and front plate mesh screen). Additionally, we covered the sensor with shielding paper to prevent potential
- 135 influences of optical radiation from UV lamps on temperature detection during this process. In addition to the internal

temperature, the temperature of the inner/external surface, and the temperature in the gas output of the PAM-OFR were also measured for comparison. A temperature and relative humidity (RH) sensor (referred to as a "primary T/RH sensor", Sensirion SHT21, Sensirion AG) was mounted on the back plate at the factory. Consequently, the default primary T/RH sensor was utilized for temperature measurement in all the experiments. In addition to the temperature measurement in OFR, we measured

the residence time distribution (RTD) at different voltages to explore the effect of temperature on RTD. Specifically, we first turned on the lights to make the temperature stable. Then, a 2 s pulse of 50 ppm SO₂ was injected into a 5 L min⁻¹ carrier gas (N₂) with RH <10%. N₂ was selected as the carrier gas to prevent the reaction between SO₂ and the generated oxidant when UV lamps were turned on. We measured the RTD with lamp driving voltage set at 0 V, 5 V and 10 V. Note that we only used the outlet for aerosol line for sampling (5 L min⁻¹) during the RTD measurement for better comparison with simulation results
in Sec. 2.3. Most of the temperature experiments were done with sampling exhaust line from the ring flow.

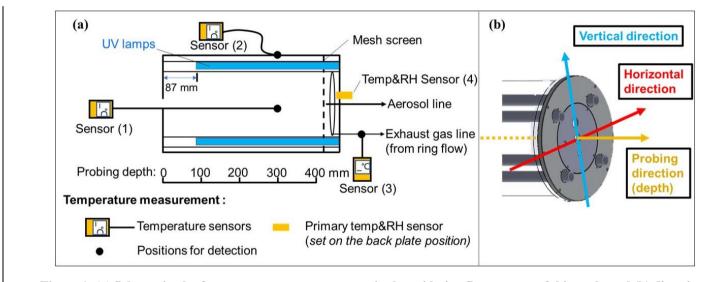


Figure 1: (a) Schematic plot for temperature measurement in the oxidation flow reactor of this study and (b) directions for temperature measurement. The center inlet, nut, and mesh screen near the front plate were removed when the temperature sensor was probed in the front direction. The information of different temperature sensors used can be found in Table S1.

2.3 Model simulations on temperature distribution and flow field inside OFR

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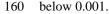
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Computational Fluid Dynamics (CFD) simulations were performed using the ANSYS Fluent software (Version 14.5) in three dimensions to simulate the temperature distribution and flow field within the PAM-OFR. ANSYS has been used to simulate the flow field within flow reactors in past studies (Li et al., 2019; Ihalainen et al., 2019). The temperature distribution and flow field under unheated and heated conditions were both simulated with the CFD model. The simulated experimental condition was 5 L min⁻¹ of air as the carrier gas and 0.3 L min⁻¹ of SO₂ which was injected for 2 s as the tracer gas. Note that

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during modeling, the airflow within OFR was only sampled through output for the aerosol line as considering the ring flow

manifold for gas phase sampling would significantly increase the complexity for modeling. The convergence of this model was defined when the residuals of physical quantities (e.g., pressure, temperature, velocity, density, and viscosity, etc.) were



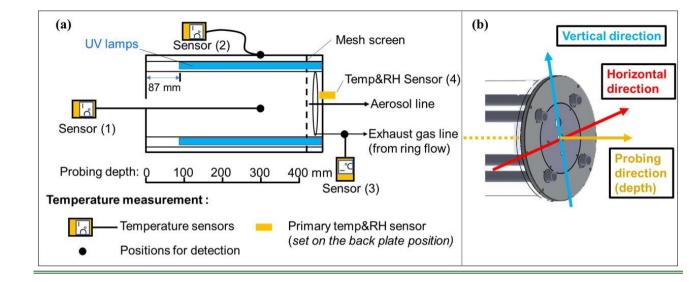


Figure 1: (a) Schematic plot for temperature measurement in the oxidation flow reactor of this study and (b) directions for temperature measurement. The center inlet, nut, and mesh screen near the front plate were removed when the temperature sensor was probed in the front direction. The information of different temperature sensors used can be found in Table S1.

For the unheated condition, the more advanced "realizable k-epsilon turbulence model" was employed (Shih et al., 1995). The simulation was solved by using the pressure-based SIMPLEC algorithm, a prevalent method in CFD models for simulating incompressible flow problems (Patankar and Spalding, 1972). For the heated condition, the thermal boundary was set to a series of fixed temperatures, derived from directly measurements in the PAM-OFR. When the driving voltages of all the PAM-OFR lamps were set to be 5 V, the model settings applied were 55 °C for the quartz UV lamp sleeve surface, 35 °C for the 170 inner wall surface, and 26 °C for the carrier gas. When the driving voltages of all the PAM-OFR lamps were set to 10 V, these values were adjusted to 62 °C, 40.5 °C, and 23 °C, respectively. The lower carrier gas temperature under 10 V conditions compared to 5V was attributed to the variations in room temperatures across different real experiments. The viscosity and thermal conductivity of the mixing gas were calculated using the mass-weighted-mixing-law (Ni et al., 2010). The Least Squares Cell-Based method and the species transport model were used for the solution (Ghia et al., 1982).

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2.4 KinSim kinetic model for gas-phase reactions

The influence of temperature on gas-phase reactions was modeled using a box model (KinSim 4.14 in Igor Pro. 6.37), incorporating the OFR radical mechanisms as utilized by Li et al. (2015), Peng et al. (2015) and Peng et al. (2019). All gasphase reactions were derived from the JPL chemical kinetic data evaluation, which incorporates temperature as a variable for

- 180 reaction rate calculation (Burkholder et al., 2019). In the model, we assumed a mixing volume of 800 ppb SO₂ injection into the PAM-OFR with a constant 2.2% water vapor mixing ratio (RH=70% at 25 °C), based on calibration experiment settings. This corresponds to an OH reactivity (OHR) of the incoming air of 20 s⁻¹. The simulated SO₂ output concentration in the model was weighted by the measured residence time distribution (RTD) at a flow rate of 5 L min⁻¹ (~700 s). Good agreement between the modeled SO₂ decay based on the KinSim model and the measured SO₂ results has been demonstrated in Hu et al. (2022).
- The OFR185 mode mechanism, which involves the generation of O₃ and OH radicals via the photolysis of O₂ and H₂O within OFR, was incorporated into the model. Note that the photon flux ratio between 185 and 254 nm, derived from lamps manufactured by Light Source Inc., remains constant regardless of their intensity (Rowe et al., 2020). However, these ratios exhibit variation with intensity for the BHK lamps (Li et al., 2015). In the model, the photon flux ratio of 185/254 nm was set to be constant (5%). Results for 25 °C to 40 °C (binned with 5 °C) were modeled, which covers the typical temperature range within the PAM-OFR under most lamp settings. These simulations were conducted using residence time distribution (RTD)
- obtained under unheated conditions in the PAM-OFR (25 °C). Since the RTD inside OFR can also be influenced by temperature (Lambe et al., 2019), we also showed the model results with measured RTD at 40 °C.

2.5 SOM model for SOA formation

The Statistical Oxidation Model (SOM) is a kinetic, process-level model designed to simulate the SOA formation. This model incorporates gas-particle partitioning, multi-generational oxidation (fragmentation and functionalization), and autoxidation for highly oxygenated molecules (HOMs) (Cappa and Wilson, 2012; Eluri et al., 2018; He et al., 2021; He et al., 2022). The SOM model has been shown to successfully capture the evolution of SOA formation and oxidation in multiple laboratory and field studies (Cappa and Wilson, 2012; Jathar et al., 2015; Eluri et al., 2018; Akherati et al., 2020; He et al., 2021; He et al., 2022). In the SOM model, the oxidation of a VOC precursor is tracked by its evolution within a carbon–oxygen grid. The volatilities and reactivity (k_{OH}) of organic species in each grid are determined based on their carbon (N_c) and oxygen numbers (N_o) (Cappa and Wilson, 2012; Jathar et al., 2015; Eluri et al., 2018). In total, six adjustable parameters are used to determine the reaction probabilities and volatility of the grid species. Four parameters (p1-p4, Table S3) indicate the number of oxygens added per functionalization reaction, and two other parameters describe the probability of fragmentation (m_{frag} , Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al., Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al., Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al., Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al., Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al., Table S3) and the reduction in vapor pressure (ΔLVP , Table S3) per oxygen atom added to the carbon backbone (Jathar et al.,

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205 2016; Akherati et al., 2019).
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In this study, we employed the SOM model in conjunction with the TwO-Moment Aerosol Sectional model (TOMAS) (Adams and Seinfeld, 2002; Pierce et al., 2007) to simulate the temperature influences on the yield, oxidation state, and size distributions of newly formed SOA within the PAM-OFR. In the model, the temperature dependence is determined by the Clausius–Clapeyron Equation:

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$$P_i^* = P_{i,ref}^* \times e^{(\frac{H_i^{vap}}{R} \times 10^3 \times (\frac{1}{298} - \frac{1}{T}))}$$
(1)

where *R* (8.314 J mol⁻¹ K⁻¹) is the ideal gas constant, P_i^* and $P_{i,ref}^*$ (Pa) are the saturation pressure of species *i* at target temperature and reference temperature (298 K), respectively. The $P_{i,ref}^*$ can be calculated based on the equation (2):

$$P_{i,ref}^{*} = \frac{C_{i,ref}^{*} \times R \times 298}{MW_{org,i} \times 10^{6}}$$
(2)

where $MW_{org,i}$ (g mole⁻¹) is the molecular weight of organic species *i* and $C_{i,ref}^*$ (µg m⁻³) is the saturation concentration 215 at 298 K. The $MW_{org,i}$ and $C_{i,ref}^*$ are calculated based on the number of C (N_C) and O (N_O) and ΔLVP of species *i* (Eluri et al., 2018). The H_i^{vap} (kJ mol⁻¹) is the evaporation enthalpy of species *i*, calculated using the equation (3) (Epstein et al., 2010):

$$H_i^{vap} = -11 \times \log C_{i,ref}^* + 131 \tag{3}$$

In addition, constant $H_i^{\nu a p}$ of 80, 100, 120 and 150 kJ mol⁻¹, derived from analysis of field data, was also tested in the model (Saha et al., 2017; Cappa and Jimenez, 2010; Louvaris et al., 2017).

- In this study, SOA formation from four typical VOC precursors including dodecane, α -pinene, toluene, and m-xylene was modeled under different OA <u>seed</u> concentrations (1-80 µg m⁻³) and NOx conditions (low NOx vs high NOx). We did not consider the evaporation and reaction of OA seed during the model simulation. Five temperature stages ranging from 20-40 °C were simulated. Similar to the gas-phase simulations, results were also calculated based on the measured RTD obtained at both ~25 °C and ~40 °C (for the modeled yields under 40 °C), with a total model time of 700 s. Additionally, we also considered
- 225 the highly oxygenated organic molecules (HOMs) in this model that contribute to new particle formation (He et al., 2021; Bianchi et al., 2019). The HOM yields and other detailed information for input parameters can be found in Table S3. These parameters were obtained by fitting the simulated results to the measured chamber results under high and low NOx conditions, respectively (Eluri et al., 2018; Cappa et al., 2016). Thus, the exact NO concentration was not considered in the SOM model during the simulation

230 3 Results and discussions

3.1 Heating effect inside OFR

To characterize the temperature distribution within the PAM-OFR, we measured the temperature as a function of lamp driving voltage, number of lamps, flow rate, lamp types, and different spatial positions.

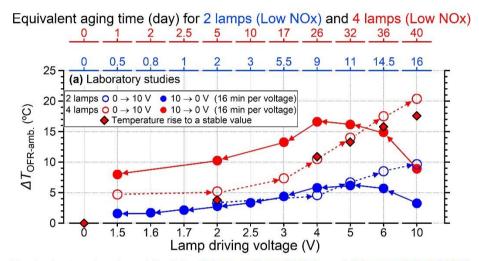
3.1.1 Enhanced temperature vs lamp driving voltage (OH exposures) and flow rate

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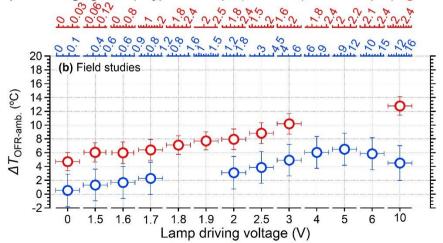
In general, a systematic temperature increase was observed within the PAM-OFR with Light Source lamps. As shown in Fig. 2a, the temperature within the PAM-OFR increased as a function of lamp driving voltage and, hence, OH exposures. When the driving voltage of the 2-lamp setup was changed in increasing fashion (0 V to 3 V, Light Source lamp), the temperature increase within the PAM-OFR was generally less than 5 °C. 3 V was approximately equivalent to a photochemical

aging time of around 5 days (assuming the water mixing ratio was 1.88%, RH=60%, external OH reactivity=30 s⁻¹). For a

- 240 higher voltage range (3 V to 10 V, which corresponds to a photochemical aging time from 5 days to two weeks), the temperature inside the PAM-OFR increased by 10 °C. Note that the relationship between the lamp driving voltage and OH exposure varied depending on the number and type of UV lamps used, as well as the operation mode of the PAM-OFR (Fig. S5). When four lamps were turned on and the lamp driving voltage was increased from 2 to 10 V, the temperature inside the PAM-OFR increase inside of S-20 °C for the laboratory tests (Fig. 2a and 3a). These results indicated that the temperature increase inside of
- 245 the PAM-OFR was mainly due to the heat from the lamps, which was further confirmed by Fig. 3b, which showed that the temperature increase inside the PAM-OFR decreased as a function of the flow rate from 3 L min⁻¹ to 7 L min⁻¹ (Fig. 3b). The anti-correlation between the temperature elevation and flow rate was mainly attributed to the larger gas mass provided by the increased air flow, so that a lower temperature increase was required to transfer excess heat from the lamps.



Equivalent aging time (day) for 2 lamps (Low NOx) and 4 lamps (High NOx)



- 250 Figure 2: (a) Temperature elevation inside the PAM-OFR (measured temperature in OFR minus ambient temperature) as a function of the lamp driving voltage using two lamps and four lamps in the laboratory studies. Note that without specific notification, all the temperature measurement results shown in the main text are obtained with lamps produced by Light Source Inc. The relationship between lamp driving voltage and OH exposures for using two lamps and four lamps can be found in Fig. S5. The OH exposures were calculated based on the empirical parameters in Hu et al. (2022)
- assuming a mixing water ratio of 1.88% and an external OH reactivity of 30 s⁻¹. The equivalent aging days (top axis) were estimated by assuming ambient OH concentration of 1.5x10⁶ molecules cm⁻³ (Mao et al., 2009). The lamp types applied here were uncovered for field studies with four lamps in Fig. 2b and 80% covered for other conditions. The temperatures were measured at the centerline with a 300 mm probing. The flow rate was 5 L min⁻¹. (b) Temperature elevation inside the PAM-OFR as a function of light settings in the field studies. Two lamps were applied for low NOx conditions, while four lamps were used for high NOx conditions. The high NOx reaction regimes were achieved by the
- introduction of extra N₂O as illustrated in Peng et al. (2018) and Lambe et al. (2017).

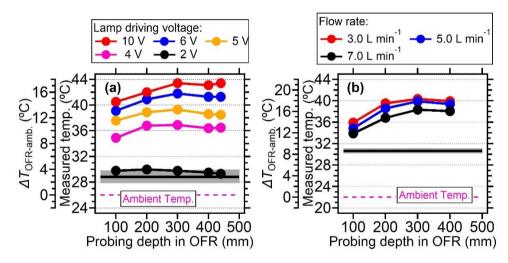


Figure 3: (a) The measured temperature and the temperature elevation (measured temperature in OFR minus ambient temperature) under different lamp driving voltage and (b) at different flow rates for Light Source lamp. The
temperature was measured in the centerline at different probing positions. Black lines and gray shadows represented the temperature measured by the primary T/RH sensor. For panel (a) four lamps were all turned on during measurement. The flow rate was 5 L min⁻¹; For panel (b), four lamps were set in 5 V.

When the lamp driving voltage was set in a monotonically decreasing fashion (e.g., from 10 V to 0 V), the maximum temperature increase did not occur at the highest voltage setting of lamps (10 V), but in the range of 4-6 V, as shown in Fig.
270 2a and b. This discrepancy was primarily attributed to the fact that the lamps were initiated at 10 V under cooler conditions (e.g., room temperatures or lower voltage settings), while the OFR reactor had a thermal mass that required time to accumulate or dissipate heat. As depicted in Fig. 4, the entire system necessitated over 100 minutes to achieve a thermal steady state.

However, a much shorter durations (15-24 minutes) were usually applied in the laboratory and field studies when voltages were systematically varied (Link et al., 2016; Murschell and Farmer, 2018; Hu et al., 2016; Ortega et al., 2016; Palm et al.,

- 275 2016; Palm et al., 2018; Saha et al., 2018; Shah et al., 2020; Hu et al., 2022). These brief constant lamp power periods led to diminished temperature variation between different power settings, as well as inconsistencies between maximum temperature peak with maximum power setting. To elucidate, the time series of measured temperature when the lamp driving voltage was set under a representative lamp voltage cycle (decreasing fashion: 10-6-5-4-2-0 V) were presented in Fig. 5. Two scenarios with two and four lamps being turned on were both shown. The reason for initiating the lamp voltage at 10 V in this typical
- 280 setting was to optimize the efficiency of filament ignition in UV fluorescent lamps. Even though the thermal steady state was not achieved at each voltage, temperature increases of 2-8 °C for two lamps and 6-16 °C for four lamps were observed. In general, the temperature increase inside the PAM-OFR is a function of the voltage profile and the time spent at each voltage. The maximum SOA formation was typically observed after 1-2 days of equivalent age (Ortega et al., 2016; Palm et al., 2016; Hu et al., 2022). In most cases, the temperature increase inside the PAM-OFR was generally less than 5 °C below 5-7 days of
- 285 equivalent atmospheric OH exposure in laboratory and field studies (Figs. 2a and 2b). The main exceptions were specific OFR modes that incorporate N₂O or isopropyl nitrite precursors to establish high-NOx conditions (Lambe et al., 2017; Lambe et al., 2019). In these cases, four lamps were beneficial to compensate for the absorption of 185 nm radiation by N₂O (Peng et al., 2018) that inhibited HO_x production, or the relatively weak absorption of UVA radiation by isopropyl nitrite, respectively. This also results in more uniform radiation within the OFR as when only two lamps are used, the area with another two lamps
- 290 off would be darker due to the absorption of radiation.

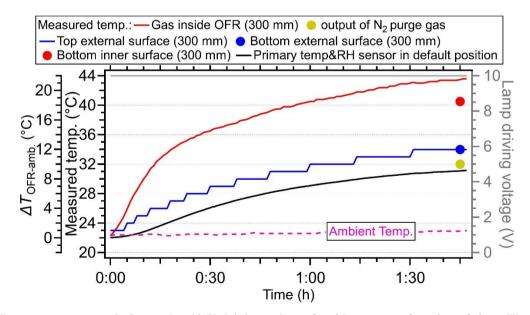


Figure 4: The temperature variation under 10 V driving voltage for 4 lamps as a function of time. The starting time was defined as the moment when the lamps were turned on. The temperature sensors were set at a depth of 300 mm in

the central line to measure the temperature inside the PAM-OFR. The flow rate was 5 L min⁻¹. The temperature of the

295 external surface of OFR was also measured at the top and bottom positions. The temperature measured by the default OFR sensor installed on the backplate was also shown in the black line. The purple dotted lines represent the ambient temperature.

3.1.2 Temperature increase vs lamp types.

- The temperature increase as a function of lamp types was also investigated. The four types of lamps tested were shown 300 in Fig. S2. Fig. S6 showed similar temperature distribution inside the PAM-OFR with 80% covered or uncovered lamps, as well as with only 254 nm or 254/185 nm lamps. These results indicated that the heat transfer from the hot guartz sleeve (heated by the lamps) was the main source of heating inside the PAM-OFR, rather than their optical radiation. Therefore, different lamp types mainly impact OH exposures, but not heating effects. All the three lamps applied here were manufactured by Light Source Inc., so they have similar power supplied to each lamp (8.9 W). In addition, we measured the temperature increase in 305 the OFR with lamps from another manufacturer (BHK Inc.). A temperature increase of 6 $^{\circ}$ C inside the OFR was found at the centerline when two BHK lamps at full power (Fig. S7b) were used with a flow rate of 4.5 L min⁻¹. The lower temperature increase with BHK lamps was due to the lower input heating energy (6.3 W per lamp) compared to the lamps from Light Sources. For the lower driving voltage of 0.95 V for BHK lamps during a field campaign, a temperature increase of 1-2 °C with an equivalent aging time of around 1.5 days was observed (Fig. S7a and S7b). During that campaign, the OFR was operated mostly continuously at ~1.5 days equivalent aging, since most SOA formation is often observed at these moderate 310
- exposures, and is low enough that heterogeneous oxidation is not vet significant (e.g., Palm et al. (2016), Ortega et al. (2016) and Hu et al. (2016)).

3.1.3 Mapping out the temperature increase inside the PAM-OFR

- In this section, the temperature increase within the PAM-OFR as a function of position was explored. In our case, when 315 the voltages of four lamps were set to be 5 V (~30 days' equivalent aging time and flow rate of 5 L min⁻¹), the temperatures in the PAM-OFR were generally 9-15 °C higher (Fig. 6a) than the ambient (26 °C). Vertically, the temperature increase was higher at the top position ($\sim 14 \circ C$) compared to the bottom ($\sim 9 \circ C$), due to the warm air ascending in the PAM-OFR resulting from its lighter density. A similar conclusion was found for BHK lamps (Fig. S7) with a lower temperature increase and smaller temperature difference in the vertical direction for the same equivalent aging. Horizontally, the temperature distribution was 320 symmetrical, with a slightly lower temperature value in the middle and an increased temperature on the edges (Fig. 6b). These
- temperatures values were measured until their reading varied no more than 0.1 °C. The lower center temperature could be attributed to the faster flow rate (shorter residence time) of air mass in the middle due to the removal of the inlet diffuser and the longer distance from the lamps. However, the largest temperature gradient at different horizontal axial positions was within 2-3 °C, indicating that the general temperature distribution measured here was comparable to that when the inlet diffuser was 325

higher from the middle position to the back in the central line, mainly due to the airflow flowing from the inlet to the outlet being warmed, as well as the set position of lamps having a gap with the front plate, as demonstrated in Fig. 1.

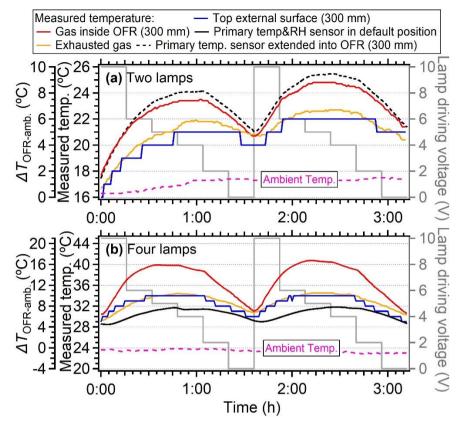
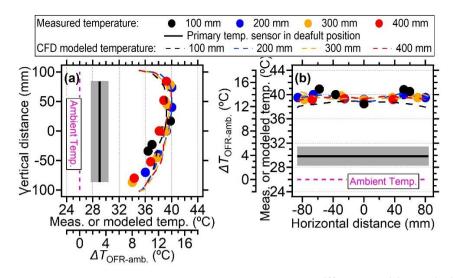


Figure 5: Temperature variation under different lamp driving voltage cycles of 10-6-5-4-2-0 V for: (a) Two symmetrical
lamps on the diagonal direction were used and the OFR backplate sensor was extended into the PAM-OFR (from the backplate) at a depth of 300 mm from the inlet. (b) Four lamps were used and the OFR sensor was set on the backplate.
Each lamp setting was operated for a duration of 16 min. The flow rate of sampling air was 5 L min⁻¹ (residence time of 167 s).

3.1.4 Loss of heating energy in OFR

The gain of the heating energy inside the PAM-OFR generally comes from the UV lamps, while the energy loss inside the PAM-OFR is mainly through three pathways: (1) The dissipation of energy through the exhaust air (from the ring flow set in this study) from the PAM-OFR; (2) The convection and radiation-induced heat energy transfer from the PAM-OFR surface to the ambient air. (3) The energy loss through the purge nitrogen between the lamps and quartz sleeves (Fig. S8).



- 340 Figure 6: The temperature measured by external temperature sensor at different positions within the PAM-OFR or under different settings: (a) the measured and CFD modeled temperatures on the vertical direction at different probing depths; (b) the measured and CFD modeled temperatures on the horizontal direction at different probing depths. All the four lamps were turned on during measurement. The four lamps' driving voltages were 5 V. The black lines and grey shadings were the average ± standard deviation for temperature measured by the backplate sensor.
- 345 To elucidate the energy balance across the three pathways, we measured the temperatures of the PAM-OFR tubeenclosure, the purge nitrogen, and the exhaust air. Specifically, our findings were based on maximum lamp driving voltages of four UV lamps (10 V) at a flow rate of 5 L min⁻¹. Figure 4 displayed the measured temperature of the PAM-OFR tubeenclosure as a function of time and at different positions (inner vs external surface, bottom vs top surface). The temperature at the top external surface increased as the gas temperature within the PAM-OFR rose, indicating that the PAM-OFR tube absorbed the heating 350 energy from lamps. The temperature detected at the inner surface of the OFR (40.5 $^{\circ}$ C) was lower than that of gases (43.5 $^{\circ}$ C), yet higher than that of the external tube surfaces (34 $^{\circ}$ C). The lower temperature of the external surface than the air masses inside the PAM-OFR could be attributed to i) there arewere heat losses on the OFR tube surface since the ambient air temperature (23 °C) iswas substantially lower than that of the OFR tubesenclosure, resulting in heat transfer. This heat transfer was also reflected by the diminishing temperature gradient between inner and external OFR tube surfaces ($40.5 \rightarrow 34$ °C). We 355 further measured the temperature of purged nitrogen at a default flow rate of 0.2 L min⁻¹. In this case, the temperature of exhausted nitrogen was $\sim 32 \,^{\circ}$ C (output), which was 9 $^{\circ}$ C higher than the temperature of input nitrogen (23 $^{\circ}$ C). ii) When the temperature equilibrium between the air and OFR was not balanced, an additional reason will cause the lower temperature in
- OFR tubeenclosure. The aluminum OFR chamberenclosure has a higher thermal mass than the air. Although the specific heat capacity of metal (0.908 J g⁻¹ K⁻¹ at 301.60 K) is similar to that of air (1.005 J g⁻¹ K⁻¹ at 300 K) (Giauque and Meads, 2002;
 Kieffer, 1956), the flow tube is considerably heavier than the air due to its significantly higher density (2700 Kg m⁻³ vs 1.29 Kg m⁻³), resulting in a lower temperature for the OFR tube than the inner air.

In addition to the air inside the PAM-OFR, the temperature of exhausted air (from the ring flow, Fig. S1) was also examined closely. A temperature sensor was set in the Teflon Tee connector near the output of the PAM-OFR backplate. We found a slightly lower temperature increase (\leq 5 °C, Fig. 5a) in the exhausted air compared to the air measured directly inside

- 365 the PAM-OFR. This discrepancy was probably due to the cooler surfaces of the fitting or sampling lines. Using these temperatures shown above, we roughly calculated the fraction of energy loss among three pathways. Detailed information on calculation could be found in Sect. S2 of the supporting information. Those model results indicated that after 105 min of heating, 51% of the total power (35.6 W, 8.9 W for each lamp, 4 lamps in total) during the heating process was converted into energy causing the temperature increase of the PAM-OFR. The remaining 49% of power was lost due to the conversion
 370 efficiency or converted into other energy that did not cause the warming of airflow inside the PAM-OFR. For the fraction
 - (51%) of energy that causing warming, the energy loss fractions through purged nitrogen gas (at flow rate 0.2 L min⁻¹), heated air, and OFR tubesenclosure were 0.3%, 9.8%, and 89.9%, respectively (Fig. S9a). This indicated that the dominant pathway for heat transfer was through metal tubesenclosure. Cooling the OFR tubesenclosure was an effective method to maintain the PAM-OFR near ambient temperature. As shown in the following sect. 3.5, with two fans blowing on the OFR tube, the heat dissipation of the OFR tube increases, resulting in a significantly lower temperature increase inside the PAM-OFR.
 - In some OFR systems, a higher flow rate of nitrogen-purged air was applied (Zhao et al., 2021; Bruns et al., 2015; Li et al., 2019). For example, Li et al. (2019) set the purged nitrogen flow rate at around 30 L min⁻¹ for their custom-designed OFR system with exterior lamps to keep the temperature at around 25 °C. We attempted to introduce a nitrogen gas flow at 20 L min⁻¹ through the lamps to increase the energy loss for the PAM-OFR. This was almost the maximum flow rate of purged nitrogen that could be tested due to the small inner diameter of the fitting connected to the lamp tubes. After nitrogen was injected at such a high flow rate, we found the temperature of the lamp sleeve, the inner surface of flow tubestube, and gas inside the PAM-OFR dropped from 62, 40.5, and 44 °C (four lamps at 10 V) to 42, 34 and 36.5 °C (36-51% decreased in temperature increase, with ambient temperature at 23 °C), respectively. Based on the measured temperature, we found the energy loss fraction through purged nitrogen increased from 0.3% to 32% (Fig. S9b). This was helpful, but it still could not balance the heating energy input from the UV lamps. The temperatures of air in the PAM-OFR (36.5°C) were still significantly higher than the room temperature (23 °C). The large consumption of pure nitrogen gas for running such a high flow rate would also pose a challenge for long-term experiments, especially for field studies.

3.1.5 Artificially low temperature measured by primary T/RH sensor in ARI OFR

During the experiment, we found that the primary T/RH sensor installed in the OFR backplate (see the sensor in Fig. S1) always showed a significantly lower temperature (by 1-14 °C) than the temperature sensor probed inside the PAM-OFR (Figs. 3-6). We hypothesized that the lower temperatures detected by the primary sensor at the default backplate position were mainly due to the direct contact of this sensor with the metal backplate which was at lower temperatures. When the primary sensor was placed at 300 mm into the PAM-OFR from the backplate (closer to the lamps than the centerline, as the default location of the sensor on the backplate was not in the centerline, Fig. s1), a similar temperature was measured by the primary T/RH 395 sensor and the one probed into the PAM-OFR (maximum difference of 1 °C), as shown in Fig. 5a. This indicated that the primary T/RH sensor in the backplate with default OFR settings led to underestimation of the temperature inside of the PAM-OFR, which should be verified and corrected by the users based on the configuration of their instrument.

3.2 Temperature influence on the flow field

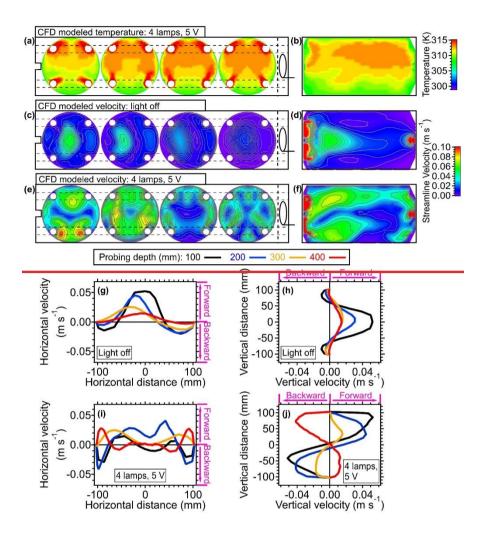
- In this section, we discuss the impact of elevated temperature on fluid dynamics within the PAM-OFR based on Computational Fluid Dynamics (CFD) simulations. Detailed setting parameters were introduced in Sect. 2.3. The temperature field where the voltages of four UV lamps were all set to 5 V was tested here. As shown in Figs. 6a and b, the simulated temperature distribution generally showed good agreement with the values measured directly with the temperature sensor within the PAM-OFR, validating the reasonableness and reliability of both simulated and measured temperature distributions. In Fig. 7a, the simulated 2-D temperature distributions revealed the hottest air (up to 45 °C) encircling the UV lamps. The rest air parcels exhibited a pronounced vertical axial temperature gradient (~10 °C), with temperatures ranging from 35-45 °C persisting in the upper region of flow tubestube. Such a pronounced temperature gradient was anticipated to induce significant recirculation within the PAM-OFR, as evidenced by the Richardson number calculation (Ri = 3974, which is far above 10 and indicates the existence of turbulence) (Huang et al., 2017; Holman, 2010). Details of the Ri calculation can be found in Sect. S3 of the supporting information.
- To investigate the non-isothermal effect on fluid dynamics within the PAM-OFR, the simulated flow distributions with and without heating effects are demonstrated in Figs. 7c-j. As illustrated in Figs. 7c-d, the flow velocity peaked following injection through an inlet diffuser, resulting in recirculation near the edge of the walls. The other place showing a higher air velocity was around the output of exit (Figs. 7d and S10), which was generally used for particle output measurements. In addition to aerosol sampling, the air for gas phase measurements wasis usually sampled through a perforated ring flow manifold in the back of the PAM-OFR to obtainreduce wall effects and recirculation, which makes the airflow more evenstable and better mixed airuniform (Fig. S1). Under the typical operating conditions, the flow distribution when both gas and aerosol wereare sampled would beis different from that when only the aerosol line wasis applied. However, incorporating the additional gas phase output significantly increases to the complexity of this CFD simulation. Thus, to simplify the simulation, we designated the airflow to be sampled solely through the exit port located at the center of the OFR backplate. Moreover, variations in the flow ratio between gas and aerosol lines would alter the flow distribution within the PAM-OFR.
 - Upon activation of the UV light, there was a significant alteration in flow distribution, characterized by an increased presence of flow bifurcation and recirculation, as shown in Figs. 7e and 7f. There was a pronounced recirculation in the lower region of the flow tube. This recirculation was further elucidated in Figs. 7g-j and Fig. S10. In the absence of heat effects within the PAM-OFR, the 1-D flow profile generally exhibited symmetry in the vertical direction (Fig. 7h). A slight distortion
- 425 on the 1-D flow profile in the horizontal direction was reasonable due to the influence of the random motion and pressure gradient of gas (Fig. 7g). In the presence of a vertical axial temperature gradient, 1-D flow profiles exhibited a skewed pattern due to the buoyancy of the warmer air. This recirculation effect manifested when the temperature gradient was larger, as well

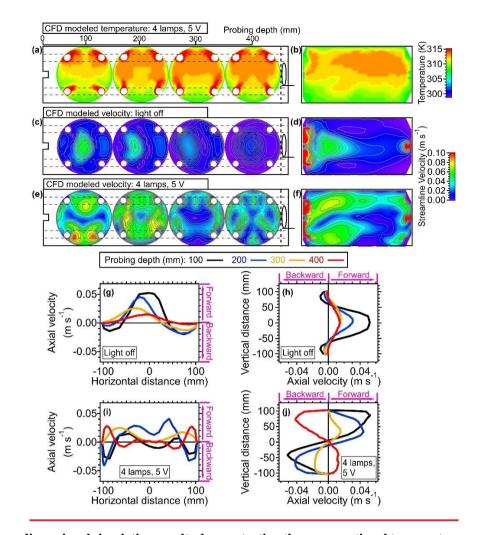
as when the flow rate was lower, leading to substantially alterations in both the residence time distribution (RTD) and <u>itsthe</u> average value-residence time (τ_{avg}). Details of the τ_{avg} calculation can be calculated as the sum of the integrals of signal (such

430 as the signal of SO₂ after introducing SO₂-pulses) over time versus the sum of the signals found in (Huang et al., 2017) Huang et al. (2017).

The average RTD-values<u>residence time (τ_{avg})</u> within the PAM-OFR under heat and non-heat scenarios were also measured and simulated in Fig. 8. Similar to the modeled results in Huang et al. (2017) and the measured results in Lambe et al. (2019), the measured RTDs under higher temperatures in this study exhibit shorter τ_{avg} (135-145 s at 5-10 V vs. 177 s at 0

- 435 V) due to the acceleration of air upon heating. This acceleration was mainly reflected in the early arrival time and shorter tails, as shown in Fig. 8. Huang et al. (2017) found that even minor temperature deviations (0.2 °C) in non-isothermal conditions could induce secondary flows, thereby significantly affecting the RTD and τ_{avg} . The RTD variation when lamps were turned on and off were also simulated in the CFD model, as shown in Fig. 8. Compared with the measured results, the simulated RTD generally exhibited an earlier arrival time and broader distribution at different light settings. The simulated τ_{avg} upon heating
- 440 (173-180 s) exceeded the value when lights were off (167 s), indicating that the recirculation in the model introduced by heating prolonged the τ_{avg} rather than reducing it. This discrepancy from the observed trend in τ_{avg} (Huang et al., 2017; Lambe et al., 2019) could be attributed to that the recirculation was weighted more in the <u>calculationsimulation</u> than the real conditions, which also underscored the complexities of accurately simulating the orthogonal forces induced by both pressure gradient-driven forced convection (horizontal) and buoyancy-induced free convection (vertical) (Huang et al., 2017). Note the
- simulated τ_{avg} under a lamp setting of 10 V (173 s) was lower than the τ_{avg} under 5 V (180 s). This trend aligned with the measured results, suggestingindicating the increased gas diffusion upon heating was properly considered except the recirculation.

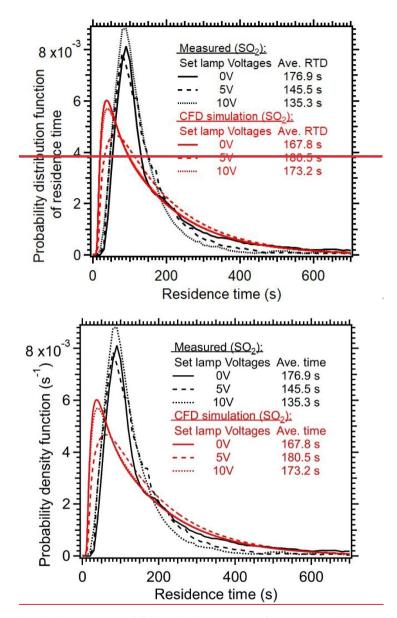




450 Figure 7: (a) Three-dimensional simulation results demonstrating the cross-sectional temperature profiles. Four cross-sectional figures from left to right represented the results at probing depths of 100, 200, 300, and 400 mm for panel (a), (c), and (e). (b) Simulated lateral temperature profile inside of the OFR based on CFD simulation. Panel (a) and (b) were simulated with conditions that four lamps were set to be 5 V. (c) Three-dimensional simulation results illustrating cross-sectional velocity profiles and (d) lateral velocity profiles based on CFD simulation results. Panel (c) and (d) were simulated with conditions that lamps were off (room temperature: 25 °C). (e-f) the same plots as panels (c-d) with four lamps set to 5 V. One-dimensional axial velocity profiles at (g) horizontal and (h) vertical directions inside the OFR at room temperature, and one-dimensional axial velocity profiles at (i) horizontal and (hj) vertical directions with four lamps set to 5 V. The positive values indicated the velocity direction from inlet to outlet (Forward) and the negative values represented the velocity direction from outlet to inlet (Backward).

⁴⁶⁰ In summary, the heating introduced from four lamps set to 5 V decreased τ_{avg} by 18-23% in comparison to dark OFR

experimental conditions. This was considered as an upper limit variation on τ_{avg} for a typical OFR setting where the lamp voltages were usually below 3 V to obtain OH exposures of less than 5 days. The variation of RTD altered the exposure time of gas/aerosol species within the PAM-OFR, which could impact the gas and particle oxidation conditions. In the following sections, this impact will be systematically discussed.



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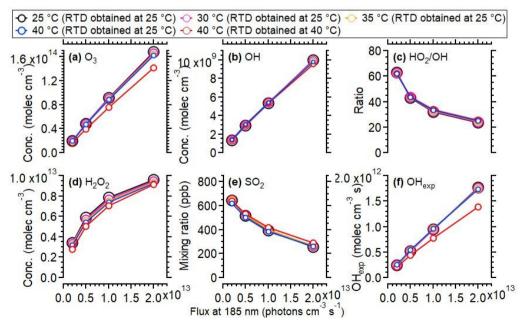
Figure 8: Residence time distribution (RTD) of SO₂ within the PAM-OFR under different lamp settings. A 2 s pulser of SO₂ was injected into the OFR. The average <u>RTD-values-wereresidence times are</u> also <u>estimatedshown</u> here. The simulated results from CFD <u>models weremodel</u> are shown in red lines.

470 **3.3 Temperature influence on gas-phase reaction and OH exposure**

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In this section, the temperature influence on gas-phase reactions was systematically investigated. We took the oxidation of SO₂ within OFR as an example to simulate its gas-phase reaction with oxidants (mainly OH) across a temperature range of 25 °C to 40 °C (binned with 5 °C) using the KinSim Model. The simulation at 25 °C emulated the typical laboratory conditions, while 40 °C simulation represented the approximate temperature observed at the upper limit of lamp voltage (5-10 V, corresponded to photochemical age ~10-30 days, Fig. 2). In addition, to account for the RTD influences on gas-phase reactions under different temperatures, the scenarios with measured RTD distributionsRTDs under 25 °C and 40 °C were both simulated here.

In general, when the temperature variation within OFR (the same RTD as measured at 25 °C being applied for cases at different temperatures) was considered, the influences of temperature increase due to lamp heating on the gas-phase reaction raterates were minimal. The concentrations of OH, HO₂, O₃, and O(¹D) all showed a maximum of ~5% increase at the highest photon flux, which was consistent with the simulated results using the same KinSim model in Li et al. (2015). The SO₂ decay and OH exposure also showed negligible variations in the model (Fig. 9e and 9f). When the temperature influences on the RTD were taken into account, the variation trend of oxidant concentration was mixed due to the combined negative effect of the reduced average residence time (τ_{avg}) and the positive effect of temperature on oxidant concentration (Li et al., 2015). The Parameter most influenced was OH exposure, which showed 18-20% lower values at 40 °C than at 25 °C due to the shorter residence time (τ_{avg}) upon heating. Our results suggested that an increase in temperature within OFR due to lamp heating would have a minimal to negligible impact on gas-phase reactions, whereas parameters related to the RTD distribution (e.g., OH exposure) should be considered in the current and future experiments.



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490 Figure 9: Simulated concentrations of different oxidants from 25 to 40 °C within the OFR utilizing the radical mechanism of the KinSim model. 800 ppb of initial SO₂ and 2.2% water vapor mixing ratio (25 °C, 70% RH) were used. The simulated results using measured RTD at 25 and 40 °C were both shown.

3.4 Temperature influence on the evaporation of ambient OA

Here, we estimated the potential losses of input ambient OA due to evaporation under enhanced temperature in OFR. This 495 estimation is mainly based on literature results and modeling work. For the existing OA which is sampled into the OFR, the evaporation of input OA upon heating can be roughly estimated based on the results from thermal denuder (TD) experiments. These experiments involved heating aerosols from ambient/room temperatures (20-25 $^{\circ}$ C) to elevated temperatures (typically 60-200 °C) over a typical residence time of 10-60 s (typically ~20 s) (Huffman et al., 2009; Xu et al., 2020; Hu et al., 2016; Saha et al., 2017; Kolesar et al., 2015; Saha and Grieshop, 2016; Lee et al., 2011). Previous studies suggest the evaporation of 500 aerosol is kinetically limited, which varies with temperature, residence time, OA mass and volatility, phase state and dissociation rates for oligomers (Cappa, 2010; Riipinen et al., 2010; Roldin et al., 2014; Schobesberger et al., 2018). Based on the previous TD studies, an evaporation rate of $1 \times 10^{-4} \cdot 2.5 \times 10^{-4}$ per (s⁻¹ °C-second)⁻¹ was usually observed under 50 °C of TD for ambient OA (typical average mass concentration: 10-30 µg m⁻³) (Huffman et al., 2009; Feng et al., 2023; Paciga et al., 2016). In an OFR experiment conducted on an aircraft, Nault et al. (2018) found an average mass loss of \sim 32% for ambient 505 OA-was -32% due to increased temperature in a dark OFR compared to the unperturbed air sampled (+17 °C on average) at a residence time of 150 s. This OFR experiment showed an evaporation rate of $1.2 \times 10^{-4} \text{ per (s^{-1} \circ C-second^{-1})}$, which was within the range of reported values obtained from the higher temperature TD experiments $(1 \times 10^{-4} - 2.5 \times 10^{-4} \text{ per (s}^{-1} \circ \text{C-second}))$.⁻¹). Theoretically, when the temperature enhancement was assumed to be ~5 $^{\circ}C$ and a residence time of 160 s was applied, a mass loss of 8-20% was estimated for ambient OA in OFR. The increased temperature within OFR would also impact other semi-510 volatile inorganic species, e.g., ammonium nitrate (Heim et al., 2020).

3.5 Temperature influence on the SOA formation

The temperature can influence the SOA formation through changing gas/particle partitioning and RO₂ fate, thus affecting the SOA yield and chemical composition (Takekawa et al., 2003; Li et al., 2007; Zhang et al., 2015; Price et al., 2016; Quéléver et al., 2019; Kristensen et al., 2020; Atkinson et al., 1987).-Obvious SOA decrease mass was observed in OFR at different

temperatures.

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For The formation of SOA from the newly formed SOA in the oxidation of different VOC precursors within OFR, the temperature impact was simulated based on at different temperatures using the SOM model (He et al., 2022; Eluri et al., 2018). Specifically, the kinetic phase partitioning of SOA generated via OH-oxidation of typical ambient VOCs was simulated (Figs. 10-11, S12-17) as a function of OFR temperature ranging from 20-40 °C (binned in 5 °C) and OA seed mass concentration

from 1 to 80 µg m⁻³. The evaporation and chemical reaction of existing OA seed under different temperatures were not

considered in the model. Note that the results, including SOA yield, size distribution, and O:C ratio for n-dodecane (Figs. 10 and 11), α -pinene (Figs. S12 and S15), toluene (Figs. S13 and S16) and m-xylene (Figs. S14 and S17), were examined under both high NOx and low NOx conditions. For dodecane, the simulated temperature-dependent SOA under high NOx condition in the SOM model was generally consistent with the chamber results presented in Lamkaddam et al. (2017).

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Generally, the higher temperatures result in lower SOA yields due to the increased evaporation partitioning of oxidation products in gas-phase products (Hildebrandt et al., 2009; Warren et al., 2009; Qi et al., 2010; Denjean et al., 2015). As shown in Figs. 10a and S12-S14, when RTD at 25 °C was used for different temperatures, the SOA yield of different VOC species including dodecane, α -pinene, toluene, and xylene could decrease by ~20% for a typical temperature increase of 5 °C in the

- 530 OFR, and by up to 40-50% at 40 °C compared to the values at a typical 25 °C under high NOx condition. This decline in SOA yield indicated significant temperature effects on SOA formation within the OFR due to heating. To confirm the model results, we did a simple laboratory experiment and found the formed SOA masses was indeed substantially decreased in OFR due to the heating effect (Fig. S19), which is consistent with the simulated model results. The simulated particle size also showed decreases as the OFR temperature increased. The higher SOA mass and larger size of particles formed at lower temperatures
- 535 were consistent with more gas-to-particle phase partitioning, and had also been observed in various temperature-controlled chamber studies (Clark et al., 2016; Lamkaddam et al., 2017; Boyd et al., 2017; Gao et al., 2022; Pathak et al., 2007; Tillmann et al., 2010; Price et al., 2016; Kristensen et al., 2020). When the measured RTD at 40 °C was applied in the model, an even lower SOA yield was achieved due to the shorter residence time of reactants. However, this influence was weaker than the directly influences caused by the temperature increase on SOA formation. A decreased of ~8% of dodecane SOA yield was
- 540 found at 40 °C under high NOx condition and 10% under low NOx compared to the results with RTD measured at 25 °C (Fig. 10). Under low NOx conditions, a smaller reduction in size distribution (Fig. 11 and Figs. S15-S17) and SOA yield, which were 5-10% for a temperature increase of 5 °C and up to 15-35% for 15 °C as shown in Fig. 10 and Figs. S12-S14, was found compared to high NOx conditions. This smaller reduction was mainly due to the formation of more SOA with lower volatility under low NOx conditions (e.g., acids, hydroperoxide) than under high NOx conditions (Kroll and Seinfeld, 2008; Srivastava
- 545 et al., 2022; Presto et al., 2005; Aruffo et al., 2022). The parameters of the SOM model were obtained based on fitting the results to the chamber results under high and low NOx conditions, respectively (Eluri et al., 2018; Cappa et al., 2016), thus, these parameters were set such that the volatility of SOA decreased larger as a function of the functional groups added under low NOx conditions than under high NOx conditions (Cappa et al., 2013). Note that in the model we did not specifically treat the temperature effect on autoxidation reaction rate of RO₂ fate e. E.g., a-varied fractionyields of highly oxygenated organic
- 550 molecules (HOMs) from autoxidation shall be used at different temperatures. Using a, while constant yieldyields for HOMs were used during the simulation in this study. The constant yields for HOMs used in the model could lead to a lower HOMs mass fraction in total SOA at high temperatures, which would result in an underestimation of the oxidation level and an overestimation of the volatility of SOA formed under low NOx conditions (Bianchi et al., 2019). In addition, the wall loss was corrected in the SOM model with a constant wall loss rate of 2.5x10⁻³ s⁻¹, which has been verified in the comparison of SOA
- 555 model work between OFR and chamber studies (He et al., 2022). In theory, when the temperature of the OFR tube increased,

the wall loss rate of low volatile organic compounds should be smaller than under ambient temperature. Therefore, using a constant wall loss rate here would underestimate the SOA yield.

In previous studies, to correct the heating effects on SOA yield, Chen et al. (2013) and Lambe et al. (2015b) adjusted the SOA yield by 2% per K of temperature increase relative to 298 K (Stanier et al., 2008). However, this is a rough correction,

because the SOA yields of different precursors and reaction conditions are affected by temperature in varying degrees. For example, 0.41-0.52% per K was found for dodecane under high NOx conditions based on the SOM model while 0.87-0.89% per K was found for α-pinene (Table S4). Note that in the OFR experiments, the reduction of SOA yield could be even larger due to the potential mass loss of seed OA upon heating in the OFR. The simulated results from the SOM model here provided an approximate reference to help recalibrate the SOA formation inside of OFRs. The detailed numbers calculated by the SOM model for different species under high and low NOx conditions can be seen in Table S4. For a specific recalibration, e.g., mixed precursors, a more detailed model or temperature-controlled experiments considering the mixing effect of precursors.

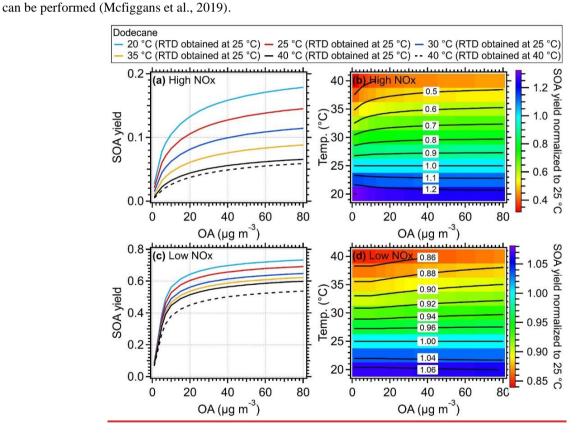


Figure 10: Simulated SOA yield of dodecane as a function of mass concentration of OA seed (inlet mass concentration) and temperature within the OFR under (a) high NOx and (c) low NOx conditions, respectively. The simulated results using the measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of dodecane from

<u>different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions.</u> <u>The equivalent aging</u> <u>time was 1 day by assuming the ambient OH concentration equated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).</u>

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For the SOA chemical composition, the higher temperature within the OFR led to an increase in O:C ratios of SOA, e.g., ~0.35 (25 °C) vs. ~0.42 (40 °C) in dodecane experiments under high NOx conditions and ~0.23 (25 °C) vs. ~0.28 (40 °C) under low NOx condition. The increased O:C ratio under higher temperatures was also found in the chamber results for m-xylene/NOx photooxidation in Qi et al. (2010) and O₃ oxidation of α -pinene in Denjean et al. (2015). The higher O:C at higher temperatures was probably caused by the evaporationless partitioning of semi-volatile and less-oxidized components into particle phase with increased temperatures (Clark et al., 2016; Gao et al., 2022).

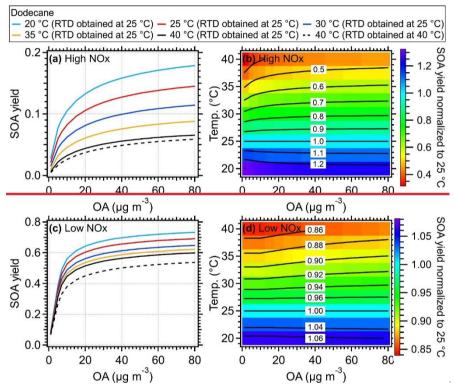
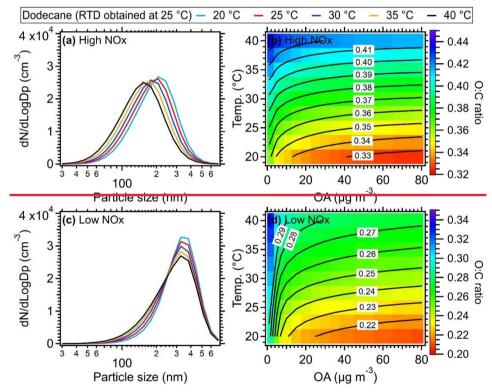


Figure 10: Simulated SOA yield of dodecane as a function of mass concentration of organic aerosol and temperature within the OFR under (a) high NOx and (c) low NOx conditions, respectively. The simulated results using the measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of dodecane from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the OH concentration equated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

In the model, the evaporated SOA massgas-particle partitioning of oxidation products as a function of temperature was mainly determined by the enthalpy (H_i^{vap}) , as described by the Clausius–Clapeyron Equation (Eq. (1)). A variable enthalpy

 H_i^{vap} dependent on saturation concentration (C*, $H_i^{vap} = -11 \times log C_{ref}^*$) was applied as the default setting based on Epstein et 390 al. (2010). Various experimental studies using thermodenuders to measure OA volatility showed that the ambient H_i^{vap} for OA varied within a range of 50-150 kJ mol⁻¹ (Epstein et al., 2010; Saha et al., 2017; Cappa and Jimenez, 2010). To further explore the sensitivity of temperature-dependent SOA formation to enthalpy, we demonstrated the SOA yield as a function of temperature under constant H_i^{vap} values in Fig. 12 and S18. The results suggestedindicated that the SOA yield obtained with varying H_i^{vap} was generally comparable to that when a constant H_i^{vap} of 100 kJ mol⁻¹ was applied, which iswas the most commonly reported H_i^{vap} for ambient OA. HigherIncreasing H_i^{vap} suggests thatincreases the sensitivity of SOA formation is more sensitive to the temperatures. When the upper (150 kJ mol⁻¹) and lower limit (50 kJ mol⁻¹) of H_i^{vap} were applied, the simulated results of SOA yield suggested a maximum of 22% and 90% variation, respectively, under high NOx conditions and 18% and 42% variation, respectively, forunder low NOx conditions based on. These variations were observed across different speciesprecursors and temperatures.



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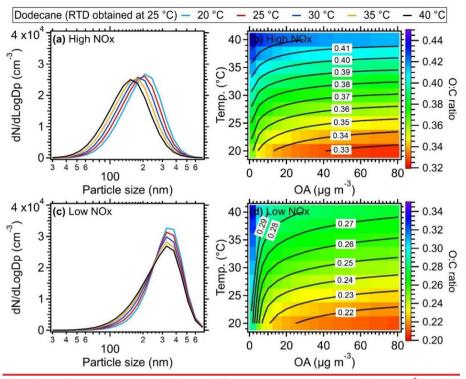


Figure 11: Size distribution of dodecane underSOA at different temperatures and 30 µg m⁻³ organic aerosol for under
(a) high NOx and (c) low NOx conditions, respectively. <u>A mass concentration of 30 µg m⁻³ for OA seed (inlet mass concentration) was assumed for size distribution simulation here.</u> The O:C ratio of dodecane under differentSOA as a
function of temperatures and organic aerosolmass concentration of OA seed (inlet mass concentration) under (b) high and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the ambient OH concentration equated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

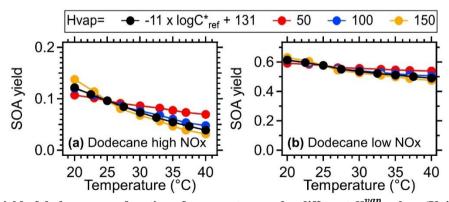


Figure 12: SOA yield of dodecane as a function of temperature under different $H_i^{\nu ap}$ values (Unit: kJ mol⁻¹). The mass concentration of organic aerosolOA seed (inlet mass concentration) was assumed to be 15 µg m⁻³. The equivalent aging time was 1 day by assuming the <u>ambient</u> OH concentration equated to 1.5×10^6 molecule cm⁻³ (Mao et al., 2009).

In addition to the direct influences, the increase of temperature within OFR decreases the relative humidity (RH), which can also impact SOA formation. However, the literatures show that the impact of RH on SOA formation remains inconclusive. For example, Tillmann et al. (2010) found the SOA yield was higher at humid conditions (RH: 40-70%) compared to dry

615 conditions (RH: 0-10%) as the RH influenced the formation of products in α -pinene ozonolysis experiments. In contrast, Zhang et al. (2019)Zhang et al. (2019) found the SOA yield of m-xylene-OH oxidation decreased as RH increased in a chamber study, as the high RH led to the less formation of oligomers and inhibited the reaction of RO_2 autoxidation. Thus, elucidating the influence of humidity on various SOA formations is still a challenge and falls outside the purview of our research topic here. In addition, given the short residence time within OFR (seconds to minutes), the impact of liquid phase reactions to SOA

620 formation should be minimal.

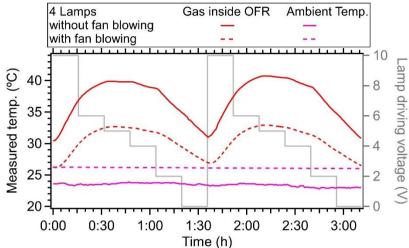
In summary, the heating effect induced by the lamps could significantly influence the SOA formation within OFR for certain high-OH exposure applications. This showed impact of temperature varied extents for different depending on the specific precursors and reaction conditions. Simulation results suggested that the decreased ratio of SOA output to preexisting OA at higher OH exposures (e.g., equivalent aging time $>\sim 5$ days under low NOx conditions) observed in previous studies 625 (Hu et al., 2022; Lambe et al., 2015a; Ortega et al., 2016; Palm et al., 2016; Saha et al., 2018) may not only due to heterogeneous reactions and/or enhanced gas-phase reaction. Instead, it could also be attributed to the heating evaporation.lower SOA yield resulting from the temperature increase. However, the yield and ambient OFR results under equivalent aging time <~4 days should be remained valid (Palm et al., 2018). The temperature increase would also impact the phase of aerosols by changing the chemical composition of OA (viscosity, O:C, etc.), as the PAM-OFR temperature covered the usual range of glass transition 630 temperature of ambient OA (2-87 °C) (Li et al., 2020b; Derieux et al., 2018). The impact of temperature increases on the phase state (i.e., viscosity) of aerosol phases, wall loss or other effects needs to be further studied.

3.6 Approaches to reduce the heating effect

In the PAM-OFR, one approach to reduce the heating influence of the lamps is to shorten the OFR residence time, at the expense of decreasing the maximum achievable OH exposure and time available for LVOC condensation onto aerosols (Peng

- 635 and Jimenez, 2020). Another method involves using fewer lamps with lower voltage settings; for example, using two lamps at less than 3 V maintains a temperature increase of less than 5 °C while still achieving OH exposures of up to 5 days under low NOx conditions. In addition, it can also be useful to enhance heat transfer away from the PAM-OFR to reduce its operating temperature e.g., blowing air with fans or air conditioners. To verify this, we used two large fans (45 cm in diameter at a distance of 30 cm from the PAM-OFR) directed towards the lower parts of the PAM-OFR. We found the maximum delta
- temperature (OFR minus ambient air) for a typical high light setting decreased from 16 °C to 7 °C (44% deductionreduction), 640 as shown in Fig. 13. This experiment demonstrated that blowing the flow tube with fans is an extremely effective way to compensate for the lamp heating, and is simple without major trade-offs. Moving the UV lamps outside the tube and designing a cooling system on the outer surface of OFR with circulating water or cold air can also be effective ways to improve the temperature control inside of OFR (Watne et al., 2018; Xu and Collins, 2021; Huang et al., 2017; Liu et al., 2018; Chu et al.,

645 2016; Zhao et al., 2021; Li et al., 2019), however, these will require a substantial redesign of the hardware of OFR tubes<u>enclosure</u> and are beyond the scope of this manuscript. And mounting the lamps outside of the OFR limits the use of OFR185 mode due to the low transmission efficiency of quartz glass for light at 185 nm (Simonen et al., 2017) and OFR254 mode is usually used. Cooling down the OFR would also affect RTD since the heater transfer occurs via convection inside of OFR, which needs to be further investigated in the future.



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Figure 13: The measured temperature in OFR with or without fan <u>bellowingblowing</u> on the flow tube in the laboratory. The ambient temperature was also shown. Two fans were used, with a diameter of 45 cm and a rotation rate of 1400 r min⁻¹.

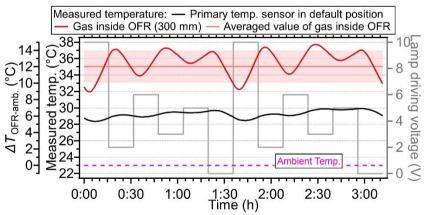
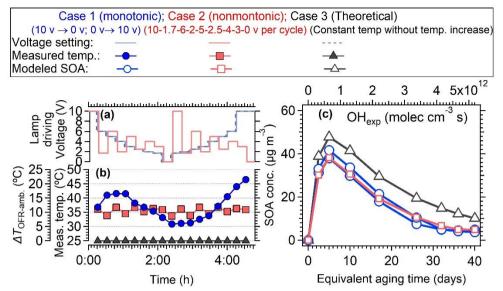


Figure 14: The measured temperature variation when lamp driving voltage cycles were set in a non-monotonic pattern (10-2-6-3-5-0 V for one cycle). The red line and shading were the average temperature and standard deviation (35.05±1.97 °C) measured at the centerline (probing distance: 300 mm) inside the PAM-OFR. The purple dotted lines represented the ambient temperature. Each lamp voltage was set for 16 min.



660 Figure 15: (a, b) The temperature variation with lamp driving voltage was explored using a monotone (10→0→10V) and non-monotone pattern lamp power change pattern, respectively. (c) the modeled SOA formation from oxidation of 10 ppb toluene (OMOA seed=30 µg m⁻³) with OH radicals as a function of OH exposure. The SOA formation under monotone and non-monotone scenarios were both simulated. The case 3 of "theoretical" indicates the temperature was set to be constant (i.e., 25 °C).

665 The voltage setting strategy in the PAM-OFR also can be improved. In most of the OFR laboratory and field studies, OFR users usually changed the light setting monotonously from 0 to 10 V or from 10 to 0 V, which resulted in a continuously changing temperature within the PAM-OFR (Fig. 2, Fig. 5 and Fig. S4), therefore resulting in a variable SOA formation yield at different temperatures (Fig. 10). To mitigate the variable heating effect, we suggest alternating between high and low voltage settings to minimize the heat accumulation. Fig. 14 showed an example of such a light setting cycle using 10-2-6-3-5-0 V. In 670 such a way, although the average temperature within the PAM-OFR was still higher than the ambient temperature, the variation of measured temperature withininwithin the PAM-OFR can be maintained within a narrow range, exhibiting a smaller temperature deviation (± 1.97 °C) compared to the usual settings (Fig. 14a, ± 4.76 °C). Furthermore, this method allowed for less uncertainly in the variation trend of SOA yield as a function of OH exposure compared to those performed under monotonically increasing or decreasing light settings. As shown in Fig. 15c, when using the measured temperature to simulate 675 the SOA formation from toluene in the OFR, the SOA showed two different trendsconcentration curves (2-32% differences) when monotonic and non-monotonic light setting cycles were applied. The SOA formed from the proposed non-monotonic lamp setting cycle showed better agreement on mass concentration variation (Fig. 15c) and mass ratio (Fig. S20) compared to the SOA formation at 25 °C (40.4-80.0% for non-monotone setting vs. 32.9-87.3% for monotone setting), which would introduce fewer uncertainties in the SOA yield and other aspects, e.g., chemical composition.

680 4 Conclusion

We systematically measured the temperature distribution within the lamp-enclosed Aerodyne PAM oxidation flow reactor. Our findings indicated that the lamps within the PAM-OFR generated heating energy, thus leading to temperature increase within the PAM-OFR. A brief summary of the temperature increases and its influencing factors can be found in Table A1. The rise in air temperature was proportional to the lamp driving voltage (OH exposures) and the number of lamps applied, while it decreased with increasing flow rate due to shorter residence times at higher flows. The distribution of this temperature increases varied depending on special positions, influenced by the complex interplay of thermal transfer and flow mixing. With default lamps from Light Source Inc. installed, the temperature increase of air in the PAM-OFR was generally below 5 °C (at central line) when the driving voltages of two lamps were below 3 V (typically < 5 days of equivalent atmospheric OH exposure under low-NOx conditions) and the flow rate was 5 L min⁻¹ (average residence time, τ_{avg} =150-180 s). The use of BHK lamps typically resulted in a smaller temperature increase in the PAM-OFR at the same OH exposure due to their lower power dissipation. The heating energy loss of the OFR system was mainly through the walls of the reaction chamber, followed by exiting air within the PAM-OFR and/or purged nitrogen.

The impact of temperature increase on the flow distribution, gas, and aerosol phase chemistry within the PAM-OFR was systematically evaluated. The pulsed tracer measurements suggested that the increased temperature in the PAM-OFR accelerated the diffusion, The pulsed tracer measurements suggested that the increased temperature in the PAM-OFR induced the axial dispersion (Lambe et al., 2019), leading to a shorter average residence time (τ_{avg}). Although box model simulation results showed that the temperature increase in OFR had a negligible impact on gas-phase oxidant concentrations (<~5%), however, had a certain impact on the τ_{avg} related parameters, e.g., OH exposure (~20% decreased due to a temperature increase of 15 °C).

- The increase of temperature has larger impacts on aerosol phase chemistry than on gas phase. When the temperature increase within the OFR was 5 °C at a flow rate of 5 L min⁻¹, the evaporation loss of ambient OA was found to be 8-20% based on thermodenuder and field experiments. The simulation from the SOM model suggestedshowed the SOA yield from four typical precursors (n-dodecane, α -pinene, toluene, and m-xylene) could decrease <20% under high NOx conditions and <10% under low NOx conditions when the temperature in OFR increased by 5 °C. As temperature increased, the size distributions
- 705 also showed a substantial decrease while while O:C ratios showed an increase. This work demonstrated the substantial influence of temperature on SOA formation and highlights the necessity of considering temperature effects when using the PAM-OFR for aerosol chemistry research. Based on the SOM model simulation results in Table S4, we recommend 0.19-1.6% and 0.26-3% per K for temperature effect correction for SOA yield from four typical precursors under high NOx and low NOx conditions, respectively.
- 710 In general, applying higher flow rate and lower lamp power, cooling the reactor with fans are recommended to keep the temperature increase low in the OFR system. In addition, to control the variation of enhanced temperature introduced by the monotonic trend for lamp settings (e.g., $0 \rightarrow 10$ V or $10 \rightarrow 0$ V), we propose to set the voltage with high and low voltage

alternatively (e.g., 10-2-6-3-5-0 V) to reduce the heating accumulation and keep the temperature variation within a narrow range. In summary, our evaluation of the temperature increase inside of lamp-enclosed OFR helps to improve our

715 understanding of flow distribution and chemistry inside of this type of OFR, which can help to reduce the uncertainty of OFR usage in the future.

Appendix

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Table A1: Summary on the effect of different dimensional factors on the temperature of air inside of OFR, as well as the impact of temperature enhancement on flow, gas and aerosol chemistry inside OFR.

Factors influence on temperature (T) of air inside OFR		
	Impact factors	Effect
Heating energy input	Driving voltage of lamps	Driving voltage $\uparrow \rightarrow T\uparrow$
	Number of lamps	NO. of lamp used $\uparrow \rightarrow T\uparrow$
	Lamp types	No differences for the same brand
	Lamps lasting time	Time $\uparrow \rightarrow T \uparrow$ before balance
	Setting voltage sequence	Set voltage \uparrow monotonically \rightarrow T \uparrow ; Set voltage \downarrow monotonically \rightarrow usually delayed T \uparrow peak
Heating energy loss	Flow rate (corresponds to Residence time distribution, RTD)	Flow rate \uparrow (RTD \downarrow) \rightarrow T \downarrow
	N_2 purge air	Flow rate \uparrow or N ₂ temperature $\downarrow \rightarrow T \downarrow$
	Surrounding T of OFR	Surrounding $T \downarrow \rightarrow T \downarrow$
	Metal tube temperature	Metal tube $T \downarrow \rightarrow T \downarrow$
Temperature distribution	Measured position	Closer to lamp sleeve $\rightarrow T\uparrow$
	Vertical	Generally, T \uparrow in the upper position
	Horizontal	Symmetrically distributed.
	Probing depth	Probing depth $\uparrow \rightarrow T\uparrow$ for ARI OFR; Probing depth $\uparrow \rightarrow T\downarrow$ for Penn State OFR
Temperature influences on flow, gas, and aerosol chemistry		
	Factors being influenced	Effect
Flow	Average RTD	$\uparrow \uparrow \rightarrow \text{RTD} \downarrow$
Gas-phase	absolute concentration of oxidants	$T\uparrow \rightarrow \text{Minor impact } (<5\%)$
	OH exposures	$T\uparrow \rightarrow OH exposure \downarrow$
	HOM yield	$T\uparrow \rightarrow HOM \text{ yield }\uparrow$
Aerosol-phase	input/seed OA	T↑→ OA masses \downarrow
	SOA yield*	$T\uparrow \rightarrow SOA yield \downarrow$
	Size distribution of SOA*	$T\uparrow \rightarrow \text{Peak sizes }\downarrow$
	Oxidation level of SOA*	$T\uparrow \rightarrow \text{Oxidation level} \downarrow$

*More impact on high NOx regime than low NOx regime.

Data availability. The data shown in the paper are available on request from the corresponding author (weiweihu@gig.ac.cn)

Author contributions. HW, AL, QH, YH, MM, SJ, YZ, ZP, YH, DD, PJ, and JJ: conceptualization, methodology, investigation

725 and revision. MH: simulation of flow in OFR. QH and HC: provide the solid work design of OFR. WH and XM: supervision, project administration and funding acquisition. TP and WH wrote the paper, and all co-authors supported the interpretation of the results and contributed to improving the paper.

Competing interests. The authors declare that they have no conflict of interest.

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735 document are solely those of the authors and do not necessarily reflect those of the Agency. EPA does not endorse any products or commercial services mentioned in this publication.

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Supplementary material for:

A comprehensive evaluation of enhanced temperature influence on gas and aerosol chemistry in the lamp-enclosed oxidation flow reactor (OFR) system

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S1 Supply power for Light Source and BHK lamps

For the UV lamps from Light Source Inc., the supply power (8.9 W) was calculated as 185 mA/425 mA ×21 W, where 185 mA is the measured current controlled by the ballast at 10 VAC (full) output; 425 mA and 21 W are the manufacturer specified current and power. For BHK lamps, the supply power (6.3 W) was measured directly with a Kill-A-Watt sensor on the outlet of the lamp controller box at full AC output.

S2 Calculation of the heating energy in OFR

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For the temperature measured for a lamp control voltage of 10 V (full AC power) and flow rate of 5 L min⁻¹ (Fig. 4), we 1280 calculated the fraction of heating energy transferred from the UV lamps to the gas inside the OFR (f_g), the N₂ purge gas (f_{N_2}), and the OFR tube wall (f_s). Results were estimated on the assumption that all the electrical input power of the lamps was finally converted into heat, which led to the rise in temperature. We did not consider the heat exchange between the gas inside the OFR, N₂ purge gas, and OFR surface. The energy of gas inside the OFR (or N₂ inside the lamp sleeves) would be lost due to the gas (or N₂) entering and leaving the OFR (or lamps sleeve), depending on the flow rate and the temperature of the ambient gas (or N₂,0.2 and 20 L min⁻¹). Also, the OFR surface dissipate heat to the ambient air. Based on the timeseries of measured temperature in Fig. 4, the f_g , f_s , and f_{N_2} could be calculated as follows:

$$f_g = \frac{Q_g}{Q_{Total}} = \frac{C_g \times M_g \times \Delta T_{i-(i-1)} + C_g \times m_g \times \Delta T_{i-a}}{Q_{Total}}$$
(1)

$$f_s = \frac{Q_s}{Q_{Total}} = \frac{C_s \times M_s \times \Delta T_{j-(j-1)} + F \times A \times \Delta T_{j-a}}{Q_{Total}}$$
(2)

$$f_{N_2} = \frac{Q_{N_2}}{Q_{Total}} = \frac{c_{N_2} \times M_{N_2} \times \Delta T_{k-(k-1)} + c_{N_2} \times m_{N_2} \times \Delta T_{k-a}}{Q_{Total}}$$
(3)

1290 Where Q_g , Q_s , and Q_{N_2} were the energy in 1 second of lamps allocated to the gas inside OFR, surface of OFR and N₂ purge gas, respectively; Q_{Total} is the total energy from 4 lamps in 1 s (35.6 J, 8.9 W for each lamp at full VAC). C_g , C_s and C_{N_2} were the specific heat capacity of gas (1.005 kJ kg⁻¹ K⁻¹ at 300 K), OFR surface (aaluminumaluminium, 0.879 kJ kg⁻¹ K⁻¹ at 293 K) and N₂ (1.038 kJ kg⁻¹ K⁻¹ at 298 K); M_g , M_s and M_{N_2} were the mass of gas inside OFR, OFR surface, and N₂ in lamp sleeves; $\Delta T_{i-(i-1)}$ was the temperature difference between ith and (i-1)th second for gas inside OFR. $\Delta T_{j-(j-1)}$ and $\Delta T_{k-(k-1)}$ were similar, for the temperature of OFR surface and N₂ purge gas; m_g was the mass of gas entered or left OFR in one second; ΔT_{i-a} was the temperature difference between the gas left OFR at ith second and ambient air; *F* was the Heat dissipation area for OFR surface; *A* was the heat transfer coefficient (3.48 J m⁻² s⁻¹ K⁻¹) and ΔT_{i-a} was the temperature difference between the OFR surface at jth second and ambient air; m_{N_2} was the mass entered or left lamps sleeve in one second; ΔT_{k-a} was the temperature difference between the N₂ left lamps sleeve at kth second and ambient air. Results were shown in Fig. S8.

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S3 Calculation of the Richardson number

The Richardson number, a dimensionless number that represents the ratio of buoyancy term to flow shear term, can be calculated as follow (Holman, 2010; Huang et al., 2017):

$$R_i = \frac{g\beta D^3 \Delta T/v^2}{(\rho U_{avg} D/\mu)^2} \sim \frac{gD}{T U_{avg}^2} \Delta T \qquad (4)$$

1305 where g is the gravitational acceleration (9.78 m s⁻²), β is the thermal expansion coefficient of air (T⁻¹ for ideal gases), D is the diameter of the flow tube (202 mm), *T* is the temperature at centerline (39 °C), ΔT is the temperature difference between the centerline and tube wall (4 °C), ν is the kinematic viscosity of air (m² s⁻¹), ρ is the density of air (kg m⁻³), U_{avg} is the average velocity on the cross-section of the flow tube (m s⁻¹), calculated based on the flow rate (5 L min⁻¹) and D, μ is the dynamic viscosity (N s m⁻²). When Ri<0.1, the natural convection is negligible; when Ri>10, the forced convection is negligible, and the buoyancy forces may lead to flow bifurcation and recirculation (Huang et al., 2017).

Temperature sensors	Model	Manufacturer		
OFR RH/T sensor	Sensirion SHT21	Sensirion AG		
Vaisala	HMT130	Vaisala Inc.		
Thermocouple	TM-902C, type K	Shenzhen APUHUA Electronic Technology CO. LTD		
CEM	DT-83	Shenzhen EVERBEST machinery industry, CO, LTD.		

Table S1: Temperature sensors used in temperature measurement.

Exp.	Flow rate (L min ⁻¹)	Control Voltage (V)	Lamps ¹ (num. of lamps×lamp type)	Mesh screen	OFR sensor Position ³	Position of Probe within OFR ⁴	Temp. of surface	Temp. of exhaust
1	5	5	4×185 covered	Back	In backplate	Vertical and horizontal at different depth	/ 5	/
2	5	10/6/5/4/2	4×185 covered	Back	In backplate	Different depth from the inlet in the center	/	/
3	3/5/7	5	4×185 covered	Back	In backplate	Different depth from the inlet in the center	/	/
4	5	10	4×185 covered	Back	In backplate	300 mm from the inlet in the center	Measured	/
5	5	10-6-5-4-2-0 6	4 ×185 covered	Back	In backplate	300 mm from the inlet in the center	Measured	Measured
6	5	10-6-5-4-2-0	2 ×185 covered	Back	In backplate	300 mm from the inlet in the center	Measured	/
7	5	10-6-5-4-2-0	2 ×185 covered	/	300 mm from inlet	300 mm from the inlet in the center	Measured	Measured
8	5	10-6-5-4-2-0	4 × 185	Back	In backplate	300 mm from the inlet in the center	/	/
9	5	10-6-5-4-2-0	2 × 254	Back	In backplate	300 mm from the inlet in the center	/	/
10	5	10-6-5-4-2-0	4 ×185 covered	Front	300 mm from inlet	/	Measured	Measured
11	5	10-6-5-4-2-0	2 ×185 covered	Front	300 mm from inlet	/	Measured	Measured
12	5	10-2-6-3-5-0	4 ×185 covered	Back	In backplate	300 mm from the inlet in the center	/	/

 Table S2: Detailed parameters of OFR temperature experiments.

1315 ¹ Three types of lamps were used (Figure S2). '185 covered' transmits both 185 and 254 nm radiation, with 80% surface covered with heat-shrink tubes. Lamps of '185' are the same type as '185 covered', but without covering. The lamp of '254' transmits only 254 nm radiation and is not covered.

² Two mesh screens are set inside OFR, one near the inlet (Front) and one near the outlet (Back).

³ The OFR sensor is set in the backplate by default, as shown in Fig. S1.

⁴ Extending the external temperature sensor into OFR from the inlet (so the 'Front' mesh screen must be removed). 4 depths were measured for Exp.1-3 (100, 200, 300, and 400 mm from the inlet, respectively)

⁵ '/' means no installation or no measurement.

⁶ Each voltage was set to last for 16 min.

1325 Table S3: SOM parameters used in this study.

precursor	VOC surrogate	NOx	m _{frag}	ΔLVP	p_1	p_2	p ₃	p_4	HOM yield ¹	reference
dodecane	dodecane	low	2	1.83	0.999	0.001	0.001	0.001		Cappa et al. (2013)
		high	0.2627	1.4629	0.9657	0.0010	0.0020	0.0314		Loza et al. (2014)
α-pinene	α-pinene	low	0.305	1.97	0.419	0.426	0.140	0.014	0.44%	Chhabra et al. (2011)
		high	0.1312	1.9139	0.5991	0.2923	0.1079	0.0007	0.44%	Chhabra et al. (2011)
toluene	toluene	low	1.31	1.77	0.185	0.001	0.002	0.812	0.1%	Zhang et al. (2014)
		high	1.3064	1.4169	0.5634	0.3413	0.0016	0.0937	0.1%	Zhang et al. (2014)
m-xylene	m-xylene	low	1.08	2.05	0.102	0.001	0.878	0.019	1.7%	Ng et al. (2007)
		high	0.0736	1.4601	0.1418	0.2971	0.4571	0.1040	1.7%	Ng et al. (2007)

¹ Values are obtained in Bianchi et al. (2019).

	NO	H_i^{vap} evaporation enthalpy (kJ mol ⁻¹)							
precursors	NOx	Equation ¹	50	100	150				
dodecane	high	0.0041-0.0052	0.0019-0.0022	0.0036-0.0050	0.0053-0.0095				
	low	0.0062-0.0074	0.0026-0.0029	0.0053-0.0070	0.0078-0.010				
α-pinene	high	0.0087-0.0089	0.0037-0.0039	0.0077-0.0088	0.011-0.015				
	low	0.011-0.013	0.0041-0.0053	0.0091-0.013	0.01-0.011				
toluene	high	0.0060-0.0068	0.0023-0.0026	0.0050-0.0063	0.0075-0.010				
	low	0.0083-0.023	0.0044-0.0068	0.0077-0.018	0.0095-0.030				
m-xylene	high	0.0049-0.099	0.0025-0.0039	0.0045-0.0094	0.0064-0.016				
	low	0.0078-0.018	0.0043-0.0063	0.0073-0.015	0.0091-0.023				

Table S4: The modeled variation of SOA yield per temperature (K). The concentration of organic aerosol <u>seed</u> is 15 μ g m⁻³ for all cases. The range of model temperature is 20-40 °C.

¹ The equation is taken from Epstein et al. (2010), $H_i^{vap} = -11 \times \log C_{i,ref}^* + 131$.

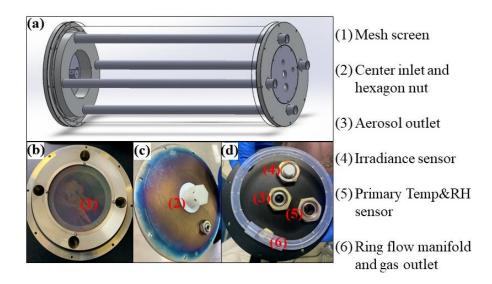


Figure S1: Schematic diagram of (a) OFR and UV lamps and photographs of (b) mesh screen near the inlet, (c) inlet 1335 and hexagon nut and (d) outlets and sensors of OFR.

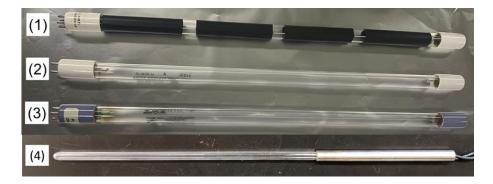
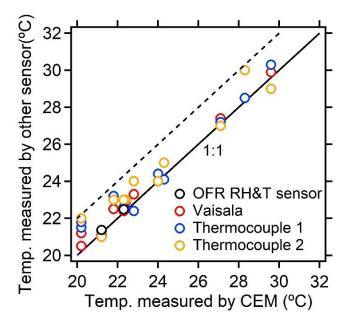


Figure S2: Four types of lamps used in this research. Type (1) transmits both 185 and 254 nm radiation, with 80% surface covered with heat shrink tubes (GPH436T5VH/4, Light Sources, Inc.). Type (2) is the same as type (1) but not covered. Type (3) transmits only 254 nm radiation and is not covered (GPH436T5L/4, Light Sources, Inc.). Type 1340 (4) transmits both 185 and 254 nm radiation (model no. 82-9304-03, BHK Inc.).



1345 Figure S3: Comparison between different temperature measurements used in this research. The measured temperatures from the CEM sensor, which was used to measure the room temperature, are shown on the x-axis. The Vaisala sensor is used to measure the temperature inside the OFR. Thermocouple 1 and Thermocouple 2 are used to measure the temperature of the OFR exhaust and outside surface. Detailed information about different sensors can be found in Table S1.

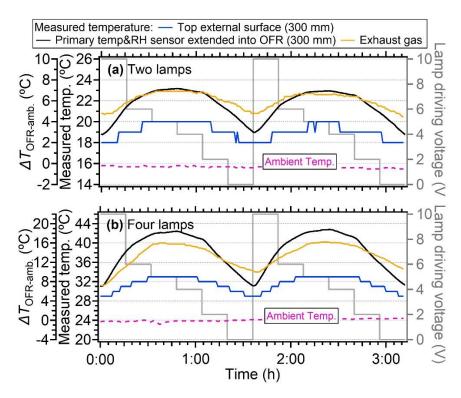


Figure S4: Temperature variation for (a) four lamps and (b) two lamps. In this case, the front plate with a hexagon nut and mesh screen was installed, and the OFR sensor set in the backplate was extended into the center of OFR (probing depth: 300 mm). The mesh screen near the back plate was removed.

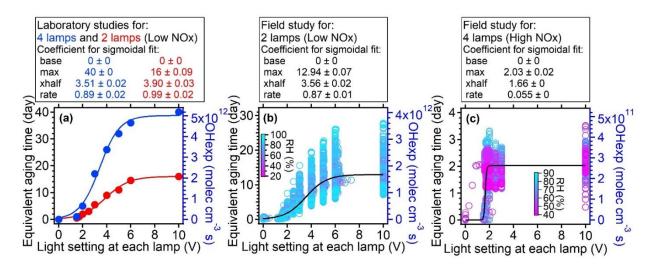
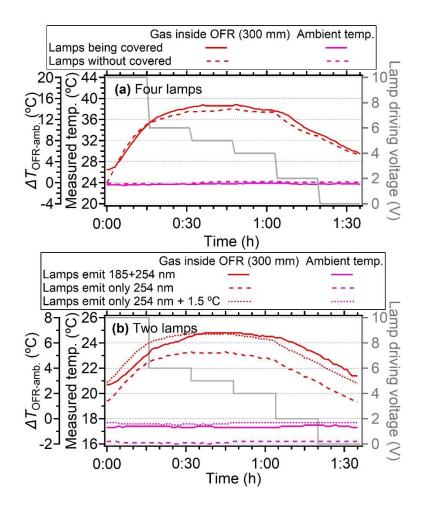


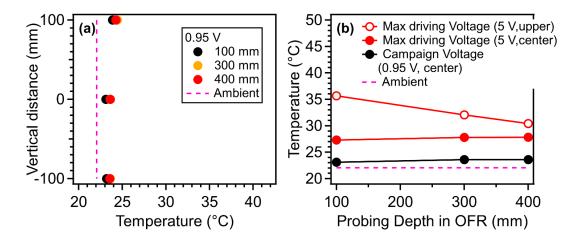
Figure S5: The correlation between OH exposures (right axis) and equivalent aging time (left axis) vs. light settings at each lamp. A sigmoidal function was used to fit the scatter plots. The OH exposures under low NOx condition in panel (a) and (b) were estimated based on the empirical parameterization in Hu et al. (2022), while OH exposures in panel (c) under high NOx conditions was estimated based on the parameterization reported in Peng et al. (2018).

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A water mixing ratio of 1.88% (60% RH at 25 °C) under low NOx conditions was assumed in the laboratory studies (Panel (a)). The mixing ratio in field studies (Panel (b) and (c)) were measured directly by RH&T sensor. The input flow rate was 5 L min⁻¹, which corresponds to a residence time of 167 s.

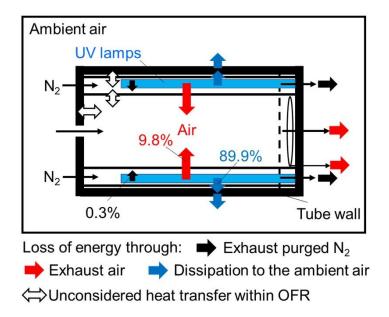


1365 Figure S6: The measured temperature variation with different types of Light Source lamps: (a) lamps with 80% surface covered with heat-shrink tubes and lamps without covered, (b) lamps emit both 185 and 254 nm radiation and lamps emit only 254 nm radiation. The temperature of the gas inside OFR at a depth of 300 mm was measured.

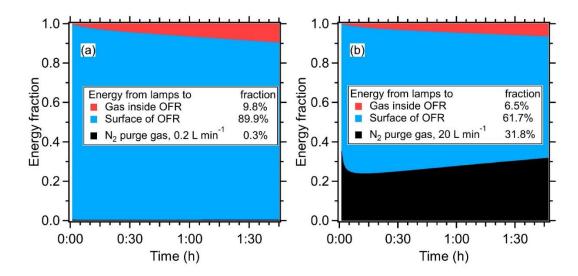


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Figure S7: Temperature measured by an external temperature sensor for an OFR with BHK lamps (a) in the vertical direction at different depths inside OFR, with the driving voltage set to 0.95 V for two lamps; (b) the measured temperature at different depths inside the OFR under different driving voltages; the "upper" indicates the position of 100 mm in the vertical direction and the "center" indicated the position measured at centerline. Flow through the OFR was 4.5 L min⁻¹.



1375 Figure S8: Schematic plot for the transfer of the heating energy inside the OFR from the UV lamps and the loss of energy to the ambient air. The fraction of energy from the UV lamps was obtained from Fig. S9. Note that only the power leading to the temperature increase (51% of total power, which is 35.6 W based on the calculation in Sec S1 and S2) within OFR was considered for these three pathways.



1380 Figure S9: (a) Energy from UV lamps (51% (based on calculation in Sect. S2) of total power (35.6 W), 8.9 W for each lamp, 4 lamps in total) to gas inside OFR, surface of OFR and N₂ purge gas (0.2 L min⁻¹) as a function of time, with 4 lamps set to 10 V. The start time was when the lamps were turned on. The flow rate was 5 L min⁻¹. (b) Same as Fig. S9a, with the flow rate of N₂ purge gas increased to 20 L min⁻¹. Details of the energy calculation were presented in Sect. S2.

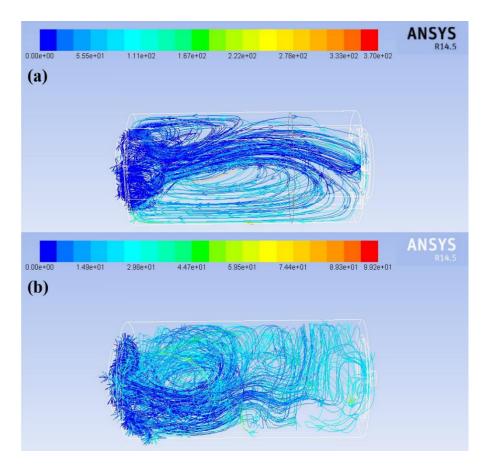


Figure S10: CFD simulation of the gases in OFR (a) without and (b) with the heating of lamps. In panel (b), the 1390 scenario of four lamps at 5 V was simulated.

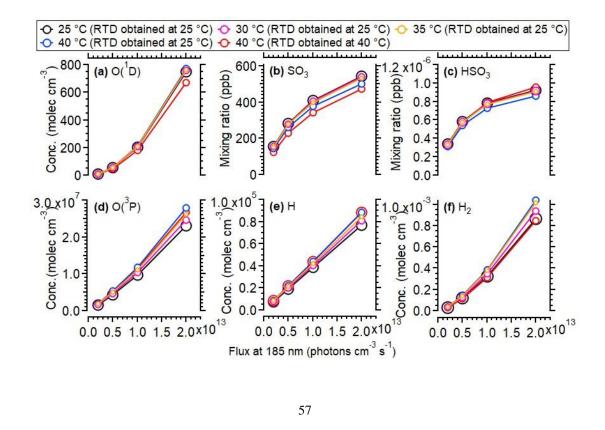


Figure S11: Simulated concentration of oxidant species from 25 to 40 °C in OFR as a function of OH exposure.photon flux at 185 nm. In this scenario, the 800 ppb of initial SO₂, 2.2% water vapor mixing ratio (25 °C, 70% RH), and different photon flux at 185 nm and 254 nm (photon flux ratio of 254/185 nm= 0.05) were used. The simulated oxidant concentrations with measured RTD in OFRat 25 and 40 °C were also both shown.

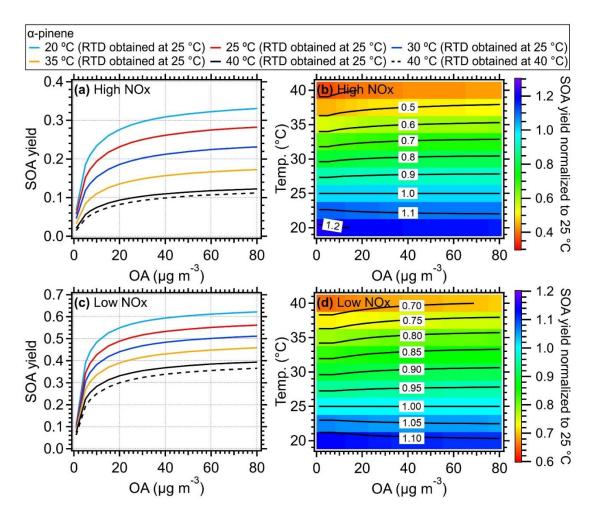


Figure S12: Simulated SOA yield of α -pinene as a function of mass concentration of organic aerosolOA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of α -pinene from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 0.5 days by assuming the <u>ambient</u> OH concentration was equivalentequated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

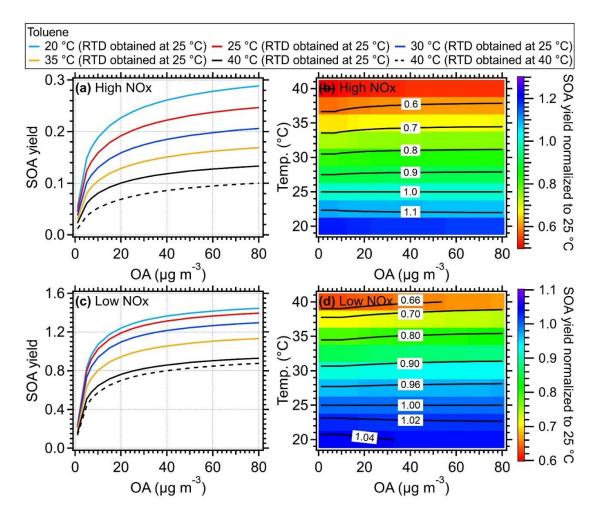


Figure S13: Simulated SOA yield of toluene as a function of mass concentration of organic aerosolOA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of toluene from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the <u>ambient</u> OH concentration <u>was equivalentequated</u> to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

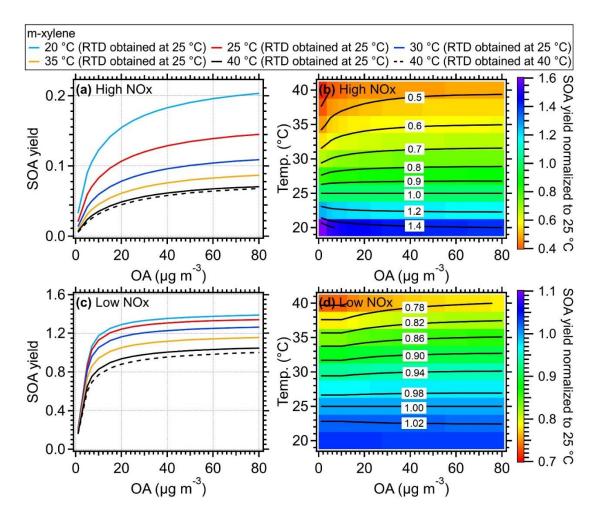


Figure S14: Simulated SOA yield of xylene as a function of mass concentration of organic aerosolOA seed (inlet mass concentration) and temperature inside of the OFR for (a) high NOx and (c) low NOx conditions, respectively. The simulated results using measured RTD obtained at 40 °C were shown as black dashed lines. The ratio of SOA yield of xylene from different temperatures compared to that of 25 °C under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the <u>ambient</u> OH concentration was equivalent<u>equated</u> to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

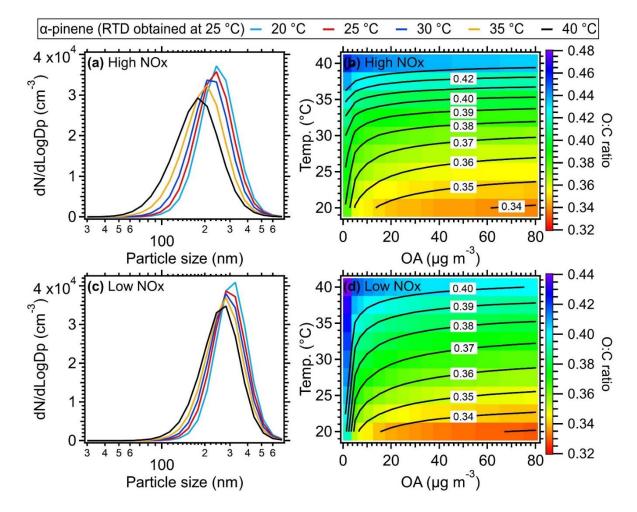


Figure S15. Simulated size distribution of α -pinene <u>SOA</u> as a function of temperature by assuming the mass concentration of OA was 30 µg m⁻³ for <u>OA seed (inlet mass concentration) under (a)</u> high NOx and (c) low NOx conditions, respectively. Simulated O: C ratio of α -pinene <u>under different temperaturesSOA as a function of temperature</u> and <u>organic aerosol concentrationsmass concentration of OA seed (inlet mass concentration)</u> under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 0.5 days by assuming the <u>ambient_OH</u>

concentration was equivalentequated to 1.5×10⁶ molec cm⁻³ (Mao et al., 2009).

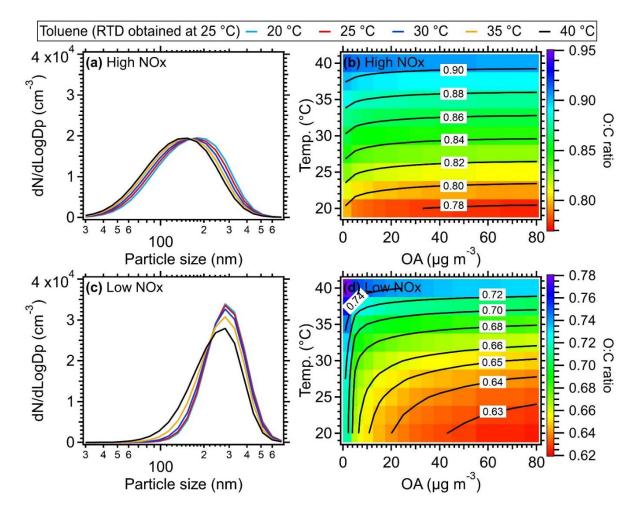


Figure S16: Simulated size distribution of toluene <u>SOA</u> as a function of temperature by assuming the mass concentration of OA was-30 μg m⁻³ for <u>OA seed (inlet mass concentration) under (a)</u> high NOx and (c) low NOx conditions, respectively. Simulated O:C ratio of toluene <u>under different temperatureSOA as a function of temperatures</u> and <u>organic aerosolmass</u> concentration <u>of OA seed (inlet mass concentration)</u> under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the <u>ambient OH</u> concentration was equivalentequated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

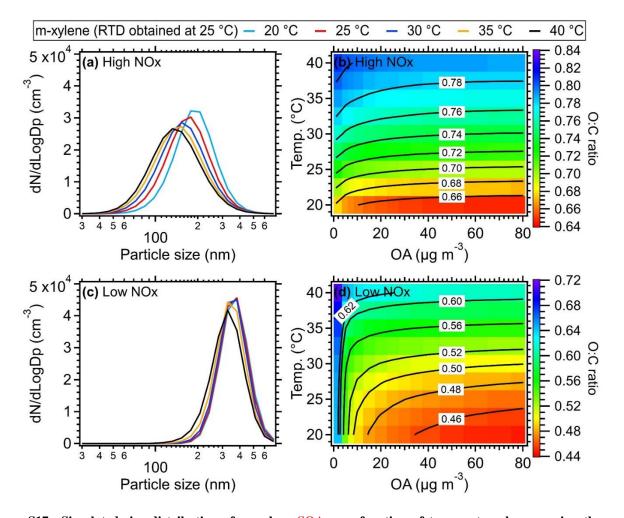
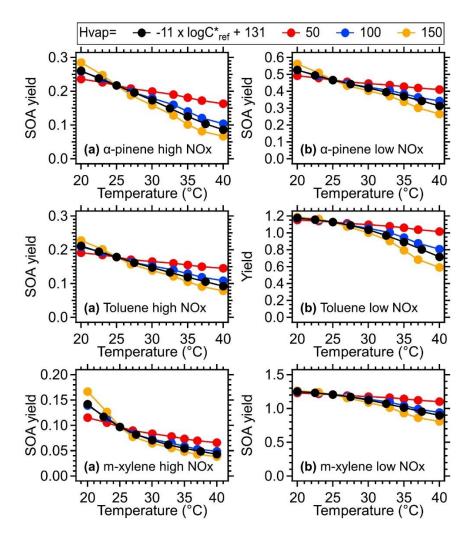


Figure S17: Simulated size distribution of m-xylene <u>SOA</u> as a function of temperature by assuming the mass concentration of OA was 30 μ g m⁻³ for <u>OA seed (inlet mass concentration) under (a)</u> high NOx and (c) low NOx conditions, respectively. Simulated O:C ratio of m-xylene <u>under differentSOA as a function of</u> temperatures and <u>organic acrosolmass</u> concentration <u>of OA seed (inlet mass concentration)</u> under (b) high NOx and (d) low NOx conditions. The equivalent aging time was 1 day by assuming the <u>ambient</u>OH concentration <u>was equivalentequated</u> to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).



1445Figure S18: Simulated SOA yield of (a-b) α-pinene, (c-d) Toluene, (e-f) m-xylene as a function of temperature under
different H_i^{vap} values, (Unit: kJ mol⁻¹). The mass concentration of organic aerosolOA seed (inlet mass concentration)
was assumed to be 15 µg m⁻³. The equivalent aging time was 1 day assuming the ambient OH concentration was
equivalent equated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

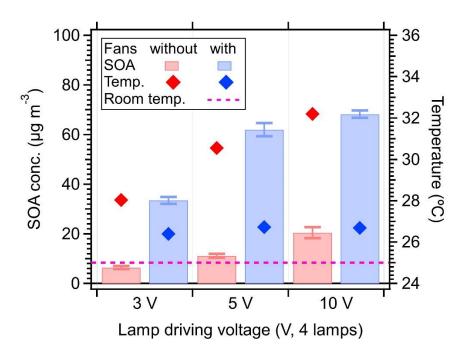
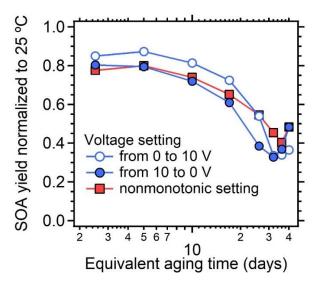


Figure S19. The SOA formation from benzene and OH radicals in the PAM-OFR as a function of light intensity. Two cases including PAM-OFR was blown with fans and without fans were both shown. The room temperature and temperature measured with the primary Temp&RH sensor set in the back panel were shown in the right axis.

1455 Note the OFR temperature reported here is the lower limit as discussed in section 3.1.5. The gas-phase benzene (99.80%, Sigma-Aldrich) was generated with syringe pumps. Benzene was used as gas-phase precursor in this experiment due to its lower kOH, since benzene will not be totally consumed under the high OH exposure at high voltage settings in OFR. The flow rate in this experiment was 4.5 L min⁻¹, and the RH was ~30%.



1460 Figure S20. Simulated ratio of SOA yield with measured temperature vs. that under 25 °C under varied lamp settings. A 10-ppb toluene with OA-mass concentration of 30 μg m⁻³ of OA seed (inlet mass concentration) was assumed. The equivalent aging time was calculated by assuming the <u>ambient</u> OH concentration was equivalentequated to 1.5×10⁶ molecule cm⁻³ (Mao et al., 2009).

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